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# CHEMISTRY OF OZONE IN WATER AND WASTEWATER TREATMENT

From Basic Principles to Applications



**Clemens von Sonntag**  
**Urs von Gunten**

# Chemistry of Ozone in Water and Wastewater Treatment

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# Chapter 1

## Historical background and scope of the book

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The discoverer of ozone, *Christian Friedrich Schönbein* (1799–1869, cf. Figure 1.1) was born in Metzingen (Germany) as the son of a dyer. With only one exam in his life, which he passed on his own, without a regular education, he became one of the leading chemists in Europe. Before being nominated Professor at the University of Basel, he studied in Germany, England and France. In 1830, he received an honorary doctoral degree from the University of Basel. He also became an honorary citizen of the City of Basel in 1840 and later on was politically active in the legislative and executive government of this city (Nolte, 1999). He is best known for his discovery of ozone (1839), but he also discovered the principle of the fuel cell (1839), and gun cotton (1846). The test for ozone that he had developed on the basis of the guajac resin led to the discovery of peroxidases (1855) and is still in use as a simple screening test for colon cancer (the haemoglobin in the faeces act like peroxidases). He also was the first (von Sonntag, 2006) to use the  $\text{Fe}^{2+}$  plus  $\text{H}_2\text{O}_2$  reaction (Schönbein, 1859), which was later termed the Fenton reaction after *Henry John Horstman Fenton* (1854–1929) who nearly forty years later looked into the reaction in more detail (Fenton, 1894; Fenton & Jackson, 1899). *Schönbein* gave the new oxygen species the name “ozone” because of its strong smell [taken from Greek “ὄζειν” (ózein): to smell (see Chapter 2) (Schönbein, 1840)] and was very close to deducing the right structure (Schönbein, 1854). He also described the reaction with iodide and the most sensitive indigo assay (Schönbein, 1854). This assay is still in use today (Chapter 2). His famous 1854 review was requested by *Justus von Liebig* (1803–1873) to be published in his “Annalen”, in which he writes: “*Herr Professor Schönbein hat auf meinen Wunsch seine Untersuchungen über diesen Gegenstand für die Leser der Annalen zusammengestellt. Ich betrachte die Erscheinungen und Beobachtungen, welche dieser ausgezeichnete Forscher beschreibt, für eben so wichtig wie bedeutungsvoll für die Wissenschaft, denn es ist von jeher die Entdeckung einer neuen Eigenschaft der Materie die Quelle neuer Naturgesetze und die Quelle der Einsicht in bis dahin unerklärliche Erscheinungen gewesen.* – On my request, professor Schönbein has compiled his studies on this subject. I consider the phenomena and observations described by this distinguished scientist as important as well as significant for science, since the discovery of a novel property of matter has always been the source of new laws of nature and the source of comprehension of hitherto unexplainable phenomena.”

*Schönbein* was not only an excellent scientist but must also have been good company (Oesper, 1929a; Oesper, 1929b). *Justus von Liebig* wrote to *Friedrich Wöhler* (1800–1882): “*Schönbeins Humor ist unschätzbar; wenn ich nur seinen Magen hätte.* – Schönbein’s sense of humour is invaluable; I wish I had his stomach.”



**Figure 1.1** *Christian Friedrich Schönbein (1799–1868)*. University Library Basel, Portrait Collection, with permission.

The history of the first hundred years of ozone chemistry has been reported in eight excellent articles by M.C. Rubin (Rubin, 2001, 2002, 2003, 2004, 2007, 2008, 2009; Braslavsky & Rubin, 2011), and here we can give only a very short account.

*Schönbein* had discovered ozone when he electrolysed dilute sulfuric acid and observed that it was also formed in the autoxidation of white phosphorus (“the phosphorus smell”). The latter was the standard method for obtaining ozone in the first years of ozone chemistry. He reported his discovery to the Basel Natural Science Society on 13 March 1839: “*Über den Geruch an der positiven Elektrode bei der Elektrolyse des Wassers* – On the odour at the positive electrode during electrolysis of water.” *Schönbein* had already realised that low concentrations of carbon, iron, tin, zinc and lead hindered ozone production (*Schönbein*, 1844). For *Schönbein*, this was proof of the oxidising properties of ozone. Yet, it was more difficult at the time to derive the structure of ozone. Originally, *Schönbein* thought that ozone is related to halogens, because of its smell, which is similar to chlorine and bromine. Later, he hypothesised that it contained oxygen and hydrogen (*Schönbein*, 1844). Only years later, did he accept that ozone was a modification of oxygen as was described by *Jacob Berzelius* (1779–1848) in 1846 (Nolte, 1999). He writes to *Michael Faraday* (1791–1861): “*Wir können nicht länger an der Tatsache zweifeln, dass Sauerstoff in zwei verschiedenen Zuständen, in einem aktiven und einem inaktiven, in dem ozonischen und dem normalen Zustand existiert.* – We can no longer doubt the fact that oxygen exists in two different states, an active and an inactive one, in the ozonic and normal state.”

The ozone generator that we use today for its production was invented by *Werner von Siemens* (1816–1882) in 1857, and only this invention made industrial applications of ozone possible.

Applications often very rapidly follow technical progress. It was less than a fortnight after the discovery of x-rays by *Wilhelm Konrad Röntgen* (1845–1923), when a physicist in Chicago realised that this biologically active radiation might be used in cancer therapy, and the first patient was treated (Grubbé, 1933; von Sonntag, 1987). Also, when reliable UV-lamps became available (Perkin, 1910), the first plant providing UV-disinfected drinking water to a community of 20,000 people was installed in the same year (von Sonntag, 1988). Similarly, very shortly after the discovery of the pathogenic agents of anthrax in 1876 and of cholera in 1884 by *Robert Koch* (1843–1910), the disinfecting power of ozone was reported (Sonntag, 1890) in the same issue as that of chlorine (Nissen, 1890). The implementation of ozone in water treatment followed about one decade later (see below and Chapter 5).

The ozone chemistry of organic compounds was first studied systematically by *Carl Friedrich Harries* (1866–1923), professor at the University of Kiel and son-in-law of *Werner von Siemens*, and it was he who coined the name “ozonide” for compounds formed in the reaction of ozone with organic compounds, notably olefins (Rubin, 2003).

A breakthrough in the understanding of ozone reactions mechanistically was achieved by *Rudolf Criegee* (1902–1975, Figure 1.2), with experiments starting in the late 1940s, and the reaction of olefins with ozone (Criegee, 1975) rightly carries his name. One of us (CvS) knew Criegee quite well, as Criegee had been his PhD examiner in Organic Chemistry at the Technical University of Karlsruhe, but, at the time, trained as a photochemist and as a radiation chemist; the candidate would never have dreamt that, one day, ozone chemistry may find his own interest as well.



**Figure 1.2** *Rudolf Criegee* (1902–1975). Chemistry Department of the Karlsruhe Institute of Technology (formerly the Technical University of Karlsruhe), with permission.

In those times, ozone chemistry was carried out largely in organic solvents (Bailey, 1978; Bailey, 1982) [for aqueous solutions see (Bailey, 1972)]. *Werner Stumm* (1924–1999) (Giger & Sigg, 1997), director of Eawag (1970–1992) realised the high potential of ozone in water treatment, but also the very limited knowledge of its reactions in aqueous solution (Stumm, 1956). He thus enforced his group by asking *Jürg Hoigné* (Giger & Sigg, 1997) to join in, and due to *Hoigné's* pioneering work on ozone chemistry in aqueous solution, the topic of this book, found more than a little interest. It was he who showed that ozone reactions in aqueous solution may induce free-radical reactions (Hoigné & Bader, 1975), reactions that seem not to occur in organic solvents. *Hoigné* also started off as a radiation chemist, and a friendship with one of us (CvS) dates back to the mid-1960s, when *Hoigné* was still an active member of the radiation chemistry community. With this background knowledge, he introduced radiation-chemical tools for elucidating aspects of ozone chemistry in aqueous solution (Bühler *et al.*, 1984; Staehelin *et al.*, 1984). The other author of this book (UvG) joined the *Hoigné* group at Eawag in 1992 and later became his successor. We (CvS and UvG) profited greatly from discussions with *Jürg Hoigné*, and it is our great pleasure to dedicate this book to him.

The disinfecting power of ozone (Sonntag, 1890) and chlorine (Nissen, 1890) were realised practically at the same time in the late 19th century. The first ozone disinfection unit was installed in 1906 in Nice (France)

(Kirschner, 1991). Not much later (1911), a UV-disinfection plant was built in nearby Marseille (von Sonntag, 1988). Despite this very early start of ozone- and UV-disinfection technologies, chlorination dominated over many decades, and it was only in the 1970s and even later, when the shortcomings of chlorination became apparent (chlorination by-products, lack of inactivation of the cysts of *Giardia* and oocysts of *Cryptosporidium*) that disinfection with ozone and UV gained in importance. Later on, the oxidation of micropollutants also became an important field of ozone application (Chapter 5).

Based on the increasing importance of ozone in drinking water and wastewater, a number of books appeared on this topic (Evans, 1972; Langlais *et al.*, 1991; Beltrán, 2004; Rakness, 2005; Gottschalk *et al.*, 2010). They often dealt with technical aspects or, when ozone chemistry was in the foreground, they no longer covered the recent developments in this area of research. Most scientific papers at conferences and in publications report interesting details, but they are not embedded in a general mechanistically based concept of ozone chemistry in aqueous solution. The present book intends to fill this apparent gap and should enable researchers to sharpen their research by applying basic mechanistic principles. Mechanistic considerations “hypotheses” are the basis of scientific progress: “*Hypothesen sind Netze, nur der wird fangen, der auswirft.* – Hypotheses are nets, only those who cast will catch.” (Friedrich Philipp Freiherr von Hardenberg (1772–1801), “Novalis”, German poet and scholar). Yet, there is a caveat that we should not stick to these concepts slavishly: “*Hypothesen sind Wiegenlieder, womit der Lehrer seine Schüler einlullt, der denkende treue Beobachter lernt immer mehr seine Beschränkung kennen, er sieht: je weiter sich das Wissen ausbreitet, desto mehr Probleme kommen zum Vorschein.* – Hypotheses are lullabies, by which the teacher lulls his pupils; the thinking and careful observer increasingly realises his limitations; he sees: the further knowledge expands, the more problems appear.” (Johann Wolfgang von Goethe (1749–1832), German poet and scholar). Mechanisms are always open to revision, since concepts in science can never be proven and must contain the potential of falsification – otherwise they are too general and useless [Karl Raimund Popper (1902–1994), Austrian philosopher]. The reader will see this principle operating in relation to our work also; we had to revise our already published mechanistic suggestions when new experimental data became available. Here, we are in accord with Schönbein who is reported (Oesper, 1929a) to have said: “As for me, the determination of the truth is far more important than the maintenance of my views, for why should one hold fast to notions that will not withstand the criticisms of facts. The sooner they fall, the better, even though prima facie they appear ever so ingenious.”

Yet, mechanistic considerations are not hatched in the ivory tower for the amusement of physical chemists, but are of great predictive value. As in analytical chemistry, one typically only finds what one is looking for. Mechanistic considerations lead to more detailed and in-depth studies.

With this concept in mind, Maggie Smith, responsible for IWA Publishing, and the authors agreed to launch this book at as low a price as possible to make it not only affordable for senior scientists but also for students of environmental sciences and engineering. For expanding the knowledge in ozone chemistry and application or finding an entry into the field, as many references as possible were included and updated in early 2012. Ozone rate constants in aqueous solution are compiled, updating an earlier compilation (Neta *et al.*, 1988). Managers of water supplies and wastewater treatment plants will find here the state-of-the-art in disinfection and pollution abatement using ozone and ozone-based advanced oxidation processes and a discussion of certain limitations that may be caused by problematic by-products such as bromate. Furthermore, examples of the incorporation of ozone into water and wastewater treatment schemes are given. Finally, as our drinking water resources become scarcer, notably in arid countries, a paragraph is devoted to the contribution of ozone treatment in reclamation technologies.

While writing this book, we spent much of our limited spare time in front of the computer screen or correcting drafts. This was a considerable burden on our families, and in particular on our wives, Ilsabe and Birgit, who had to miss activities that would have been fun to share. We were in the most fortunate situation that despite these sacrifices Ilsabe and Birgit gave us their loving support, which is reflected in the successful termination of this project. We are more than just most thankful for this.



# Chapter 2

## Physical and chemical properties of ozone

---

### 2.1 INTRODUCTORY REMARKS

*Schönbein* gave ozone its name because of its strong smell (Chapter 1). In his 1854 review, he calculated that ozone should be detectable by its smell at a concentration of 1 ppm (*Schönbein*, 1854). He also raised the question of why the nose is that sensitive in detecting ozone. One of us (CvS) hypothesises that the receptors in the nose do not record ozone as such but a strongly smelling as yet unknown product formed upon the reaction of ozone with some material contained in the skin. Evidence for this comes from a typical lab experience. When one spills some ozone water on one's hands, they smell like ozone, even after a time, when all the ozone must have evaporated/reacted completely. The smell of iron is due to the formation of unsaturated aldehydes and ketones on the skin which are in contact with iron (*Glindemann et al.*, 2006). Similarly, it might be possible that strongly smelling volatile compounds form when ozone is in contact with skin.

The nose is a most sensitive instrument for warning that some ozone must be in the air with an indicative level of about  $15 \mu\text{g}/\text{m}^3$  and a clear detection at around  $30\text{--}40 \mu\text{g}/\text{m}^3$  (*Cain et al.*, 2007). However, the sensitivity soon fades away, and one has the impression that ozone is no longer present to the same extent. Thus measures have to be taken *immediately* to ventilate the room and free it from toxic ozone.

The toxicity of ozone has already been described by *Schönbein*, and he mentions that about 2 mg kills a large rabbit (*Schönbein*, 1854). Prolonged exposures should hence be avoided. The maximum daily allowance in air at work is  $200 \mu\text{g}/\text{m}^3$  (8-h-value) in most industrialised countries (*Rakness*, 2005). Information on the human toxicity limits for ozone exposure is available (*Kirschner*, 1991; *Rakness*, 2005).

Some physical properties of ozone are compiled in Table 2.1.

**Table 2.1** Compilation of some physical properties of ozone

Property	Value
Molecular weight	48 Da
Dipole moment	0.537 Debye
Bond length	1.28 Å

(Continued)

**Table 2.1** Compilation of some physical properties of ozone (*Continued*)

Property	Value
Bond angle	117°
Melting point	-192.7°C
Boiling point	-110.5°C
Solubility in water at 0°C	$2.2 \times 10^{-2}$ M
Solubility in water at 20°C	$1.19 \times 10^{-2}$ M
Henry constant at 0°C	35 atm M <sup>-1</sup>
Henry constant at 20°C	100 atm M <sup>-1</sup>
Explosion threshold	10% Ozone

## 2.2 GENERATION OF OZONE

*Schönbein* discovered ozone, when he electrolysed dilute sulfuric acid. Electrolysis of sulfuric acid (20%) with gold or platinum anodes at high current density and cooling may yield oxygen with an ozone content of 4–5%. Yields may be even further increased using a platinum wire anode and by cooling to -14°C.

Electrolysis, albeit with other electrodes and ozone-resistant membranes, continues to be a convenient means for producing ozone in aqueous solution (*McKenzie et al.*, 1997). Such equipment is commercially available, but most commercial ozone generators work on the basis of a silent discharge first developed by *Werner von Siemens* in 1857. Dry air or oxygen (dew point minimum -65°C) may be used. With air, an ozone concentration of 1–5% (by weight) and with oxygen 8–16% may be reached (*Rakness*, 2005). Depending on pressure and energy of ignition, ozone concentrations >10% can be explosive (*Koike et al.*, 2005). Thus, high-ozone-yield systems have to be operated according to the guidelines of the suppliers. The energy requirement for ozone production is about 12–15 kWh/kg for ozone including oxygen production, transport and destruction (*Hollender et al.*, 2009; *Katsoyiannis et al.*, 2011). Based on this approach to generating ozone, the cost/energy requirements of ozone in technical applications has been evaluated (*Ried et al.*, 2009) and will be discussed in more detail in Chapter 3.

The chemistry in the plasma of the microdischarge columns is quite complex with about 300 reactions that may have to be considered (*Eliasson et al.*, 1987; *Okazaki et al.*, 1988). Under optimised conditions, the major fraction of the energy of the electrons gained in the electric field leads to excited atomic and molecular states of oxygen (feed gases: O<sub>2</sub> and air) and nitrogen (feed gas: air). The excited states of O<sub>2</sub> (O<sub>2</sub><sup>\*</sup>, A<sup>3</sup>Σ<sub>u</sub><sup>+</sup>, B<sup>3</sup>Σ<sub>u</sub><sup>-</sup>) dissociate according to reactions (1) and (2) (*Kogelschatz et al.*, 1988; *Kogelschatz*, 2003).



In this oversimplified scheme, there is no differentiation between triplet O atoms, O(<sup>3</sup>P), and singlet O atoms, O(<sup>1</sup>D). Since O<sub>2</sub> has a triplet ground state, reaction (3) proceeds only readily with O(<sup>3</sup>P) (spin conservation rule). Ozone formation is facilitated through a three-body reaction (3) with M (O<sub>2</sub>, O<sub>3</sub>, O, or in case of air, N<sub>2</sub>) being a collision partner.



$O_3^*$  is the initial transient excited state of ozone. Ozone formation in reaction (3) is in competition with reactions (4)–(6) which also consume O atoms (Kogelschatz, 2003).



When air is used as the feed gas, several nitrogen species such as  $N^+$ ,  $N_2^+$ , N and excited atomic and molecular species increase the complexity of the reaction system. This leads to the additional reactions (7)–(10), involving nitrogen atoms and excited molecular states of  $N_2$  (A:  $^3\Sigma_u^+$ , B:  $^3\Pi_g$ ) (Kogelschatz, 2003).



Approximately 50% of the ozone formed in air-fed systems is produced from these nitrogen-based processes. Ozone formation through these processes is slower (ca. 100  $\mu$ s) than in  $O_2$  (10  $\mu$ s), and a significant part of the electron energy which is lost through collisions with nitrogen molecules can be recovered for ozone formation by reactions (7)–(10) followed by reaction (3) (Kogelschatz, 2003). In addition to reactions (7)–(10), several other nitrogen oxide species,  $\bullet NO_2$ ,  $\bullet NO_3$ ,  $N_2O_5$ , are formed that consume ozone [reactions (11)–(14)] (Kogelschatz & Baessler, 1987).



$\bullet NO_2^*$  is an excited form of  $\bullet NO_2$ . In typical air-fed ozone generators,  $\bullet NO_x$  formation is nearly 2% of ozone formation.

Feed-gases for ozone generators should be dry to avoid undesired effects on ozone generation. The singlet O atom,  $O(^1D)$ , reacts very quickly with water vapour by insertion [reaction (15)], cf. (Taube, 1957). The thus-formed  $H_2O_2$  retains much vibrational energy and readily decomposes into two  $\bullet OH$  radicals [reaction (16)], which induce the decomposition of ozone (Chapter 13).



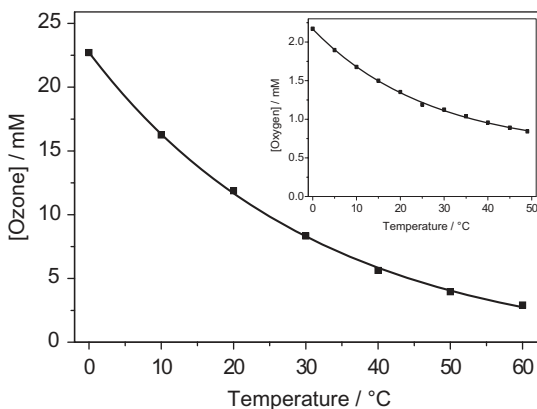
Furthermore,  $\bullet OH$  radicals react readily with  $\bullet NO$  and  $\bullet NO_2$  to  $HNO_2$  and  $HNO_3$ .  $N_2O_5$  also hydrolyses to  $HNO_3$  in water (Kogelschatz & Baessler, 1987). Therefore, when the air-feed is not dry, formation of nitrous and nitric acids can lead to corrosion of metal parts in ozone generators and tubing (Kaiga *et al.*, 1997).

Even in large-scale ozone generators where typically pure oxygen is used, the presence of nitrogen (1%) has a beneficial effect on ozone generation by increasing the ozone yield compared to pure oxygen owing to the O-forming reactions (7)–(10) (Kogelschatz, 2003).

## 2.3 OZONE SOLUBILITY IN WATER

Ozone is about ten times more soluble in water than oxygen (Figure 2.1), and this allows one to obtain rather high ozone concentrations by saturating water with an ozone/oxygen mixture from an ozone generator that

is still rich in oxygen. For the solubility of ozone at high ozone concentrations in the gas phase, see Mizuno & Tsuno (2010).

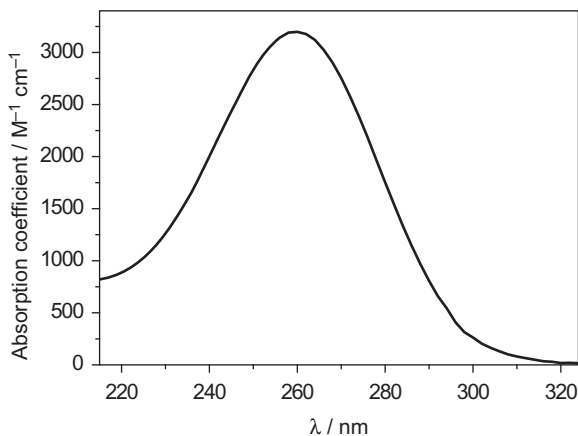


**Figure 2.1** Solubility of ozone and oxygen (inset) in water as a function of the temperature for pure gases. The maximum aqueous ozone concentration for a given ozone/oxygen gas mixture can be calculated by Henry's law according to the ozone partial pressure which is achieved by a given ozone generation system.

Ozone solubility strongly depends on temperature. Ozone solubility is about twice as high at 0°C than at room temperature (Figure 2.1). Hence, cooling with ice can be used with advantage when ozone-rich stock solutions are desired. Ozone concentrations then range near 1–1.5 mM as is often required for kinetic studies (Ramseier *et al.*, 2011).

## 2.4 UV-VIS SPECTRUM OF OZONE

The first absorption band of ozone in aqueous solution is at 590 nm. Its absorption is only weak [ $\epsilon = 5.1 \pm 0.1 \text{ M}^{-1}\text{cm}^{-1}$  (Hart *et al.*, 1983)], and this weak absorption in the visible region causes the blue colour of concentrated solutions. The second absorption band is in the UV region, and its maximum centres at 260 nm (Figure 2.2).



**Figure 2.2** Ozone spectrum in the UV region taking a molar absorption coefficient of  $3200 \text{ M}^{-1}\text{cm}^{-1}$  at the maximum (260 nm) (courtesy A. Tekle-Röttering).

Its absorption coefficient at the maximum is a matter of continuing debate. This is not an academic question, as the ozone concentration in water is often determined by measuring the ozone absorption. The difference between the highest and the lowest reported values is about 20% (Table 2.2). This may not seem much, but when a complete material balance is attempted, 20% is non-negligible.

**Table 2.2** Molar absorption coefficient of ozone at 255–260 nm in aqueous solution

Molar absorption coefficient/ $\text{M}^{-1} \text{cm}^{-1}$	Reference
3600	Taube, 1957
$2930 \pm 70$	Kilpatrick <i>et al.</i> , 1956
2000	Boyd <i>et al.</i> , 1970
2900	Bader & Hoigné, 1982
$3314 \pm 70$	Forni <i>et al.</i> , 1982
2950	Gilbert & Hoigné, 1983
$3292 \pm 70$	Hart <i>et al.</i> , 1983
3150	Hoigné, 1998

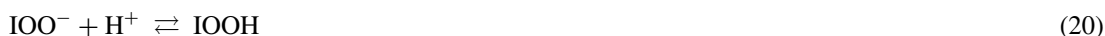
For two of those (Hoigné, 1998; Forni *et al.*, 1982), no information is given as to how these values have been obtained. Except for the value that was based on the oxidation of  $\text{Fe}^{2+}$  (Hart *et al.*, 1983), all values were determined by reacting ozone with  $\text{I}^-$  and measuring the iodine formed. It has been mostly assumed that one mole of ozone produces one mole of iodine according to reactions (17) and (18).



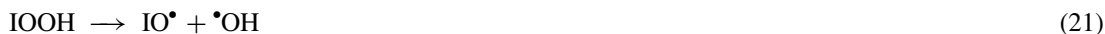
Yet, a ratio of 1.5 (without explaining the chemistry behind this higher value) has also been given (Boyd *et al.*, 1970); reported ratios range between 0.65 and 1.5 mol/mol (Rakness *et al.*, 1996). Experiments confirming a somewhat higher value have as yet not been carried out, but a speculation may still be at place here. It is recalled that in reaction (17) oxygen is released to some extent as singlet oxygen ( $^1\text{O}_2$ ) (Muñoz *et al.*, 2001).  $\text{I}^-$  reacts moderately fast with  $^1\text{O}_2$  ( $k = 7.2 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$ ) in competition with a decay to the ground state ( $k \approx 3 \times 10^5 \text{ s}^{-1}$ , in  $\text{H}_2\text{O}$ ) (Wilkinson *et al.*, 1995). At an  $\text{I}^-$  concentration near  $4 \times 10^{-2} \text{ M}$  about 50% of  $^1\text{O}_2$  has reacted with  $\text{I}^-$ . This reaction is reported to lead to  $\text{I}_3^-$  (Wilkinson *et al.*, 1995). Thus, reaction (19), which gives rise to peroxyiodide ( $\Delta G^0 = -11 \text{ kJ mol}^{-1}$ , Naumov and von Sonntag, 2010, unpublished results) may take place.



Peroxyiodide is in equilibrium with its conjugate acid [reaction (20)].



The free acids of this group of compounds have very low O–O BDEs [cf. ONOOH:  $92 \pm 8.5 \text{ kJ mol}^{-1}$  (Brusa *et al.*, 2000)], and undergo rapid homolysis such as reaction (21).



$\text{IO}^\bullet$  provides three oxidation equivalents and  $^\bullet\text{OH}$  provides one leading to the overall reaction (22).



Reaction (19) is in competition with the reversion of  $^1\text{O}_2$  to the ground state ( $t_{1/2} = 5 \mu\text{s}$  in  $\text{H}_2\text{O}$ ) and hence its importance should depend on the  $\text{I}^-$  concentration used in such experiments. Reactions (19) and (20) have to occur only to a small extent to increase the value of the absorption coefficient, as two molecules of iodine are formed per  $^1\text{O}_2$  reacting according to reaction (22). It is noteworthy, that Hoigné used increasingly higher absorption coefficients as his experience with ozone reactions increased (Table 2.2). There is also some information that may be drawn from the ozonolysis of olefins (Chapter 8). Without steric hindrance by bulky substituents, they give rise to a carbonyl compound and an  $\alpha$ -hydroxyalkylhydroperoxide. Taking an absorption coefficient of  $3314 \text{ M}^{-1} \text{ cm}^{-1}$ , a material balance (mol product per mol ozone) is obtained with a tendency of an excess of up to 5% (typically less, near 2%, cf. Table 6.3). This seems to indicate that the chosen absorption coefficient may be somewhat on the high side. Correcting for this, the value would come very close to the most recent value chosen by Hoigné, and it is suggested here to use a molar absorption coefficient of  $3200 \text{ M}^{-1} \text{ cm}^{-1}$  for the determination of the ozone concentration in water.

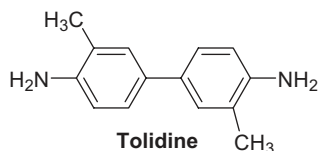
## 2.5 DETERMINATION OF THE OZONE CONCENTRATION

Analytical methods for determining ozone concentrations in water and the gas phase have been reviewed (Gottschalk *et al.*, 2010). The most straightforward method is measuring its absorption at 260 nm (the spectrum near the maximum is relatively broad, and an absorption maximum at 258 nm is also found in the literature. Due to this broadness, measurements at either 260 nm or 258 nm give practically identical results). We suggested above basing such measurements on an absorption coefficient of  $\epsilon(260 \text{ nm}) = 3200 \text{ M}^{-1} \text{ cm}^{-1}$ . It is well suited for the determination of ozone in stock solutions (Ramseier *et al.*, 2011b) and in waters with low UV absorbance [ $A(258 \text{ nm}) < 1 \text{ m}^{-1}$ ] (Hoigné & Bader, 1994). Such measurements require, however, that there is no other material such as dissolved organic matter (DOM), turbidity and iron that absorb at this wavelength (Hoigné, 1994). For coping with such conditions, assays have been developed that are discussed below (Hoigné & Bader, 1994).

For on-line measurements of ozone, amperometric electrodes without and with membranes can be used (Stanley & Johnson, 1979; Langlais *et al.*, 1991; Rakness, 2005; Gottschalk *et al.*, 2010). Many systems are commercially available and are not discussed any further.

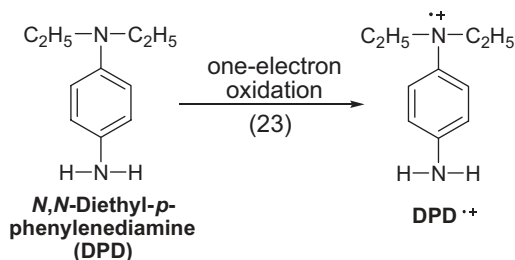
### 2.5.1 The *N,N*-diethyl-*p*-phenylenediamine (DPD) method

The first studies with *p*-phenylenediamines for the determination of ozone used tolidine as a substrate (Zehender, 1952; Zehender & Stumm, 1953).



The yellow colour that is formed was measured at 440 nm, but this colour faded away too rapidly, and quenching ozone first with  $\text{Mn}^{2+}$  in sulfuric acid solution has been suggested. This reaction gives rise to  $\text{MnO}_2$  solution (Chapter 12). The subsequent addition of tolidine gave a more stable colour. *p*-Phenylenediamine and its *N*-alkylated derivatives have low reduction potentials. For the parent, a value

of +309 mV and for *N,N,N',N'*-tetramethyl-*p*-phenylenediamine (TMPD) a value of +266 mV is given (Wardman, 1989). The value for DPD must lie in-between. In its reactions with one-electron oxidants, stable radical cations are formed [reaction (23)]. For TMPD this is commonly known as Wurster's blue. DPD is widely used for the determination of free and combined chlorine in drinking water (Eaton *et al.*, 2005). The DPD radical cation is red and absorbs strongly at 551 nm.



DPD has also been proposed as an agent for the determination of ozone (Gilbert, 1981; Gilbert & Hoffmann-Glewe, 1983; Gilbert & Hoigné, 1983). Based on  $\epsilon_{\text{app}}(260 \text{ nm}) = 2.950 \text{ M}^{-1} \text{ cm}^{-1}$  for ozone, an absorption coefficient of  $\epsilon = 19.900 \pm 400 \text{ M}^{-1} \text{ cm}^{-1}$  has been derived (Gilbert & Hoigné, 1983). This value is different from that given for the  $\text{H}_2\text{O}_2$  assay:  $\epsilon_{\text{app}}(551 \text{ nm}) = 21.000 \pm 500 \text{ M}^{-1} \text{ cm}^{-1}$  (Bader *et al.*, 1988). This difference may be due to an error in the absorption coefficient of ozone (see above) and/or in a more complex reaction.

In the reaction of TMPD with ozone,  $\bullet\text{OH}$  radicals are generated (via  $\text{O}_3^{\bullet-}$ ) in a yield near 70% (Chapter 8, Table 8.4) [reaction (24)].



Based on the DMSO test for  $\bullet\text{OH}$  formation (Chapter 14), the  $\bullet\text{OH}$  yield in the reaction of ozone with DPD is only 23% [Jarocki & von Sonntag (2011), unpublished results], that is, its precursor  $\text{O}_3^{\bullet-}$  and hence primary  $\text{DPD}^{\bullet+}$  is also only 23%. A detailed study that would have elucidated other potential reactions giving rise to  $\text{DPD}^{\bullet+}$  has still to be carried out. From radiation-chemical studies it is known that  $\bullet\text{OH}$  in its reaction with the stronger reductant TMPD gives rise to  $\text{TMPD}^{\bullet+}$  (partially via an adduct), and the reduction potential of TMPD is so low that even peroxy radicals can also undergo this reaction. Rate constants range from  $1.1 \times 10^6$  to  $1.9 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  depending on the nature of the substituents (Neta *et al.*, 1989; Schuchmann & von Sonntag, 1988). To what extent all this also holds for the less reducing DPD is not yet known. If not,  $\bullet\text{OH}$  scavenging by the water matrix may lower  $\text{DPD}^{\bullet+}$  yields.

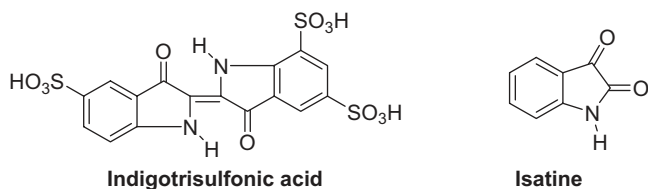
In Mn(II)-containing waters, the  $\text{MnO}_2$  colloids that are formed upon ozonation (Chapter 12) also readily oxidise DPD. This may result in an overestimate of residual ozone concentrations when such waters are assayed by the DPD method. At an extremely high Mn(II) concentration of 8.5 mg/L (154  $\mu\text{M}$ ) converted to  $\text{MnO}_2$ , an ozone equivalent of 1.01 mg/L (21  $\mu\text{M}$ ) has been reported (Gilbert, 1981). For more typical Mn(II) concentrations of the order of 1 mg/L, the interference would be much smaller but still mimic an ozone residual. Additionally, the presence of  $\text{Br}^-$  and its oxidation to HOBr during ozonation (Chapter 10) can result in a false positive ozone residual because HOBr also reacts with DPD (Pinkernell *et al.*, 2000). Similar interferences are observed with the indigo method (see below).

## 2.5.2 The indigo method

For the quantification of ozone, Schönbein developed the indigo method, and in his 1854 review (Schönbein, 1854) he writes at the end of it: “Um die in einem gegebenen Luftvolumen vorhandene Menge ozonisirten

*Sauerstoffes dem Gewichte nach zu bestimmen, bediene ich mich schon seit Jahren der Indigolösung, und vielfache Versuche haben mich überzeugt, daß dieses Mittel rasch zum Ziele führt; denn mit Hülfe desselben läßt sich der Gehalt einiger Liter Luft an ozonisirtem Sauerstoff in wenigen Minuten bis zu einem kleinen Bruchtheil eines Milligrammes bestimmen, wie sich aus nachstehenden Angaben ergeben wird.* – For the determination of the amount per weight of ozonised oxygen in a given volume of air, I have been using a solution of indigo for years, and many experiments have convinced me that this agent leads quickly to the goal; with its help the content of ozonised oxygen can be determined up to a fraction of a milligram within a few minutes, as can be seen from the ensuing description.”

The indigo solution that *Schönbein* used has also been sulfonated. At present, the bleaching of indigotrisulfonate by ozone is measured to determine ozone concentrations. As a decrease (base: 100% with a given uncertainty) rather than an increase (base: 0%, no uncertainty) is measured, there is an intrinsic analytical uncertainty. The indigotrisulfonate that is commercially available is a technical product with an unknown purity (possibly near 85%). This material reacts very quickly with ozone,  $k = 9.4 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$  (Muñoz & von Sonntag, 2000a). Details of the reaction have not yet been investigated, but if the site of ozone attack is the central C–C double bond, sulfonated isatine and the corresponding  $\alpha$ -hydroxyhydroperoxide should be the primary products (Chapter 6). In contrast to the reaction of ozone with DPD, no  $\cdot\text{OH}$  is generated in the reaction of ozone with indigotrisulfonate [Jarocki & von Sonntag (2011), unpublished results].



The indigo method, now a kind of standard method, is not a primary method, and the extent of bleaching has been based on the molar absorption coefficient of ozone (for its value see above). The purity of the indigo sample, the ozone absorption coefficient and the reaction efficiency thus determine the value of  $\epsilon(600 \text{ nm})$  to be used for the indigo assay. A value close to  $20,000 \text{ M}^{-1} \text{ cm}^{-1}$  has been found (Bader & Hoigné, 1982; Muñoz & von Sonntag, 2000a).

Indigotrisulfonate is also readily oxidised by some products that may be generated by ozone with water containing impurities such as Mn(II). The rate constant with the  $\text{MnO}_2$  colloids is  $k > 10^7 \text{ M}^{-1} \text{ s}^{-1}$  and with permanganate, which is also formed to some extent, it is  $k = 1.3 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ . The Mn(III) species dominating in acid solution reacts at  $2 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  (Reisz *et al.*, 2008). HOBr may also react with indigo. Currently, the extent of interference is, however, not entirely clear.

The use of indigotrisulfonate for the determination of ozone residual concentrations in drinking water plants has been assessed. Indigo stock solutions are not stable and using solutions that have been standing for several weeks can cause a major underestimate of ozone residual concentrations (Rakness *et al.*, 2010).

## 2.6 METHODS FOR MEASURING OZONE KINETICS

To measure rate constants for the reaction of ozone with a substrate under first-order conditions, experiments can be performed in excess of ozone or the selected substrate. Typically, a substrate concentration is chosen in excess of ozone (e.g. tenfold), and the ozone decrease is measured as a function of time. Because, the stoichiometry of the ozone–substrate reaction may deviate from 1.0, more than 1 mol of ozone may be consumed per mol of degraded substrate. Therefore, under first-order conditions, the determined rate



constant for the decrease of ozone or the decrease of the substrate may deviate by more than a factor of 3 (e.g. phenol, triclosan and diclofenac, paragraph 2.6.4; monochloramine, Chapter 8). For water treatment, this has to be considered, because in real systems ozone is typically in large excess over the substrate. Thus, the second-order rate constant determined by the decrease of the substrate should be used for the assessment of substrate abatement.

There are several methods for determining the rate constant of ozone with a given compound. The most reliable ones are the direct methods. A larger error may be involved in the method that uses competition kinetics, as there is already an uncertainty, albeit typically small, in the rate constant of the competitor. Direct methods, however, may also have their problems, but these are not as straightforward. In all cases, the determination of rate constants with ozone requires extreme care to avoid reactions with  $\bullet\text{OH}$ , which may be formed during ozonation. Therefore, kinetic measurements should be carried out at low pH, where ozone is more stable and/or in presence of  $\bullet\text{OH}$  scavengers (Hoigné & Bader, 1983a). Methods based on reactive ozone absorption are not easy to perform and some have led to results not compatible with more straightforward methods (see below) and should be avoided if possible.

### 2.6.1 Ozone decay measurements

Following ozone decay as a function of time is a direct method and thus possibly the most reliable one. Here, the compound whose rate constant is to be determined is typically present in large excess (e.g. tenfold) over ozone. The other way round, ozone in a large excess over the substrate is also feasible but often not as convenient. Under such conditions, the reaction is kinetically of (pseudo-) first order. For the substrate (**M**) in excess, one may write equations (25) and (26).



$$\frac{-d[\text{O}_3]}{dt} = k_1[\text{O}_3] \times [\text{M}] \quad (26)$$

As the concentration of **M** does not significantly change during the reaction, **[M]** becomes a constant and equation (26) can be integrated to equation (27).

$$\ln\left(\frac{[\text{O}_3]}{[\text{O}_3]_0}\right) = -k_1[\text{M}] \times t = -k_{\text{obs}} \times t \quad (27)$$

A plot of  $\ln([\text{O}_3]/[\text{O}_3]_0)$  vs. the time ( $t$ ) yields a straight line from the slope of which  $k_{\text{obs}}$  is calculated and division by **[M]** yields the bimolecular rate constant  $k_1$  (unit:  $\text{M}^{-1} \text{s}^{-1}$ ). The ozone decay can be followed spectrophotometrically at 260 nm. The absorption coefficient of ozone at this wavelength is high ( $3200 \text{ M}^{-1} \text{ cm}^{-1}$ ; for a discussion see above), but its exact value is not required here as only the absorption ratios are of relevance. Absorption of **M** in the same wavelength region as ozone does usually not affect the determination of the rate constant by this method as the same kinetics are followed even if **M** is bleached or an absorption due to the formation of **P** builds up. Strong absorptions by **M** may impede such measurements. This is typically avoided in the batch quench method (see below).

For low rate constants, kinetics can be followed in a UV-spectrophotometer set at the time-drive mode. A variation of the direct determination of ozone rate constants is the batch quench method. Here, a solution of indigotrisulfonate is added at different times, and the remaining ozone concentration is determined by the bleaching of the indigotrisulfonate (Bader & Hoigné, 1981). Alternatively, the reaction solution is

dispensed into sampling tubes containing indigotrisulfonate, which quenches the residual ozone (Hoigné, Bader, 1994). The reaction of ozone with indigo is so fast [ $k = 9.4 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$  (Muñoz, von Sonntag, 2000)] that it occurs practically instantaneously.

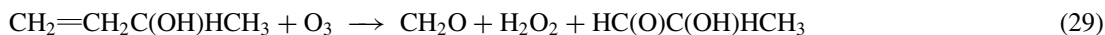
For high rate constants, the stopped-flow technique is of advantage. Here, the available time range allows the determination of rate constants near  $10^6 \text{ M}^{-1} \text{ s}^{-1}$ . Alternatively, quench flow techniques can be used, in which the ozone consumption is measured for various predetermined reaction times by quenching the solution with indigotrisulfonate. The bleaching of indigo, a measure for the ozone residual concentration, can then be measured off-line by spectrophotometry. The determination of rate constants with this method is in a similar range as stopped-flow – in the order of  $10^5$ – $10^6 \text{ M}^{-1} \text{ s}^{-1}$  (Buffle *et al.*, 2006b). For higher rate constants, methods based on competition kinetics are required.

For dissociating compounds where the base reacts too fast to be monitored, kinetics may be carried out in a more acidic environment. Sufficiently far from the  $\text{p}K_{\text{a}}$ , the observed rate constant,  $k_{\text{obs}}$ , drops by one order of magnitude per pH unit as does the concentration of the more reactive base in equilibrium. This allows one to measure the rate of reaction on a convenient timescale. Taking the  $\text{p}K_{\text{a}}$  of the substrate into account, extrapolation to high pH allows the calculation of the rate constant of the highly reactive base (Hoigné, Bader, 1983b). Typical examples are amines and phenols, where this difference in the rate constants is several orders of magnitude. At lower pH, the poorly reactive conjugate acid ( $\text{BH}^+$ ) is present in excess, but the base (B) dominates the rate of reaction. Under such conditions, the pH-specific rate constant ( $k_{\text{obs}}$ ) can be conveniently determined by equation (28).

$$k_{\text{obs}} = k(\text{BH}^+) + k(\text{B}) \times 10^{(\text{pH} - \text{p}K_{\text{a}})} \quad (28)$$

## 2.6.2 Quenching of ozone with buten-3-ol

There may be conditions where spectral interference does not allow following the 260 nm absorption as a function of time and quenching with indigotrisulfonate cannot be used because oxidising species build up during ozonation, the progress of the reaction may then be followed by quenching ozone with buten-3-ol (Chapter 6) and measuring formaldehyde [e.g. spectrophotometrically (Nash, 1953)] generated in a 100% yield according to reaction (29) (Dowideit & von Sonntag, 1998).



## 2.6.3 Reactive absorption

Ozone rate constants are sometimes also determined by making use of reactive absorption measurements. In a typical setup, 0.5 ml of a solution containing the compound whose rate constant is to be determined is placed in a polystyrene tube (12 mm i.d.) (Kanofsky & Sima, 1995). An ozone/oxygen flow passes 1.2 cm above the solution at  $1.25 \text{ ml s}^{-1}$ . The difference between the ozone concentration in the gas inlet and outlet is measured, and the fraction of ozone absorbed after 2 min is plotted against the logarithm of the substrate concentration. Such data are evaluated on the basis of the *Reactive Absorption Theory* discussed in detail in the given reference. Another approach has also been described (Utter *et al.*, 1992). In some cases, reliable (supported by more direct methods) rate constants were obtained. This approach has been extended to ozone and substrate uptake measurements in a stirred bubble column (Andreozzi *et al.*, 1996). As long as there is a 1:1 ratio of ozone uptake and substrate disappearance, this approach may also yield acceptable rate constants. But when this prerequisite is not met, the method may fail (typically, values may come out too low). For example, the rate constant of diclofenac by this method gave a value of  $1.8 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  (Vogna *et al.*, 2004), while the more reliable determination by

competition kinetics yielded  $6.8 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  (Sein *et al.*, 2008) (Chapter 8). Therefore, we recommend that, whenever possible, one should stick to more direct methods including determination by competition kinetics. These methods are addressed in the next paragraph.

### 2.6.4 Competition kinetics

The determination of ozone rate constants of a given compound **M** requires that the ozone rate constant of the competitor **C** is known to a high accuracy, that is, it should have been determined by a reliable direct method.

In competition kinetics, two substrates **M** and the competitor **C** react with ozone [reactions (30), rate constant  $k_m$  and (31), rate constant  $k_c$ ] (Dodd, 2008).

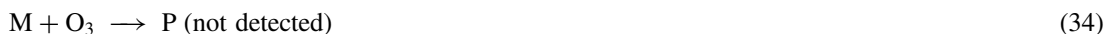


The relative degradations as a function of the ozone concentration are then given by equation (32).

$$\ln\left(\frac{[\text{M}]}{[\text{M}]_0}\right) = \ln\left(\frac{[\text{C}]}{[\text{C}]_0}\right) \times \frac{k_m}{k_c} \quad (32)$$

For this approach, it is required that **M** and **C** are degraded by ozone with the same efficiency, for example, unity efficiency. An efficiency of unity is often found, for example, with olefins (Chapter 6). But, with some aromatic compounds, marked deviations from an efficiency of unity have been reported, for example, phenol [ $\sim 0.42$  (Mvula & von Sonntag, 2003)], triclosan [0.41 (Suarez *et al.*, 2007)] and diclofenac [ $\sim 0.4$  (Sein *et al.*, 2008)] (Chapters 7 and 8). The reasons for such deviations are not yet fully understood. Apparently, there are fast side reactions that compete with the destruction of the substrate. These will continue to occur under the conditions of the competition kinetics as well. Thus, such deviations will result in an under/overestimation of the rate constant when determined according to equation (32). The error will be typically not more than a factor of two or three, and this is often quite acceptable.

The second approach is based on the measurement of just the competitor **C**. While the product of the reaction with **C** can be monitored, the reaction with **M** remains silent. Detection can be by bleaching of **C** or build-up of absorption or by the formation of a specific product due to the formation of **C\***.



At a given ozone concentration ( $[\text{O}_3]_0 \ll [\text{M}]$  and  $[\text{C}]$ ) relationship (35) holds ( $[\text{C}^*]_0$  is the concentration of **C\*** in the absence and  $[\text{C}^*]$  in the presence of **M**).

$$\frac{[\text{C}^*]}{[\text{C}^*]_0} = \frac{k_c[\text{C}]}{k_c[\text{C}] + k_m[\text{M}]} \quad (35)$$

This can be rearranged into equation (36).

$$\frac{[\text{C}^*]_0}{[\text{C}^*]} = \frac{k_c[\text{C}] + k_m[\text{M}]}{k_c[\text{C}]} = 1 + \frac{k_m[\text{M}]}{k_c[\text{C}]} \quad (36)$$

Plotting  $([C^*]_0/[C^*] - 1)$  vs.  $[M]/[C]$  yields a straight line with a slope of  $k_m/k_c$ . Since  $k_c$  is known,  $k_m$  can be calculated.

Various potential competitors have been discussed (Muñoz & von Sonntag, 2000a). A most convenient one is buten-3-ol. Its solubility in aqueous solution is high, as is its ozone rate constant [ $k = 7.9 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  (Dowideit & von Sonntag, 1998)]. One of its ozonation products, formaldehyde, can be readily determined (cf. Paragraph 2.6.2). The use of competitors with pH-dependent rate constants, for example, phenol or olefinic acids should be avoided, as a small uncertainty in the pH changes the observed rate constant significantly.

## 2.7 REDUCTION POTENTIALS OF OZONE AND OTHER OXYGEN SPECIES

The reduction potential of ozone is of relevance, whenever one-electron transfer reactions have to be considered. Although other ozone reactions dominate (e.g. Chapters 6, 7 and 8), one-electron transfer reactions often take place in competition. There are two potential routes, an inner sphere type electron transfer, that is, when an adduct is formed first that subsequently decays into  $\text{O}_3^{\bullet-}$  and the corresponding radical cation. Alternatively, an outer-sphere electron transfer may take place. The energetics of the latter is given by the reduction potential shown in Table 2.3. Reduction potentials [indicated by (g)] corrected for the solubility of ozone and oxygen can be calculated by equation (37).

**Table 2.3** Reduction potentials,  $E^\circ$  (vs. NHE) at pH 7 in V at 25°C, of  $\text{O}_2$  and water, partially reduced intermediates, ozone, and singlet dioxygen according to (Koppenol *et al.*, 2010). Reduction potentials of gases are based on their saturated solutions, that of other solutes on their 1 M solution. For making reduction potentials comparable with the reduction potentials of solids, such standard reduction potentials [indicated by (g)] were converted in the table to the basis of 1 M according to the solubility of ozone and  $\text{O}_2$  (see Figure 2.1)

Reaction	Reduction potential/V
$\text{O}_2 + e_{\text{aq}}^- \rightleftharpoons \text{O}_2^{\bullet-}$	-0.18
$\text{O}_2(\text{g}) + e_{\text{aq}}^- \rightleftharpoons \text{O}_2^{\bullet-}$	-0.35
$^1\text{O}_2 + e_{\text{aq}}^- \rightleftharpoons \text{O}_2^{\bullet-}$	+0.81
$^1\text{O}_2(\text{g}) + e_{\text{aq}}^- \rightleftharpoons \text{O}_2^{\bullet-}$	+0.64
$\text{O}_3 + e_{\text{aq}}^- \rightleftharpoons \text{O}_3^{\bullet-}$	+1.03
$\text{O}_3(\text{g}) + e_{\text{aq}}^- \rightleftharpoons \text{O}_3^{\bullet-}$	+0.91
$\text{O}_2^{\bullet-} + e_{\text{aq}}^- + 2\text{H}^+ \rightleftharpoons \text{H}_2\text{O}_2$	+0.91
$\text{HO}_2^{\bullet} + e_{\text{aq}}^- + \text{H}^+ \rightleftharpoons \text{H}_2\text{O}_2$	+1.05
$\text{O}_2 + 2e_{\text{aq}}^- + 2\text{H}^+ \rightleftharpoons \text{H}_2\text{O}_2$	+0.36
$\text{O}_2(\text{g}) + 2e_{\text{aq}}^- + 2\text{H}^+ \rightleftharpoons \text{H}_2\text{O}_2$	+0.28
$\text{H}_2\text{O}_2 + e_{\text{aq}}^- + \text{H}^+ \rightleftharpoons \bullet\text{OH} + \text{H}_2\text{O}$	+0.39
$\text{H}_2\text{O}_2 + 2e_{\text{aq}}^- + 2\text{H}^+ \rightleftharpoons 2 \text{H}_2\text{O}$	+1.35
$\text{O}_2 + 4e_{\text{aq}}^- + 4\text{H}^+ \rightleftharpoons \text{H}_2\text{O}$	+0.85
$\text{O}_2(\text{g}) + 4e_{\text{aq}}^- + 4\text{H}^+ \rightleftharpoons \text{H}_2\text{O}$	+0.81
$\bullet\text{OH} + e_{\text{aq}}^- + \text{H}^+ \rightleftharpoons \text{H}_2\text{O}$	+2.31

$$E = E^0 - 0.059 \log[\text{red}]/[\text{ox}] \quad (37)$$

For O<sub>2</sub> reduction to O<sub>2</sub><sup>•-</sup> ([O<sub>2</sub>] ≈ 1.2 mM) this leads to equations (38)–(40).

$$E = E^0 - 0.059 \log[\text{O}_2^{\bullet-}]/[\text{O}_2] = E^0 + 0.059 \log[\text{O}_2] - 0.059 \log[\text{O}_2^{\bullet-}] \quad (38)$$

$$E = -0.18 - 0.059 \times 2.92 - 0.059 \log[\text{O}_2^{\bullet-}] \quad (39)$$

$$E = -0.35 - 0.059 \log[\text{O}_2^{\bullet-}] \text{ (i.e., } E^0[\text{O}_2]/[\text{O}_2^{\bullet-}] = -0.35\text{V for a saturated oxygen solution)} \quad (40)$$

## 2.8 STABILITY OF OZONE SOLUTIONS

Aqueous ozone solutions are unstable. Many effects contribute to this instability, but not all of them are fully elucidated. In basic solutions, ozone is especially unstable. This is due to the formation of •OH by OH<sup>-</sup> (Chapter 11) and the reaction of •OH with ozone (Chapter 13). This reaction proceeds even in neutral solutions, where the OH<sup>-</sup> concentration is very low (1 × 10<sup>-7</sup> M). Acidification and the addition of •OH scavengers such as bicarbonate further increase the ozone stability in aqueous solutions. In acid solutions and at 31°C, the rate constant of ozone decomposition has been reported at 3 × 10<sup>-6</sup> s<sup>-1</sup> (E<sub>a</sub> = 82.5 ± 8.0 kJ mol<sup>-1</sup>) (Sehested *et al.*, 1992). Mechanistic details of the ‘spontaneous decomposition’ are not yet fully understood.

In natural waters, the dissolved organic matter (DOM) contributes significantly to ozone decay, and waters that have a low DOM and high bicarbonate content show relatively high ozone stability (Chapter 3), which is of relevance for the disinfection efficiency of ozone (Chapter 4).

## 2.9 REACTIVITY OF OZONE

In micropollutant abatement, for example, the reactivity of a micropollutant determines the efficiency of its elimination by an ozone treatment. Ozone rate constants may vary 8–10 orders of magnitude even within one group of compounds. Cases in point are olefins (Chapter 6) and aromatic compounds (Chapter 7) and also compounds which carry C–H functions as only ozone-reactive sites (Chapter 10). In general, ozone rate constants depend on temperature, but there are only very few cases, where details have been measured. The temperature dependence of the second order rate constants can be expressed by the Arrhenius equation [A: pre-exponential factor, E<sub>a</sub>: Activation energy, R: Universal gas constant, T: absolute temperature (K)] (41).

$$k = A \times e^{-\frac{E_a}{RT}} \quad (41)$$

To determine the parameters A and E<sub>a</sub>, equation (41) can be logarithmised, yielding equation (42).

$$\log k = \log A - \frac{1}{2.3} \frac{E_a}{RT} \quad (42)$$

A plot of log k versus 1/T allows the determination of log A and E<sub>a</sub>. Available data are compiled in Table 2.4 and some plots are shown in Chapters 9 and 10.

All these compounds react only slowly with ozone. For the more reactive ones, much lower activation energies are expected and hence the temperature dependence of the rate constants will be less pronounced.

There may be a dramatic effect of pH when the site of ozone attack can be deprotonated/protonated, such as in the case of phenols/amines or inorganic ions (Chapters 7, 8, 11 and 12).

**Table 2.4** Compilation of available reaction parameters (rate constants at 20°C) for ozone reactions in aqueous solution

Compound	$k/M^{-1}s^{-1}$	log A	$E_a/kJ\ mol^{-1}$	Reference
Cl <sup>-</sup>	$1.4 \times 10^{-3}$	10.3	74	Yeatts & Taube, 1949
Br <sup>-</sup>	160	8.8	37	Haag & Hoigné, 1983a
ClO <sup>-</sup>	35	12.2	59.8	Haag & Hoigné, 1983b
BrO <sup>-</sup>	505	13.4	60	Haag & Hoigné, 1983a
(CH <sub>3</sub> ) <sub>2</sub> SO	1.8	11.5	63.1	Reisz & von Sonntag, 2011*
H <sub>2</sub> O <sub>2</sub>	0.036	11.5	73.5	Sehested <i>et al.</i> , 1992
HC(O)O <sup>-</sup>	82	10.9	50.3	Reisz & von Sonntag, 2011*
HC(O)O <sup>-</sup>	46**	11.4	54.6	Reisz & von Sonntag, 2011*
HC(CH <sub>3</sub> ) <sub>2</sub> OH	0.83	12.5	70.7	Reisz & von Sonntag, 2011*
(CH <sub>3</sub> ) <sub>3</sub> COH	0.0011	9.3	68.7	Reisz & von Sonntag, 2011*

\*Reisz &amp; von Sonntag, 2011 (unpublished results)

\*\*In the presence of tBuOH

### 2.9.1 pH dependence of ozone reactions and the “reactivity pK”

Whenever ozone reacts with a compound that can be present in different protonation states, there will be a pH dependence of the rate constant. When deprotonated, the electron density within a given molecule is higher, and due to the electrophilicity of ozone the rate constant for the reaction with ozone is also higher. The magnitude of this pH effect strongly depends on the type of ozone reaction. With amines, for example, where ozone adds to the lone pair at nitrogen, the high reactivity of the free amine (in the order of  $10^6\ M^{-1}\ s^{-1}$ ) drops to nearly zero when this reaction site is blocked upon protonation or is significantly lowered by complexation with a transition metal ion (Chapter 8). With phenols, on the other hand, there is already a marked activation of the aromatic ring by the OH group ( $k = 1.3 \times 10^3\ M^{-1}\ s^{-1}$ ). This is, however, strongly increased upon deprotonation of the phenol, resulting in a rate constant of  $1.4 \times 10^9\ M^{-1}\ s^{-1}$  for the phenolate ion (Chapter 7). In olefinic acids the anion supplies some additional electron density to the C–C double bond, and in acrylic acid, for example, the rate constant of the free acid is  $k = 2.8 \times 10^4\ M^{-1}\ s^{-1}$ , while that of the anion is  $1.6 \times 10^5\ M^{-1}\ s^{-1}$  (Chapter 6). This is only a factor of 5.7, while deprotonation of phenol increases the rate constant by a factor of about one million. Quantum-chemical calculations discussed in Chapter 7 can account for this dramatic difference.

pH effects are not restricted to organic compounds but are also observed with inorganic compounds. A case in point is As(III). With As(OH)<sub>3</sub>, ozone reacts with  $5.5 \times 10^5\ M^{-1}\ s^{-1}$ , while As(OH)<sub>2</sub>O<sup>-</sup> reacts with  $1.8 \times 10^8\ M^{-1}\ s^{-1}$  (Chapter 12). Similarly, HS<sup>-</sup> reacts five orders of magnitude faster than H<sub>2</sub>S (Chapter 11).

Such differences in the rate constants may result in marked effects on product distribution as a function of pH, which does not follow the pK<sub>a</sub> of the starting material. This effect has been termed “reactivity pK”.

If compound **MH** is an acid that is in equilibrium with its anion **M<sup>-</sup>** [equilibrium (43)], it reacts with ozone according to equation (44), where  $\alpha$  is the degree of dissociation and  $k(O_3+MH)$  and  $k(O_3+M^-)$  are the ozone rate constants of **M** and **M<sup>-</sup>**, respectively.

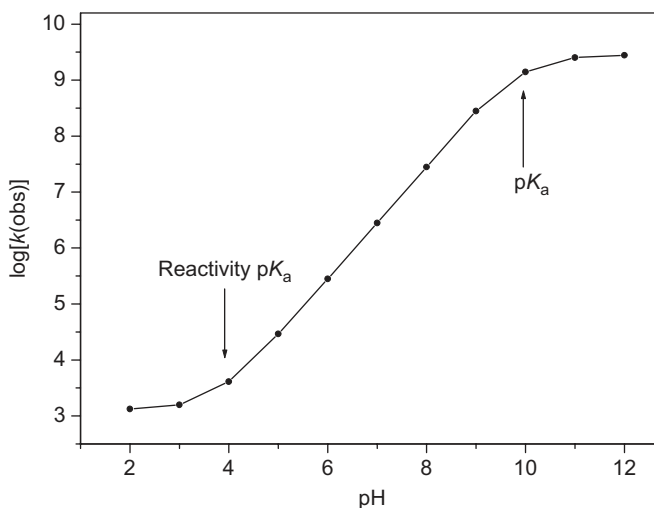


$$d[MH]_{\text{total}}/dt = (\alpha \times k(O_3 + MH) + (1 - \alpha) k(O_3 + M^-)) \times [MH]_{\text{total}} \times [O_3] \quad (44)$$

The degree of dissociation ( $\alpha$ ) can be calculated on the basis of the dissociation constant ( $K$ ) and the pH [equation (45)].

$$\alpha = 1/(1 + K/[H^+]) \quad (45)$$

The situation for phenol is shown in Figure 2.3. On the basis of the above rate constants, a reactivity  $pK_a$  of 4 is calculated. This means that despite the fact that phenol has a  $pK_a$  of 10, a predominant reaction of ozone with the neutral form will only occur below pH 4.



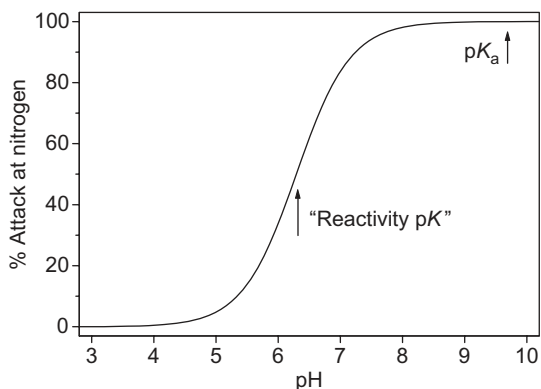
**Figure 2.3** Plot of the logarithm of the observed rate constant of the reaction of phenol with ozone as a function of pH.  $pK_a$ (phenol) and its reactivity  $pK_a$  are indicated by arrows.

## 2.9.2 Multiple reaction sites within one molecule

There may be different ozone-reactive sites within a molecule such as an aromatic ring and an aliphatic amino group. This situation is found in some pharmaceuticals such as in the beta blocker metoprolol. For other compounds with multiple sites of attack, the situation may become more complicated.

In metoprolol, a compound containing an amino group and an aromatic ring (for its structure see Chapter 8), the amino group loses its ozone reactivity upon protonation. Thus at low pH, the overall reactivity will only be due to the rate constant of the aromatic ring [in the case of metoprolol:  $k(\text{metoprolol-H}^+) = 330 \text{ M}^{-1} \text{ s}^{-1}$ , (Benner *et al.*, 2008)], while at high pH the ozone reactivity is determined by the reaction of the free amine [ $pK_a(\text{metoprolol}) = 9.7$ ;  $k(\text{metoprolol}) = 8.6 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  (Benner *et al.*, 2008)]. The percentage of ozone reacting with the free amine in equilibrium as a function of pH is shown in Figure 2.4.

The pH at which the two reaction sites, aromatic ring and amino group, react equally fast is again a kind of “reactivity  $pK$ ”. Due to the much higher rate constant of the free amine, the reactivity  $pK$  of metoprolol is much lower than its  $pK_a$  value. The reactivity  $pK$  for metoprolol (Meto) is calculated at 6.3 on the basis of equations (46–52).



**Figure 2.4** Reaction of ozone with metoprolol ( $pK_a = 9.7$ ). Percentage of ozone attack at nitrogen as a function of the pH. The “reactivity  $pK$ ” is at 6.3.

$$k(\text{Meto} - \text{H}^+) \times [\text{Meto} - \text{H}^+] = k(\text{Meto}) \times [\text{Meto}] \quad (46)$$

$$[\text{Meto}] = [\text{Meto}]_{\text{total}} \times K_a / (K_a + [\text{H}^+]) \quad (47)$$

$$[\text{Meto} - \text{H}^+] = [\text{Meto}]_{\text{total}} \times [\text{H}^+] / (K_a + [\text{H}^+]) \quad (48)$$

$$k(\text{Meto} - \text{H}^+) \times [\text{Meto}]_{\text{total}} \times [\text{H}^+] / (K_a + [\text{H}^+]) = k(\text{Meto}) \times [\text{Meto}]_{\text{total}} \times K_a / (K_a + [\text{H}^+]) \quad (49)$$

$$k(\text{Meto} - \text{H}^+) \times [\text{H}^+] = k(\text{Meto}) \times K_a \quad (50)$$

$$\log[k(\text{Meto} - \text{H}^+)] - \text{pH} = \log[k(\text{Meto})] - pK_a \quad (51)$$

$$\text{“reactivity } pK\text{”} = pK_a - \log[k(\text{Meto})] + \log[k(\text{Meto} - \text{H}^+)] \quad (52)$$

This is of a practical consequence for the formation of transformation products. In wastewater that has typically a pH of 7–8, metoprolol is almost entirely degraded via a reaction of ozone at the amino group despite the fact that the  $pK_a$  of protonated metoprolol is 9.7. Therefore, under these conditions, mainly transformation products resulting from an ozone attack on the amino group will be formed.



# Chapter 3

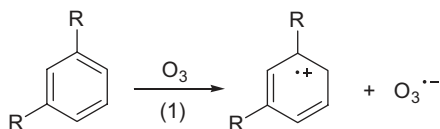
## Ozone kinetics in drinking water and wastewater

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### 3.1 STABILITY OF OZONE IN VARIOUS WATER SOURCES

The stability of ozone in drinking water and in wastewater is largely determined by its reaction with the dissolved organic matter (DOM). The nature of DOM varies among waters of different origin as does its concentration. For example, in drinking waters, DOM, measured as DOC, is typically below 4 mg/L, while in wastewaters it ranges between 5 and 20 mg/L. The nature of DOM has an influence on the rate of its reaction with ozone and thus on the ozone lifetime in these natural waters, drinking waters and wastewaters. Carbonate alkalinity influences ozone stability by scavenging  $\bullet\text{OH}$  (see below). This is of major importance, as the two desired effects of ozone, disinfection and micropollutant abatement, depend on the lifetime of ozone in these waters (see below). Therefore, it will be necessary to discuss the properties of aquatic DOM as much as they are known today and then discuss the lifetime of ozone in different waters.

An aspect of considerable consequence in this context is  $\bullet\text{OH}$  production, resulting from a side reaction of ozone with DOM. The  $\bullet\text{OH}$  radical is an important intermediate in the decomposition of ozone in water (Hoigné & Bader, 1975). In a study on wastewater that may be generalised on this point to other DOMs as well, it has been suggested that ozone reacts with the electron-rich aromatic components of DOM by electron transfer [reaction (1)] (Nöthe *et al.*, 2009; Pocostales *et al.*, 2010).



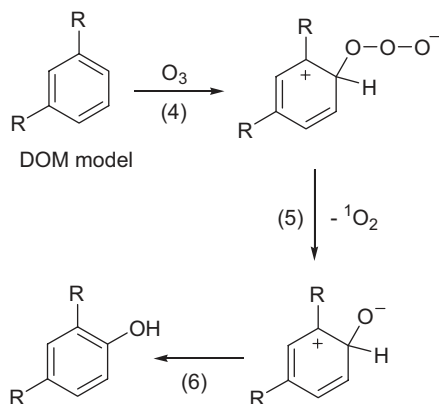
DOM model

The  $\text{O}_3^{\bullet-}$  radical gives rise to  $\bullet\text{OH}$  [reactions (2) and (3)] (Merényi *et al.*, 2010a) (Chapter 11).

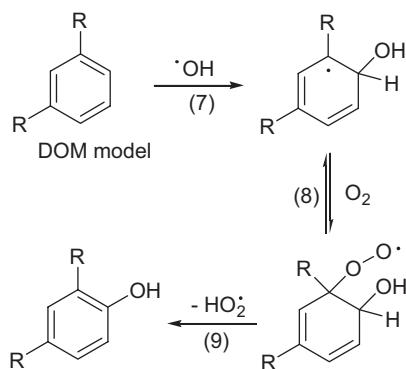


Production of  $\bullet\text{OH}$  does not cease when the electron-rich aromatics present in DOM have reacted with ozone (Nöthe *et al.*, 2009). Hence, new electron-rich sites must be created upon the action of ozone. A

typical reaction of ozone with aromatic compounds is hydroxylation, and it has been suggested that phenols thus formed are responsible for the continuing  $\bullet\text{OH}$  production (Nöthe *et al.*, 2009). In this context, it may be recalled that ozone adducts to aromatic compounds [reaction (4)] can eliminate singlet oxygen [ $^1\text{O}_2$ , reaction (5)], and the resulting zwitterion rearranges into phenol [reaction (6)] (Mvula *et al.*, 2009) (cf. Chapter 7).



Phenols belong to the group of electron-rich aromatics that undergo electron transfer to ozone, cf. reaction (1) (Mvula & von Sonntag, 2003) and thus are capable of continuing  $\bullet\text{OH}$  production according to reactions (2) and (3). Moreover,  $\bullet\text{OH}$  adds to aromatic compounds of DOM [reaction (7)].

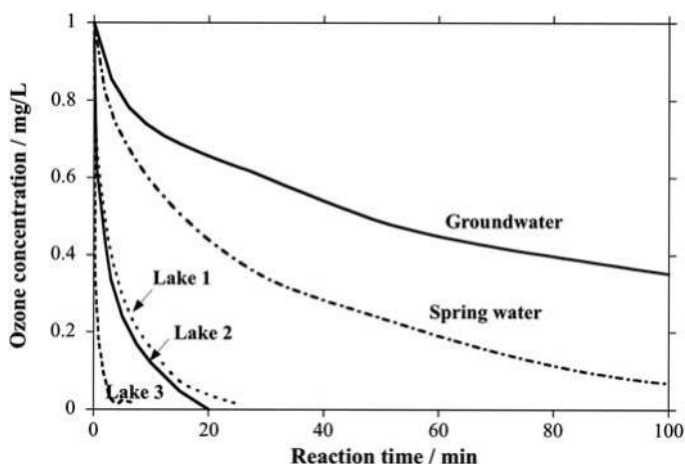


In the presence of  $\text{O}_2$  (available at high concentrations during ozonation), the thus-formed hydroxycyclohexadienyl radicals are in equilibrium with the corresponding peroxy radicals [equilibrium (8)], which eliminate  $\text{HO}_2^\bullet$  (in competition with other reactions) (Pan *et al.*, 1993; Fang *et al.*, 1995; Naumov & von Sonntag, 2005) [reaction (9)]. In wastewater but also in drinking water,  $\text{HO}_2^\bullet$  is deprotonated to  $\text{O}_2^{\bullet-}$  [equilibrium (10),  $\text{p}K_a(\text{HO}_2^\bullet) = 4.8$  (Bielski *et al.*, 1985)], and the latter reacts rapidly with ozone [reaction (11)] (Chapter 13). There are indications of the formation of  $\text{O}_2^{\bullet-}$  in the reaction of ozone with DOM [cf. reaction (9) and (10)] (Stahelin & Hoigné, 1982).



In these reactions, the aromatic DOM subunits are not yet mineralised but only hydroxylated. This is the likely reason why  $\cdot\text{OH}$  generation does not cease during ozonation even at elevated ozone doses. In addition, other moieties of DOM such as aliphatic C—H bonds also lead to superoxide and eventually  $\cdot\text{OH}$  through the above reactions (see below and Chapter 14). These reactions also apply to DOM in drinking waters.

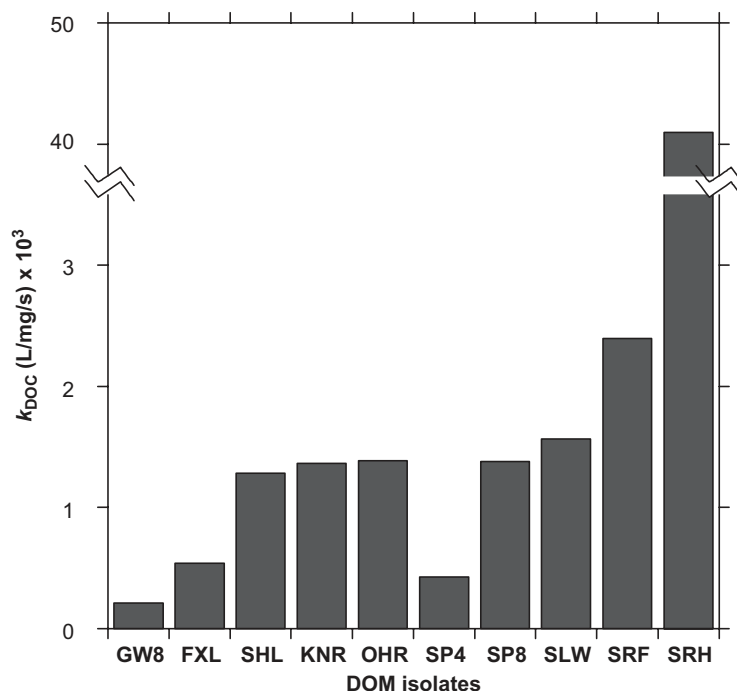
Figure 3.1 shows the ozone stability in five Swiss waters with various compositions (DOC and alkalinity).



**Figure 3.1** Stability of ozone in various Swiss natural waters at pH 8 and 15°C (ozone dose 1 mg/L). Water quality data: Groundwater (DOC 0.7 mg/L, carbonate alkalinity 6.7 mM); Spring water (DOC 0.9 mg/L, carbonate alkalinity 5.4 mM); Lake 1 (DOC 1.3 mg/L, carbonate alkalinity 2.5 mM); Lake 2 (DOC 1.6 mg/L, carbonate alkalinity 3.6 mM); Lake 3 (DOC 3.2 mg/L, carbonate alkalinity 3.4 mM). From Urfer *et al.*, 2001 with permission.

At pH 8, ozone stability decreases in the sequence groundwater > spring water > lake water 1, 2 > lake water 3. This corresponds to an increasing trend in DOC concentration and a decreasing trend in alkalinity. Ozone has a very similar stability in lake waters 1 and 2, even though the DOC is higher in lake water 2. Carbonate alkalinity which has a stabilising effect on ozone is, however, higher in lake water 2. The effect of carbonate alkalinity has been systematically tested in Lake Zurich water, by varying the carbonate/bicarbonate concentration from 0 to 2.5 mM at pH 8. While keeping the DOC constant, an increase in carbonate alkalinity leads to a significantly lower rate of ozone decomposition (Elovitz *et al.*, 2000a).

In a survey of eleven DOM isolates, a hundredfold variation of the approximate pseudo-first-order rate constant,  $k_{\text{DOC}}$ , for the ozone decrease was observed for synthetic waters containing 2 mg/L of the DOM isolate and 2.5 mM  $\text{HCO}_3^-$  at pH 7 (Figure 3.2) (Elovitz *et al.*, 2000b). This figure shows that Suwannee River fulvic and especially humic acids are outliers and do not represent ozone consumption kinetics of typical DOM in surface waters. Therefore, results from the wide application of these sources of organic matter to simulate drinking water ozonation have to be interpreted with caution and do not allow generalisations on other water sources.



**Figure 3.2** First-order rate constants of ozone decomposition ( $k_{\text{DOC}}$ ) in model waters containing  $\cong 2$  mg/L DOC,  $2.5 \text{ mM HCO}_3^-$  at pH 7. DOM isolates XAD-8: GW8, Groundwater Minnesota, USA; FXL, Lake Fryxell, Antarctica; SHL, Lake Shingobee, Minnesota; KNR, Yakima River, Washington; OHR, Ohio River, Ohio; SP8, California State Project Water, California; SLW, Silver Lake, Colorado. DOM isolate XAD-4: SP4, California State Project Water, California. SRF and SRH: Suwannee River, Georgia fulvic and humic acid, respectively. Reprinted with permission from Elovitz *et al.*, 2000b. Copyright (2000) American Chemical Society.

The role of DOM and alkalinity for ozone stability can be explained by (i) the direct reaction of DOM with ozone and (ii)  $\bullet\text{OH}$  scavenging by DOM and carbonate/bicarbonate. Whereas the type of DOM is highly relevant for ozone reactions, it is of minor importance for  $\bullet\text{OH}$  scavenging. Second order rate constants for the reaction of various DOM sources with  $\bullet\text{OH}$  are reported to vary within about a factor of two with an average value of  $(2.3 \pm 0.77) \times 10^4 \text{ (mgC/L)}^{-1} \text{ s}^{-1}$  (Brezonik & Fulkerson-Brekken, 1988; Reisz *et al.*, 2003). This value is very close to a more recent study with DOM isolates with an average value of  $1.9 \times 10^4 \text{ (mgC/L)}^{-1} \text{ s}^{-1}$  (Westerhoff *et al.*, 2007). The DOM isolate with the highest rate constant is a wastewater [ $3.9 \times 10^4 \text{ (mgC/L)}^{-1} \text{ s}^{-1}$ ] which might have significantly different properties, that is, less coiling and a higher fraction of the carbon available for reaction with  $\bullet\text{OH}$  compared to natural DOM sources. In other wastewater studies, values of  $3 \times 10^4 \text{ (mgC/L)}^{-1} \text{ s}^{-1}$  and  $3.5 \times 10^4 \text{ (mgC/L)}^{-1} \text{ s}^{-1}$  were found (Nöthe *et al.*, 2009; Katsoyiannis *et al.*, 2011).

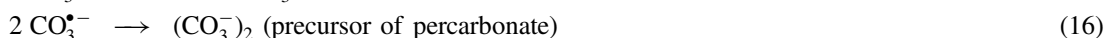
The scavenging of  $\bullet\text{OH}$  by DOM and bicarbonate has different effects on ozone stability. Note that at the typical pH values of drinking water and wastewater ( $\text{pH} \leq 8.5$ ) the contribution of  $\bullet\text{OH}$  scavenging by carbonate is smaller despite the fact that the rate constant of carbonate with  $\bullet\text{OH}$  ( $k = 3.9 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ) is higher than that of bicarbonate ( $k = 8.5 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$ ). The reason for this is the high  $\text{p}K_a$  of

bicarbonate [ $pK_a(\text{HCO}_3^-) = 10.3$ ; the corresponding reactivity  $pK$  (cf. Chapter 2) is 8.6]. The reaction of  $\bullet\text{OH}$  with bicarbonate leads to carbonate radicals,  $\text{CO}_3^{\bullet-}$  [reaction (15);  $pK_a(\text{HCO}_3^{\bullet-}) < 0$  (Czapski *et al.*, 1999)], Part of the  $\bullet\text{OH}$  reaction with DOM leads to  $\text{O}_2^{\bullet-}$  (see above), and  $\text{O}_2^{\bullet-}$  reacts quickly with ozone to  $\bullet\text{OH}$ , whereas  $\text{CO}_3^{\bullet-}$  further reacts by self-reaction [reaction (16)] and with DOM [Suwannee River Fulvic acid,  $k = 280 \pm 90$  (mg of C/L) $^{-1}$  s $^{-1}$  (Canonica *et al.*, 2005)].

Because of the fast reaction of  $\text{O}_2^{\bullet-}$  with ozone, leading to  $\bullet\text{OH}$  (Chapter 13), this pathway leads to a destabilisation of ozone. Hoigné introduced the concept of “promoter” and “inhibitor” for compounds that accelerate or reduce the rate of ozone decay (Staehelin & Hoigné, 1985). This concept, often cited in the literature and repeated like a prayer wheel, is sometimes misunderstood, and it seems to be helpful to discuss it here in some detail. A typical promoter is methanol at pH 8. The reaction may be induced by the slow reaction of ozone with methanol, which may generate  $\bullet\text{CH}_2\text{OH}$  radicals (cf. Chapter 10). These react readily with  $\text{O}_2$  present in excess [reaction (12)]. The resulting peroxy radical can eliminate  $\text{HO}_2^{\bullet-}$ , but this reaction is slow ( $k < 3$  s $^{-1}$ ) (Rabani *et al.*, 1974). At pH 8, the  $\text{OH}^-$  concentration is  $1 \times 10^{-6}$  M.  $\text{OH}^-$  induces an  $\text{O}_2^{\bullet-}$  elimination with a bimolecular rate constant close to  $1.8 \times 10^{10}$  M $^{-1}$  s $^{-1}$  (Rabani *et al.*, 1974). Thus at pH 8, the rate of  $\text{O}_2^{\bullet-}$  formation is near  $1 \times 10^4$  s $^{-1}$  [reaction (12)–(14), for details see Chapter 14].



The product of reaction (16) gives rise to percarbonate upon hydrolysis. This sequence induces a very efficient chain reaction, that is, ozone decay is promoted. Scavenging of  $\bullet\text{OH}$  by bicarbonate [reactions (15) and (16),  $2k_{16} = 1.25 \times 10^7$  M $^{-1}$ s $^{-1}$  (Weeks & Rabani, 1966)] or carbonate, interrupts the chain and enhances the lifetime of ozone. It acts as an inhibitor.



The formation of percarbonate according to reaction (16) deserves a note. Percarbonate is in equilibrium with  $\text{H}_2\text{O}_2$  and bicarbonate (Richardson *et al.*, 2000), and is a stronger oxidant than  $\text{H}_2\text{O}_2$  (Bennett *et al.*, 2001; Yao & Richardson, 2000). It has been suggested as a suitable agent for pollution control, at least in a limited number of cases (Xu *et al.*, 2011).

Other  $\bullet\text{OH}$  scavengers such as tertiary butanol (tBuOH) and acetate also interrupt the chain, although some  $\text{O}_2^{\bullet-}$  is also formed in the bimolecular decay of their peroxy radicals [for tBuOH see Schuchmann & von Sonntag (1979), details in Chapter 14, for acetate see Schuchmann *et al.*, (1985)], the dominant decay routes do not give rise to  $\text{O}_2^{\bullet-}$ . Thus, these compounds also act effectively as inhibitors, although with a small promoting contribution. Other organic compounds act in a similar way, promoting and inhibiting as well. A case in point is DOM as discussed above. Thus, a careful look at the concept of “promoter” and “inhibitor” is required, and its discussion should take into consideration the advantages and the limitations of this approach.

To mimic the interaction between DOM moieties leading to  $\text{O}_2^{\bullet-}$  formation and components (promoters) that scavenge  $\bullet\text{OH}$  without further reaction with ozone (inhibitors), ozone stability was investigated in a synthetic system containing methanol which releases  $\text{O}_2^{\bullet-}$  after H-abstraction by  $\bullet\text{OH}$  and oxygen addition and either acetate, tBuOH or bicarbonate, which do not react further with ozone (Elovitz & von Gunten, 1999).

Table 3.1 shows the results for the synthetic systems at pH 8. For a methanol concentration of 70  $\mu\text{M}$  (scavenging rate  $k(\bullet\text{OH} + \text{MeOH}) \times [\text{MeOH}] = 7 \times 10^4$  s $^{-1}$ ), the pseudo-first-order rate constant for ozone decrease  $k_d$  is very similar for all scavengers, which act as inhibitors in this case.

**Table 3.1** Pseudo first-order rate constants for ozone decomposition ( $k_d$ ) and calculated  $R_{ct}$  values for model systems containing 70  $\mu\text{M}$  methanol and the inhibitors acetate, tertiary butanol (tBuOH) and bicarbonate at pH 8 [according to Elovitz & von Gunten, 1999]

Inhibitor S	Conc./ $\mu\text{M}$	$k(\bullet\text{OH} + [\text{S}]) \times [\text{S}]/\text{s}^{-1}$	$k_d (\text{s}^{-1})$	$R_{ct}$
None	–	–	$\sim 1.4 \times 10^{-2}$	–
Acetate	350	$2.8 \times 10^4$	$1.9 \times 10^{-3}$	$1.4 \times 10^{-8}$
tBuOH	46	$2.7 \times 10^4$	$1.9 \times 10^{-3}$	$1.3 \times 10^{-8}$
$\text{HCO}_3^-$	2600	$2.7 \times 10^4$	$2.4 \times 10^{-3}$	$1.9 \times 10^{-8}$

This shows that the interplay between promotion and inhibition of ozone decomposition is independent of the inhibitor and leads to similar ozone stability. Furthermore, the  $R_{ct}$ , the ratio between the concentrations of  $\bullet\text{OH}$  and ozone also is very similar in the range of  $(1.3\text{--}1.9) \times 10^{-8}$  (see below). Due to their high reactivity towards the water matrix and ozone,  $\bullet\text{OH}$  radicals have very low steady-state concentrations during ozonation, typically below  $10^{-12}$  M. Because direct measurement of  $\bullet\text{OH}$  concentrations during ozonation is impossible, there are basically two ways to tackle this problem: (i) Modelling ozone decay and thereby calculating the  $\bullet\text{OH}$  concentrations (Chelkowska *et al.*, 1992; Westerhoff *et al.*, 1997). The application of these models to natural waters is difficult due to the varying reactivity of DOM (see above). Usually, some rate constants have to be fitted to mimic kinetics of ozone decay in real water systems (Chelkowska *et al.*, 1992; Westerhoff *et al.*, 1997). Therefore, model predictions for transient  $\bullet\text{OH}$  concentrations generally disagree with experimental observations. (ii) Experimental calibration of  $\bullet\text{OH}$  formation by ozone in natural waters with the help of an ozone-resistant probe (Hoigné & Bader, 1979; Elovitz & von Gunten, 1999; Haag & Yao, 1992; Haag & Yao, 1993). Here, the decrease of an added probe (in low concentrations,  $\leq 1 \mu\text{M}$ ) which does not react with ozone but reacts quickly with  $\bullet\text{OH}$  is measured either as a function of the ozone dose (Hoigné & Bader, 1979) or continuously during ozonation (Elovitz & von Gunten, 1999; Haag & Yao, 1992; Haag & Yao, 1993). The first approach leads to the integral  $\bullet\text{OH}$  exposure and the corresponding ozone dose required for eliminating a particular compound to a certain percentage. The latter approach yields information on the dynamics of the oxidation by ozone and  $\bullet\text{OH}$ . Haag & Yao (1993) used continuous ozonation experiments for arriving at steady-state concentrations of  $\bullet\text{OH}$ . Part of the scavenging capacity of DOM was lost during these experiments and the mean steady-state concentration of  $\bullet\text{OH}$  became very high, resulting in a ratio of the concentrations of  $\bullet\text{OH}$  and  $\text{O}_3$  of about  $10^{-7}$ . In single ozone dosage experiments, ratios in the order of  $10^{-8}$ – $10^{-9}$  were obtained (Elovitz & von Gunten, 1999). Such ratios are more typical for ozonation and ozone-based AOPs under more realistic conditions.

The kinetics of the decrease of a probe (e.g. *p*-chlorobenzoic acid, pCBA) can be expressed as follows [equations (17) and (18)] (Elovitz & von Gunten, 1999).

$$-\frac{d[\text{pCBA}]}{dt} = k(\bullet\text{OH} + \text{pCBA}) \times [\text{pCBA}][\bullet\text{OH}] \quad (17)$$

Rearranging and integrating equation (17) leads to equation (18).

$$-\ln\left(\frac{[\text{pCBA}]}{[\text{pCBA}]_0}\right) = k(\bullet\text{OH} + \text{pCBA}) \times \int [\bullet\text{OH}] dt \quad (18)$$

The term  $\int [\bullet\text{OH}]dt$  represents the time-integrated concentration of  $\bullet\text{OH}$ , which is equal to  $\bullet\text{OH}$  exposure or  $\bullet\text{OH}\text{-ct}$ . The  $\bullet\text{OH}$  exposure can therefore be determined by measuring the relative decrease of, for example, pCBA as a function of the reaction time. The term  $R_{\text{ct}}$  defined in equation (19) describes the ratio of  $\bullet\text{OH}$  exposure to ozone exposure (or  $\bullet\text{OH}\text{-ct}$  and  $\text{O}_3\text{-ct}$ ) (Elovitz & von Gunten, 1999).

$$R_{\text{ct}} = \frac{\int [\bullet\text{OH}] dt}{\int [\text{O}_3] dt} \quad (19)$$

Substitution of equation (19) into equation (18) results in equation (20).

$$-\ln\left(\frac{[\text{pCBA}]}{[\text{pCBA}]_0}\right) = k(\bullet\text{OH} + \text{pCBA}) \times R_{\text{ct}} \int [\text{O}_3] dt \quad (20)$$

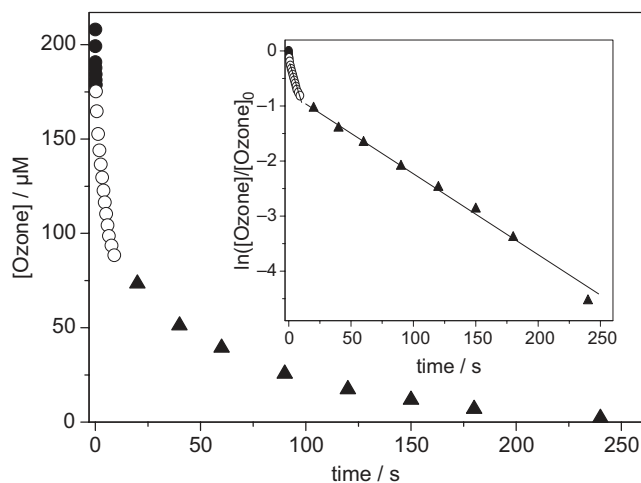
Ozone exposure can be calculated from the integral of “ozone concentration versus time data” (von Gunten & Hoigné, 1994).

For many natural waters, a plot of the logarithm of the relative decrease of pCBA vs. ozone exposure showed basically two phases for which fairly good linear correlations of the two parameters were obtained (Elovitz *et al.*, 2000a, b). This is quite similar to the behaviour of ozone (see below). This means that the ratio  $R_{\text{ct}}$  of the exposures (*ct* values) of  $\bullet\text{OH}$  and ozone remains constant, and for these conditions the ratio of the concentrations of  $\bullet\text{OH}$  and ozone ( $[\bullet\text{OH}]/[\text{O}_3]$ ) can be considered constant. This empirical concept is based on the observation that during ozonation the pseudo-first-order rate constant for transforming ozone into  $\bullet\text{OH}$  and scavenging of  $\bullet\text{OH}$  or their ratios remain constant.  $R_{\text{ct}}$  is typically in the range of  $10^{-8}$ – $10^{-9}$  (M/M) for various waters and varying water quality parameters such as pH, alkalinity, DOC and temperature (Elovitz *et al.*, 2000a). During the initial fast decomposition of ozone, the ratio is usually higher (by about a factor of 10) and varies as a function of the ozone dose (Pinkernell & von Gunten, 2001). Even during the initial phase of ozonation,  $R_{\text{ct}}$  can be approximately expressed by just one value without significant deviations in calculated micropollutant degradation (Acero *et al.*, 2000, 2001). Therefore, measurement of the ozone concentration and the oxidation of a probe allow prediction of the oxidation of a particular micropollutant during ozonation when rate constants for its reaction with ozone and  $\bullet\text{OH}$  are known (Acero *et al.*, 2000; Peter & von Gunten, 2007).

Ozone kinetics in most waters is multi-phasic (e.g. Figure 3.3). In drinking waters and wastewaters, kinetics may be adequately described by breaking it down in to three components following first-order kinetics (Nöthe *et al.*, 2009) (Figure 3.3) or to two components when the very fast and comparatively little ozone consuming component is disregarded (Schumacher *et al.*, 2004b; Buffle *et al.*, 2006b).

At a DOC of 7.2 mg/L and an ozone dose of 10 mg/L, the first component consumes  $\sim 1$  mg/L ozone at  $k = 0.071$  (mg DOC) $^{-1}$  s $^{-1}$ . The second component ( $k = 0.011$  (mg DOC) $^{-1}$  s $^{-1}$ ) consumes 5 mg/L ozone, while the third component consumes 4 mg/L ozone at 0.0019 (mg DOC) $^{-1}$  s $^{-1}$ . These data are normalised to the DOC in Table 3.2.

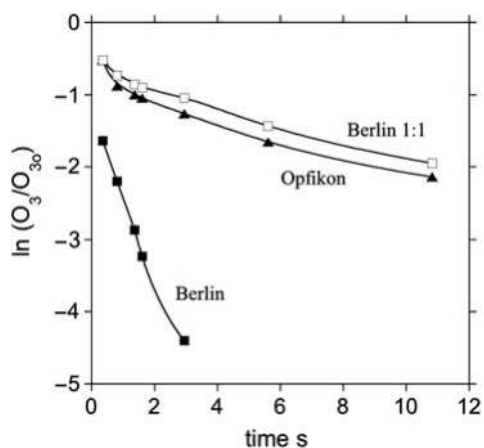
It seems that the variability of the ozone decomposition rate in wastewaters with similar DOC concentrations is much smaller than in natural waters which contain DOM of quite variable composition (see above). Figure 3.4 shows results for ozone decrease in Opfikon wastewater (DOC 4.5 mg/L) and Berlin wastewater (DOC 8.5 mg/L). For the same ozone dose (2.5 mg/L) and pH 8, ozone consumption in undiluted Berlin wastewaters is much faster than in Opfikon wastewater. However, for a 1:1 dilution of Berlin wastewater, adjusting the DOC to a similar level, ozone consumption rate is very similar for both waters. Thus, the concentrations of the ozone-reactive moieties must be very similar.



**Figure 3.3** Ozone decay as followed by stopped flow (circles) and batch-quench (triangles) at 17.3 °C and pH 8. Wastewater (WWTP Bottrop) and ozone solution were mixed in a 4:1 ratio leading to concentrations of  $[\text{DOC}] = 7.2 \text{ mg/L}$  and  $[\text{O}_3] = 10 \text{ mg/L}$  (208  $\mu\text{M}$ );  $[\text{HCO}_3^-] = 5.08 \text{ mM}$ . Inset: data plotted as  $\ln([\text{ozone}]/[\text{ozone}]_0)$  vs. time. Reprinted with permission from Nöthe *et al.*, 2009. Copyright (2009) American Chemical Society.

**Table 3.2** Rate of ozone decay and ozone consumption in wastewater according to (Nöthe *et al.*, 2009)

Process	Rate/ $(\text{mg DOC})^{-1} \text{ s}^{-1}$	Ozone consumption/ $\text{mg O}_3 (\text{mg DOC})^{-1}$
Initial	0.071	0.15
Fast	0.011	0.7
Slow	0.0019	>0.85



**Figure 3.4** Ozone consumption in Berlin (DOC 8.5 mg/L) and Opfikon (DOC 4.5 mg/L) wastewater for an ozone dose of 2.5 mg/L at pH 8. Data for a 1:1 dilution of Berlin wastewater (DOC 4.25 mg/L) with ultrapurified water are also shown. According to Buffle *et al.*, 2006a, with permission.

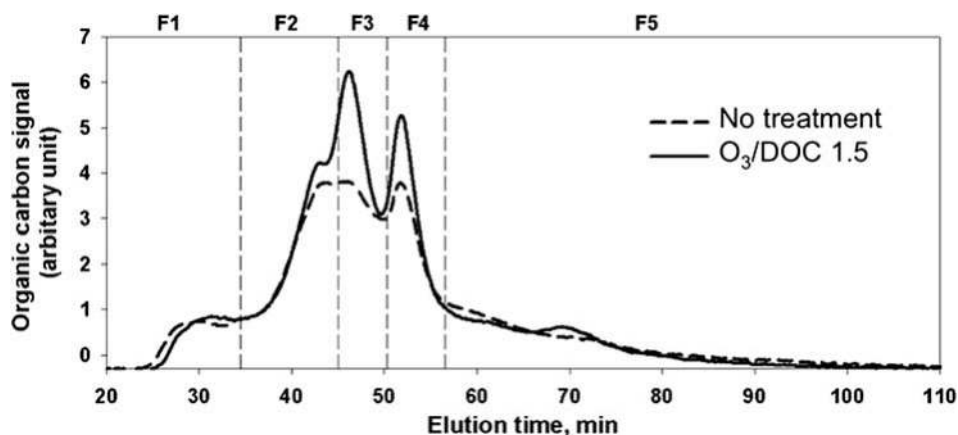


To reflect the continuum of the reactive moieties in DOM, the reactivity of ozone with DOM can conceptually be described by a model in which DOM is divided into, for example, five classes of compounds with second-order rate constants ranging from 10 to  $10^7 \text{ M}^{-1}\text{s}^{-1}$  (Buffle *et al.*, 2006a). For a wastewater, these individual moieties were assigned with fictitious concentrations in the range between 10 and  $70 \mu\text{M}$ . With this approach it was possible to describe the ozone decrease in a particular wastewater (Buffle *et al.*, 2006a). A similar approach allowed the modelling of reactions occurring in a bubble column (Nöthe *et al.*, 2010).

### 3.2 MOLECULAR WEIGHT DISTRIBUTION OF DISSOLVED ORGANIC MATTER

Gel permeation chromatography (GPC), also called size exclusion chromatography (SEC), has been widely used for the determination of the distributions of molecular weights of the DOMs in various waters. In brief, a solution of the analyte (here DOM) is injected onto a chromatographic column containing the separation gel. Low-molecular-weight material can penetrate into the pores of the gel, wherefrom it is eluted slowly while high-molecular-weight material that cannot penetrate the pores elutes faster. Lacking exact reference material, it is not possible to correlate a given retention time with the exact molecular weight of that fraction, but the order of elution, high-molecular-weight material first, low-molecular-weight material later will continue to be approximately correct. In wastewater, for example, the various GPC fractions have a different specific UV absorbance (SUVA). This is a clear indication, that one deals with polymers of different chemical properties and that the above caveat as to the uncertainties of the molecular weights of the various fractions is justified.

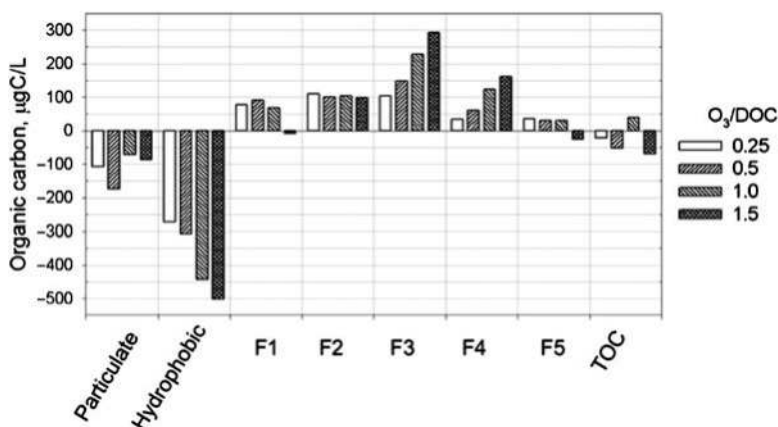
The development of detection systems that record not only UV absorbance but also DOC have been essential for the present topic (Huber *et al.*, 1990; Huber & Frimmel, 1991; Huber & Frimmel, 1992; Huber & Frimmel, 1996; Her *et al.*, 2002). Figure 3.5 shows an example of a SEC-OCD chromatogram of a wastewater before and after ozonation.



**Figure 3.5** Changes in the SEC-OCD chromatogram due to ozonation of 8- $\mu\text{m}$ -filtered secondary effluent of the Kloten-Opfikon wastewater treatment plant (Switzerland). SEC-OCD chromatogram before and after ozonation (specific ozone dose  $1.5 \text{ gO}_3/\text{g DOC}$ ). Regensdorf wastewater: TOC  $5 \text{ mg/L}$ , DOC  $4.7 \text{ mg/L}$ ,  $\text{HCO}_3^-$   $2.86 \text{ mM}$ , pH 7.0. F1, Biopolymers; F2, Humics; F3, Building blocks; F4, Low-molecular-weight humics and acids; F5, Low-molecular-weight neutrals (Lee & von Gunten, unpublished).

Irrespective of the origin of a water, there are always various partially-separated fractions detected. In natural waters and wastewaters, there is barely a fraction that may be associated with really low-molecular-weight material (<150 Da). SEC-OCD chromatograms of natural waters, drinking waters, soluble microbial products and wastewater have been published (Fuchs, 1985a, b, c; Allpike *et al.*, 2005; Meylan *et al.*, 2007; Jiang *et al.*, 2010). As expected, waters from different origins such as groundwaters, surface waters and wastewaters show substantial differences. Waters contained in barrages that are fed by nutrients from nearby agricultural activities may be rich in extracellular organic matter (EOM) of algae (Hoyer *et al.*, 1985) or groundwaters in peaty areas may be enriched in humics. Such differences are reflected in differences in ozone reactivity (Figure 3.2) but (obviously) also in SEC-OCD chromatograms. Common study objects are fulvic and humic acids, and data as to their structures are becoming increasingly available (Reemtsma & These, 2005; Reemtsma *et al.*, 2006a, b, 2008; These & Reemtsma, 2003, 2005; These *et al.*, 2004)

Figure 3.6 shows the changes of the various DOM fractions caused by ozone reactions. The so-called hydrophobic DOM fraction is retained by the chromatographic column, that is, not the entire DOC is accounted for by SEC-OCD.



**Figure 3.6** Changes in the SEC-OCD chromatogram due to ozonation of 8- $\mu$ m-filtered secondary effluent of the Kloten-Opfikon wastewater treatment plant (Switzerland). Changes of individual fractions (mgC/L) for various specific ozone doses between 0.25–1.5 gO<sub>3</sub>/gDOC. Regensdorf wastewater: TOC 5 mg/L, DOC 4.7 mg/L, HCO<sub>3</sub><sup>-</sup> 2.86 mM, pH 7.0. F1, Biopolymers; F2, Humics; F3, Building blocks; F4, Low-molecular-weight humics and acids; F5, Low-molecular-weight neutrals (Lee & von Gunten, unpublished).

The hydrophobic fraction can be determined from the difference between measured DOC and the sum of all fractions. This hydrophobic fraction decreases significantly with increasing ozone dose. This means that this part of DOC becomes detectable upon ozone treatment as fractions denoted ‘building blocks and low-molecular-weight humics and acids’. The higher molecular weight fractions ‘biopolymers’ and ‘humics’ are only marginally changed. Note that at the very high ozone dose of 7.5 mg/L only about 10% of the DOM-DOC is converted to low-molecular-weight compounds.

The specific ozone doses in Figures 3.5 and 3.6 are given on a gO<sub>3</sub>/gDOC basis. This unit has been chosen, because it is very practical for water treatment purposes, notably in wastewaters (Hollender *et al.*, 2009).

For any calculations of the reaction of ozone with DOM on the molecular level, the ozone concentration has to be given in units of M instead of mg/L and for the DOM (unit: mgC/L) an equivalent unit also has to be found. Considering that DOM is polymeric, one may express its concentration, as conveniently done with other polymers, in subunits. In DOM, which is not made up of repeating subunits of known molecular weight, this is not possible, but one may make the assumption that such subunits are made up of ten carbon atoms on average (Nöthe *et al.*, 2009). For aromatic subunits (see below), this would imply six for the core benzene ring and four for substituents and linking these subunits to one another. Potential polymeric carbohydrate-based polymers would have six carbon atoms for the core unit and two further carbon atoms when *N*-acetylated. This is not far from the ten carbon atoms assumed for the aromatic units. Heteroatoms (O, N, S) and hydrogens do not have to be included in this simplified approach, as it is only based on carbon atoms (DOC). With this assumption, water that has a DOC of 12 mgC/L is 100  $\mu$ M in DOM subunits. This approach now allows us to discuss many aspects of ozone chemistry in drinking water and wastewater on the molecular level. For example in a wastewater that contains a DOC of 10 mg/L (83  $\mu$ M in subunits), at an ozone dose of only 4 mg/L (83  $\mu$ M), each DOC subunit has reacted with ozone – on average. This approach will be used for a semi-quantitative assessment of certain DOM properties [Chemical Oxygen Demand (COD), absorption spectra, etc.].

### 3.3 MINERALISATION AND CHEMICAL OXYGEN DEMAND

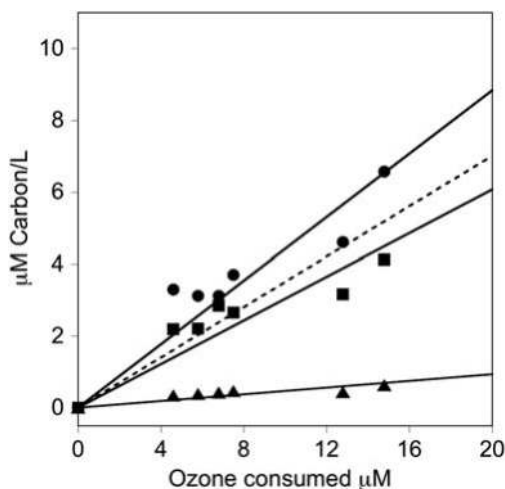
The degree of mineralisation of DOM is typically very small, of the order of 10% for an ozone/DOC mass ratio of 1.0 (Nöthe *et al.*, 2009). For the determination of the chemical oxygen demand (COD), another bulk method to characterise the organic matter in water treatment systems, two oxidants, namely dichromate and permanganate, are in use. Dichromate is the stronger oxidant and is capable of oxidising >95% of the DOC. Thus the COD value as determined with dichromate is typically 1.5 times higher than the permanganate value.

It has been observed in a wastewater that the COD drops by ~23% at an ozone to DOC mass ratio of 1.0. Typically, one out of the three O-atoms in ozone is transferred in ozone reactions. This indicates that the COD is reduced by about 0.65 mol O<sub>2</sub> (1.3 mol O) at an ozone/DOC mass ratio of 1.0. From the above, one would expect a value of 0.5 mol O<sub>2</sub> (1.0 mol O). Thus, it seems that the oxidation of wastewater is somewhat more efficient than suggested by the above stoichiometry. This is most likely due to the formation of •OH radicals which induce peroxy radical reactions, where O<sub>2</sub> serves as the oxidant (Chapter 14). In comparison, the DOC concentration is much less affected (Nöthe *et al.*, 2009). This is understood, as the DOC concentration only decreases when decarboxylation reactions set in, that is, when already substantially oxidised material is further oxidised (note that naturally occurring DOM is already partially oxidised). Mechanistic aspects of ozone-induced decarboxylation reactions are discussed in Chapters 6 and 14.

### 3.4 FORMATION OF ASSIMILABLE ORGANIC CARBON

As a consequence of the reaction of ozone with DOM, assimilable organic carbon (AOC) or biodegradable organic carbon (BDOC) is formed. This leads to the formation of smaller oxygen-rich molecules, such as carboxylic acids, aldehydes, ketones, etc. (Richardson *et al.*, 1999b), which are typically more biodegradable and can be summarised under AOC or BDOC (Hammes *et al.*, 2006; van der Kooij *et al.*, 1989; Siddiqui *et al.*, 1997). The mechanisms and kinetics of the formation of these compounds is governed by the reaction of ozone with DOM moieties such as phenols or other activated aromatic systems (Chapter 7). Upon ozonation, this leads to various olefins and eventually small organic acids

and aldehydes (Chapter 6). Even though this is only a model approximation of the interaction between DOM and ozone, similar processes occur under realistic conditions (Figure 3.7).



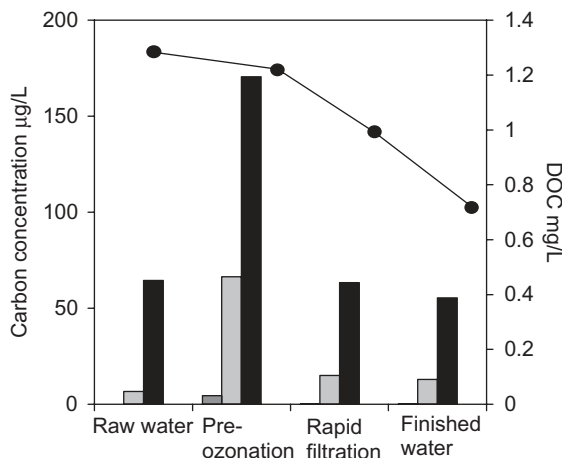
**Figure 3.7** Formation of AOC (circles), organic acids (squares) and aldehydes (triangles) during ozonation of Lake Zurich water. Dashed line: sum of acids, ketones and aldehydes. DOC 1.4 mg/L, T = 22 °C, pH 8, bicarbonate = 2.6 mM. Adapted from Hammes *et al.*, 2006, with permission.

In presence of tBuOH (as an  $\cdot\text{OH}$  scavenger), formation of organic acids is almost identical to that in absence of tBuOH in natural waters (Hammes *et al.*, 2006). Therefore, the formation of AOC which is mostly composed of carboxylic acids and aldehydes in the investigated waters is most likely due to direct ozone reactions with fast reacting moieties present in the humic fraction of DOM. In the case of Lake Zurich water, AOC can be mostly explained by carboxylic acids, whereas aldehydes and ketones contribute little. The results look different when algae are present during (pre-) ozonation. In this case, a significant portion of the AOC results from the lysis of algal cells and consists of intracellular cytoplasmic DOM (Hammes *et al.*, 2007). This material is released very quickly, even though the algae are not completely destroyed. Significant AOC formation of up to 740  $\mu\text{g C/L}$  has also been observed during ozonation of wastewater (Zimmermann *et al.*, 2011).

The removal of these compounds, measured as AOC or BDOC, is one of the major tasks in water treatment plants containing an ozonation step. Their removal can be achieved in a biological filtration step (sand, biological activated carbon filtration) after ozonation (cf. Chapter 5). This avoids regrowth of micro-organisms in the distribution systems, which is particularly important in countries where no or only limited disinfectant residual is used in the distribution systems (e.g. Germany, Netherlands, Austria, Switzerland).

Figure 3.8 shows the formation and removal of AOC, carboxylic acids and aldehydes/ketones during ozonation and biological filtration, respectively, in a drinking water treatment plant. Even though the AOC concentration at the effluent of the plant is similar to that of Lake Zurich water, the treatment train including pre- and intermediate ozonation and several biological filtration steps leads to a significant overall reduction of DOC which is very beneficial for the general water quality. Similarly, during

post-sand filtration of ozonated wastewater, AOC concentration was reduced significantly (up to 50%) (Zimmermann *et al.*, 2011).



**Figure 3.8** Formation and removal of AOC, carboxylic acids, aldehydes and ketones in the Lake Zurich drinking water treatment plant (Lengg, Zurich, Switzerland). Shaded bar: aldehydes and ketones; grey bars: total organic acids; black bars: assimilable organic carbon (AOC); circles: DOC. Adapted from Hammes *et al.*, 2006, with permission.

### 3.5 FORMATION AND MITIGATION OF DISINFECTION BY-PRODUCTS

As shown above, the application of ozone leads to a transformation of electron-rich moieties of the DOM. This has consequences for the formation of disinfection by-products (DBPs) during post-disinfection in, for example, the distribution system, and mostly leads to a reduced formation of DBPs. Nevertheless, for certain DBPs an increased formation has also been found after ozonation. One of the early applications of ozone was its significant potential to mitigate the formation of chlorophenols and bromophenols which are potent taste and odour compounds that can be formed during post-chlorination of phenol-containing waters (Bruchet & Duguet, 2004; Acero *et al.*, 2005; Piriou *et al.*, 2007). Under typical ozonation conditions, phenol is efficiently destroyed and therefore, halo-phenols cannot be formed any more (Chapter 7). Related to this, ozonation of natural waters generally reduces the formation of trihalomethanes (THMs) and haloacetic acids (HAAs) during post-chlorination (Reckhow *et al.*, 1986; Chaiket *et al.*, 2002; Chang *et al.*, 2002; Gallard & von Gunten, 2002; Chin & Bérubé, 2005; Meunier *et al.*, 2006; Hua & Reckhow, 2007; Li *et al.*, 2008). HAA formation was found to increase when chlorination was replaced by chloramination (Hua & Reckhow, 2007). The formation of trichloronitromethane (chloropicrin) and other halonitromethanes increased if natural waters were treated with ozone/chlorine compared to chlorine alone (Hoigné & Bader, 1988; Krasner *et al.*, 2006). In  $\text{Br}^-$ -containing waters, a shift to bromonitromethanes was observed (Krasner *et al.*, 2006; Krasner, 2009).

These studies did not use a biological filtration step between ozonation and post-chlorination/chloramination. It can be expected that some of the halonitromethane-precursors are biodegradable and

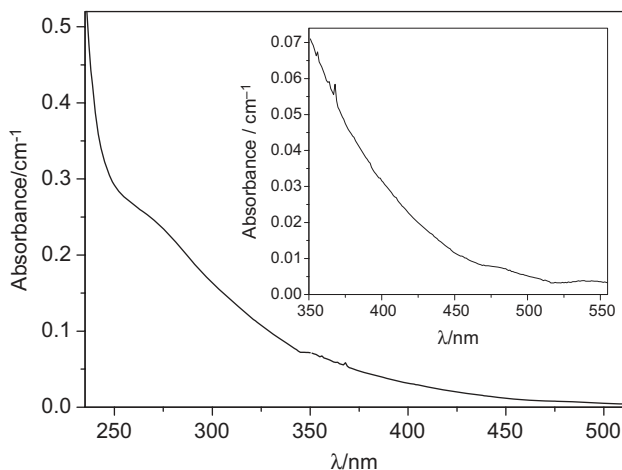
that biofiltration would reduce formation of halonitromethanes during post-chlorination/chloramination (Krasner, 2009).

In  $\text{Br}^-$ -containing waters, bromate is the main ozone disinfection by-product of concern (Chapters 11 and 14). However, numerous organic by-products such as bromoform, bromopicrin, (di)bromoacetic acid, dibromoacetone, cyanogen bromide, bromoketones, bromonitriles, bromoalkanes and bromohydrins can also be formed during ozonation or in combination with chlorine or chloramine (Richardson *et al.*, 1999a). In  $\text{I}^-$ -containing waters, ozonation rapidly oxidises  $\text{I}^-$  to iodate, which hinders the formation of iodo-organic compounds (Chapter 11).

NDMA precursors are generally oxidised during ozonation which leads to a reduction of NDMA formation during post-chloramination (Lee *et al.*, 2007b; Krasner, 2009; Shah *et al.*, 2012). Ozonation, however, may also enhance NDMA formation, as discussed in Chapters 8 and 11.

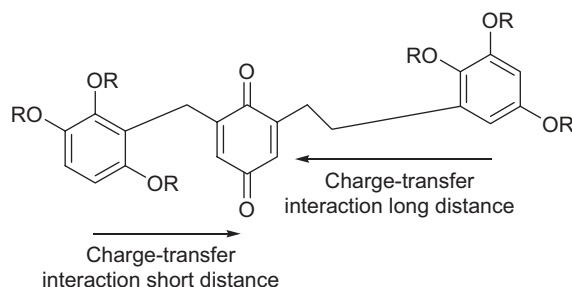
### 3.6 UV ABSORBANCE OF DISSOLVED ORGANIC MATTER

All natural DOMs have in common that they show strong UV absorptions. There is, however, a considerable variation in the specific UV absorbance (SUVA, absorbance at 254 nm per mg DOC) (Huber & Frimmel, 1992) The UV absorption of a typical wastewater is shown in Figure 3.9.



**Figure 3.9** UV–Vis spectrum of a typical wastewater (effluent of the municipal WWTP Neuss, Germany). Inset: blow-up of the long-wavelength side. At the short-wavelength side the absorbance rises steeply (not shown). Courtesy T. Nöthe.

The absorption of natural water, drinking water and wastewater DOM is characterised by a continuous increase in absorption on going to shorter wavelength without any noticeable peak. This is most uncommon for any isolated UV-absorbing (e.g. aromatic) compound (Nöthe *et al.*, 2009), and it has been convincingly shown that absorptions generally observed with aquatic DOMs must be due to charge transfer transitions of electron-donating (e.g. phenolic or alkoxyated) subunits to electron-accepting (e.g. quinoid) subunits present in close neighbourhood within this polymeric material (Del Vecchio & Blough, 2004). This is schematically shown in Figure 3.10.



**Figure 3.10** Schematic drawing of a quinone (electron acceptor) and alkoxyated benzenes (electron donors) at different distances. Charge transfer interactions between these sites in DOM give rise to electronic transitions (absorptions). The longer the distance the weaker the transition and thus the longer the wavelength of absorption.

The first electronic transition of isolated aromatic compounds that is near 250–260 nm is a forbidden transition with molar absorption coefficients of only a few hundred. Charge transfer transitions such as suggested by the Blough model (Del Vecchio & Blough, 2004) (Figure 3.10) are, however, allowed transitions and are characterised by high absorption coefficients. In a wastewater containing a DOM of 11 mg/L, the absorption at 254 nm was  $30 \text{ m}^{-1}$  (Schumacher, 2006; Nöthe *et al.*, 2009). Based on the above estimate of the concentration of subunits of this polymeric material, this relates to a molar absorption coefficient of the DOM subunits near  $3300 \text{ M}^{-1} \text{ cm}^{-1}$ , which is a much higher value than that of a typical aromatic compound. The featureless absorption, rising from the visible light into the UV region (Figure 3.9) can also be explained on the basis of this model. The absorption maxima of such charge transfer transitions vary with the distance between donor and acceptor (Figure 3.10). Structural conditions as depicted in Figure 3.10 and fluctuations of these distances induced by thermal motions are the reason for this featureless and very broad absorption.

Since the UV-active moieties in DOM (activated aromatic systems) have a certain reactivity with ozone, the UV absorption and SUVA have been used as empirical surrogate parameters to predict the ozone consumption rate in natural waters (Elovitz *et al.*, 2000b). A reasonable correlation between the pseudo-first-order rate constant for ozone decrease and  $\text{SUVA}_{254}$  with a correlation coefficient  $R^2 = 0.79$  was found for nine DOM isolates (Elovitz *et al.*, 2000b). In these correlations, especially Suwannee river humic acid, but also Suwannee river fulvic acid, DOM isolates, often used to simulate drinking water DOM, proved to be outliers with significantly higher ozone reactivity (see Figure 3.2).

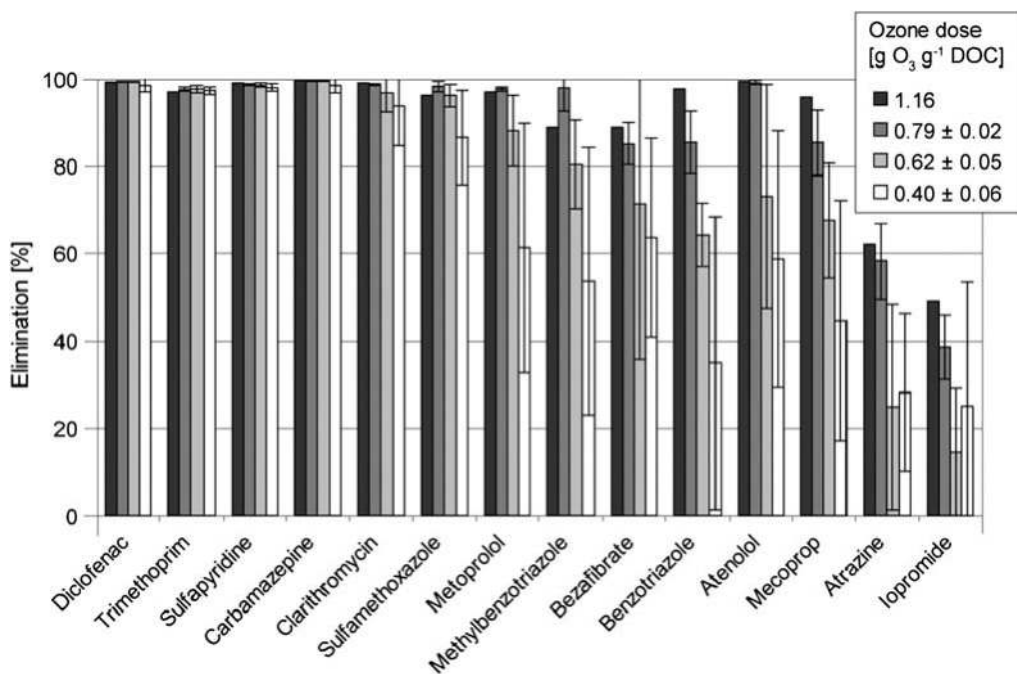
The change in the UV absorption of DOM has been used as an empirical parameter for predicting micropollutant removal during ozonation of wastewaters (Nanaboina & Korshin, 2010; Buffle *et al.*, 2006a; Wert *et al.*, 2009b; Bahr *et al.*, 2007), but such changes cannot be used for mechanistic interpretations as attempted by Nanaboina & Korshin (2010).

### 3.7 RELEVANCE OF OZONE KINETICS FOR THE ELIMINATION OF MICROPOLLUTANTS

For the elimination of micropollutants, competition between DOM of the water matrix and pollutant (P) for ozone has to be taken into account [reactions (21) and (22)].



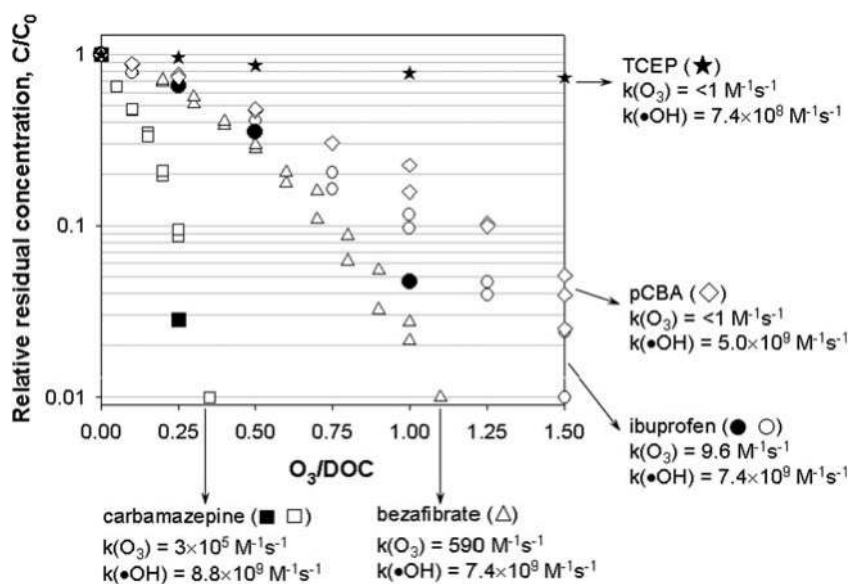
The kinetics of the reaction of ozone with DOM thus strongly affects the efficiency of micropollutant transformation by ozone (Katsoyiannis *et al.*, 2011). Only those micropollutants that react rapidly stand a chance of being oxidised directly by ozone. Here, we only consider the very first step in the sequence of events that eventually will lead to mineralisation. This is justified, because in most cases, the biological activity of the micropollutant is practically fully suppressed by this very first oxidation step (Chapter 4). For a wastewater (DOC = 10 mg/L, pH 8), one can neglect the slow process for an ozone dose of, for example, 5 mg/L. Based on the example shown in Figure 3.3, the ozone decay can be simulated by breaking up the process into several kinetic phases. A simulation has shown (Nöthe *et al.*, 2009) that during the consumption of the first mg ozone per L all micropollutants that have ozone rate constants  $>10^5 \text{ M}^{-1}\text{s}^{-1}$  are completely ( $>90\%$ ) eliminated, micropollutants that react with  $10^4 \text{ M}^{-1}\text{s}^{-1}$  are eliminated to about 25% remaining, and micropollutants that react an order of magnitude more slowly are practically not affected. This situation is substantially improved by the reaction of the next 4 mg/L ozone. Here, the lower rate constant of ozone consumption by the wastewater matrix and the higher ozone dose cooperate. Complete elimination is now achieved for all micropollutants that react with  $3 \times 10^3 \text{ M}^{-1}\text{s}^{-1}$  and micropollutants that react with  $1 \times 10^3 \text{ M}^{-1}\text{s}^{-1}$  are eliminated to about 50%. For the elimination of less reactive micropollutants, higher ozone doses would be required. For an ozone dose of 10 mg/L (1 gO<sub>3</sub>/gDOC), micropollutants that react with  $1 \times 10^3 \text{ M}^{-1}\text{s}^{-1}$  are fully eliminated, and the concentrations of even less reactive ones are noticeably lowered ( $k = 300 \text{ M}^{-1}\text{s}^{-1}$  to 25%;  $k = 100 \text{ M}^{-1}\text{s}^{-1}$  to 65% remaining). The elimination of micropollutants with varying second-order rate constants for their reaction with ozone is illustrated in Figure 3.11 as a function of the specific ozone dose.



**Figure 3.11** Elimination of selected micropollutants during ozonation of secondary effluent of a full-scale ozonation plant for various specific ozone doses (Regensdorf, Switzerland). DOC  $5.2 \pm 0.6 \text{ mg/L}$ , pH 7. Reprinted with permission from Hollender *et al.*, 2009. Copyright (2009) American Chemical Society.



Fast reacting compounds from diclofenac to sulfamethoxazole ( $k > 10^4 \text{ M}^{-1}\text{s}^{-1}$ ) are fully eliminated at specific ozone doses of 0.4 g ozone per g DOC. For compounds with intermediate ozone reactivity, (metoprolol to atenolol,  $2 \times 10^2 \text{ M}^{-1}\text{s}^{-1} < k < 10^4 \text{ M}^{-1}\text{s}^{-1}$ ) significantly higher specific ozone doses of about 1 g ozone per g DOC are necessary for complete elimination. For compounds with second order rate constants near  $100 \text{ M}^{-1}\text{s}^{-1}$  and below (mecoprop to iopromide), specific ozone doses of 1 gO<sub>3</sub>/gDOC lead to eliminations of 50–90%. For these compounds, elimination is dominated by  $\bullet\text{OH}$ . The dependence of the degree of elimination of micropollutants in a wastewater on the reactivity with ozone and  $\bullet\text{OH}$  is further illustrated in Figure 3.12 for compounds that cover the full range of ozone and  $\bullet\text{OH}$  rate constants.



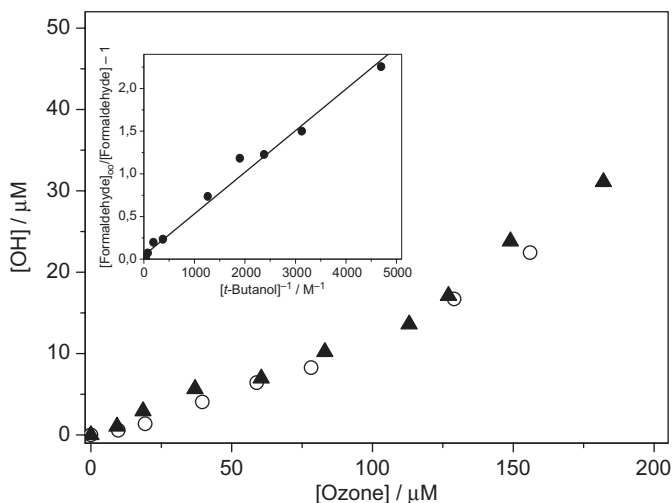
**Figure 3.12** Residual concentrations of selected spiked micropollutants at sub to low  $\mu\text{g/L}$  ranges after ozonation of Klöten-Opfikon wastewater effluent with variable ozone doses up to ratios of ozone : DOC of 1.5 (g/g). Filled and open symbols represent experiments with low ( $\sim 1 \mu\text{g/L}$ ) and high dosage ( $\sim 200 \mu\text{g/L}$ ) of the micropollutants. pCBA: *p*-chlorobenzoic acid, TCEP: Tris-(2-chloroethyl) phosphate. Second order rate constants for the reaction with ozone and  $\bullet\text{OH}$  are given. According to Lee, Gerrity, Snyder & von Gunten unpublished.

Micropollutants such as the chlorinated trialkylphosphates have considerably lower  $\bullet\text{OH}$  rate constants than the aromatic x-ray contrast media such as iopromide (Table 3.3). These are hence degraded to an even lesser extent (cf. Figure 3.14).

### 3.8 HYDROXYL RADICAL YIELD AND $\bullet\text{OH}$ -SCAVENGING RATE OF DISSOLVED ORGANIC MATTER

Ozone reacts with a number of organic compounds, notably amines (Chapter 8) and electron-rich aromatic compounds (e.g. phenols and alkoxyated benzenes; Chapter 7) by giving rise to  $\bullet\text{OH}$  in side reactions, and hence  $\bullet\text{OH}$  is always formed when drinking water and wastewater are treated with ozone. The  $\bullet\text{OH}$  yield in wastewater has been determined making use of the tertiary butanol (tBuOH) assay (Chapter 14). In brief,

tBuOH is added in large excess to overrun the  $\bullet\text{OH}$  scavenging rate of the wastewater (see above), and one of the products of the reaction of  $\bullet\text{OH}$  with tBuOH, formaldehyde, is determined. Formaldehyde is not formed in the reaction of ozone with wastewater in the absence of tBuOH. As a rule of thumb, the  $\bullet\text{OH}$  yield is twice the formaldehyde yield (Flyunt *et al.*, 2003a). Using this approach, the data shown in Figure 3.13 were obtained. In the inset of this figure, a competition plot of tBuOH and the water matrix for  $\bullet\text{OH}$  is shown (for competition kinetics see Chapter 2).



**Figure 3.13** The  $\bullet\text{OH}$  radical yield as a function of the ozone dose in a wastewater (WWTP Bottrop, pH 8, DOC after dilution by ozone-containing water 8.0 mg/L). Inset: Competition of the water matrix and tertiary butanol for  $\bullet\text{OH}$  radicals formed upon the addition of ozone (112  $\mu\text{M}$ , 5.6 mg/L) to wastewater (WWTP Neuss, pH 8, DOC = 9.05 mg/L, 3.8 mM bicarbonate). Reprinted with permission from Nöthe *et al.*, 2009. Copyright (2009) American Chemical Society.

As seen from Figure 3.13, the  $\bullet\text{OH}$  yield continues to remain constant or even slightly increases up to an ozone dose of 190  $\mu\text{M}$ . At a DOC of 8 mg/L (67  $\mu\text{M}$  in subunits) the ozone concentration is 2.8 times that of the DOM subunits. Thus, the capacity of the DOM for  $\bullet\text{OH}$  production does not become exhausted but rather new  $\bullet\text{OH}$ -generating sites are formed in the reaction of ozone with DOM, as discussed above.

The  $\bullet\text{OH}$  yield can vary significantly from one water source to another. By increasing the ozone:DOC ratio (g/g) to 2.0 the  $\bullet\text{OH}$  yield may rise to  $\sim 30\%$  (Lee & von Gunten, in preparation). Apparently, there is no general  $\bullet\text{OH}$  yield, and for each water to be treated with ozone  $\bullet\text{OH}$  formation has to be assessed.

### 3.9 ELIMINATION OF OZONE-REFRACTORY MICROPOLLUTANTS BY THE $\bullet\text{OH}$ ROUTE

Ozone-refractory micropollutants are eliminated to a certain extent by the  $\bullet\text{OH}$  route. There is not such a high variation in  $\bullet\text{OH}$  rate constants [for a compilation see (Buxton *et al.*, 1988)] as for ozone. Yet for ozone-refractory micropollutants that we are concerned with in drinking water and wastewater, a variation of the  $\bullet\text{OH}$  rate constant by a factor of ten ( $4.5 \times 10^8$  to  $7 \times 10^9 \text{ M}^{-1}\text{s}^{-1}$ ) is typical (Table 3.3), and this is of relevance for the elimination efficiency and therefore the ozone dose required for achieving a desired elimination.

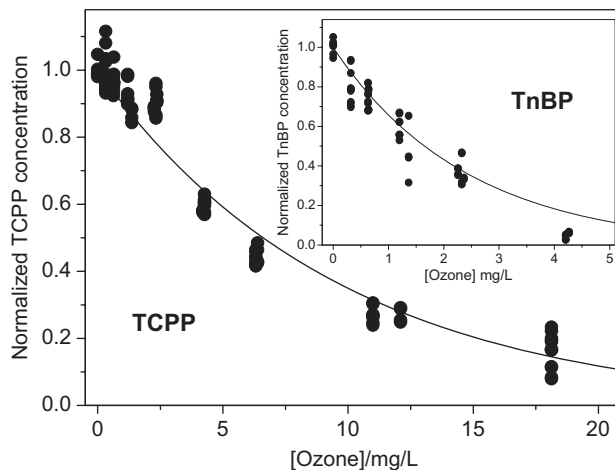
**Table 3.3** Compilation of ozone and  $\bullet\text{OH}$  rate constants (unit:  $\text{M}^{-1}\text{s}^{-1}$ ) of selected ozone-refractory micropollutants in drinking water and wastewater at pH 7

Compound	Source/application	$k$ (ozone)	$k(\bullet\text{OH})$	Reference
Atrazine	Herbicide	6	$3 \times 10^9$	Acero <i>et al.</i> , 2000
Iopromide	X-ray contrast agent	$<0.8$	$3.3 \times 10^9$	Huber <i>et al.</i> , 2003
Diazepam	Tranquiliser	0.75	$7.2 \times 10^9$	Huber <i>et al.</i> , 2003
NDMA	Oxidation by-product	$5 \times 10^{-2}$	$4.5 \times 10^8$	Lee <i>et al.</i> , 2007a
Tris-(2-chloro-isopropyl) phosphate (TCPP)	Flame retardant	$\ll 1$	$7 \times 10^8$	Pocostales <i>et al.</i> , 2010
Tris-(2-chloro-ethyl) phosphate (TCEP)	Flame retardant	$\ll 1$	$7.4 \times 10^8$	Watts & Linden, 2009
Tri- <i>n</i> -butyl phosphate (TnBP)	Plasticiser	$\ll 1$	$\approx 2.8 \times 10^9$	Pocostales <i>et al.</i> , 2010

For the elimination of ozone-refractory micropollutants, one may write the competing reactions (23) and (24), where M denotes the water matrix (DOC plus bicarbonate, see above) and P the micropollutant.



The  $\bullet\text{OH}$  scavenging rate that determines the rate of reaction (24) and  $\bullet\text{OH}$  yields (in wastewater) has been given above. Based on this, the elimination efficiency of a given ozone-refractory micropollutant can be calculated. This is shown in Figure 3.14 for two organic phosphates.



**Figure 3.14** Experimental data (symbols) and simulation (solid lines) of the degradation of TCPP and TnBP (inset) in diluted Neuss wastewater (DOC = 5.5 mg/L). Reprinted with permission from Pocostales *et al.*, 2010. Copyright (2010) American Chemical Society.

The  $\bullet\text{OH}$  scavenging rate of a water can be determined by measuring the rate of the apparent rate constant for the decrease of a probe compound [e.g. 4-chlorobenzoic acid (pCBA)] as a function of varying tBuOH concentrations (Katsoyiannis *et al.*, 2011). Without knowing the  $\bullet\text{OH}$  scavenging rate of a given water, one can also follow the elimination of an ozone-refractory test compound such as pCBA for which the  $\bullet\text{OH}$  rate constant is known ( $k = 5 \times 10^9 \text{ M}^{-1}\text{s}^{-1}$ , Figure 3.12), and with the knowledge of the  $\bullet\text{OH}$  rate constants of other micropollutants, their degradation can be calculated (Acero *et al.*, 2000; Acero & von Gunten, 2001; Huber *et al.*, 2003; Peter & von Gunten, 2007). The  $\bullet\text{OH}$  rate constants of selected ozone-refractory micropollutants are compiled in Table 3.3.

### 3.10 OZONE-BASED ADVANCED OXIDATION PROCESSES

There are three ozone-based Advanced Oxidation Processes (AOPs) that lead to the formation of  $\bullet\text{OH}$ , (i) the reaction of ozone with  $\text{H}_2\text{O}_2$  or, more correctly, with its anion,  $\text{HO}_2^-$  (peroxone process), (ii) photolysis of ozone with UV light (UV/ozone) and (iii) reaction of ozone with activated carbon (carboxone process). In principle, this can also provide the means for coping with ozone-refractory pollutants, as  $\bullet\text{OH}$  radicals are much more reactive than ozone. To what extent, this expectation can be realised in practice, will be discussed below.

#### 3.10.1 Peroxone process

The best-known of the three ozone-based AOPs is the peroxone process. Details of its chemistry are discussed in Chapter 11. Here, it is recalled that  $\text{H}_2\text{O}_2$  does not react efficiently with ozone, but that the reaction with  $\text{HO}_2^-$  is fast, and that the  $\text{HO}_2^-$  reaction dominates over a wide pH range that extends even into the acid pH region. This pH dependence is given by equation (25).

$$k_{\text{obs}} = k(\text{HO}_2^- + \text{O}_3) \times 10^{(\text{pH} - \text{p}K_{\text{a}})} \quad (25)$$

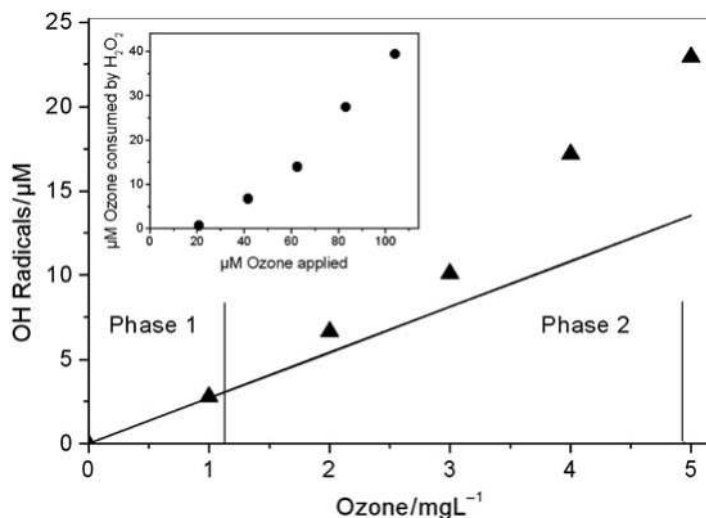
Due to this marked pH dependence and the high  $\text{p}K_{\text{a}}$  of  $\text{H}_2\text{O}_2$  [ $\text{p}K_{\text{a}}(\text{H}_2\text{O}_2) = 11.8$ ], this reaction is fast only at high pH. For example at pH 8,  $k_{\text{obs}}$  is  $1.5 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$  and at pH 7 one order of magnitude lower,  $k_{\text{obs}} = 150 \text{ M}^{-1} \text{ s}^{-1}$ . This slow reaction has to compete with other ozone decay processes such as the reaction with DOM (for an example see below). Moreover, the  $\bullet\text{OH}$  yield is only half of the value that a simplified stoichiometry (Staehelin & Hoigné, 1982) suggests (von Sonntag, 2008) (for the reason for this, see Chapter 11).

Increasing the rate by increasing the  $\text{H}_2\text{O}_2$  concentration may under certain conditions not be an advantage as  $\text{H}_2\text{O}_2$  also acts as an  $\bullet\text{OH}$  scavenger [reaction (26),  $k = 2.7 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$  (Buxton *et al.*, 1988)].



In a sequence of reactions,  $\text{HO}_2\bullet$  reacts with ozone [reactions (2)/(3) and (10)/(11)] giving again rise to  $\bullet\text{OH}$  (for details, see Chapter 13). As a result, ozone and  $\text{H}_2\text{O}_2$  are destroyed without the desired effect of pollutant degradation. Yet compared to other  $\bullet\text{OH}$  reactions, the rate constant of reaction (26) is very low, and this prevents this chain reaction from becoming of importance when the  $\bullet\text{OH}$  scavenging rate of the matrix is high, for example, in surface waters or wastewaters.

For a wastewater, the effect of  $\text{H}_2\text{O}_2$  on the formation of  $\bullet\text{OH}$  has been simulated on the basis of known rate constants (Figure 3.15).

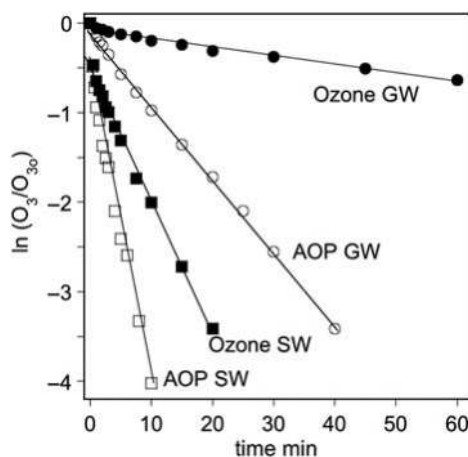


**Figure 3.15** Simulation of the  $\bullet\text{OH}$  yield for a wastewater containing a DOC of 5.5 mgC/L (diluted Neuss wastewater). The solid line is based on 13%  $\bullet\text{OH}$  yield in the reaction of ozone with the DOC in the absence of  $\text{H}_2\text{O}_2$  (cf. Figure 3.14). The symbols indicate the total  $\bullet\text{OH}$  yields formed in the reaction of ozone with the DOC and in the peroxone process (molar ratio ozone/ $\text{H}_2\text{O}_2 = 2.0$ ). Inset: ozone consumption from the peroxone process as a function of the applied ozone concentration (units:  $\mu\text{M}$ , note that 1 mg/L ozone = 21  $\mu\text{M}$ ). Lines near 1 and 5 mg/L ozone indicate the ranges of first and second phase in ozone kinetics of this wastewater (cf. Table 3.2). Reprinted with permission from Pocostales *et al.*, 2010. Copyright (2010) American Chemical Society.

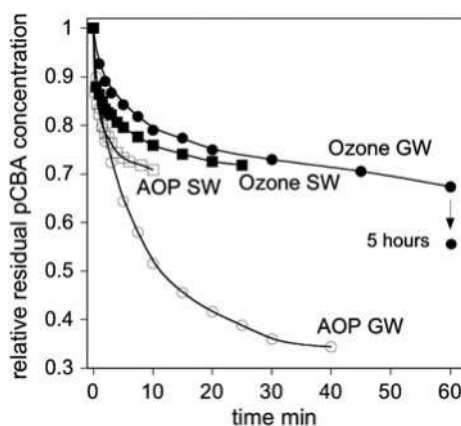
As  $\bullet\text{OH}$  formation in the Neuss wastewater is 13% of ozone consumption and in the peroxone process only 50% (see above), the excess gain in  $\bullet\text{OH}$  formation is only 37% when ozone reacts with  $\text{H}_2\text{O}_2$  instead of reacting with the wastewater DOM. Because ozone reacts rapidly with the water matrix at the early stage,  $\text{H}_2\text{O}_2$  can barely compete. Only when the matrix reaction becomes slower and the  $\text{H}_2\text{O}_2$  concentration higher, is there a surplus of  $\bullet\text{OH}$ . This surplus of  $\bullet\text{OH}$  has to be paid for by a considerable depletion of ozone (inset in Figure 3.15) and a shortening of ozone lifetime, with the effect that disinfection and micropollutant destruction by the direct ozone reaction are now much less effective. This mainly affects micropollutants that have a low to medium ozone rate constant. Whether this loss in micropollutant destruction by ozone is offset by an  $\bullet\text{OH}$ -induced destruction has not yet been tested experimentally.

In water treatment practice, AOPs are often considered as processes with a “magic” touch. In the case of the AOP ozone/ $\text{H}_2\text{O}_2$ , a better elimination of micropollutants is suggested compared to the conventional ozonation process. In Figure 3.16, the ozone stability is shown for a groundwater (DOC 1 mg/L, alkalinity 5.2 mM) and a surface water (DOC 3.2 mg/L, alkalinity 3.8 mM). Ozone stability is affected by the addition of  $\text{H}_2\text{O}_2$  in both waters even at pH 7 (Figure 3.16).

The effect is more pronounced in the groundwater than in the surface water. The larger effect in the groundwater is due to the lower DOC which results in a higher stability of ozone in the absence of  $\text{H}_2\text{O}_2$ . When  $\text{H}_2\text{O}_2$  is added, the relative contribution of  $\text{H}_2\text{O}_2$  to ozone decomposition is very high in the groundwater, whereas in the surface water it is small. The relative residual concentration of pCBA, an ozone-refractory compound, is shown in Figure 3.17 for the same experimental conditions.



**Figure 3.16** Ozonation of a groundwater (GW) (DOC 1 mg/L, alkalinity 5.2 mM) and a surface water (SW) (DOC 3.2 mg/L, alkalinity 3.8 mM). First order kinetic representation of the ozone decrease. Experimental conditions: ozone dose  $2.1 \times 10^{-5}$  M,  $\text{H}_2\text{O}_2$  dose  $1.0 \times 10^{-5}$  M, pCBA dose  $2.5 \times 10^{-7}$  M, pH 7, 11 °C. Adapted from Acero & von Gunten, 2001. Reprinted by permission *Journal AWWA*. Copyright American Water Works Association.



**Figure 3.17** Ozonation of a groundwater (GW) (DOC 1 mg/L, alkalinity 5.2 mM) and a surface water (SW) (DOC 3.2 mg/L, alkalinity 3.8 mM). Kinetics of the transformation of pCBA. Experimental conditions: ozone dose  $2.1 \times 10^{-5}$  M,  $\text{H}_2\text{O}_2$  dose  $1.0 \times 10^{-5}$  M, pCBA dose  $2.5 \times 10^{-7}$  M, pH 7, 11 °C. From Acero & von Gunten, 2001, reprinted by permission *Journal AWWA*. Copyright American Water Works Association.

Two features should be highlighted: (i) the kinetics of the transformation of pCBA and (ii) the extent of pCBA transformation. In both waters, the rate of pCBA transformation is higher in the presence of  $\text{H}_2\text{O}_2$ , with a more pronounced effect in the groundwater. For a hypothetical contact time in a reactor of 15 min, the relative transformation in the absence and in the presence of  $\text{H}_2\text{O}_2$  is 20% and 55%, respectively. This shows

that the addition of  $\text{H}_2\text{O}_2$  allows a higher degree of transformation for a given hydraulic residence time. The extent of transformation has to be compared for the complete depletion of ozone in the absence and presence of  $\text{H}_2\text{O}_2$ . In the surface water, the overall extent of transformation is fairly similar for both scenarios, whereas in the groundwater,  $\text{H}_2\text{O}_2$  addition improves the elimination of pCBA from about 40 to 65%. Thus, depending on water quality, a similar or only small increase of the extent of transformation is observed in presence of  $\text{H}_2\text{O}_2$ .

### 3.10.2 UV photolysis of ozone

In his pioneering work, Taube concluded that only  $\text{H}_2\text{O}_2$  is formed upon the photolysis of ozone in water (Taube, 1957). This conclusion was based on the apparent 1:1 stoichiometry of ozone consumption and  $\text{H}_2\text{O}_2$  formation in the presence of acetate as an  $\bullet\text{OH}$  scavenger. At this time, it was not yet known that in its  $\bullet\text{OH}$ -induced reactions in the presence of  $\text{O}_2$ , acetate gives rise to relatively large amounts of  $\text{H}_2\text{O}_2$  (Schuchmann *et al.*, 1985). Later on, when it was realised that  $\bullet\text{OH}$  radicals are generated in this reaction, the ozone/UV system was widely discussed among potential AOPs (Glaze *et al.*, 1982; Peyton *et al.*, 1982; Peyton & Glaze, 1987, 1988; Takahashi, 1990; Gurol & Vatistas, 1987; Ikemizu *et al.*, 1987; Morooka *et al.*, 1988). The reactions in this rather complex system are now reasonably well understood (Reisz *et al.*, 2003).

Upon photolysis, ozone is decomposed into  $\text{O}_2$  and oxygen atoms  $\text{O}({}^1\text{D})$  (excited state) and  $\text{O}({}^3\text{P})$  (ground state) (Wayne, 1987; Schriver-Mazzuoli, 2001; Bauer *et al.*, 2000; Smith *et al.*, 2000; Taniguchi *et al.*, 2000). In the gas phase and below 300 nm, the main processes (quantum yield,  $\Phi \approx 0.9$ ) are reactions (27) and (28), that is, the formation of  $\text{O}({}^1\text{D})$  and singlet oxygen,  $\text{O}_2({}^1\Delta_g)$ , as well as oxygen in its ground state,  $\text{O}_2({}^3\Sigma_g^-)$ . Reactions that yield  $\text{O}({}^3\text{P})$  [reactions (29) and (30)] are of lower importance ( $\Phi \approx 0.1$ ) (Wayne, 1987; Hancock & Tyley, 2001; Wine & Ravishankara, 1982).



The quantum yield of  $\text{O}({}^1\text{D})$  formation falls to a value near 0.1 above a wavelength of about 320 nm but not to zero. This shows that the spin-forbidden formation of  $\text{O}({}^1\text{D})$  and  $\text{O}_2({}^3\Sigma_g^-)$  [reaction (28)] is possible (Bauer *et al.*, 2000; Smith *et al.*, 2000; Taniguchi *et al.*, 2000; Jones & Wayne, 1970).  $\text{O}({}^1\text{D})$  is very energetic [heat of formation,  $437 \text{ kJ mol}^{-1}$  (Taniguchi *et al.*, 1999)] and therefore reacts rapidly even with water [reaction (31),  $k = 1.8 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$  (Biedenkapp *et al.*, 1970), by insertion (Taube, 1957)].



In the gas phase, the excess energy of the  $\text{H}_2\text{O}_2$  molecule so formed results in the fragmentation of the O–O bond [reaction (32); BDE =  $210 \text{ kJ mol}^{-1}$  (McKay & Wright, 1998)].



In aqueous solution, the rapid thermalisation of the “hot”  $\text{H}_2\text{O}_2$  [reaction (33)] competes with reaction (32).



In addition, the solvent-cage effect inhibits the escape of  $\bullet\text{OH}$ , that is, recombination competes with diffusion into the bulk. Hence, most of the  $\text{O}(^1\text{D})$  will be converted into  $\text{H}_2\text{O}_2$ .

In contrast, the reaction of  $\text{O}(^3\text{P})$  with water is endergonic by about  $75 \text{ kJ mol}^{-1}$  (Amichai & Treinin, 1969) and can be neglected here. Most of the  $\text{O}(^3\text{P})$  disappears by reacting with ground state oxygen [ $\text{O}_2(^3\Sigma_g^-)$ ] regenerating ozone [reaction (34);  $k = 4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Kläning *et al.*, 1984)].



Reactions of  $\text{O}(^3\text{P})$  with organic material are slow in comparison (Bucher & Scaiano, 1994; Herron & Huie, 1969) and may be neglected for typical AOP conditions.

The quantum yield of *direct* ozone photolysis is  $\Phi = 0.5$ , and, using *t*BuOH to scavenge  $\bullet\text{OH}$  radicals, it has been shown that only about 10% of the photolysed ozone furnish  $\bullet\text{OH}$  ( $\text{O}_3 + \text{H}_2\text{O} + h\nu \rightarrow 2 \bullet\text{OH}$ ) (Reisz *et al.*, 2003). Thus, the quantum yield of  $\bullet\text{OH}$  production is relatively low,  $\Phi \approx 0.1$ , when compared with the photolysis of  $\text{H}_2\text{O}_2$  [ $\Phi(\text{H}_2\text{O}_2) = 1.0$  (Legrini *et al.*, 1993)].

The UV/ozone process has never gained much practical application in water treatment. In comparison with the UV/ $\text{H}_2\text{O}_2$  process, it is not capable of minimising the bromate problem. Yet, there are many lab-scale studies. A considerable number of these do not take into account that ozone reacts rapidly with the substrate molecules resulting in an ozone steady-state concentration which is so low that ozone photolysis cannot contribute to product formation. The reported differences in product yields can thus not be related to ozone photolysis but rather to a photolysis of starting material and products.

### 3.10.3 Reaction of ozone with activated carbon

The reaction of ozone with activated carbon (AC) leads to the formation of  $\bullet\text{OH}$ , and it has been believed that this is a catalytic reaction (Jans & Hoigné, 1998). Yet, a more detailed study has shown that electron-donating residues within AC, notably its nitrogen content, cause this  $\bullet\text{OH}$  production, and when this source is exhausted,  $\bullet\text{OH}$  production comes to a halt (Sánchez-Polo *et al.*, 2005). XPS measurements indicated that the pyrrole content of the AC decreases during ozonation. Based on this characterisation and the measurement of  $\text{O}_2^{\bullet-}$  formation (Sánchez-Polo *et al.*, 2005) by the tetranitromethane method [ $\text{O}_2^{\bullet-}$  reacts quickly with ozone giving rise to  $\bullet\text{OH}$  (Chapter 13)], a hypothetical mechanism for the ozone reaction with AC has been formulated [reaction (35)].

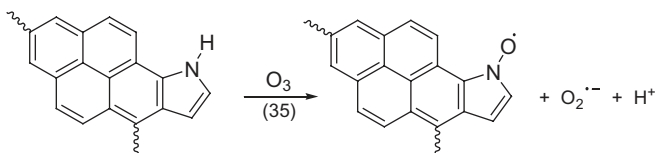
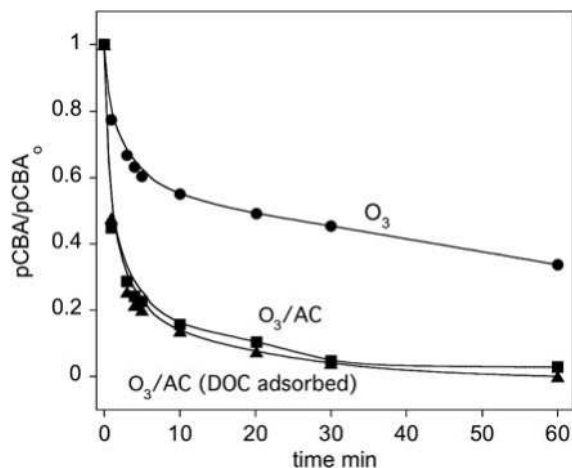


Figure 3.18 shows the kinetics of the transformation of pCBA in the absence and presence of AC. The presence of AC leads to a significant increase of the rate of pCBA transformation (adsorption is much slower and can be excluded). The presence of DOC does not affect the rate of pCBA transformation in the AC experiment.





**Figure 3.18** Kinetics of the transformation of pCBA during ozonation of Lake Zurich water in absence and presence of activated carbon. All experiments: pH 7, 5 mM phosphate buffer, ozone dose 1 mg/L, activated carbon 0.5 g/L. Circles ( $\text{O}_3$ ), ozone only; squares ( $\text{O}_3/\text{AC}$ ), ozone in presence of activated carbon F400; triangles ( $\text{O}_3/\text{AC}$ , DOC adsorbed), ozone in presence of activated carbon F400 pre-equilibrated with DOM. From Sánchez-Polo *et al.*, 2005, with permission.

In this process, AC does not serve as a catalyst. When the pyrrole groups are exhausted upon repeated ozonation, the effectiveness of the AC decreases significantly (Sánchez-Polo *et al.*, 2005). In the case of compounds that adsorb well on AC, adsorption may be the main removal mechanism (Sánchez-Polo *et al.*, 2006). An experiment in the presence of AC and in the absence of ozone shows that the main removal mechanism of atrazine is its adsorption. Therefore, for compounds with high affinity to AC, a combined process has only a limited advantage over AC alone. However, the combination of activated carbon with ozone is an optimal process for removing adsorbable and non-adsorbable ozone-refractory compounds simultaneously in a one treatment step if AC is continuously renewed.

## Chapter 4

# Inactivation of micro-organisms and toxicological assessment of ozone-induced products of micropollutants

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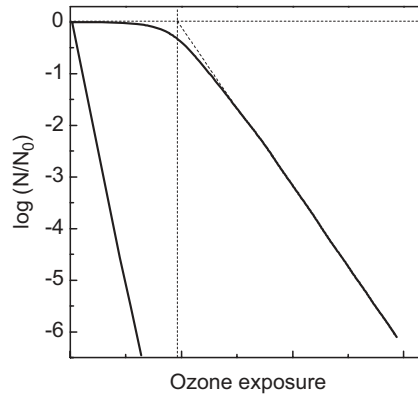
### 4.1 DISINFECTION KINETICS

The disinfecting power of ozone has already been recognised in the 19th century (Chapter 1). Ozone has been applied for primary disinfection in drinking water treatment since the beginning of the 20th century (Chapter 5). Ozone is the best chemical disinfectant currently applied in drinking water treatment (Katzenelson *et al.*, 1974; Ellis, 1991; von Gunten, 2003b; Dahi, 1976; Hoff & Geldreich, 1981; Trukhacheva *et al.*, 1992; Bünning & Hempel, 1999). It readily copes with viruses (Katzenelson *et al.*, 1979; Kim *et al.*, 1980; Thurston-Enriquez *et al.*, 2005; Katzenelson *et al.*, 1974; Kim *et al.*, 1980; Roy *et al.*, 1980; Nupen *et al.*, 1981; Roy *et al.*, 1981a, b; 1982a, b; Finch & Fairbairn, 1991; Hall & Sobsey, 1993; Botzenhart *et al.*, 1993; Lin & Wu, 2006), with bacteria and their spores (Scott & Leshner, 1963; Broadwater *et al.*, 1973; Katzenelson *et al.*, 1974; Finch *et al.*, 1988; Botzenhart *et al.*, 1993; Finch *et al.*, 1993; Hunt & Marinas, 1997; Driedger *et al.*, 2001; Larson & Marinas, 2003; Facile *et al.*, 2000; Cho *et al.*, 2002; Jung *et al.*, 2008; Komanapalli & Lau, 1996) as well as with protozoa (Wickramanayake *et al.*, 1984a, b; Rennecker *et al.*, 1999).

For bacteria, spores and protozoa, the inactivation kinetics is typically characterised by a shoulder as schematically depicted in Figure 4.1 (right curve). But in many cases, the shoulder is quite small and a fit according to a mono-exponential decay is adequate (Figure 4.1, left curve).

This is analogous to the inactivation of cells by short-wavelength UV-radiation (UVC) and by ionising radiation. In these cases, the target is definitely DNA, whereas with long-wavelength UV-radiation (UVA), a spectral range where DNA absorbs only very little, protein damage, a much less efficient process, is the molecular basis of (solar) disinfection (Bosshard *et al.*, 2010). From UVC and ionising radiation studies, it became apparent that inactivation is not due to a single lesion, but that many DNA lesions are required for preventing reproduction [reproductive cell death, for a study on ozone-induced DNA damage and repair see Hamelin & Chung (1989)]. The shoulder arises from a competition of repairing these lesions with the help of repair enzymes and the attempt to generate a second set of complete double-stranded DNA and for dividing into two daughter cells. Strains that lack such repair enzymes no longer show the shoulder. Moreover, starving the cells (“liquid holding”) prevents cells from undergoing rapid reproduction, and repair becomes more efficient. When this competition is not very pronounced, the inactivation curve may show up as a straight line (Figure 4.1, left).

To a certain extent, viruses may also make use of the repair enzymes provided by their host cells.



**Figure 4.1** Schematic representation of the two types of inactivation curves. Mono-exponential (left), mono-exponential with shoulder (right).

The importance of repair processes may be illustrated by some numbers that are available for the lesions set by ionising radiation. The lesions set by ozone must be different, but some lesions will be similar such as single-base lesions. The more severe lesions such as DNA double-strand breaks and DNA crosslinks are possibly of minor importance in the case of ozone as a damaging agent. With ionising radiation, a dose of 1 Gy induces 0.2–0.8 lethal events in (mammalian) cells and about 1000 DNA single-strand breaks. For the same conditions, many more single-base lesions (for a typical yet not the most abundant damage, 8-oxo-adenine, 700 such lesions were estimated), 40 DNA double-strand breaks and 150 DNA-protein crosslinks occur (von Sonntag, 2006). These extraordinary large numbers show the high efficiency of the cellular repair enzymes, and it is concluded that also in the case of damages set by ozone, the majority can be repaired. It thus does not come as a surprise that some  $10^8$  ozone molecules are required for the inactivation of a bacterium (Scott & Lesher, 1963; Finch *et al.*, 1988).

Ionising radiation induces chromosome aberration to a similar extent as lethal effects (von Sonntag, 2006), and mutations are also observed with ozone (Rodrigues *et al.*, 1996; Dubeau & Chung, 1982; Dillon *et al.*, 1992).

Starting with Chick and Watson in 1908, there were many attempts to fit experimental data (Zhou & Smith, 1995) and to model inactivation of micro-organisms by disinfectants. A compilation and discussion of current models is given by Gyürék & Finch (1998). All of these models have in common that they neglect repair processes. For the inactivation of micro-organisms showing a shoulder, kinetics can be formulated by an empirical approach (Rennecker *et al.*, 1999; Gujer & von Gunten, 2003) [Equations (1)–(4)].

$$CT_{\text{lag}} = \frac{1}{k} \ln \left( \frac{N_1}{N_0} \right) \quad (1)$$

$$\text{if } CT \leq CT_{\text{lag}} \text{ then } \frac{N}{N_0} = 1 \quad (2)$$

$$\text{else } \frac{N}{N_0} = \frac{N_1}{N_0} \exp(-k \times CT) \quad (3)$$

$$\text{or } \frac{N}{N_0} = \exp(-k \times [CT - CT_{\text{lag}}]) \quad (4)$$

$N$ : number of micro-organisms per unit volume;  $N_0$ : initial number of micro-organisms;  $N_1$ : intercept with ordinate resulting from extrapolating pseudo-first order line;  $CT$ : ozone exposure (see below);  $CT_{lag}$ : ozone exposure without measureable inactivation of micro-organisms;  $k$ : disinfection rate constant.

The surviving fraction ( $N/N_0$ ) of a given micro-organism population when plotted as  $\log(N/N_0)$  vs. the ozone CT or ozone exposure (for definitions see below) shows typically a shouldered curve (right curve in Figure 4.1). There are cases, where the shoulder is so little pronounced that this plot turns into a straight line (left curve in Figure 4.1).

Repair takes place during ozonation and any post-ozonation period including the time required for the assay measuring the surviving fraction. Table 4.1 gives an overview of inactivation parameters for various micro-organisms with ozone.

**Table 4.1** Selected kinetic parameters for the inactivation of micro-organisms by ozone at 20–25°C

Micro-organism	$k$ L mg <sup>-1</sup> min <sup>-1</sup>	$CT_{lag}$ mg min L <sup>-1</sup>	Ozone exposure mg min L <sup>-1</sup> for inactivation of		Reference
			2-log	4-log	
<i>E. coli</i>	7800	*	0.0006	0.0012	Hunt & Marinas, 1997
<i>B. subtilis</i> spores	2.9	2.9 ~3 (varying)	4.5	6.1	Driedger <i>et al.</i> , 2001 Larson & Marinas, 2003
Rotavirus <sup>a</sup>	76	*	0.06	0.12	Langlais <i>et al.</i> , 1991
<i>G. lamblia</i> cysts	29	*	0.16	0.32	Wickramanayake <i>et al.</i> , 1984b
<i>C. parvum</i> oocysts	0.84	0.83	6.3	11.8	Rennecker <i>et al.</i> , 1999

<sup>a</sup>5°C; \*very small, not detectable by applied methods

The rate of inactivation of micro-organisms by ozone depends on the type of organism and varies over about four orders of magnitude (Table 4.1). Although, compared to the reactivity of organic compounds, this is a narrower distribution, it is very important for the design of disinfection systems. Disinfection parameters ( $k$ ,  $CT_{lag}$ ) depend strongly on temperature (data in Table 4.1 are given for 20–25°C only), with a higher disinfection efficiency at higher temperature (Gallard *et al.*, 2003; Rakness *et al.*, 2005). Reactor hydraulics are critical for disinfection because inactivation of micro-organisms over several orders of magnitude is required (Gujer & von Gunten, 2003; Do-Quang *et al.*, 2000). This is only possible if disinfection systems approach plug-flow behaviour (Roustan *et al.*, 1992). In practice, this can be achieved by a series of completely stirred tank reactors (CSTRs), for example by dividing a reactor into chambers with baffles (Roustan *et al.*, 1991). It is the most ozone-resistant target micro-organism that determines the required ozone exposure. Lag phases are most important for the required ozone exposure as may be seen from columns 4 and 5 in Figure 4.1. Stochastic modelling indicates that the largest uncertainty in predicting inactivation of *C. parvum* oocysts lies more in the experimental determination of the lag-phase than in the inactivation rate constant (Neumann *et al.*, 2007).

There is only scarce information in the literature concerning the inactivation mechanisms of micro-organisms by ozone. During chlorination, the inactivation of *E. coli* proceeds in the following order of viability indicators: (i) loss of culturability, (ii) loss of substrate responsiveness, (iii) loss of membrane

potential, (iv) loss of respiratory activity, and finally (v) loss of membrane integrity (Lisle *et al.*, 1999). Today, culturability is the main parameter for the assessment of disinfection. With a better understanding of other endpoints, (ii)–(v), and the development of new analytical tools [e.g. flow cytometry (Hammes *et al.*, 2011)], other parameters might gain in importance for the assessment of disinfection efficiency in practice.

In waters containing significant concentrations of bromide, the required ozone exposures for a certain degree of inactivation may lead to high bromate concentrations (Driedger *et al.*, 2001; Kim *et al.*, 2004, 2007a; Buffle *et al.*, 2004). Thus bromate formation may be a limiting factor, and measures have to be taken to comply with the drinking water standard (cf. Chapters 11, 14).

## 4.2 INACTIVATION MECHANISMS: ROLE OF MEMBRANES AND DNA

The relatively narrow distribution of inactivation rate constants for various micro-organisms may be caused by the similar types of constituents that are attacked during inactivation of all micro-organisms. Main targets for ozone may be the nucleic acids; to what extent membrane damage contributes is as yet not known.

The kinetic parameters for the inactivation of viruses are given for rotavirus in Table 4.1. In viruses, the genetic information, represented by the nucleic acids DNA or RNA, is only protected against ozone attack by a thin protein coat. Generally, only a few protein constituents react with ozone with high rate constants. The aliphatic amino acids and also phenylalanine (note that benzene reacts at  $2 \text{ M}^{-1} \text{ s}^{-1}$ ) are barely reactive. The basic amino acids, incorporated in the protein, will only show ozone reactivity to the extent present as free bases. Intrinsically high reactivity can only be expected from histidine (Chapter 8) and the sulfur-containing amino acids methionine, cysteine and cystine (Chapter 9). It is thus conceivable that the viral coat is not an efficient barrier for ozone diffusing to the nucleic acids. Therefore, the high rate constant (Table 4.1) is probably due to the attack of ozone on DNA/RNA.

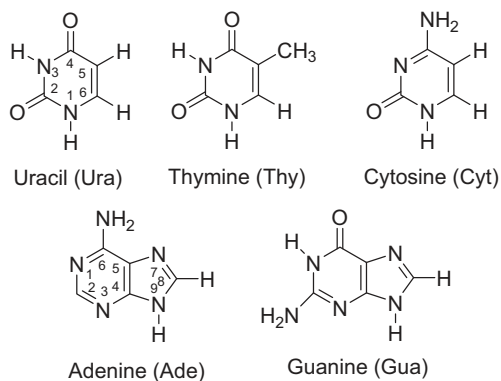
With bacteria, the situation is more complex. Here, DNA is attached to the bacterial membrane. Some  $10^8$  ozone molecules are required for the inactivation of a bacterium (Scott & Lesher, 1963; Finch *et al.*, 1988). Based on this assumption for a lake water with a total cell count of  $10^9$  cells/L (Hammes *et al.*, 2008),  $10^{17}$  ozone molecules/L will be required for their inactivation. This corresponds roughly to  $0.2 \text{ }\mu\text{M}$  ( $0.01 \text{ mg/L}$ ) ozone which is far below typically applied ozone doses ( $>10 \text{ }\mu\text{M} = 0.5 \text{ mg/L}$ ). Therefore, disinfection processes do not contribute significantly to the ozone consumption under typical treatment conditions. It has been suggested that inactivation of planktonic bacterial cells is due to a destruction of the bacterial cell wall and subsequent leakage of cellular contents (Scott & Lesher, 1963). Even though there is membrane damage in the early stage of ozonation, cell viability of *E. coli* is only affected by the oxidation of DNA (Komanapalli & Lau, 1996). This is supported by the fact that the inactivation rate constant for *E. coli* (Table 4.1) is only a factor of two different from that of rotavirus, suggesting that DNA might still be the main target for ozone. Upon ozonation of a natural consortium of bacteria, membrane damage occurs simultaneously to the loss of cell numbers. For other disinfectants such as chlorine dioxide, chlorine and monochloramine, membrane integrity decreases before cell numbers are reduced (Ramseier *et al.*, 2011a). The kinetics of membrane damage of natural bacteria is slower than the kinetics of inactivation of pure cultures as determined by cultivation methods. Even though this points towards DNA damage, the two experimental systems cannot be compared directly (Ramseier *et al.*, 2011a). Therefore, further studies are needed to fully elucidate the importance of membrane damage in disinfection processes.

In addition to inactivation, ozone also causes mutations (Rodrigues *et al.*, 1996; Dubeau & Chung, 1982; Dillon *et al.*, 1992). This may be taken as evidence for DNA damage (with the cell remaining adequately

intact), but the possibility that ozone by-products (e.g. formed in the reaction with the cell wall) have caused the mutagenic effect cannot be excluded. For example, hydroperoxides and  $\text{H}_2\text{O}_2$  are typical ozonation by-products, and the latter is known to be weakly mutagenic (Thacker, 1975; Thacker & Parker, 1976). With this in mind, ozone by-products derived from membrane damage may also contribute to cell mortality.

### 4.3 REACTIONS WITH NUCLEIC ACID COMPONENTS

The ozone-reactive components of the nucleic acids are the nucleobases: thymine, cytosine, adenine and guanine in DNA. Some viruses contain RNA instead of DNA, and here thymine is replaced by uracil.

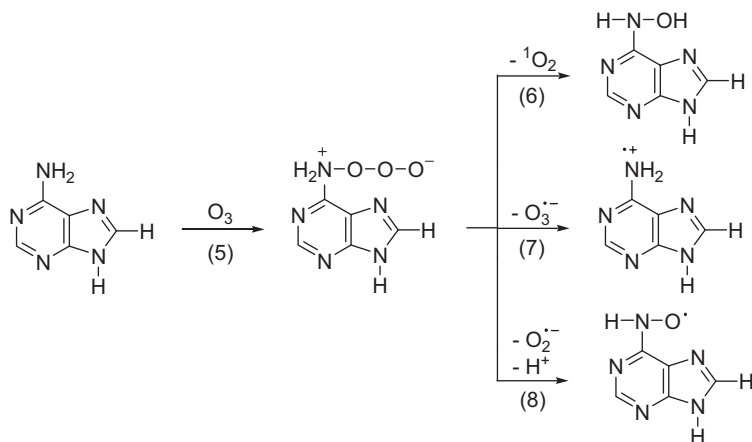


There is a remarkable spread of ozone rate constants among the nucleic acid constituents (Chapter 6, Table 6.1). Notably, the rate constants of the Ade nucleosides, adenosine (Ado) and deoxyadenosine (dAdo), are very low. This is in great contrast to  $\cdot\text{OH}$  reactions that are close to diffusion-controlled for all nucleobases (von Sonntag, 2006).

The ozone chemistry of thymine and thymidine has been elucidated in quite some detail (Flyunt *et al.*, 2002) (Chapter 6). The reactive site is the quasi-olefinic C(5)–C(6) double bond. This may also hold for uracil and cytosine. The substantial increase in the rate of reaction of the pyrimidines with ozone upon deprotonation may be largely due to an increase in the electron density in the reacting double bond. With Cyt and cytidine (Cyd)/deoxycytidine (dCyd), protonation at the exocyclic nitrogen acts in the opposite direction, that is, it lowers the rate of reaction.

With the pyrimidine free bases, the formation of some singlet oxygen, notably at high pH is observed, but not with the corresponding nucleosides (Table 6.7) (Muñoz *et al.*, 2001). Mechanistic aspects are also discussed in Chapter 6.

The rate of reaction of Ado and dAdo are very low, and this may be due to the fact that the aromatic ring contains two nitrogens. Nitrogen-containing heteroaromatics react only very slowly with ozone (Chapter 8). The electron density at the exocyclic amino group must be also low, but the formation of singlet oxygen (20%, Table 6.7) and of  $\cdot\text{OH}$  radicals [43% (Flyunt *et al.*, 2003a)] point to this nitrogen as the preferred site of attack. The *N*-oxide at N1 is formed upon the reaction of  $\text{H}_2\text{O}_2$  with dAdo (Mouret *et al.*, 1990). This *N*-oxide is not formed in the reaction of ozone with dAdo (Muñoz *et al.*, 2001). A more detailed product study is still missing, but reactions (5)–(8) may be tentatively suggested to account for the formation of  $^1\text{O}_2$  and of  $\cdot\text{OH}$ . Potential precursors of  $\cdot\text{OH}$  are  $\text{O}_3^-$  [reaction (7)] or  $\text{O}_2^-$  [reaction (8); for the ensuing chemistries see Chapter 8].



Singlet oxygen (40%, Table 6.7) but no  $\bullet OH$  (Flyunt *et al.*, 2003) are formed with Gua derivatives. The latter is surprising as the reduction potential of the guanine riboside Guo is lower ( $E_7 = 1.29$  V) than that of adenine riboside Ado ( $E_7 = 1.56$  V) (von Sonntag, 2006). This may exclude reaction (7) and favour reaction (8) as the precursor of  $\bullet OH$ .

#### 4.4 REACTION WITH DNA

In the reaction of ozone with DNA,  $\bullet OH$  plays an important role (Van der Zee *et al.*, 1987; Theruvathu *et al.*, 2001). This  $\bullet OH$  formation must be due to the reaction of ozone with the adenine moiety (Ishizaki *et al.*, 1984; Theruvathu *et al.*, 2001). For the determination of the intrinsic ozone rate constant with DNA, tertiary butanol has to be added. Under such conditions, the rate of reaction of DNA is only  $410 \text{ M}^{-1}\text{s}^{-1}$  (in the absence of tertiary butanol  $k_{obs} = 1.1 \times 10^3 \text{ M}^{-1}\text{s}^{-1}$ ), i.e. much lower than that of the weighted average of the nucleobases. In the case of  $\bullet OH$ , which reacts with the nucleobases and their derivatives at close to diffusion-controlled rates [ $k \approx 3 \times 10^9 \text{ M}^{-1}\text{s}^{-1}$  (Buxton *et al.*, 1988)], the rate constant of  $\bullet OH$  with DNA is considerably lower [ $k = 2.5 \times 10^8 \text{ M}^{-1}\text{s}^{-1}$  (Udovicic *et al.*, 1994)], since in this non-homogeneous reaction with the macromolecule DNA two terms, a diffusion term ( $k_{diff}$ ) and a reaction term ( $k$ ) have to be considered (Udovicic *et al.*, 1991). The observed overall rate constant ( $k_{obs}$ ) is the harmonic mean of these two rate constants [cf. Equation (9)].

$$\frac{1}{k_{obs}} = \frac{1}{k} + \frac{1}{k_{diff}} \quad (9)$$

In contrast to  $\bullet OH$ , ozone reacts with the nucleobases at rates much below the diffusion-controlled limit, and the second term must fall away. Hence, the rate of reaction of ozone with the nucleic acids is only given by the first term, that is, it should be close to that of the weighted average of the concentrations of the various nucleobases in the nucleic acid times their rate constants with ozone. This is not observed. The reason for this is as yet not understood. As on this basis, the dAdo moiety can barely contribute (cf. the low rate constant given in Table 6.1) and the explanation that  $\bullet OH$  production must be due to an ozone reaction with this moiety must fall away. It is tentatively suggested that in double-stranded DNA, hydrogen bonding between the nucleobases and base stacking may be the reason for these unexpected effects.

Corresponding experiments with RNA are as yet not available. From the rate constants given in Table 6.1, one would assume that in RNA the guanine moiety is the most likely one to become degraded upon ozone treatment. This has indeed been observed (Shinriki *et al.*, 1981). In DNA, the situation might be somewhat different. Besides guanine, thymine may be the other preferred target.

## 4.5 APPLICATION OF OZONE FOR DISINFECTION IN DRINKING WATER AND WASTEWATER

To assess the disinfection efficiency in water treatment, the CT-concept is applied.  $C$  stands for the concentration of disinfectant (ozone) and  $T$  for the contact time;  $CT$  is the product of the aqueous disinfectant concentration and contact time. In laboratory systems where ozone can be directly measured, the  $CT$  can be expressed as ozone exposure. This corresponds to the integral under the ozone decay curve of an ozone vs. time plot (von Gunten & Hoigné, 1994). In real reactor systems, the  $CT$  value is not easily accessible. Often, time-resolved ozone concentration profiles and contact times are not readily available. To overcome this problem, several concepts have been developed (Rakness, 2005; Rakness *et al.*, 2005). A conservative approach is the calculation of  $CT_{10}$ , where  $C$  is the reactor effluent concentration (or concentration at last sampling point) and  $T_{10}$  is the travel time of the first 10% of the water going through the reactor.  $T_{10}$  is typically much shorter than the hydraulic retention time  $\tau$ ; the  $T_{10}/\tau$  ratio is often around 0.5 (Roustan *et al.*, 1993). This approach does not take into consideration that the ozone concentration is significantly higher near the influent of the reactor, and ozone exposure is underestimated. Especially for ozone-resistant micro-organisms such as *C. parvum* oocysts (Table 4.1), this approach may lead to higher required ozone doses and hence to an increased formation of disinfection by-products such as bromate (Chapters 11 and 14). To make a better approximation of the real ozone concentration in the reactor, calculating the geometric mean of the ozone concentrations at the inlet and outlet [ $C = (C_{in} \times C_{out})^{0.5}$ ] has been suggested (Rakness *et al.*, 2005). This method is an improvement compared to the standard  $CT_{10}$  approach. Yet, it is still far from the real ozone exposure. To further improve the prediction of disinfection efficiency, combined models including reactor hydraulics (determined by tracer experiments), ozone decay kinetics and disinfection kinetics have to be used (Roustan *et al.*, 1993; von Gunten *et al.*, 1999; Do-Quang *et al.*, 2000; Gallard *et al.*, 2003; Kim *et al.*, 2004; Smeets *et al.*, 2006). To include the variability of parameters such as inactivation rate constant,  $CT_{lag}$ , ozone decay rate, temperature, changes in water quality and hydraulics, “uncertainty modelling” is a powerful tool for assessing the variability in the disinfection efficiency (Neumann *et al.*, 2007). With increasing computing power, methods based on computational fluid dynamics can make even more accurate predictions and are a valuable tool in reactor design (Wols *et al.*, 2010).

In wastewater, ozone decay is typically too fast for using measured ozone concentrations to calculate CT values (Chapter 5). Parameters for process design in wastewater disinfection by ozone have been discussed (Xu *et al.*, 2002).

## 4.6 TOXICOLOGICAL ASSESSMENT OF OZONE INDUCED TRANSFORMATION PRODUCTS

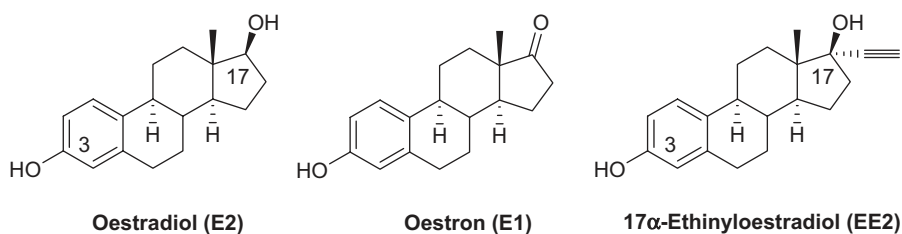
The abatement of organic micropollutants during ozonation does typically not lead to their mineralisation but to the formation of transformation products (Huber *et al.*, 2004; McDowell *et al.*, 2005; Radjenovic *et al.*, 2009; Benner & Ternes, 2009a, b; Dodd *et al.*, 2010; Lange *et al.*, 2006; Schumacher *et al.*, 2004a). Thus, ozonation products may contain more or fewer structural similarities to the original



compounds, and the question arises, whether the original biological effects (e.g. antimicrobial activity, oestrogenicity, herbicidal properties, etc.) are lost even when the molecules are only slightly modified. There is also some concern about new biological effects resulting from the transformation of micropollutants. Since these questions can rarely be answered by elucidating the structures of the transformation products only, ozonated solutions of a biologically active compound may have to be tested for remaining or new biological activity (Mestankova *et al.*, 2011; Escher & Fenner, 2011). In the following, some of the most important classes of biologically active compounds and the change in biological activity upon ozonation will be discussed.

#### 4.7 ENDOCRINE DISRUPTING COMPOUNDS

Compounds behaving like hormones and disturbing the hormonal status of an organism are called endocrine disrupting compounds (EDCs). Among many other bioactive compounds, they are considered the most important class in terms of adverse effects to aquatic life (Runnalls *et al.*, 2010). The general implication for the water industry of the presence of EDCs and other micropollutants and their removal has been addressed (Snyder *et al.*, 2003, 2006; Broséus *et al.*, 2009). The simplest way to disturb the hormonal system of an organism is to interact with a receptor in a way similar to the hormone itself. The receptor of the female hormone oestrone is a typical example and is called an oestrogen receptor, because it also binds other oestrogenic compounds such as the natural hormone oestradiol and the synthetic hormone 17 $\alpha$ -ethinyloestradiol. These oestrogenic compounds are phenols, and the phenolic group is essential for binding to the oestrogen receptor (Lee *et al.*, 2008). They are found in WWTP effluents in concentrations of up to several ng/L (Andersen *et al.*, 2003; Ning *et al.*, 2007a). One of the main concerns of the release of oestrogenic compounds is the feminisation of male fish (Sumpter & Johnson, 2008). In an experimental lake in north-western Ontario, Canada, the fish population was almost extinct after a seven-year exposure to 5–6 ng/L 17 $\alpha$ -ethinyloestradiol (Kidd *et al.*, 2007).

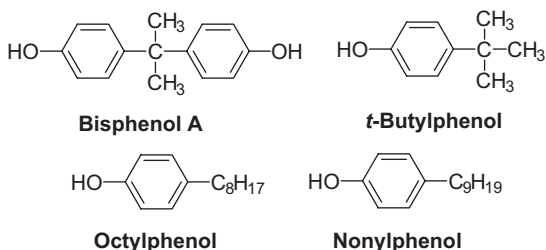


Besides the phenol function, there are hydrophobic binding sites that influence the equilibrium constant of equilibrium (10).

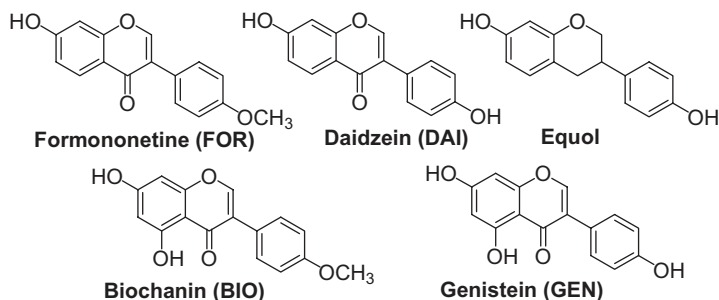


Because of structural similarities to oestrogenic compounds, many industrial and natural compounds can also bind to oestrogen receptors with different equilibrium constants of equilibrium (10) and hence exert different endocrine disrupting potentials (Bonefeld-Jørgensen *et al.*, 2007). A critical review on *in vitro* and *in vivo* effects of synthetic organic chemicals including phenol-containing compounds is available (Tyler *et al.*, 1998). Some examples of such compounds will be discussed in the following.

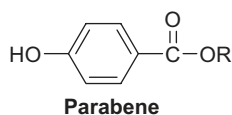
Bisphenol A, *t*-butylphenol, octylphenol and nonylphenol are technical products and abundant in wastewaters and surface waters (Ahel *et al.*, 1994; Voutsas *et al.*, 2006; Ning *et al.*, 2007a).



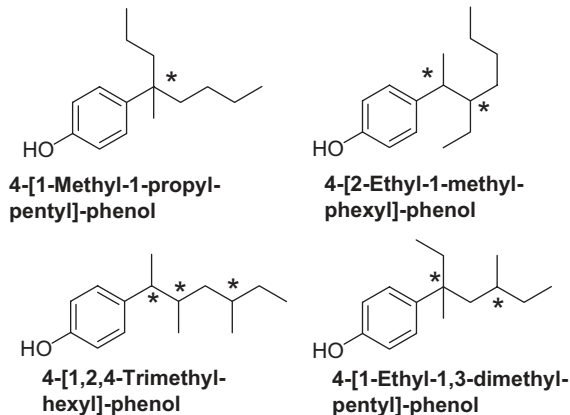
The isoflavone family (formononetine, daidzein, equol, biochanin, genistein) is typically found in surface waters (Hoerger *et al.*, 2009).



Parabenes, esters of the *p*-hydroxybenzoic acid, also belong to the group of EDCs. They seem to be mainly taken up by cosmetics (Darbre & Harvey, 2008).



A typical example of an endocrine disruptor is nonylphenol. There are more than 500 isomers, including stereoisomers, conceivable (Günther, 2002). To visualise this, four of them are shown below.



They differ by orders of magnitude in their binding constants and hence in their endocrine disrupting potential. The daily intake of nonylphenols by food has been estimated at 7.5 µg for an adult in Germany (Günther, 2002). This high value indicates that drinking water may not be the major source of EDCs to man, but the main concern of these EDCs is related to their adverse effects on aquatic life (Oehlmann *et al.*, 2000, 2006; Kidd *et al.*, 2007; Sumpter & Johnson, 2008). Nonylphenols lead to feminisation of aquatic organisms and a decrease in male fertility and the survival of juveniles at concentrations below 10 µg/L (Soares *et al.*, 2008). Prosobranch snails have been suggested as test organisms (Duft *et al.*, 2007; Oehlmann *et al.*, 2007). For a comparison of prosobranch snails and fish see Jobling *et al.* (2004). Similar concerns are related to bisphenol A. Its mode of action and potential human health effects have been reviewed (Vandenberg *et al.*, 2009).

Tin compounds show a strong endocrine disrupting activity for aquatic life (Duft *et al.*, 2003a; Duft *et al.*, 2003b; Wirzinger *et al.*, 2007). Tributyl- and triphenyl tin have a very different mode of action as xeno-androgens (Schulte-Oehlmann *et al.*, 2000).

Even drugs such as carbamazepine (Oetken *et al.*, 2005) or the herbicide atrazine (Hayes *et al.*, 2002) seem to have endocrine disrupting properties.

As there are so many different compounds that give rise to endocrine disrupting activity, *in vivo* and *in vitro* test systems have been developed to assess water samples experimentally. Two test systems that are widely used for *in vivo* and *in vitro* oestrogenicity assessment are based on *in vivo* measurement of the blood plasma vitellogenin (VTG) concentrations in male rainbow trout (*Oncorhynchus mykiss*) and *in vitro* measurement of the oestrogen binding to a human oestrogen receptor (yeast oestrogen screen, YES) [for a review see (Sumpter & Johnson, 2008), for some recent developments requiring shorter reaction times (LYES) see (Schultis & Metzger, 2004)]. For the YES assay, two plasmids have been introduced into a yeast cell. The first plasmid generates the human  $\alpha$ -oestrogen receptor. Upon addition of the EDC to be tested, it binds to the receptor according to equilibrium (10) and changes its structure. This receptor complex now binds to the second plasmid and triggers the formation of a marker enzyme. The resulting enzyme activity is measured. In these assays, bisphenol A and the mixture of technical nonylphenols are about four orders of magnitude less potent than oestradiol.

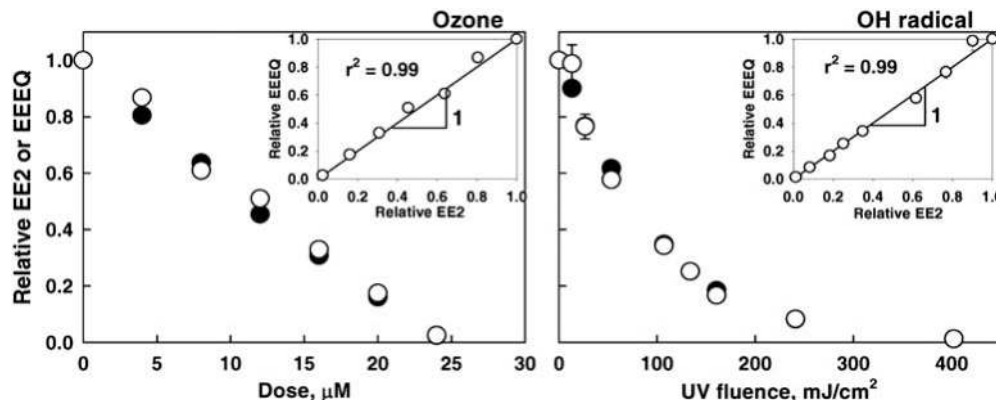
The effect of ozonation on the oestrogenic activity of natural and synthetic EDCs has been investigated in laboratory and full-scale studies.

### 4.7.1 Laboratory studies

Ozonation of nonylphenols leads to an intermediate increase in the oestrogenicity (Sun *et al.*, 2008). Hydroxylation is a major process in the ozone chemistry of phenols (Chapter 7), and 4-nonylcatechol has a higher oestrogenic activity than 4-nonylphenol itself. When all phenolic compounds are degraded, oestrogenic activity disappears. In contrast to this study, it has been reported that there is still some residual oestrogenicity (E-screen assay with MCF-7 cells) even after full transformation of bisphenol A, E1 and EE2 (Alum *et al.*, 2004). This is in contrast to studies that have shown a stoichiometric loss of the oestrogenicity with the transformation of EE2 by ozone and  $\bullet$ OH radicals (Huber *et al.*, 2004; Lee *et al.*, 2008). Figure 4.2 shows the decrease of the relative EE2 concentration (open circles) as a function of the ozone dose (in presence of tBuOH as a scavenger for  $\bullet$ OH radicals) and as a function of the fluence in the UV/H<sub>2</sub>O<sub>2</sub> process (oxidation by  $\bullet$ OH radicals; direct photolysis can be neglected) (Lee *et al.*, 2008).

Figure 4.2 also shows the oestrogenic activity expressed as EEEQ (17 $\alpha$ -ethinyloestradiol equivalents, open circles). In the insets, the relative EEEQ is plotted vs. the relative EE2 concentrations. The good correlation between the two parameters with a slope of unity indicates that both oxidants lead to a loss of oestrogenicity by the first attack on the EE2 molecule. Loss of oestrogenicity upon  $\bullet$ OH attack was also

confirmed for E2 and EE2 (Linden *et al.*, 2007). Other oxidants such as chlorine, bromine, chlorine dioxide and ferrate (VI) also efficiently destroy the oestrogenicity of EE2 (Lee *et al.*, 2008).



**Figure 4.2** Decrease of the relative EE2 concentration (filled circles) and oestrogenic activity (open circles) EEEQ, 17 $\alpha$ -ethinyloestradiol equivalents due to the oxidation by ozone and  $\cdot$ OH radicals. Insets show plots of the relative EEEQ versus the relative EE2 concentration. Experimental conditions: [EE2]<sub>0</sub> = 10  $\mu$ M, pH = 8,  $T$  = 23°C, ozonation in presence of tBuOH (5 mM). When filled circles are invisible, data overlap with open circles. Reprinted with permission from (Lee *et al.*, 2008). Copyright (2008) American Chemical Society.

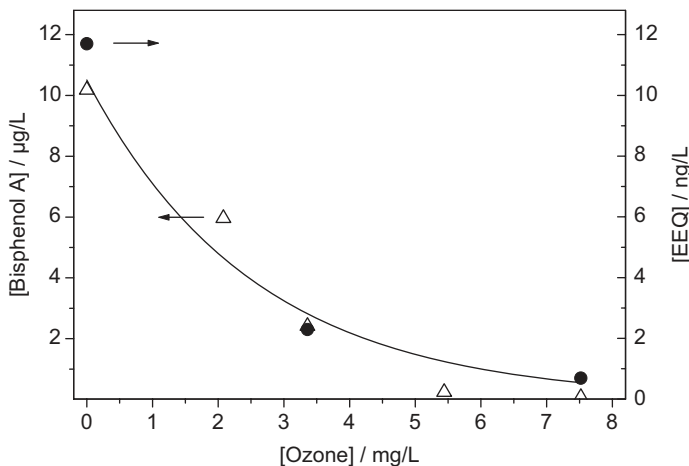
#### 4.7.2 Full-scale studies

A considerable number of EDCs have been detected in WWTPs (Spengler *et al.*, 2001). In many WWTPs, oestrogenicity is controlled by oestrogenic compounds (E1, E2 and EE2) with concentrations in the ng/L range rather than industrial compounds such as alkylphenols, alkylphenolmonoethoxylates and alkylphenoldiethoxylates, even though present in  $\mu$ g/L levels (Aerni *et al.*, 2004). However, this might be different in WWTPs with a high contribution of industrial wastewater. Oestrogenicity in wastewater is eliminated well by activated sludge processes (> 90% removal) (Escher *et al.*, 2009). Since many EDCs are phenols, they are readily eliminated by an ozonation step and lose their hormonal activity upon attack by chemical oxidants (see above). This was demonstrated in a full-scale WWTP in Switzerland where a > 95% elimination of oestrogenicity (YES assay) was found upon ozonation (Escher *et al.*, 2009). In another study, the oestrogenicity was reduced by 90% for an ozone dose of about 0.4 mgO<sub>3</sub>/mg DOC (Stalter *et al.*, 2011). The effective removal of oestrogenic activity by ozonation has been confirmed by an additional test with yolk-sac larvae (Stalter *et al.*, 2010b). A significant reduction of vitellogenin levels was observed in fish exposed to ozonated wastewater compared to fish reared in conventionally treated wastewater.

In other WWTPs, oestrogenicity (YES assay) decreases in parallel to the degradation of bisphenol A by ozone (Figure 4.3).

The same effect is also apparent in the effluent of two other WWTPs where bisphenol A and EEQ were 10% (Köln-Stammheim) and 1% (Bottrop) of the given example. In these wastewaters, there is a very close correlation between the presence of the technical product bisphenol A and oestrogenicity. This points to the predominance of industrial sources (contraceptives were below detection) for the observed oestrogenicity in these wastewaters. However, bisphenol A and alkylphenols (data not shown) can only account for about 10% of the observed oestrogenicity. Therefore, there must be other, as yet unknown, oestrogenic

micropollutants that give rise to the YES assay response. They may belong to the phenol family, as bisphenol A and YES assay show the same ozone response (Figure 4.3). Such a discrepancy between YES assay and detected micropollutants with ED activity is not uncommon. Also in estuarine sediments the oestrogenic activity is not adequately reflected (<1%) by the concentrations of known oestrogens (Thomas *et al.*, 2004). Nevertheless, in other municipal wastewaters with less industrial influence the oestrogenicity could be reasonably well predicted by summing up the effects of individually measured compounds such as E1, E2 and EE2 (Aerni *et al.*, 2004).

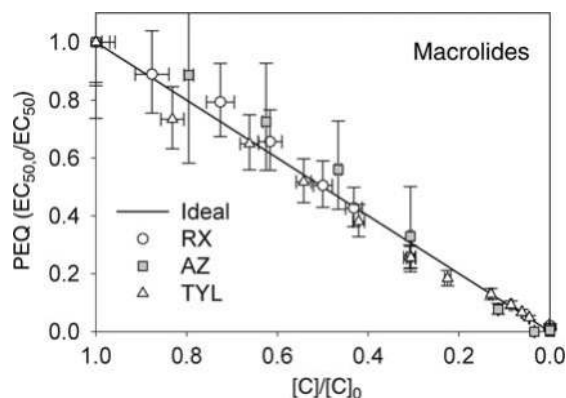


**Figure 4.3** Decrease of the bisphenol A concentration (triangles, left axis) and of the oestrogenicity (YES assay, E2 equivalent (EEQ), circles, right axis) in the effluents of the WWTPs of Düsseldorf-Süd (DOC = 16 mg/L). Adapted from (Nöthe, 2009), with permission.

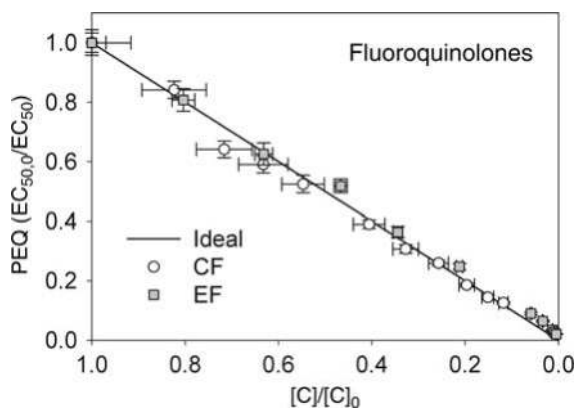
## 4.8 ANTIMICROBIAL COMPOUNDS

A quasi-definition of a micropollutant is that the compound in question must show some biological activity. Two commonly asked questions are whether ozonation decreases or increases the biological activity, and when it decreases the biological activity, how many moles of ozone are required for reducing the biological activity to an insignificant level. A group of compounds that lose their biological activity are the phenolic EDCs discussed above. The fact that after ozonation  $\leq 3\%$  of the starting material is slowly regenerated after ozonation (Chapter 7) is considered insignificant in the present context. Clinically important antibiotics are found in individual concentrations from 0.5 to 3 µg/L in raw and primary wastewaters, and a reduction of 60–90% of their concentration typically occurs during activated sludge treatment [(Dodd *et al.*, 2006a) and references therein]. In general, resulting effluent concentrations are below levels affecting bacteria and aquatic life, but there might still be effects of certain antibiotics on aquatic organisms and on bacteria in the activated sludge process (Dodd *et al.*, 2006a). The main concern related to antibiotics is the development of antibiotic resistance in microbial consortia (Kümmerer, 2009a, b). To date it is, however, not yet clear, whether this can happen in activated sludge processes or in the aquatic environment (Kümmerer, 2009b). Antibiotics comprise many classes of compounds containing ozone-reactive moieties: macrolides (tertiary amines, Chapter 8), sulfonamides (anilines, Chapter 8), fluoroquinolones (piperazines, Chapter 8), lincosamide (thioether, Chapter 9),  $\beta$ -lactams (olefins, Chapter 6; thioethers, Chapter 9), tetracycline (olefins, Chapter 6;

phenols, Chapter 7), glycopeptides (phenols, methoxytoluene, Chapter 7), aminoglycosides (primary amines, Chapter 8) (Dodd *et al.*, 2006a). With the exception of  $\beta$ -lactams, all investigated antibiotics (9 classes, 14 compounds) lost their antimicrobial activity during ozonation in parallel to the loss of the parent compound (Dodd *et al.*, 2009; Lange *et al.*, 2006). This means that the primary attack of ozone (exclusion of  $\bullet\text{OH}$  reactions) on the parent compound efficiently removes its antimicrobial activity. This is shown in Figure 4.4 for macrolides and Figure 4.5 for fluoroquinolones.



**Figure 4.4** Deactivation stoichiometries of macrolides by ozone at pH 7 (tBuOH = 5 mM). PEQ: Potency equivalent derived from growth inhibition tests; RX: roxithromycin; AZ: azithromycin; TYL: tylosin. Reprinted with permission from (Dodd *et al.*, 2009). Copyright (2009) American Chemical Society.



**Figure 4.5** Deactivation stoichiometries of fluoroquinolones by ozone at pH 7 (tBuOH = 5 mM). PEQ: potency equivalent derived from growth inhibition tests; CF: ciprofloxacin; EF: enrofloxacin. Reprinted with permission from (Dodd *et al.*, 2009). Copyright (2009) American Chemical Society.

Similar data as shown in Figure 4.4 have been reported for the macrolide antibiotic clarithromycin (Lange *et al.*, 2006). For the attack of  $\bullet\text{OH}$  on antibiotics, a slight deviation of the ideal loss of antibacterial activity was observed for  $\beta$ -lactams (Dodd *et al.*, 2009). This was attributed to the formation of hydroxylated analogues of the parent compounds which are known to exert an antibacterial activity similar to or

higher than the parent compounds themselves (Kavanagh, 1947). For higher degrees of transformation, however, the residual antibacterial activity was destroyed.

A discussion of ozone-reactivity of the two  $\beta$ -lactams penicillin G and cephalexin and the products formed upon ozone attack (Dodd *et al.*, 2010) is given in Chapter 9. The (*R*)-sulfoxides have some residual antimicrobial activity. With cephalexin, this is of no importance, because an attack of ozone on the remaining olefinic function leads to an efficient loss of the antibacterial activity. In the case of penicillin G, however, the (*R*)-sulfoxide is ozone-resistant and retains about 15% of the antibacterial activity of penicillin G. Yet during wastewater ozonation, penicillin-G-(*R*)-sulfoxide is efficiently oxidised by  $\bullet$ OH, and the antibacterial activity is removed at typical ozone doses (Dodd *et al.*, 2010).

The antiviral drug oseltamivir acid (active metabolite of Tamiflu<sup>®</sup>, see Chapter 6) may be applied in high quantities during pandemic influenza outbreaks and significant concentrations can be expected in wastewaters, even more so because this compound is not efficiently removed in biological wastewater treatment (Prasse *et al.*, 2010). The loss of antiviral activity due to treatment with ozone and  $\bullet$ OH was investigated by measuring neuraminidase inhibition of two viral strains (Mestankova *et al.*, 2012). For both oxidants and low doses, an increased activity was produced that disappeared at high degrees of transformation of the parent and also when solutions were analysed after 24h. Primary unstable products exerting a higher antiviral activity than the parent compound must thus be formed (Mestankova *et al.*, 2012).

Biocides are also ubiquitous compounds found in wastewater effluents. Triclosan, a common additive to soaps and personal care products reacts quickly with ozone (Chapter 7). Its antibacterial properties are lost upon the first attack of ozone (Suarez *et al.*, 2007) while some dioxin-like activity is formed (Mestankova *et al.*, in preparation.). The dioxin that is formed in the photolysis of triclosan has been characterised as 2,8-dichlorodibenzo-*p*-dioxin (Latch *et al.*, 2005).

## 4.9 TOXICITY

Tests on biological activity can reveal valuable information as to the feasibility of ozone application in micropollutant abatement (Gerrity & Snyder, 2011). Additional tests in real water systems might be necessary for ascertaining further endpoints and the role of mixtures of micropollutants and of the water matrix (e.g. DOM). Table 4.2 summarises effect-oriented studies on ozone-treated secondary wastewater effluents.

**Table 4.2** Biological test results from *in vivo* and *in vitro* tests on secondary effluents treated with ozone

Treatment system	Test systems	Results	References
Full-scale ozonation wastewater	Pre-concentration of samples –Bioluminescence inhibition –Oestrogenicity –Arylhydrocarbon receptor response –Genotoxicity –Neurotoxicity –Phytotoxicity	Significant decrease of all effects upon ozonation step	Macova <i>et al.</i> , 2010; Reungoat <i>et al.</i> , 2010

(Continued)

**Table 4.2** Biological test results from *in vivo* and *in vitro* tests on secondary effluents treated with ozone (*Continued*)

Treatment system	Test systems	Results	References
Full-scale ozonation of secondary effluent	Pre-concentration of samples –Bioluminescence inhibition –Growth inhibition –Inhibition of photosynthesis –Oestrogenicity –Inhibition of acetylcholinesterase –Genotoxicity	Significant removal of all effects during ozonation –No genotoxicity formation during ozonation	Escher <i>et al.</i> , 2009
Ozonation of secondary effluent	<i>In vitro</i> tests after pre-concentration – <i>In vivo</i> tests with whole effluent –Genotoxicity –Retionic acid receptor (RAR) agonist activity –Acute ecotoxicity ( <i>Daphnia magna</i> ) –Japanese medaka embryo exposure tests	Significant removal of genotoxicity, RAR agonist activity and acute ecotoxicity – Higher ozone doses lead to a reduction in hatching success rate of Japanese medaka embryos	Cao <i>et al.</i> , 2009
Tertiary treated sewage effluent (ozonation)	<i>In vivo</i> tests with juvenile rainbow trout <i>O. mykiss</i> in liver and kidney tissues –Glutathione S-transferase (GST) –Total glutathione (GSH) –Glutathione peroxidase (GPX) –Lipid peroxidase (LPO) –Haem peroxidase	Liver: Increased haem peroxidase, LPO and GST –Total GSH depleted –Kidney: Increased LPO, GPX observation shows oxidative stress of organism –Coagulation after ozonation reduces these effects	Petala <i>et al.</i> , 2009
Ozonation of secondary effluent	<i>In vivo</i> tests – <i>Lemna minor</i> growth inhibition –Chironomid toxicity test with the non-biting midge <i>Chironomus riparius</i> – <i>Lumbriculus variegatus</i> toxicity –Genotoxicity –Oestrogenicity	Growth inhibition –Removal of oestrogenicity –Increased genotoxicity –Enhanced toxicity for <i>Lumbriculus variegatus</i> –Effects disappear after rapid sand filtration after ozonation	Stalter <i>et al.</i> , 2010a

(Continued)



**Table 4.2** Biological test results from *in vivo* and *in vitro* tests on secondary effluents treated with ozone (*Continued*)

Treatment system	Test systems	Results	References
Ozonation of secondary effluent	Fish early life stage toxicity test (rainbow trout, <i>O. mykiss</i> )	Development retardation –Effect disappears after post-sand filtration –Removal of oestrogenicity	Stalter <i>et al.</i> , 2010b

Toxicity is not as well-defined as, for example, endocrine disruption. Endocrine disruption can be well-described by a relatively simple assay, for example, the YES assay that provides a reasonable answer. Other tests may be used for confirmation, but are not strictly required. In contrast for describing toxicity, many different test systems may have to be utilised depending on the relevant endpoints for ecosystems (Stalter *et al.*, 2010a). Different toxicity tests have been carried out with ozonated wastewater (Table 4.2). For example, the *Lumbriculus variegatus* test, based on the development of this worm within 28 days, revealed a significantly enhanced toxicity after ozonation compared to conventional treatment (Stalter *et al.*, 2010a). Moreover, a significantly increased genotoxicity was observed, detected with the comet assay using haemolymph of the zebra mussel (Stalter *et al.*, 2010a). The comet assay, originally developed for radiation-induced DNA strand breakage caused by ionising radiation in cells (Ostling & Johanson, 1984), has been later applied to the assessment of DNA-reactive agents (Collins *et al.*, 1997). Also the fish early life stage toxicity test (FELST) using rainbow trout (*Oncorhynchus mykiss*) revealed a considerable developmental retardation of test organisms exposed to ozonated wastewater (Stalter *et al.*, 2010b). All these effects were removed by subsequent sand filtration to the level of conventional treatment. Activated carbon treatment even resulted in a significant reduction of genotoxicity. The build-up of toxicity upon ozonation and its subsequent removal during post-sand filtration points to the formation of biodegradable organic compounds such as aldehydes and ketones from the reaction of ozone with DOM (Chapter 3). Apparently, these compounds show toxicity in certain test systems but not in others. It is very unlikely that the increased toxicity is caused by transformation products from micropollutants.

The above statement, that toxicity is not a simple parameter, is illustrated by the fact that other parameters that can measure toxicity such as the *Lemna minor* growth inhibition test and the *Chironomid* toxicity test did not give a response on ozonated wastewater (Stalter *et al.*, 2010a).

It seems fair to conclude that ozone-induced toxicity is mostly transient and can be eliminated by biological sand filtration or biological activated carbon filtration. Hence, toxicity may not be a major obstacle for introducing ozonation as a polishing step in wastewater treatment.

## **Chapter 5**

# **Integration of ozonation in drinking water and wastewater process trains**

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### **5.1 HISTORICAL ASPECTS**

#### **5.1.1 Drinking water**

In France, the earliest test with ozonation for disinfection dates back to 1886. In 1906, ozonation for full-scale drinking water disinfection, after slow sand filtration, was installed in Nice (France) (Le Palouë & Langlais, 1999). In the early applications of ozone in water treatment, ozonation was basically a replacement for chlorine disinfection. Especially in water supplies treating groundwater, there was a substantial carryover of ozone into reservoirs and the distribution systems, because in these waters ozone is quite stable due to the low DOC concentration and the high carbonate alkalinity (Chapter 3). In Germany, ozonation of groundwaters and surface waters also started around 1900. Several plants (Wiesbaden, Paderborn, Hermannstadt) were closed down, however, after only a few years of operation, mainly due to the lower costs of chlorination (Böhme, 1999). In the USA, the first ozone installations for taste and odour or colour removal were established in the early 1900s. Significant capacity was only installed in the mid-1980s (Rice, 1999). In other countries such as Japan, Canada, UK, The Netherlands, Belgium and Switzerland, ozone application for drinking water treatment started between the 1940s and the 1960s (Matsumoto & Watanabe, 1999; Lowndes, 1999; Kruithof & Masschelein, 1999; Geering, 1999; Larocque, 1999). A compilation of the estimated number of drinking water treatment plants in Europe and North America is shown in Table 5.1. From this comparison, it is evident that the number of ozonation plants per capita is very high in France and Switzerland, whereas it is rather low in the USA and Japan. This reflects the high affinity of many water suppliers to chlorine and related products, despite the many disadvantages of these oxidants compared to ozone (Sedlak & von Gunten, 2011).

#### **5.1.2 Municipal wastewater**

So far, there is only a limited number of wastewater treatment plants that use ozonation. Most of these plants are located in Canada, Germany, Japan, South Korea and the USA (Paraskeva & Graham, 2002) with the main objective of disinfection. Disinfection of wastewater effluent is mandatory in some states in the USA. In Europe, it is only applied occasionally for achieving bathing water quality goals. Disinfection of wastewaters is typically also applied for irrigation or other reuse purposes. Disinfection of wastewaters, however, is often achieved with chlorine or UV rather than ozone. Nevertheless, the growing importance of water reuse and the discussion on enhanced treatment of wastewaters for micropollutant removal may

render ozone more attractive because of its dual role as disinfectant and as oxidant (Ternes *et al.*, 2003; Reungoat *et al.*, 2010; Hollender *et al.*, 2009; Oneby *et al.*, 2010; Zimmermann *et al.*, 2011).

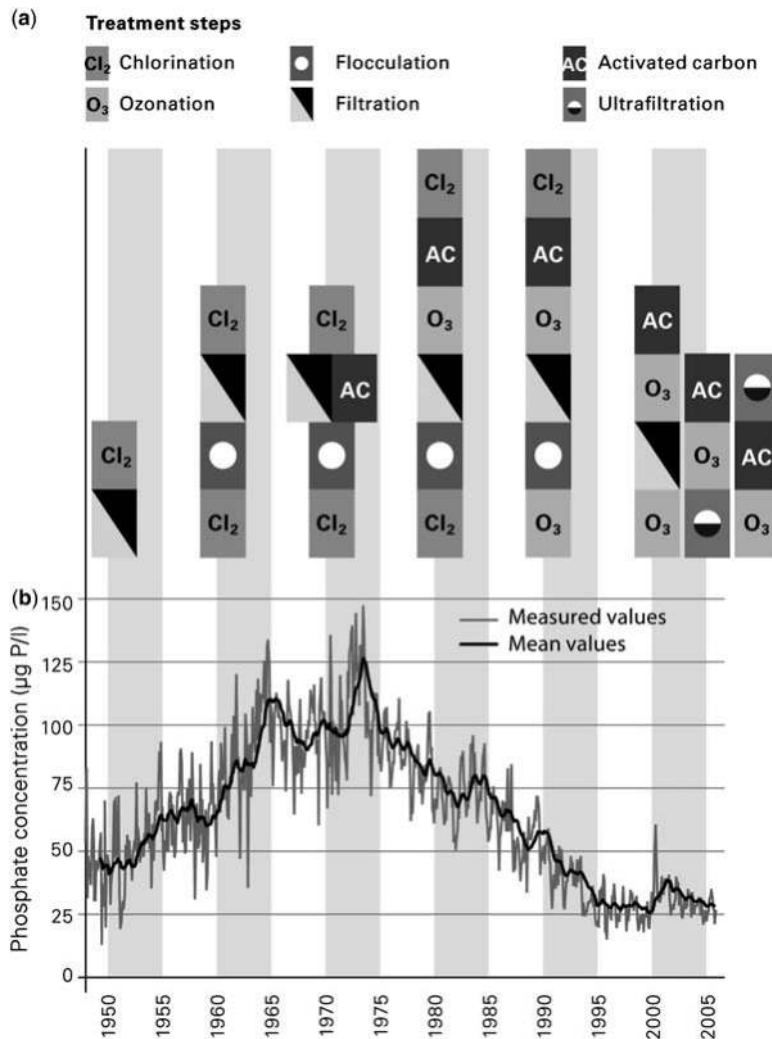
**Table 5.1** Estimated number of drinking water plants using ozone in Europe, North America and Japan (numbers from period 1997–2011)

Country	Number of plants	Number of plants per million capita	References
Switzerland	108	13.8	von Gunten & Salhi, 2003
France	700	10.6	Langlais <i>et al.</i> , 1991
Canada	68	2	Larocque, 1999
Germany	>100	1.2	Böhme, 1999; Loeb <i>et al.</i> , 2011
United Kingdom	50	0.8	Lowndes, 1999
BENELUX	ca. 20	0.72	Kruihof & Masschelein, 1999
USA	200	0.64	Rice, 1999
Japan	>50	>0.39	Loeb <i>et al.</i> , 2011

## 5.2 DRINKING WATER TREATMENT SCHEMES INCLUDING OZONATION

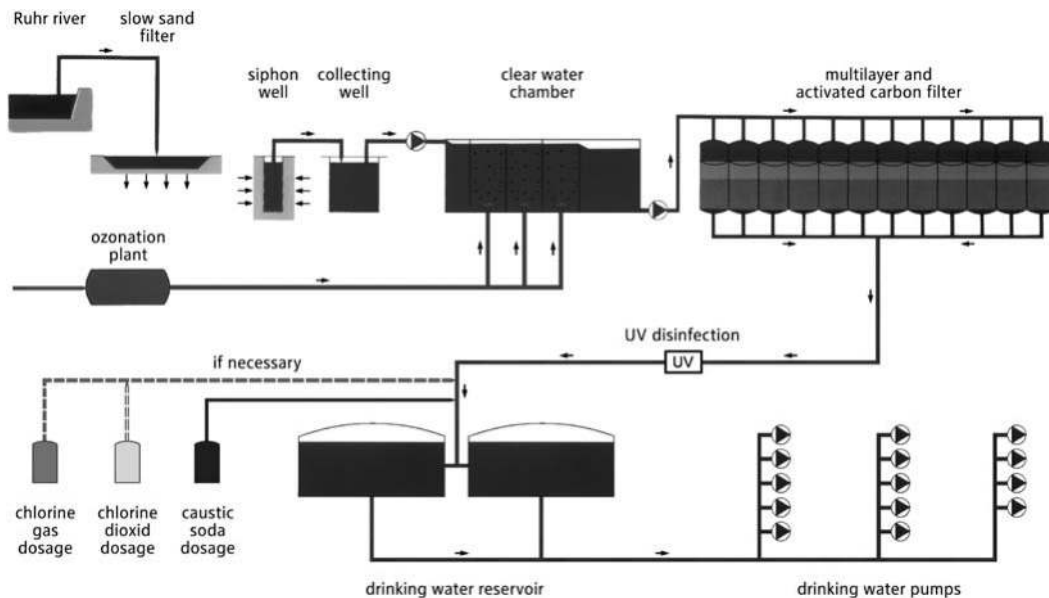
Even though ozone was originally used in one- or two-step processes, today it is widely accepted that ozone should at least be combined with a biological treatment step for removal of AOC/BDOC (Chapter 3). Nowadays, ozonation is mostly used for treatment of surface waters and is integrated into multi-barrier treatment systems (Kruihof & Masschelein, 1999). The development of the integration of ozonation into water treatment trains is shown schematically in Figure 5.1(a) for the evolution of lake water treatment in Switzerland from the 1950s to 2005.

This is representative for the development of treatment trains in other industrialised countries as well. Figure 5.1(b) shows the evolution of the phosphate concentration in Lake Zurich which is an indicator of the degree of eutrophication with a peak in the early 1970s. Drinking water treatment had to follow this development (additional treatment steps) to cope with the various problems related to eutrophication (turbidity, high DOC concentrations, taste and odour issues, etc.). The phosphate concentration in Swiss lakes was reduced by rigorous measures in water pollution control (phosphate elimination in wastewater treatment plants, phosphate ban from textile washing detergents). In the 1950s, lake water treatment started with conventional treatment (sand filtration followed by chlorination) which was supplemented with a pre-chlorination followed by a flocculation process. The introduction of activated carbon was a consequence of increasing taste and odour problems but in other contexts also a barrier against micropollutants which started to emerge in the 1970s. In the mid-1970s, the discovery of trihalomethanes and the formation of chloro- and bromophenols [potent taste and odour compounds (Acero *et al.*, 2005)] which are formed during chlorination was a motivation for moving away from chlorination to ozonation. First, an intermediate ozonation was introduced followed by biological activated carbon filtration (see also Chapter 3). Then, pre-chlorination was replaced by pre-ozonation. The combination of ozone with biological activated carbon filtration is also known as the Mülheim process which was developed in 1974 (Sontheimer *et al.*, 1978; Heilker, 1979). Mülheim is one of the cities in the most densely populated industrial area in Germany, the Ruhr area (ca. 4 million people), and draws its water from the river Ruhr. A rigorous and efficient treatment scheme was necessary to provide high-quality drinking water to the population (Figure 5.2 and discussion below).



**Figure 5.1** (a) Evolution of lake water treatment for Lake Zurich water from 1950 to 2005. (b) Evolution of the phosphate concentration as an indicator for the trophic state of the lake. According to von Gunten, 2008, with permission.

When lake water quality in Switzerland improved in the 2000s and membranes became affordable for drinking water treatment, treatment trains were simplified including a membrane filtration step (ultrafiltration, UF). Hence, treatment schemes could be reduced to three steps, always including the combination of ozone with biological activated carbon filtration and membranes. This combination guarantees a high drinking water quality with respect to hygiene, aesthetic properties and chemical contaminants and allows a distribution of drinking water without residual disinfectants such as chlorine, chloramine and chlorine dioxide. This has the advantage that no disinfection by-products are formed in the distribution system (Sedlak & von Gunten, 2011).



**Figure 5.2** The Mülheim process with the characteristic combination of ozonation and biological filtration. With permission of RWW Rheinisch-Westfälische Wasserwerksgesellschaft mbH.

As mentioned above, the implementation of the Mülheim process in 1974 was a considerable break-through in chlorine-free drinking water treatment. In a first step, the water passes through a slow sand filter. Thereby, suspended particles are retained and part of the organic matter is consumed by microbial processes. Subsequent ozonation oxidises micropollutants and transforms part of the remaining DOM to AOC/BDOC (Chapter 3), which leads to a further reduction of DOC in the following biofiltration step with multi-layer filters containing activated carbon (AC). The water is then UV-disinfected prior to distribution. In case of emergency, chlorine or chlorine dioxide dosing is possible.

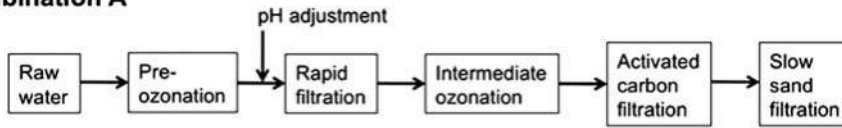
Since the 1990s, membrane filtration, in particular UF, has become an interesting alternative to deep bed sand filtration processes. UF is an efficient barrier against micro-organisms (viruses, bacteria and protozoa) but does not retain organic micropollutants (Jacangelo *et al.*, 1997). Therefore, a combination of UF with ozone oxidation and adsorption processes leads to a drinking water with good hygienic and chemical qualities.

Figure 5.3 shows a conventional process combination including ozonation and deep bed filtration processes and two possible process combinations including UF, ozonation and AC filtration (Pronk & Kaiser, 2008).

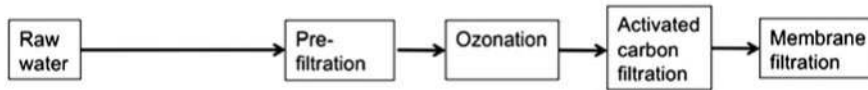
All three process combinations are currently used for the treatment of Lake Zurich water in Switzerland. Combination C may require a final disinfection with UV, because AC filters lose significant numbers of micro-organisms. In a pilot study with combination B, the total cell count determined by flow cytometry was  $\approx 10^3$  cells/mL after ozonation and  $>10^5$  cells/mL after AC filtration (cf. Figure 5.4) (Hammes *et al.*, 2008).

In the AC filter, bacteria can grow on AOC/BDOC, which leads to a significant increase in the total cell count (Figure 5.4). In combination B which is reflected in Figure 5.4, bacteria are removed by UF to below detection limit of flow cytometry, whereas in combination C, where AC filtration is the last treatment step, they would be released into the distribution system if not properly disinfected.

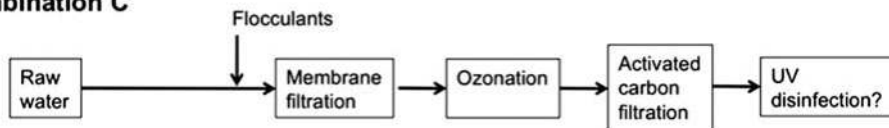
**Combination A**



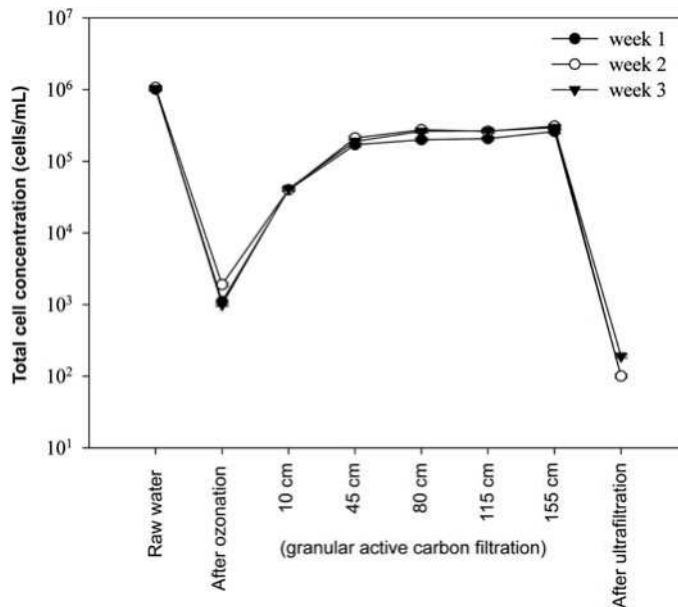
**Combination B**



**Combination C**



**Figure 5.3** Conventional multi-barrier treatment with ozonation (Combination A) and two possible alternative process combinations (B and C) including ozonation and ultrafiltration. Adapted from Pronk & Kaiser, 2008, with permission.



**Figure 5.4** Total cell concentration determined with flow cytometry as a function of the treatment step for process combination B in Figure 5.3. According to Hammes *et al.*, 2008, with permission.

### 5.3 MICROPOLLUTANTS IN WATER RESOURCES, DRINKING WATER AND WASTEWATER

A large body of compounds found in waters and wastewater are considered as micropollutants (Fahlenkamp *et al.*, 2004). There is vast literature on the occurrence of micropollutants in water resources such as ground-water and surface waters and in urban water management systems. They have also been monitored in wastewater before and after biological treatment. These studies are too numerous to be dealt with in this book and the reader is referred to some review articles and books on this topic (Ternes, 1998; Kolpin *et al.*, 2002; Snyder *et al.*, 2003; Vanderford *et al.*, 2003; Schwarzenbach *et al.*, 2006, 2010; Kümmerer, 2010; Ternes & Joss, 2006; Benotti *et al.*, 2009; Kim *et al.*, 2007b; Richardson & Ternes, 2011).

Micropollutant abatement is one of the objectives of ozone in water treatment (Gerrity & Snyder, 2011). Mechanistic studies on the degradation of micropollutants by ozone are found in Chapters 6–13. Ozone rate constants of micropollutants as much as they are known thus far are also given in these chapters. Some micropollutants react too slowly with ozone to be eliminated by ozone under such conditions. They are typically called ozone-refractory, although this is not fully correct. Their reaction is just too slow to be of relevance. They may be eliminated by the much more reactive  $\bullet\text{OH}$  radicals. For the formation of  $\bullet\text{OH}$  in the reactions of ozone with the organic part of the water matrix (DOM) and the contribution of  $\bullet\text{OH}$  to micropollutant abatement see Chapter 3. The chemistries of  $\bullet\text{OH}$  and the ensuing peroxy radicals are discussed in Chapter 14.

Combination B in Figure 5.3 was tested with regard to the potential for micropollutant removal from Lake Zurich water in pilot-scale ( $\approx 10 \text{ m}^3/\text{h}$ ). Three compounds with different physical chemical properties (rate constants for reactions with ozone and  $\bullet\text{OH}$ , adsorption behaviour on AC, see legend of Table 5.3) were investigated, the fuel additive methyl-*t*-butylether (MTBE) and the taste and odour compounds 2-isopropyl-3-methoxypyrazine (IPMP) and  $\beta$ -ionone [for a compilation of typical taste and odour compounds see Table 5.2, for their occurrence in Swiss lakes see Peter *et al.* (2009)].

**Table 5.2** Some abundant taste and odour compounds according to Peter & von Gunten (2007)

Compound	Odour	Odour threshold/ng L <sup>-1</sup>	Source	Formula in Chapter
$\beta$ -Cyclocitral	Fruity	19000	Cyanobacteria	6
Geosmin	Earthy	4	Cyanobacteria, Actinomycetes	14
<i>cis</i> -3-Hexen-1-ol	Grassy	70000	Algae	6
$\beta$ -Ionone	Violets	7	Cyanobacteria, algae	6
2-Isopropyl-3-methoxypyrazine (IPMP)	Decaying vegetation	0.2	Actinomycetes	8
2-Methylisoborneol (MIB)	Musty	15	Cyanobacteria, Actinomycetes	14
<i>trans,cis</i> -2,6-Nonadienal	Cucumber	20	Algae	6
1-Penten-3-one	Fishy-rancid	1250	Cyanobacteria, algae	6

(Continued)

**Table 5.2** Some abundant taste and odour compounds according to Peter & von Gunten (2007) (Continued)

Compound	Odour	Odour threshold/ng L <sup>-1</sup>	Source	Formula in Chapter
2,6-Di- <i>t</i> -butyl-4-methylphenol	Plastic	Not available	Leaching from polyethylene pipes	7
2,4,6-Tribromoanisole (TBA)	Earthy-musty	0.03	Methylation of bromophenol by micro-organisms	7
2,4,6-Trichloroanisole (TCA)	Musty	0.03	Methylation of chlorophenol by micro-organisms	7

After ozonation, the relative residual concentrations of MTBE, IPMP and  $\beta$ -ionone are 80%, 50% and <5%, respectively (Table 5.3).

**Table 5.3** Elimination of selected micropollutants in a multi-barrier system including ozonation, activated-carbon filtration and ultrafiltration (combination B in Figure 5.3). Relative residual concentrations are given in %. For MTBE and IPMP data are given for various activated-carbon running times (10, 150 and 200 days) MTBE:  $k(\text{O}_3) = 0.15 \text{ M}^{-1} \text{ s}^{-1}$ ,  $k(\cdot\text{OH}) = 1.9 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ,  $\log K_{\text{ow}} = 0.94$ ; IPMP:  $k(\text{O}_3) = 50 \text{ M}^{-1} \text{ s}^{-1}$ ,  $k(\cdot\text{OH}) = 5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ,  $\log K_{\text{ow}} = 2.41$ ;  $\beta$ -ionone:  $k(\text{O}_3) = 1.6 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ,  $k(\cdot\text{OH}) = 7.8 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ,  $\log K_{\text{ow}} = 3.84$ . According to von Gunten, unpublished

Micropollutant	After ozonation	After activated-carbon filtration	After ultrafiltration
	Relative residual concentrations in %		
MTBE (10 days)	80	<d.l.	<d.l.
MTBE (150 days)	75	78	77
IPMP (10/200 days)	50	<d.l.	<d.l.
$\beta$ -ionone	1	<d.l.	<d.l.

MTBE methyl-*t*-butylether; IPMP 2-Isopropyl-3-methoxy-pyrazine; d.l. detection limit.

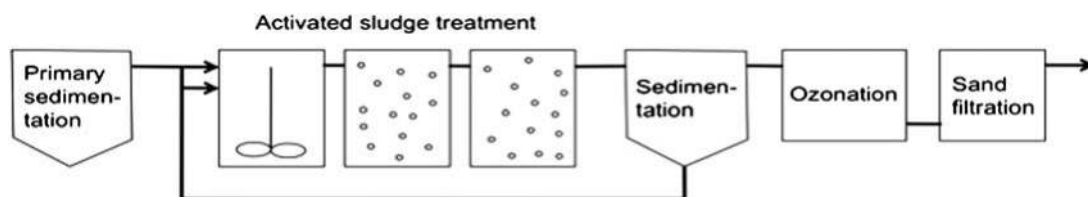
This can be explained on the basis of the rate constants for the reaction of these compounds with ozone and  $\cdot\text{OH}$ . MTBE has the lowest reactivity towards ozone and  $\cdot\text{OH}$ ; IPMP is in an intermediate range, whereas  $\beta$ -ionone reacts rapidly with ozone and  $\cdot\text{OH}$  (Table 5.3). For short running times, AC removes MTBE well, but at longer operation times (150 days) MTBE breaks through. IPMP is fully retained even after 200 days of operation of the granular activated carbon (GAC) filter. This behaviour of the two compounds can be explained by their octanol–water partitioning coefficients ( $K_{\text{ow}}$ ) taken as a measure for the affinity to GAC. Based on the  $K_{\text{ow}}$  value,  $\beta$ -ionone would be even better adsorbed. But this has no consequences, since  $\beta$ -ionone is already fully removed by ozonation. For improving MTBE removal, the AOP ozone/ $\text{H}_2\text{O}_2$  (Chapter 3 for details) was tested by injecting  $\text{H}_2\text{O}_2$  in the third chamber of the four-chamber ozone reactor. An increase in the ozone dose in combination with  $\text{H}_2\text{O}_2$  addition allowed a full elimination of MTBE (for the reaction of  $\cdot\text{OH}$  with MTBE see Chapter 14).



## 5.4 ENHANCED WASTEWATER TREATMENT WITH OZONE

As discussed above, wastewater treatment with ozone has mainly been installed for disinfection purposes. In Europe and some other countries, the need for enhanced wastewater treatment for micropollutant removal to protect aquatic ecosystems is now considered (Ternes *et al.*, 2003; Joss *et al.*, 2008; Ort *et al.*, 2009). Currently, there are two options for enhanced treatment of secondary wastewater effluent, namely the addition of a powdered AC (Nowotny *et al.*, 2007) or ozonation (Joss *et al.*, 2008). For investigating ozonation of wastewater systems, a considerable number of pilot- and full-scale tests have been performed over recent years (Ternes *et al.*, 2003; Huber *et al.*, 2005; Wert *et al.*, 2009a; Hollender *et al.*, 2009; Reungoat *et al.*, 2010; Zimmermann *et al.*, 2011; Stalter *et al.*, 2010a, 2011; Macova *et al.*, 2010).

A typical treatment train for enhanced wastewater treatment with an ozonation step is shown in Figure 5.5. For minimising ozone consumption, ozone is placed after the activated sludge treatment, where DOC concentration is lowest.

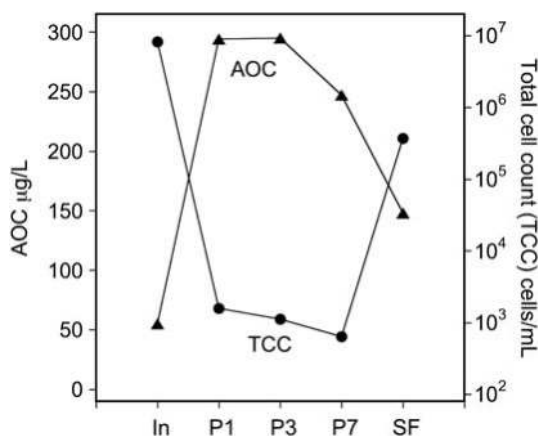


**Figure 5.5** Treatment train for enhanced wastewater treatment with ozone.

Ozonation should be followed by biological sand filtration for degrading AOC/BDOC formed during ozonation (Zimmermann *et al.*, 2011) (Chapter 3). Ozonated wastewater leads to a developmental retardation of rainbow trout, but this effect disappears after sand filtration (Stalter *et al.*, 2010b). This might be an indication that easily biodegradable compounds such as aldehydes are responsible for these adverse health effects on fish (cf. Chapter 4). Aldehyde formation during ozonation of wastewater is quite significant (Wert *et al.*, 2007).

Formation and the degradation of AOC during ozonation and post-sand filtration is shown in Figure 5.6 for a full-scale wastewater treatment plant for a specific ozone dose of 1.24 g O<sub>3</sub>/g DOC (Zimmermann *et al.*, 2011). The main increase in AOC is observed at the first sampling point in the ozone reactor (P1), where most of the ozone is consumed. Thereafter, AOC remains almost constant, mainly due to the small residual ozone concentration. After sand filtration, AOC is considerably reduced, indicating that a significant portion of low-molecular-weight compounds that are potentially toxic to fish can be removed by this process.

Figure 5.6 also shows the evolution of total cell counts (TCC) during ozonation and post-sand filtration. Depending on the ozone dose, TCC decreases by 2–4 orders of magnitude (Zimmermann *et al.*, 2011) reflecting the efficiency of ozone as a disinfectant. After sand filtration, total cell count increases again leading to an overall efficiency of the process of 1–2 logs reduction of TCC. This is in line with the observation of cell growth in activated carbon filters in drinking water treatment (Hammes *et al.*, 2008). A 0.5–3 log inactivation of *E. coli* was observed during ozonation of the same wastewater. In this case, however, sand filtration did not lead to an increase of bacterial counts for *E. coli* (Zimmermann *et al.*, 2011) suggesting that there is also no re-growth of pathogenic bacteria in the sand-filtered water after ozonation.



**Figure 5.6** Assimilable organic carbon (AOC) formation and total cell counts (TCC, determined by flow cytometry) for ozonation followed by biological sand filtration for a full-scale wastewater treatment plant, Regensdorf, Switzerland (25000 population equivalent). Ozone dose 1.24 g O<sub>3</sub>/g DOC. In: Secondary effluent, inlet to ozone reactor; P1, P3, P7 sampling points within the reactor; SF sand filtration. Adapted from Zimmermann *et al.*, 2011, with permission.

## 5.5 ENERGY REQUIREMENTS FOR MICROPOLLUTANT TRANSFORMATION IN DRINKING WATER AND WASTEWATER

Energy requirements for micropollutant transformations during ozonation and advanced oxidation processes (AOPs) depend on the matrix of the water that consumes oxidants (Chapter 3, mainly type and concentration of DOM) and the rate constant for the reaction of a target compound with ozone and •OH radicals. Table 5.4 shows a comparison of the energy requirements for a 90% transformation of selected compounds during ozonation and the AOP UV/H<sub>2</sub>O<sub>2</sub> for laboratory experiments. In general, an increase in energy of about 25% for O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub> relative to the conventional ozonation is estimated based on production energy of 15 kWh/kg and 10 kWh/kg for ozone and H<sub>2</sub>O<sub>2</sub>, respectively (Katsoyiannis *et al.*, 2011). For ozonation, Table 5.4 shows that for a given water quality, the required energy increases in the order SMX < pCBA < ATR < NDMA. This can be explained by a decrease in the second order rate constants for the reaction of these compounds with ozone and •OH from SMX to NDMA. Energy requirements also increase significantly from Lake Zurich water to Dübendorf wastewater, due to the higher concentrations of DOM (consumption of ozone and •OH, Chapter 3) and carbonate (consumption of •OH, Chapter 3). For a given water, energy requirements for UV/H<sub>2</sub>O<sub>2</sub> are typically significantly higher and depend on the penetration depth of UV radiation. Only for NDMA, with low reactivity towards ozone and •OH (Lee *et al.*, 2007b), does the energy requirement for UV/H<sub>2</sub>O<sub>2</sub> become comparable to ozonation. This is due to the fact that NDMA undergoes mainly direct photolysis (Sharpless & Linden, 2003).

For a particular full-scale study (Hollender *et al.*, 2009), the energy consumption for ozonation of secondary effluent, including all contributions (production of liquid oxygen, its transport, generation of ozone) was calculated. The energy requirement at the plant remained constant for process gas in the range of 100–170 g O<sub>3</sub> m<sup>-3</sup> at 12 kWh/kg O<sub>3</sub>. This translates into an energy requirement of 0.035 kWh m<sup>-3</sup> for a specific ozone dose of 0.6 g O<sub>3</sub>/g DOC, which corresponds to about 12% of the total energy consumption of a nutrient (C, N, P) removal plant (0.3 kWh m<sup>-3</sup>). In addition,

production of pure oxygen requires 0.01–0.015 kWh m<sup>-3</sup>. Therefore, the overall energy requirement at this ozone dose (removal of SMX) is quite similar to that shown in Table 5.4 for laboratory systems. For a large range of wastewaters (10,000 to 500,000 person equivalents) and DOC contents (6 to 20 g DOC m<sup>-3</sup>), total costs of ozonation (investment and operation including post-filtration step) were estimated to range between 0.05 and 0.15 € m<sup>-3</sup>, depending on plant size and secondary effluent quality (Joss *et al.*, 2008).

**Table 5.4** Energy requirements in kWh m<sup>-3</sup> for 90% transformation of selected micropollutants by conventional ozonation in Lake Zurich water and Dübendorf wastewater and by using UV(254 nm)/H<sub>2</sub>O<sub>2</sub> (0.2 mM) for varying optical path lengths (cm) in Lake Zurich water. Experimental conditions: target compound concentration = 0.5 μM, pH 8, *T* = 20 °C. According to Katsoyiannis *et al.*, (2011), with permission

Target compound	Lake Zurich Water	Dübendorf wastewater	Lake Zurich Water		
	Ozonation	Ozonation	UV/H <sub>2</sub> O <sub>2</sub> 1 cm	UV/H <sub>2</sub> O <sub>2</sub> 5 cm	UV/H <sub>2</sub> O <sub>2</sub> 10 cm
SMX	0.0015	0.045	0.39	0.15	0.11
pCBA	0.035	0.2	0.75	0.23	0.17
ATR	0.05	0.3	0.98	0.28	0.2
NDMA	0.5	0.9	1.62	0.44	0.3

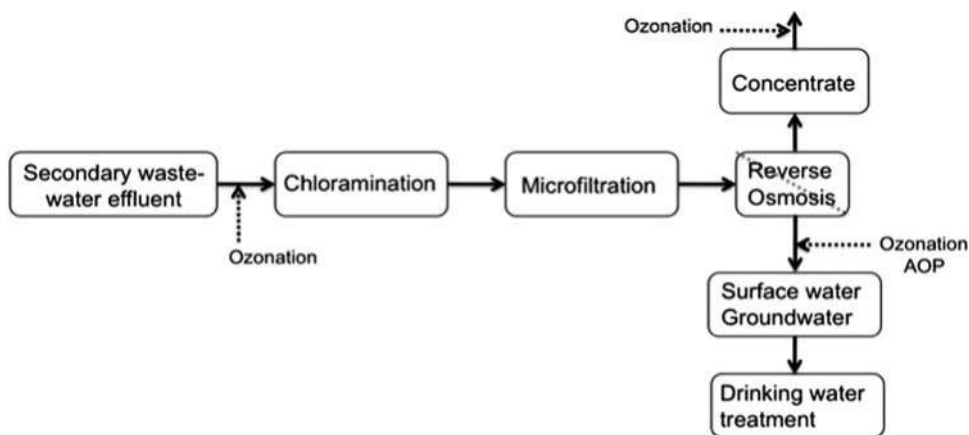
SMX sulfamethoxazole; pCBA *p*-chlorobenzoic acid; ATR atrazine; NDMA *N*-nitrosodimethylamine; Lake Zurich water, DOC 1.3 mgC/L, carbonate alkalinity 2.6 mM; Dübendorf wastewater, DOC 3.9 mg C/L, carbonate alkalinity 6.5 mM.

## 5.6 SOURCE CONTROL

The removal of micropollutants from the wastewater stream by enhanced treatment of secondary wastewater effluent is an end-of-pipe solution. Other options include treatment of source-separated urine (Larsen & Gujer, 1996) or treatment of other point sources such as hospital wastewater. Urine separation and treatment with ozone has been demonstrated to be a feasible process for micropollutant removal. Even though it only accounts for about 1% of the wastewater stream, it requires more energy to remove micropollutants by ozonation than in wastewater (Dodd *et al.*, 2008). When the treatment of source-separated urine is combined with nutrient recovery (N, P), the overall energy requirement becomes even favourable for urine treatment compared to wastewater treatment (Dodd *et al.*, 2008). Nevertheless it has to be considered that some chemicals, among them high risk chemicals such as the antiarrhythmic compound amiodarone (cf. Chapter 8), are excreted via faeces (Escher *et al.*, 2011). Therefore, the full spectrum of compounds will not be removed by this approach. The contribution of hospital wastewater to the overall load of pharmaceuticals in municipal wastewater is typically quite low in the order of <15% (Ort *et al.*, 2010). Nevertheless, source control in hospitals has quite high acceptance among stakeholders, especially if the contribution of hospitals to the overall load is high (Lienert *et al.*, 2011). In this context it is noted that municipal wastewater receives an integrated load of chemicals used in households, which also include biocides, pesticides, personal care products, etc., which will also be removed by an ozone treatment of secondary effluents (Hollender *et al.*, 2009).

## 5.7 RECLAMATION OF WASTEWATER

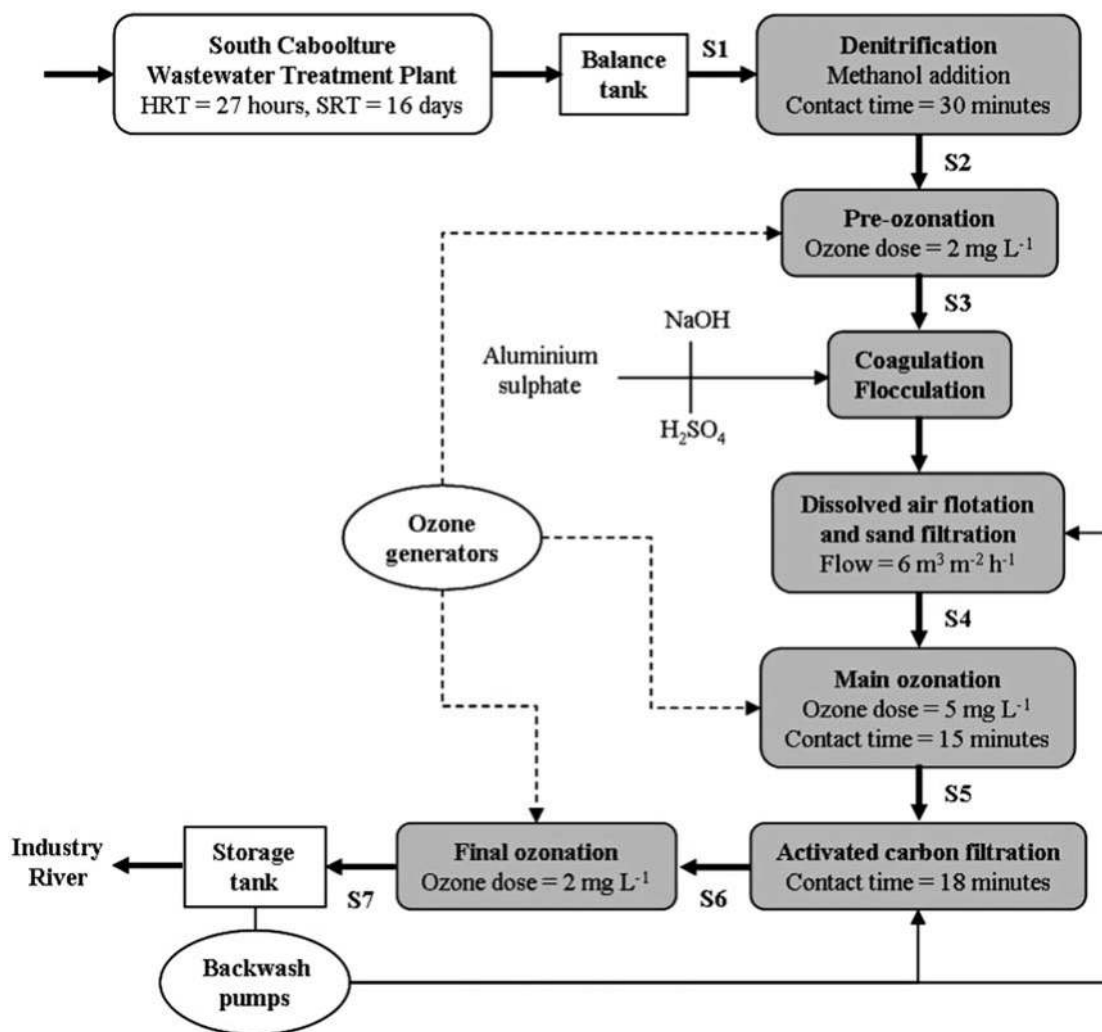
Reclamation of wastewater as a resource for drinking water and for irrigation purposes (agriculture, golf courses, etc.) has become an important issue in arid and semi-arid areas due to population growth and climate change. Today, wastewater reuse is heavily based on membrane processes. Secondary effluent is typically treated by a combination of microfiltration/ultrafiltration with reverse osmosis (RO) (Figure 5.7) (Asano *et al.*, 2007). Even in coastal areas this approach ( $<1 \text{ kWh/m}^3$ ) is more energy efficient than seawater desalination [ $3.5\text{--}4.5 \text{ kWh/m}^3$ , (Sommariva, 2010)]. Water desalination has become increasingly important worldwide with large-scale plants ( $30,000\text{--}320,000 \text{ m}^3/\text{d}$ ) in Kuwait, Singapore, USA, Australia and China (Hemmi *et al.*, 2010). The RO process is frequently followed by UV disinfection, and the water is then mostly used for replenishment of natural water bodies such as groundwaters or surface waters. In the treatment scheme outlined in Figure 5.7, ozonation is not applied. In principal, ozonation could be used to treat secondary wastewater effluent for removing NDMA precursors (Lee *et al.*, 2007a). Such (unknown) precursors may lead to NDMA during chloramination which is routinely applied to hinder biofilm growth on the RO membrane. Typically, the rejection of micropollutants by RO is  $>90\%$  (Buseti *et al.*, 2009). Advanced oxidation of the RO permeate (UV/ $\text{H}_2\text{O}_2$ , UV/ozone or ozone/ $\text{H}_2\text{O}_2$ ) is an option for an additional barrier for removing micropollutants such as NDMA, which are not fully retained by RO. AOPs in post-RO water are expected to be very efficient, because its  $\bullet\text{OH}$  scavenging rate is very low due to its low DOC of  $<0.1 \text{ mg/L}$ .



**Figure 5.7** Water reuse scheme based on ultrafiltration/reverse osmosis. Points for potential ozonation steps are also indicated.

One of the problems in the RO-based water reuse scheme is the discharge of the RO concentrate. The concentration factor for micropollutants during RO treatment of wastewater is of the order of four. In a recent study, ozonation was investigated for the elimination of beta blockers from an RO concentrate with a DOC of  $46 \text{ mg/L}$  (Benner *et al.*, 2008). For metoprolol (cf. Chapter 8) [ $k(\text{O}_3) = 2 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$  (pH 7),  $k(\bullet\text{OH}) = 7.3 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ] an ozone dose of  $>10 \text{ mg/L}$  ( $\approx 0.25 \text{ g O}_3/\text{g DOC}$ ) was required for a removal of  $>90\%$ . The bromate concentration for these conditions was of the order of  $<40 \text{ }\mu\text{g/L}$ , which is relatively low considering the high  $\text{Br}^-$  levels ( $1200 \text{ }\mu\text{g/L}$ ) in the RO concentrate. The ozonated water can then be released to the environment with less toxicological concern.

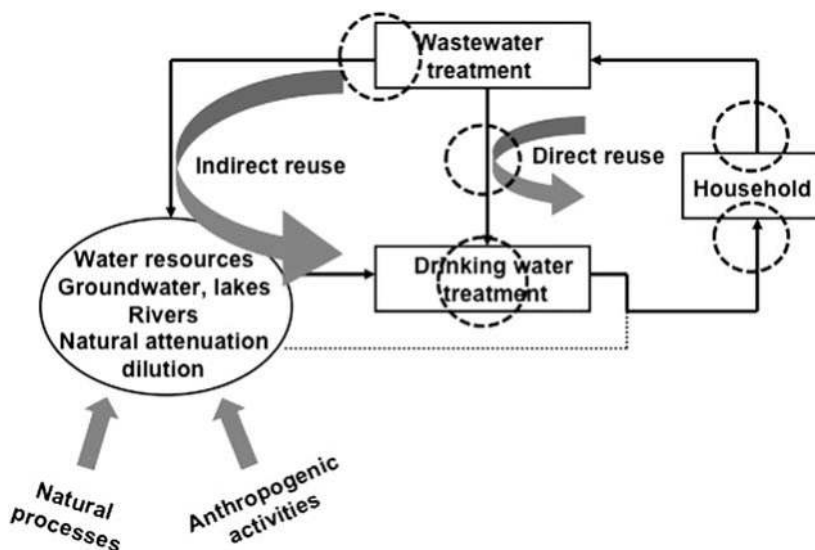
An alternative strategy for wastewater reuse consists of a combination of conventional processes such as ozonation, dissolved air flotation and active carbon filtration. Figure 5.8 shows a schematic representation of such a potential treatment train (Reungoat *et al.*, 2010). Overall, this multi-barrier treatment removed, very efficiently, micropollutants and DOC. Fifty of fifty-four compounds detected in the secondary effluent were eliminated to below detection limits. The DOC concentration was reduced by 55–60%. Furthermore, toxicity determined by various biological endpoints (e.g. oestrogenicity, neurotoxicity, phytotoxicity), was significantly lower than in the influent, often very similar to the blank (Reungoat *et al.*, 2010).



**Figure 5.8** Water reuse scheme based on conventional processes such as ozonation, dissolved air flotation and activated carbon filtration. SRT: sludge retention time. According to Reungoat *et al.* (2010), with permission.

## 5.8 COMPARISON OF THE APPLICATION OF OZONE IN THE URBAN WATER CYCLE

Based on the discussion above, potential points of application of ozonation processes for micropollutant abatement in the urban water cycle are shown in Figure 5.9.



**Figure 5.9** The urban water cycle with potential points of ozonation (marked with circles).

In principle, ozonation can be applied in households as point-of-entry or point-of-use treatment and to the wastewater, e.g. source separated urine (Dodd *et al.*, 2008). Once the wastewater is collected, oxidative treatment may be carried out as post-treatment of secondary wastewater effluent (see above). Compared to treatment of source-separated urine, this also allows oxidative transformation of micropollutants which are derived from sources other than households. Both the treatment at the household level and the treatment in centralised wastewater treatment plants lead to a reduction of the micropollutant discharge to the receiving water bodies. As a consequence, ecosystems and water resources are protected from adverse impacts. When the urban water system is mainly driven by human toxicology, oxidative treatment (mainly ozonation or AOPs) may be placed within the drinking water treatment scheme (Westerhoff *et al.*, 2005; Broséus *et al.*, 2009; Vieno *et al.*, 2007; Kruithof *et al.*, 2007; Ternes *et al.*, 2002).

This scenario has the advantage that micropollutants from diffuse sources such as agriculture, traffic and natural sources (e.g. cyanotoxins and taste and odour compounds) will also be removed (Acero *et al.*, 2000, 2001; Benitez *et al.*, 2007; Rodriguez *et al.*, 2007; Peter & von Gunten, 2007; Onstad *et al.*, 2007). For direct or indirect potable water reuse, an oxidation can be applied after a reverse osmosis treatment (Asano *et al.*, 2007). The water quality for each treatment scenario is decisive for the efficiency of an ozonation process. The main parameter is the content of the dissolved organic matter, typically expressed as DOC concentration (Chapter 3). In addition, pH, alkalinity and ammonia also play an important role (Chapter 3). Table 5.5 summarises water qualities of hydrolysed and electro-dialysed urine, municipal wastewater and water resources used for drinking water production.

**Table 5.5** Water quality parameters relevant for oxidation processes, from Dodd *et al.* (2008); Pronk *et al.* (2006); Udert *et al.* (2003)

Water type	pH	DOC mg/L	Alkalinity mM	NH <sub>3</sub> /NH <sub>4</sub> <sup>+</sup> mg/L
Hydrolysed urine	9	≈2000	≈300	≈4000
Electrodialysed urine diluate*	8	≈400*	≈30	≈400
Wastewater effluent	7–8	≈5–20	2–4	≈20
Water resources for drinking water production				
Surface water	7–8	1–20	1–2	< 0.005 to >1
Groundwater	7–8	<1 to 20	1–5	< 0.005 to >1

\*contained some methanol from dosing of micropollutants

A dramatic decrease of DOC is observed from hydrolysed urine to wastewater effluent. This is partially caused by dilution and partially by the DOC removal during activated sludge treatment. The DOC concentration in surface and groundwaters is typically much smaller and dominated by natural processes (soil weathering, algal growth, etc.). Because ozone demand is closely related to the DOM concentration, it is evident that ozone consumption gets smaller further away from the household source. However, it has to be taken into account, that human urine represents <1% of the total flow of municipal wastewater. Therefore, it might still be a feasible option for micropollutant elimination.

The water quality data (Table 5.5) have consequences for the efficiency of micropollutant elimination. A comparison of the required ozone doses for 90% micropollutant elimination is shown in Table 5.6 for hydrolysed urine, electrodialysed urine diluate, wastewater effluent and two surface waters for 17 $\alpha$ -ethinyloestradiol (EE2) a synthetic steroid oestrogen and ibuprofen (IP) an antiphlogistic.

**Table 5.6** Required ozone doses (mg/L) and corresponding O<sub>3</sub>/DOC ratios (w/w) for a 90% elimination of 17 $\alpha$ -ethinyloestradiol (EE2) and ibuprofen (IP) in various water sources (Lee & von Gunten, 2010; Dodd *et al.*, 2008; Huber *et al.*, 2003, 2005)

Water type	EE2		IP	
	O <sub>3</sub> dose mg/L	O <sub>3</sub> /DOC w/w	O <sub>3</sub> dose mg/L	O <sub>3</sub> /DOC w/w
Hydrolysed urine	≈500	0.25	≈1000	0.5
Electrodialysed urine diluate*	≈150	0.375	≈600	1.5
Wastewater 1 (7.7 mg/L DOC)	>1	>0.13	n.d.	n.d.
Wastewater 2 (5 mg/L DOC)	0.5	0.1	≈4	0.8
Lake water (3.7 mg/L DOC)	0.1	0.03	n.d.	n.d.
River water (1.3 mg/L DOC)	<0.1	<0.08	>2	>2

n.d.: not determined;

\*contained some methanol from dosing of micropollutants

While EE2 reacts quickly with ozone and  $\bullet\text{OH}$  (pH 7:  $k(\text{O}_3) \approx 3 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$ ,  $k(\bullet\text{OH}) = 9.8 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ), IP reacts mostly with  $\bullet\text{OH}$  (pH 7:  $k(\text{O}_3) = 9.6 \text{ M}^{-1} \text{ s}^{-1}$ ,  $k(\bullet\text{OH}) = 7.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ) (Huber *et al.*, 2003).

The efficiency of ozonation increases with decreasing DOC concentrations. For a 90% elimination of EE2, the ozone dose varies over more than three orders of magnitude, reflecting the difference in the DOC concentration between hydrolysed urine and the pre-treated river water. While this difference seems quite large, it has to be considered, that the volume of urine that needs to be treated is about two orders of magnitude smaller than that of wastewater. Furthermore, the ozone dose normalised to the DOC concentration for 90% abatement of the selected ozone-reactive and ozone-resistant compounds is similar for hydrolysed urine and wastewater. Therefore, urine treatment at the household level seems to be feasible, however as mentioned above, only part of the micropollutant load in the wastewater will be treated at this level. In addition, small-scale ozonation systems would have to be implemented at the household level which would require the appropriate maintenance. Table 5.6 also shows that the ozone doses and  $\text{O}_3/\text{DOC}$  ratios for drinking water sources are significantly smaller for compounds reacting rapidly with ozone and in a similar range as urine and wastewater for ozone-resistant compounds.



# Chapter 6

## Olefins

### 6.1 REACTIVITY OF OLEFINS

The rate constants for the reaction of ozone with olefins vary with the nature of the substituents at the C–C double bond by as much as eight orders of magnitude (Table 6.1).

**Table 6.1** Compilation of rate constant of ozone with olefins. Published rate constants rounded to significant figures

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Acetamidoacrylic acid		6	9.4 × 10 <sup>5</sup>	Onstad <i>et al.</i> , 2007
Aciclovir	3.4, 9.6		1.6 × 10 <sup>4</sup>	Prasse <i>et al.</i> , 2012
anion			3.4 × 10 <sup>6</sup>	Prasse <i>et al.</i> , 2012
protonated			250	Prasse <i>et al.</i> , 2012
Acrylamide			1 × 10 <sup>5</sup>	Yao & Haag, 1991
Acrylic acid	4.25		2.8 × 10 <sup>4</sup>	Leitzke & von Sonntag, 2009
anion			1.6 × 10 <sup>5</sup>	Leitzke & von Sonntag, 2009
Acrylonitrile			670	Leitzke <i>et al.</i> , 2003
			830	Pryor <i>et al.</i> , 1983
Adenine	4.15		12	Theruvathu <i>et al.</i> , 2001
protonated	9.8		5	Theruvathu <i>et al.</i> , 2001
anion			1.3 × 10 <sup>5</sup>	Theruvathu <i>et al.</i> , 2001
Adenosine	3.5		16	Theruvathu <i>et al.</i> , 2001
protonated			5	Theruvathu <i>et al.</i> , 2001
5'-Adenylic acid	4.4		200	Ishizaki <i>et al.</i> , 1984
Anatoxin-a			2.8 × 10 <sup>4</sup>	Onstad <i>et al.</i> , 2007
1,4-Benzoquinone			2.5 × 10 <sup>3</sup>	Mvula & von Sonntag, 2003
Buten-3-ol			7.9 × 10 <sup>4</sup>	Dowideit & von Sonntag, 1998

(Continued)

**Table 6.1** Compilation of rate constant of ozone with olefins. Published rate constants rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Carbamazepine			3 × 10 <sup>5</sup>	Huber <i>et al.</i> , 2003
Cephalexin		7	8.7 × 10 <sup>4</sup>	Dodd <i>et al.</i> , 2010
Chlordane			<0.04	Yao & Haag, 1991
5-Chlorouracil	8.0		4.3 × 10 <sup>3</sup>	Theruvathu <i>et al.</i> , 2001
anion			1.3 × 10 <sup>6</sup>	Theruvathu <i>et al.</i> , 2001
Cinnamic acid			5 × 10 <sup>4</sup>	Leitzke <i>et al.</i> , 2001
anion			1 × 10 <sup>5</sup>	Jans, 1996
			3.8 × 10 <sup>5</sup>	Leitzke <i>et al.</i> , 2001
			1.2 × 10 <sup>6</sup>	Jans, 1996
β-Cyclocitral			3.9 × 10 <sup>3</sup>	Peter & von Gunten, 2007
Cylindrospermopsin			~2.5 × 10 <sup>6</sup>	Onstad <i>et al.</i> , 2007
Cytidine	4.15		3.5 × 10 <sup>3</sup>	Theruvathu <i>et al.</i> , 2001
protonated			40	Theruvathu <i>et al.</i> , 2001
Cytosine	4.6, 12.2		1.4 × 10 <sup>3</sup>	Theruvathu <i>et al.</i> , 2001
protonated			930	Ishizaki <i>et al.</i> , 1984
anion			18	Theruvathu <i>et al.</i> , 2001
			1.5 × 10 <sup>6</sup>	Theruvathu <i>et al.</i> , 2001
				Ishizaki <i>et al.</i> , 1984
2'-Deoxyadenosine	3.8		14	Theruvathu <i>et al.</i> , 2001
protonated			5	Theruvathu <i>et al.</i> , 2001
2'-Deoxycytidine	4.3		3.5 × 10 <sup>3</sup>	Theruvathu <i>et al.</i> , 2001
protonated			44	Theruvathu <i>et al.</i> , 2001
5'-Deoxycytidylic acid	4.6		1.4 × 10 <sup>3</sup>	Ishizaki <i>et al.</i> , 1984
2'-Deoxyguanosine	2.5, 9.2		1.9 × 10 <sup>4</sup>	Theruvathu <i>et al.</i> , 2001
5'-Deoxyguanylic acid	2.9, 9.7		4 × 10 <sup>4</sup>	Ishizaki <i>et al.</i> , 1984
1,1-Dichloroethene			110	Dowideit & von Sonntag, 1998
<i>cis</i> -1,2-Dichloroethene			310	Yao & Haag, 1991
			540	Dowideit & von Sonntag, 1998
<i>trans</i> -1,2-Dichloroethene			6.5 × 10 <sup>3</sup>	Dowideit & von Sonntag, 1998
			6.5 × 10 <sup>3</sup>	Hoigné & Bader, 1983a
Dichloromaleic acid		3.3	10	Leitzke & von Sonntag, 2009
1,1-Dichloropropene			2.6 × 10 <sup>3</sup>	Dowideit & von Sonntag, 1998
Diethyl vinylphosphonate			3.3 × 10 <sup>3</sup>	Leitzke <i>et al.</i> , 2003
3,4-Dihydroxycinnamic acid			2 × 10 <sup>6</sup>	Jans, 1996
anion			1.2 × 10 <sup>7</sup>	Jans, 1996
1,3-Dimethyluracil			2.8 × 10 <sup>3</sup>	Theruvathu <i>et al.</i> , 2001
DNA			410	Theruvathu <i>et al.</i> , 2001
Endrin			<0.02	Yao & Haag, 1991

*(Continued)*

**Table 6.1** Compilation of rate constant of ozone with olefins. Published rate constants rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Ethene			1.8 × 10 <sup>5</sup>	Dowideit & von Sonntag, 1998
Flumequine anion	6.5		1.2 8.5 × 10 <sup>3</sup>	Dodd <i>et al.</i> , 2006a
Fumaric acid	3.0, 4.4	<3	8.5 × 10 <sup>3</sup> 1.5 × 10 <sup>5</sup> ~6.5 × 10 <sup>4</sup>	Leitzke & von Sonntag, 2009 Benbelkacem <i>et al.</i> , 2004 Leitzke & von Sonntag, 2009
dianion		2 5	6 × 10 <sup>3</sup> 1 × 10 <sup>5</sup>	Hoigné & Bader, 1983b Hoigné & Bader, 1983b
Guanosine protonated anion	2.5, 9.2		1.6 × 10 <sup>4</sup> <300 4.0 × 10 <sup>6</sup>	Theruvathu <i>et al.</i> , 2001 Theruvathu <i>et al.</i> , 2001 Theruvathu <i>et al.</i> , 2001
Hexachlorocyclopentadiene			90	Yao & Haag, 1991
2-Hexenoic acid (dianion)	6.7		2.4 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
<i>cis</i> -3-Hexen-1-ol			5.4 × 10 <sup>5</sup>	Peter & von Gunten, 2007
Indigotrisulfonic acid			9.4 × 10 <sup>7</sup>	Muñoz & von Sonntag 2000a
β-Ionone			1.6 × 10 <sup>5</sup>	Peter & von Gunten, 2007
Isoorotic acid	4.2, 8.9		3.7 × 10 <sup>3</sup>	Theruvathu <i>et al.</i> , 2001
Maleic acid	1.6		1.4 × 10 <sup>3</sup>	Leitzke & von Sonntag, 2009
monoanion	6.1		4.2 × 10 <sup>3</sup>	Leitzke & von Sonntag, 2009
dianion			~7 × 10 <sup>3</sup> 2.4 × 10 <sup>4</sup>	Leitzke & von Sonntag, 2009 Pryor <i>et al.</i> , 1984
Methacrylic acid anion	4.7		1.5 × 10 <sup>5</sup> 3.7 × 10 <sup>6</sup>	Leitzke & von Sonntag, 2009 Leitzke & von Sonntag, 2009
4-Methoxycinnamic acid anion			1.3 × 10 <sup>5</sup> 6.8 × 10 <sup>5</sup>	Leitzke <i>et al.</i> , 2001 Leitzke <i>et al.</i> , 2001
3-Methoxy-4-hydroxy cinnamic acid anion			1.1 × 10 <sup>6</sup> 7.9 × 10 <sup>6</sup>	Jans, 1996 Jans, 1996
6-Methyluracil anion	9.8		140 6 × 10 <sup>5</sup>	Theruvathu <i>et al.</i> , 2001 Theruvathu <i>et al.</i> , 2001
Microcystin-LR			4.1 × 10 <sup>5</sup>	Onstad <i>et al.</i> , 2007
<i>cis,cis</i> -Muconic acid		3.1	2.7 × 10 <sup>4</sup>	Leitzke & von Sonntag, 2009
<i>trans,trans</i> -Muconic acid	2.7, 4.7	4 3 7	1.6 × 10 <sup>4</sup> 1.5 × 10 <sup>4</sup> 1.3 × 10 <sup>5</sup>	Beltrán <i>et al.</i> , 2006 Ramseier & von Gunten, 2009
<i>cis,trans</i> -Muconic acid	1.9, 4.8	3 7	1.6 × 10 <sup>4</sup> 2.5 × 10 <sup>5</sup>	Ramseier & von Gunten, 2009
4-Nitrocinnamic acid (anion)			1.2 × 10 <sup>5</sup>	Leitzke <i>et al.</i> , 2001
<i>trans,cis</i> -2,6-Nonadienal			8.7 × 10 <sup>5</sup>	Peter & von Gunten, 2007
Orotic acid	2.1, 9.5		5.9 × 10 <sup>3</sup>	Theruvathu <i>et al.</i> , 2001

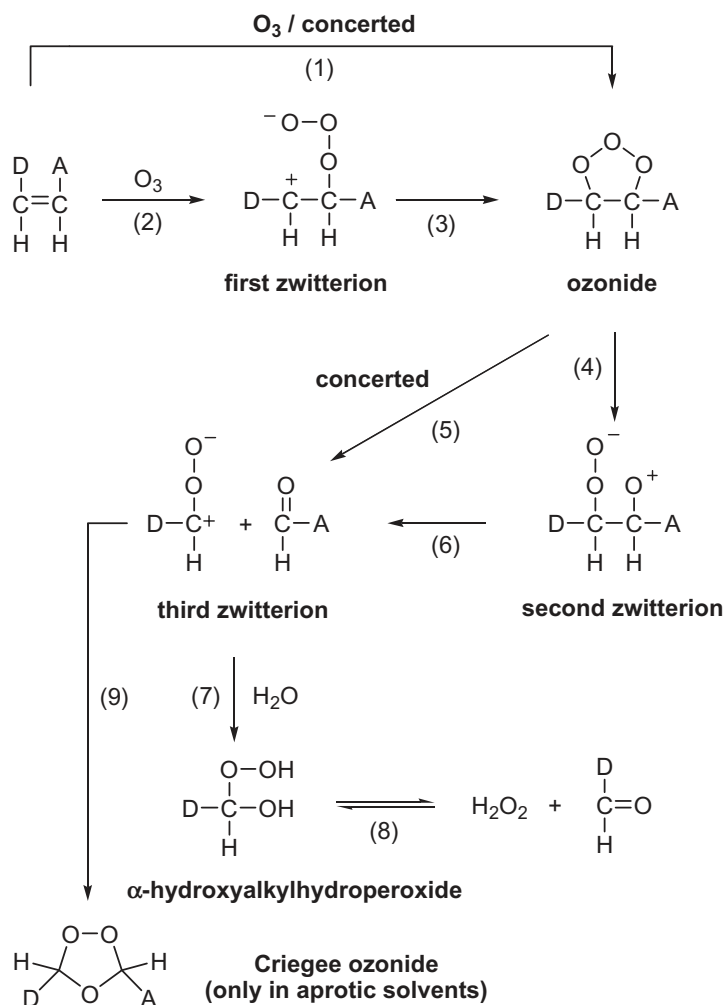
*(Continued)*

**Table 6.1** Compilation of rate constant of ozone with olefins. Published rate constants rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Oseltamivir acid		7–8	1.7 × 10 <sup>5</sup>	Mestankova <i>et al.</i> , 2012
1-Penten-3-one			5.9 × 10 <sup>4</sup>	Peter & von Gunten, 2007
Progesterone			480	Barron <i>et al.</i> , 2006
Propene			8 × 10 <sup>5</sup>	Dowideit & von Sonntag, 1998
Sorbic acid	4.76	3	3.2 × 10 <sup>5</sup>	Onstad <i>et al.</i> , 2007
anion		8	9.6 × 10 <sup>5</sup>	
Tetrachloroethene			< 0.1	Hoigné & Bader, 1983a
Tetramethylethene			> 1 × 10 <sup>6</sup>	Dowideit & von Sonntag, 1998
Thymidine	9.8		3 × 10 <sup>4</sup>	Theruvathu <i>et al.</i> , 2001
anion			1.2 × 10 <sup>6</sup>	Theruvathu <i>et al.</i> , 2001
5'-Thymidylic acid	10.0		1.6 × 10 <sup>4</sup>	Ishizaki <i>et al.</i> , 1984
Thymine	9.9		4.2 × 10 <sup>4</sup>	Theruvathu <i>et al.</i> , 2001
anion			2.3 × 10 <sup>4</sup>	Ishizaki <i>et al.</i> , 1984
			~3 × 10 <sup>6</sup>	Theruvathu <i>et al.</i> , 2001
Trichloroethene			17	Hoigné & Bader, 1983a
			15	Yao & Haag, 1991
			14	Dowideit & von Sonntag, 1998
Tylosin protonated	7.7		7.7 × 10 <sup>4</sup>	Dodd <i>et al.</i> , 2006a
Uracil anion	9.5		650	Theruvathu <i>et al.</i> , 2001
			9.2 × 10 <sup>5</sup>	Theruvathu <i>et al.</i> , 2001
Vinyl acetate			1.6 × 10 <sup>5</sup>	Leitzke <i>et al.</i> , 2003
Vinyl bromide			1 × 10 <sup>4</sup>	Leitzke <i>et al.</i> , 2003
Vinyl chloride			1.4 × 10 <sup>4</sup>	Dowideit & von Sonntag, 1998
Vinylene carbonate			2.6 × 10 <sup>4</sup>	Leitzke <i>et al.</i> , 2003
Vinyl phenyl sulfonate			~200	Leitzke <i>et al.</i> , 2003
Vinyl phosphonic acid			1 × 10 <sup>4</sup>	Leitzke <i>et al.</i> , 2003
monoanion			2.7 × 10 <sup>4</sup>	Leitzke <i>et al.</i> , 2003
dianion			1 × 10 <sup>5</sup>	Leitzke <i>et al.</i> , 2003
Vinyl sulfonate ion			8 × 10 <sup>3</sup>	Leitzke <i>et al.</i> , 2003

## 6.2 THE CRIEGEE MECHANISM

The 1,3-cyloadduct of ozone to olefins was named by *Carl Friedrich Harries* “ozonide” (Chapter 1). Mechanistic details were only later unravelled by *Rudolf Criegee* (Chapter 1), and the reaction of ozone with olefins bears his name. In water, olefins react essentially according to the Criegee mechanism [reactions (1)–(9)], originally studied in organic solvents (Criegee, 1975). In water, however, ionic intermediates are intercepted [reaction (7)], and the reaction sequence, that in organic solvents proceeds to the Criegee ozonide, is arrested at an early stage (Dowideit & von Sonntag, 1998). As here ozone reactions in aqueous solution are discussed, the Criegee ozonide [cf. reaction (9)] can be disregarded, and whenever an ozonide is mentioned, the first ozonide is referred to.



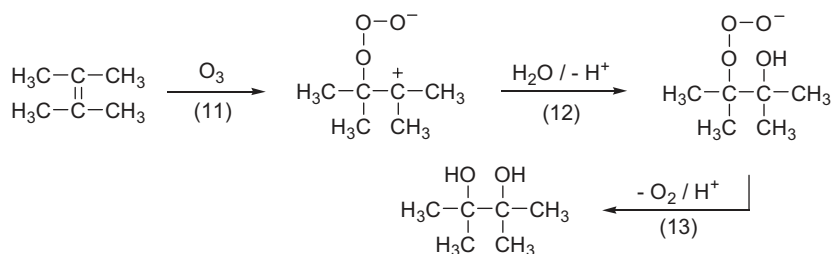
The Criegee mechanism has been challenged by suggesting that an electron transfer may occur instead [reaction (10)] (Zhang & Zhu, 1997).



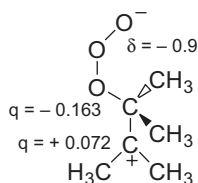
As will be seen from the following, this suggestion can be readily falsified on the basis of detailed product studies shown below. In fact, all data are in favour of the Criegee mechanism.

The reaction of ozone with olefins is usually described as a concerted, symmetry-allowed cycloaddition [reaction (1)] (Ponec *et al.*, 1997; Anglada *et al.*, 1999; Olzmann *et al.*, 1997), that is, the reaction does not proceed via the first zwitterion as an intermediate [reactions (2) and (3)]. This even holds for polarised C–C double bonds such as in vinyl chloride.

Yet with tetramethylethene, a partial oxidation product is formed in 10% yield [reactions (11)–(13)] (Dowideit & von Sonntag, 1998).



As cycloaddition proceeds, the C–C double bond turns into a C–C single bond and starts rotating to move the bulky methyl groups into positions of minimal steric hindrance (Figure 6.1).



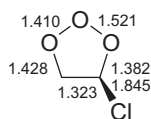
**Figure 6.1** Reaction of ozone with tetramethylethene. Rotation of the central C–C bond into positions of minimal steric hindrance of the substituents (interrupted calculation) Naumov & von Sonntag, unpublished.

Apparently, this developing zwitterion can be intercepted by water [reaction (12)] to some extent *en route* to the ozonide that must be the precursor of the major products. This observation points to a certain likelihood that in other olefins zwitterionic structures may also develop even though they are not noticeably intercepted by water.

The concerted reactions of ozone with fumaric and maleic acid give rise to two different stereoisomeric ozonides (see below). Their decay leads to the same products, but product ratios are markedly different (Leitzke & von Sonntag, 2009). This is an indication that if a primary zwitterion were formed, its lifetime would certainly be too short to allow a full equilibration of the two isomers by rotation around the central C–C bond.

In this context it is noted that in benzene and its derivatives, zwitterionic structures (ozone adducts) are sufficiently stable for calculating their standard Gibbs free energies of formation in water (Chapter 7). The reason for this marked difference to olefins may be that in aromatic compounds the developing positive charge is distributed over the entire aromatic ring, and a collapse to the ozonide is thus retarded.

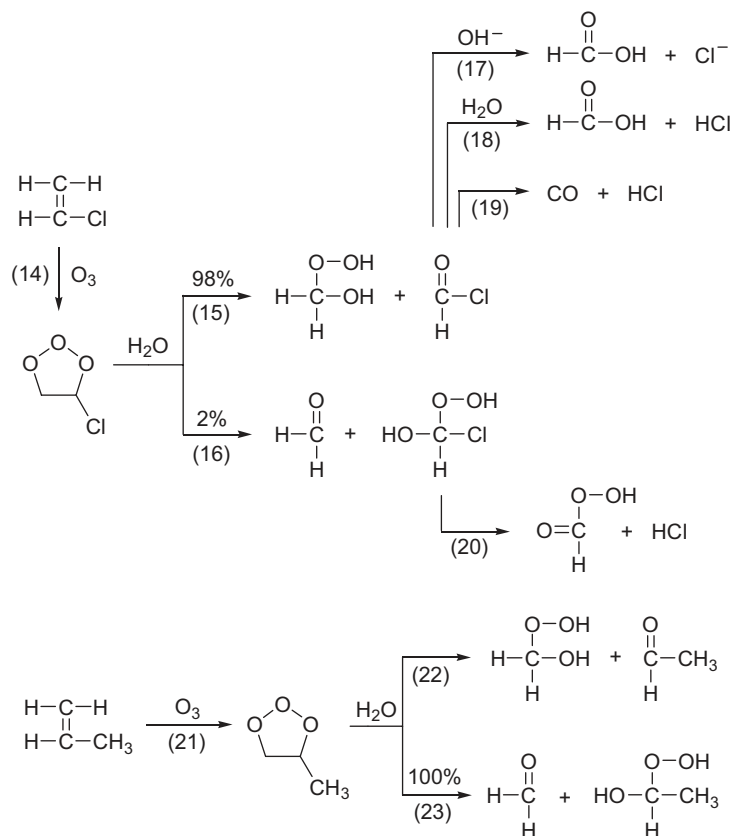
Ozonides derived from asymmetrical olefins have different O–O and C–O bond lengths. An example is shown in Figure 6.2.



**Figure 6.2** Structure of the ozonide derived from vinyl chloride according to Naumov & von Sonntag, unpublished.

These differences in bond lengths indicate the direction the ozonide will take when opening the ring. The longer O–O bond will become even longer and eventually break, while the shorter C–O bond will further contract.

In the quantum-chemical calculations, the second zwitterion [reaction (4)] is not an intermediate, and the reaction continues by breaking the central C–C bond [concerted reaction (5)]. This predisposition in the ozonides for ensuing decay routes results in the observed high regioselectivity in product formation. The ozonides of vinyl chloride and propene may serve as examples. As expected, they follow opposite decay routes [reaction (15) vs. reaction (23)].



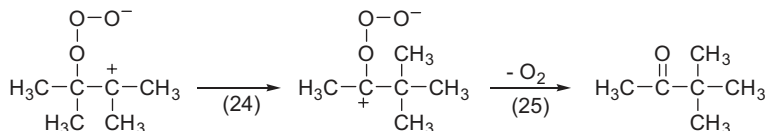
Even though the second zwitterion is neither a real intermediate nor a transition state in most ozone reactions, it is heuristically helpful. For differently substituted olefins, the route that leads to the zwitterion that can stabilise the positive charge at carbon the best is followed preferentially.

The third zwitterion is trapped by water giving rise to  $\alpha$ -hydroxyalkylhydroperoxides [reaction (7)], and this reaction is much faster than a trapping by the carbonyl compound [reaction (9)] formed next to the third zwitterion within the solvent cage. Thus in the ozonolysis of olefins in water, there are typically two primary products, an  $\alpha$ -hydroxyalkylhydroperoxide and a carbonyl compound. As will be shown below, these primary products may still be highly reactive and often decay very rapidly into the final products.

### 6.3 PARTIAL OXIDATION

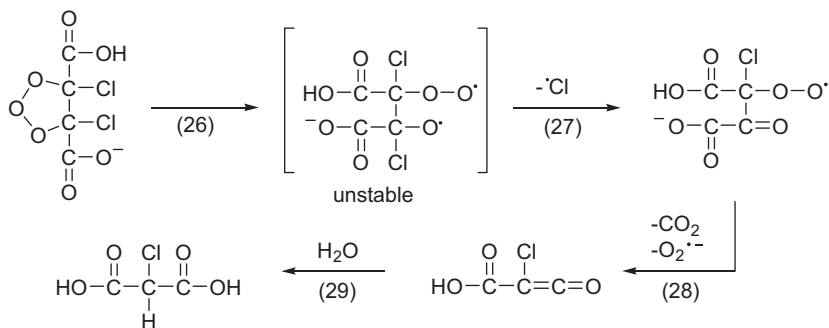
Although the Criegee mechanism is the dominating process in the reactions of olefins with ozone, products may be observed in which the former C–C double bond is not fully cleaved, that is, the carbon skeleton

remains intact. Such processes are called “partial oxidation”. An example of this has been given above [reactions (11)–(13)]. Here, ring closure to the Criegee ozonide competes with a trapping of the carbocation site by water. In organic solvents, a methyl shift is observed instead [reactions (24) and (25)].



## 6.4 DECAY OF THE OZONIDE VIA FREE RADICALS

Although heterolytic cleavage of the ozonide is by far the most important process, there seem to be cases, where homolytic cleavage can occur. Strong experimental evidence for this has been obtained from the ozonolysis of dichloromaleic acid at pH 3 (largely the monoanion). The chloride yield is 3.9 mol per mol ozone and reduces to 1.7 in the presence of tertiary butanol (see paragraph 6.6.6) pointing to the formation of  $\bullet\text{Cl}$ , which subsequently induces a short chain reaction. Quantum-chemical calculations (Naumov & von Sonntag, 2009, unpublished) indicate that, for example, reaction (26)/(27) is slightly exergonic ( $\Delta G^\circ = -2 \text{ kJ mol}^{-1}$ ) as are subsequent decarboxylation plus  $\text{O}_2^{\bullet-}$  elimination [reaction (28),  $\Delta G^\circ = -108 \text{ kJ mol}^{-1}$ ] and the hydrolysis of the ketene [reaction (29),  $\Delta G^\circ = -49 \text{ kJ mol}^{-1}$ ]. There are other potential exergonic routes to the chain carrier  $\bullet\text{Cl}$ , but at this stage it is premature to discuss other alternatives, as detailed product studies are missing.

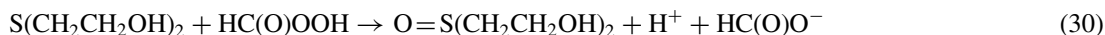


## 6.5 DETECTION OF $\alpha$ -HYDROXYALKYLHYDROPEROXIDES

$\alpha$ -Hydroxyalkylhydroperoxides are often quite stable, as equilibrium (8) is usually only slowly attained at pH 7 (Bothe & Schulte-Frohlinde, 1980).  $\alpha$ -Hydroxyalkylhydroperoxides react, similarly to  $\text{H}_2\text{O}_2$ , with molybdate-activated iodide by forming  $\text{I}_3^-$ . The kinetics of such reactions are markedly different and can be used to characterise and quantify such intermediates (Dowideit & von Sonntag, 1998; Flyunt *et al.*, 2003b; Stemmler & von Gunten, 2000). As the  $\alpha$ -hydroxyalkylhydroperoxides react much more slowly than  $\text{H}_2\text{O}_2$  (for a compilation of rate constants see Table 6.2), this approach can even be used to quantify  $\text{H}_2\text{O}_2$  and  $\alpha$ -hydroxyalkylhydroperoxides when formed side by side. The very reactive hydroperoxides, formic and acetic peracids, react even without molybdate catalysis. Formic peracid is reduced by  $\text{S}(\text{CH}_2\text{CH}_2\text{OH})_2$  to formic acid [reaction (30),  $k = 220 \text{ M}^{-1} \text{ s}^{-1}$  (Flyunt *et al.*, 2003a)], and this reaction



can be followed by changes in the conductance, as formic peracid ( $pK_a = 7.1$ ) is barely dissociated at pH 6 while formic acid ( $pK_a = 3.75$ ) is fully dissociated under such conditions.



**Table 6.2** Compilation of half-lives of the reactions of molybdate-activated iodide with some hydroperoxides

Hydroperoxide	$t_{1/2}/s$	Reference
HC(O)OOH <sup>a</sup>	0.0032	Dowideit & von Sonntag, 1998
CH <sub>3</sub> C(O)OOH <sup>b</sup>	0.022	Flyunt <i>et al.</i> , 2003b
CH <sub>3</sub> C(O)C(O)NHC(O)N=C(OOH)C(O)H <sup>b</sup>	0.12, 0.16 <sup>c</sup>	Flyunt <i>et al.</i> , 2002
5-Hydroperoxy-5-methylhydantoin <sup>b</sup>	0.71, 0.9 <sup>c</sup>	Flyunt <i>et al.</i> , 2002
H <sub>2</sub> O <sub>2</sub> <sup>d</sup>	2.5	Dowideit & von Sonntag, 1998
H <sub>2</sub> O <sub>2</sub> <sup>b</sup>	$1.8 \times 10^{-3}$	Flyunt <i>et al.</i> , 2003a
HOCH(CH <sub>3</sub> )OOH <sup>d</sup>	13.7	Dowideit & von Sonntag, 1998
HOCH <sub>2</sub> OOH <sup>d</sup>	203	Dowideit & von Sonntag, 1998
HOOCH <sub>2</sub> C(CH <sub>3</sub> ) <sub>2</sub> OH	$\sim 260^c$	Schuchmann & von Sonntag, 1979
CH <sub>3</sub> OOH	790	Flyunt <i>et al.</i> , 2003b
HOOCH <sub>2</sub> CH(CH <sub>3</sub> )OH	420 <sup>c</sup>	Flyunt <i>et al.</i> , 2003b
HOC(CH <sub>3</sub> ) <sub>2</sub> OOH <sup>d</sup>	$\sim 35\ 000$	Dowideit & von Sonntag, 1998

<sup>a</sup>Hydroperoxide reacts equally rapidly without molybdate catalysis. <sup>b</sup>Reaction without molybdate catalysis.

<sup>c</sup>Reagent A [0.4 M KI,  $3.6 \times 10^{-2}$  M KOH,  $1.6 \times 10^{-4}$  M (NH<sub>4</sub>)<sub>6</sub>Mo<sub>7</sub>O<sub>24</sub>], reagent B (0.1 M potassium hydrogen phthalate) and probe at 1 : 1 : 2. <sup>d</sup>Molybdate catalysis, [I<sup>-</sup>] = 0.17 M.

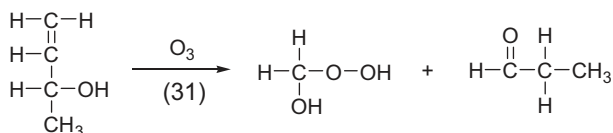
## 6.6 OZONE REACTIONS OF OLEFINS – PRODUCTS AND REACTIONS OF REACTIVE INTERMEDIATES

In this paragraph, the ozonolysis products of a large number of olefins will be presented. This information will allow predictions on the ozonolyses of olefins for which no data are available. The high regioselectivity of ozone reactions with unequally substituted olefins assists these predictions.

### 6.6.1 Methyl- and halogen-substituted olefins

Final products and some of the longer-lived intermediates of some methyl- and chlorine-substituted olefins are compiled in Table 6.3.

The reactions of propene have been discussed above [reactions (21) and (23)]. Ethene is symmetrical, and from the above one expects equal amounts of formaldehyde and hydroxymethylhydroperoxide. This is indeed observed (Table 6.3). A more convenient source to produce hydroxymethylhydroperoxide in ozone reactions is buten-3-ol [reaction (31)].



**Table 6.3** Products and their yields [with respect to ozone consumption (mol/mol)] in the ozonolysis of ethene and some of its methyl- and chlorine-substituted derivatives in aqueous solution according to Dowideit & von Sonntag (1998). Empty fields indicate that a given product is not expected to be formed and has not been looked for

Product	Ethene	Propene	Me <sub>4</sub> - Ethene	Cl- Ethene	1,1-Cl <sub>2</sub> - Ethene	1,2-Cl <sub>2</sub> - Ethene	Cl <sub>3</sub> - Ethene	1,1-Cl <sub>2</sub> - Propene
HCl				1.05	1.95	2.02	2.87	2.05
HC(O)OH				0.06	0.03	1.01	0.82	
HC(O)OOH				0.02 <sup>(a)</sup>		0.98 <sup>(a)</sup>	0.88 <sup>(a)</sup>	
HOCH <sub>2</sub> COOH					0.07 <sup>(c)</sup>			
CO				1.01		1.08	0.04	
CO <sub>2</sub>					0.90	0.02	0.95	1.01
CH <sub>2</sub> O	2.04	1.03			0.96			
CH <sub>3</sub> C(O)H		0.97						1.03
(CH <sub>3</sub> ) <sub>2</sub> CO			1.74					
HOCH <sub>2</sub> OOH	1.08 <sup>(b)</sup>			1.06 <sup>(b)</sup>	0.96 <sup>(b)</sup>			
CH <sub>3</sub> CH(OH)OOH		0.99 <sup>(b)</sup>						0.98 <sup>(b)</sup>
(CH <sub>3</sub> ) <sub>2</sub> C(OH)OOH			(d)					
Cl <sub>2</sub> CHC(O)H					<0.01 <sup>(c)</sup>			
ClCH <sub>2</sub> C(O)H					0.08 <sup>(c)</sup>			
Cl <sub>2</sub> CHC(O)OH							0.04 <sup>(c)</sup>	
[(CH <sub>3</sub> ) <sub>2</sub> C(OH)] <sub>2</sub>			~0.1					

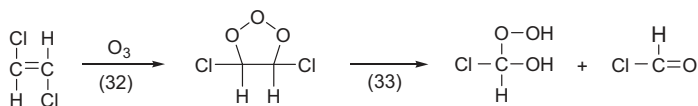
<sup>(a)</sup>Precursor of formic acid. <sup>(b)</sup>Precursor of aldehydes. <sup>(c)</sup>Product of partial oxidation reaction. <sup>(d)</sup>The reaction with molybdate-activated iodide is too slow for its determination.

Its good solubility in water and its high rate constant (Table 6.1) makes buten-3-ol a very convenient competitor for the determination of ozone rate constants (Chapter 2).

With halogenated olefins, reactive halogen-containing intermediates are formed which show an interesting chemistry. With vinyl chloride the main reaction path leads to hydroxymethylhydroperoxide and formyl chloride [reaction (15)]. Formyl chloride rapidly decomposes into CO and HCl [reaction (19),  $k = 600 \text{ s}^{-1}$ ; 94%] (Dowideit *et al.*, 1996). Its hydrolysis into formic acid plus HCl [reaction (18), 6%] is slow in comparison but gains in importance at high pH [reaction (17),  $k(\text{OH}^-) = 2.5 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ]. A minor route leads to chlorohydroxymethylhydroperoxide [reaction (16)]. The geminal chlorohydrine substructure in chlorohydroxymethylhydroperoxide is very unstable and rapidly loses HCl [on a low microsecond timescale (Köster & Asmus, 1971; Mertens *et al.*, 1994)] giving rise to formic peracid [reaction (20)]. Formic peracid is generated in the reaction of 1,2-dichloroethene (see below), and this is a convenient method for its formation [for its reactions see (Flyunt *et al.*, 2003a)].

Formyl bromide, the product of the analogous reaction of vinyl bromide with ozone also decomposes preferentially into CO plus HBr. With 3.6%, the formic acid yield is lower than the corresponding yield from formyl chloride (6%). Whether this is due to a faster decomposition or a slower hydrolysis is not yet known.

1,2-Dichloroethene is symmetrical, and the primary products are chlorohydroxymethylhydroperoxide and formyl chloride [reactions (32) and (33)]. HCl, CO and formic peracid are the main final products (see above).

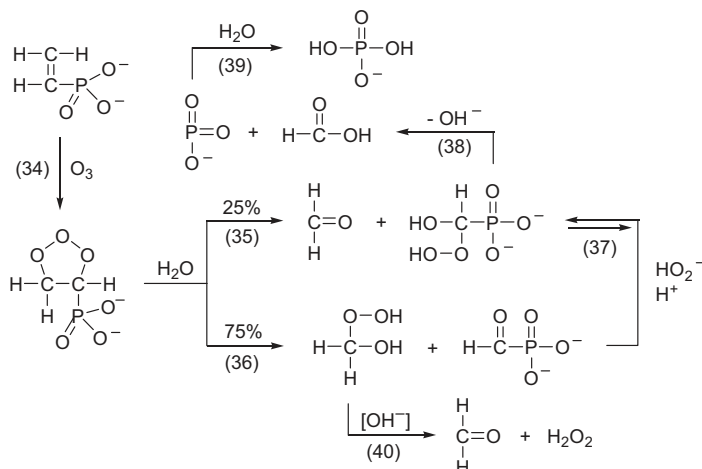


The reactions of 1,2-dibromoethene with ozone are analogous (Leitzke *et al.*, 2003).

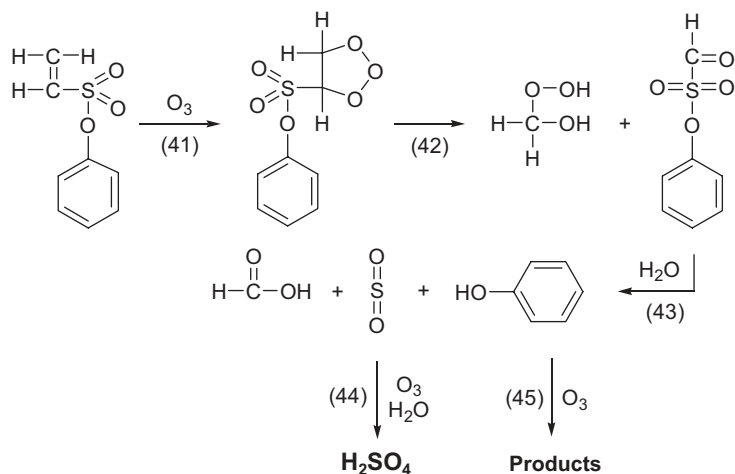
### 6.6.2 Acrylonitrile, vinyl acetate, diethyl vinylphosphonate, vinyl phenyl sulfonate, vinylsulfonic acid and vinylene carbonate

Cyano, acetyl and diethyl phosphonate groups are electron-withdrawing substituents, and the ozonolysis of acrylonitrile, vinyl acetate and diethyl vinylphosphonate follow the same regioselectivity as observed for the ozone reaction with vinyl chloride discussed above, that is, the primary products are hydroxymethylhydroperoxide and the corresponding formyl derivatives, formyl cyanide, formyl acetate and diethyl formylphosphonate, respectively (Leitzke *et al.*, 2003). These mixed acid anhydrides are not stable in water. Stopped-flow with conductometric detection allowed the determination of the rate constant for their hydrolysis: formyl cyanide [ $k = 3 \text{ s}^{-1}$ ;  $k(\text{OH}^-) = 3.8 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$ ]; formyl acetate ( $k = 0.25 \text{ s}^{-1}$ ); diethyl formylphosphonate [ $k = 7 \times 10^{-3} \text{ s}^{-1}$ ;  $k(\text{OH}^-) = 3.2 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ] (Leitzke *et al.*, 2003).

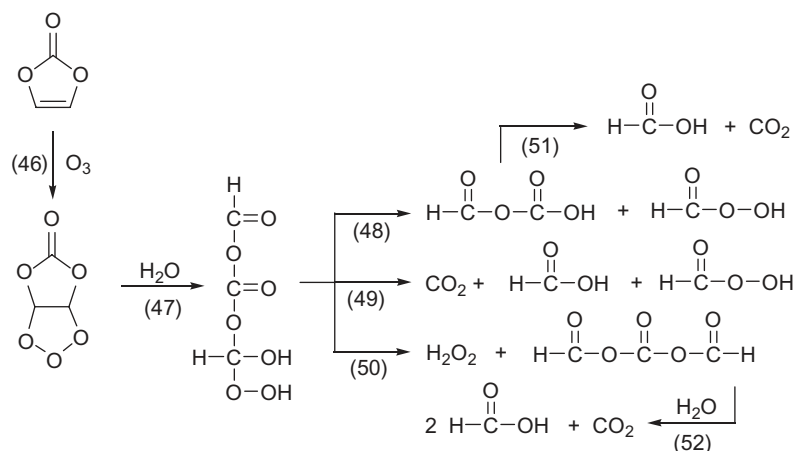
The ozonolysis of vinylphosphonic acid is somewhat more complex as the ozonide decays in two directions in a 1:3 ratio [reactions (35) and (36)] (Leitzke *et al.*, 2003). In the presence of excess  $\text{H}_2\text{O}_2$ , formic and phosphoric acids are the final products [reactions (37)–(39)]. In the presence of catalase, which destroys  $\text{H}_2\text{O}_2$  but not  $\alpha$ -hydroxyalkylhydroperoxides, the rate of formic acid formation is markedly slower and phosphonic acid is observed instead of phosphoric acid. Apparently, formylphosphonate hydrolyses only slowly [ $k(\text{OH}^-) \approx 5 \text{ M}^{-1} \text{ s}^{-1}$ ]. The slowness of this reaction when compared to the formyl compounds discussed above may be due to the fact that here  $\text{OH}^-$  has to react with a doubly negatively charged species. At pH 10.2 and in the presence of borate buffer,  $\text{H}_2\text{O}_2$  reacts with formylphosphonate with an observed rate constant of  $k_{\text{obs}} = 260 \text{ M}^{-1} \text{ s}^{-1}$  (phosphonate is not oxidised by  $\text{H}_2\text{O}_2$  at any pH). There seems to be also a pH dependence between reactions (–37) and (38). While at pH 7  $\text{H}_2\text{O}_2$  elimination is observed, decomposition is favoured at pH 10.2, where the hydroxyperoxy(hydroxy)methyl phosphonic acid is fully deprotonated.



Ozonolysis of vinyl phenylsulfonate is complex as some of the products, notably  $\text{SO}_2$  and phenol, react rapidly with ozone (Leitzke *et al.*, 2003). Hydroxymethylhydroperoxide, formic acid and sulfuric acid are products, but the material balance is incomplete and reactions (41)–(45) must remain a tentative suggestion. Similar uncertainties prevail in the ozonolysis of vinylsulfonic acid (Leitzke *et al.*, 2003).



The ozonolysis of vinylene carbonate leads to the formation of formic acid, formic peracid,  $\text{H}_2\text{O}_2$  and  $\text{CO}_2$  (Leitzke *et al.*, 2003). Potential decay reactions of this symmetrical ozonide are shown in reactions (46)–(52). The reaction that leads to  $\text{H}_2\text{O}_2$  [reaction (50)] must be minor (4%).



### 6.6.3 Acrylic, methacrylic, fumaric, maleic and muconic acids

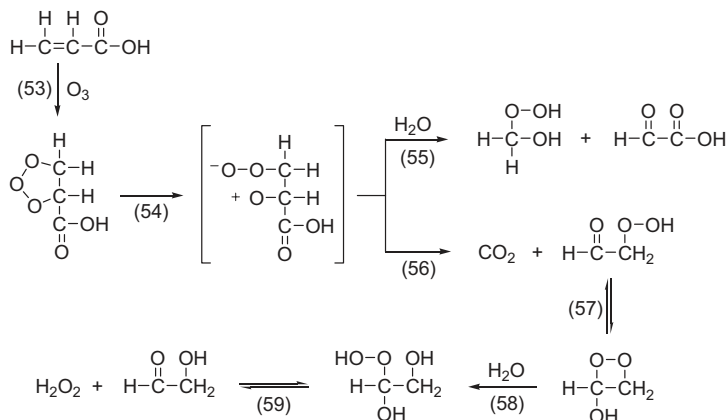
For acrylic and methacrylic acids, the yields of the product based on ozone consumption are compiled in Table 6.4.

**Table 6.4** Product yields (mol per mol O<sub>3</sub> consumed) in the reaction of O<sub>3</sub> with acrylic and methacrylic acids according to Leitzke & von Sonntag (2009)

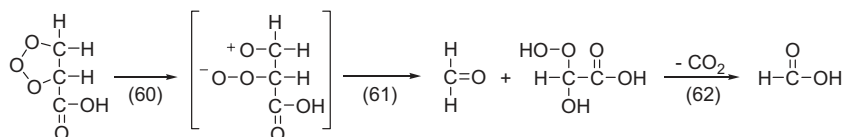
Product	Acrylic acid Anion (free acid)	Methacrylic acid Anion (free acid)
Formaldehyde <sup>(a)</sup>	0.52 (0.72)	0.43 (0.62)
Hydroxymethylhydroperoxide	0.43 (ND)	see text (ND)
1-Hydroperoxypropan-2-one	–	0.57 (ND)
Glyoxylic acid	0.54 (ND)	–
2-Oxopropanoic acid	–	0.41 (ND)
Glycol aldehyde	0.48 (ND)	–
Methylglyoxal	–	0.54 (ND)
Formic acid	absent (absent)	–
Acetic acid	–	absent (absent)
Total Peroxide	1.01 (1.0)	1.04 (1.0)
H <sub>2</sub> O <sub>2</sub>	0.58 (ND)	0.46 (ND)

<sup>(a)</sup>Includes the yield of hydroxymethylhydroperoxide that decomposes into formaldehyde during the assay, ND = not determined, – product cannot be formed.

Mechanistically, acrylic and methacrylic acids follow the same pattern [reactions (53)–(59) and reactions (63)–(67), respectively].

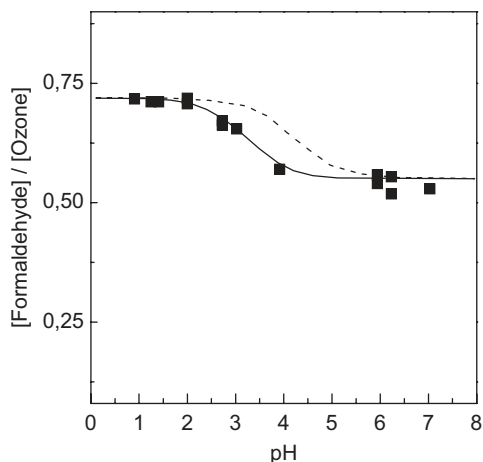


The second zwitterions are given in brackets as they may not be intermediates, but they indicate the directions the ozonides will take upon their decay. The absence of formic and acetic acids in the case of acrylic and methacrylic acids, respectively, shows that the other conceivable route, for example, reactions (60)–(62) is not taken in these acids.



Moreover, cleavage along the O–O and C–C bonds of the envisaged dioxetane intermediate [cf. reaction (57)] does not take place.

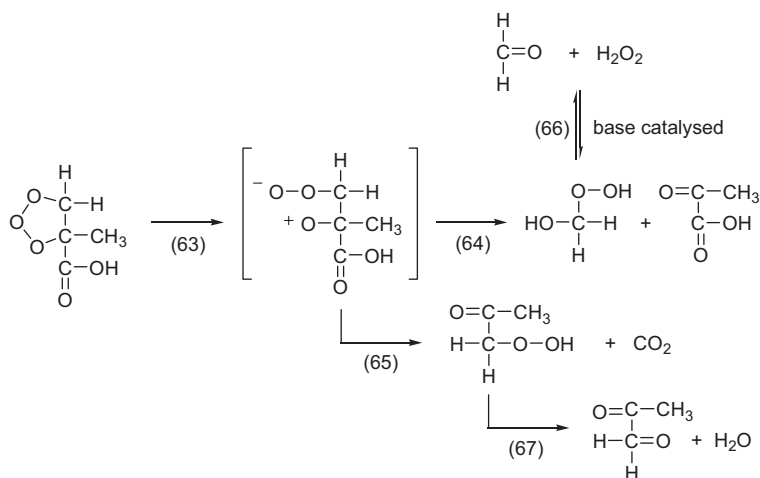
Depending on the protonation state of the carboxylic group, there is some bias in the branching between reactions (55) and (56). As expected, the deprotonated carboxyl group decarboxylates more readily favouring reaction (56). Formaldehyde, which is produced from reaction (55), can be measured with some accuracy. A plot of the formaldehyde yield as a function of pH is shown in Figure 6.3.



**Figure 6.3** The pH dependence of the formaldehyde yield in the ozonolysis of acrylic acid. The dashed line indicates how this dependence would look if it were governed by the  $pK_a$  value of acrylic acid. From Leitzke & von Sonntag, 2009 with permission.

The inflection point is at pH 3, markedly distant from the  $pK_a$  value of acrylic acid, 4.25 (dashed line). It may reflect the  $pK_a$  value of the ozonide, as the zwitterion is most likely not an intermediate, but if it were it would be too short-lived for the  $pK_a$  equilibrium to become established during its lifetime.

The reactions of methacrylic acid ozonide are depicted in reactions (63)–(67).



Interestingly, hydroxymethylhydroperoxide, formed in reaction (64), cannot be detected by its slow reaction with molybdate-activated iodide. It is too short-lived here, as the buffering properties of methacrylic acid that decompose hydroxymethylhydroperoxide into formaldehyde and  $\text{H}_2\text{O}_2$  [reaction (60)] are much more pronounced than in the case of acrylic acid. This has been shown by production of hydroxymethylhydroperoxide in the reaction of buten-3-ol with ozone [reaction (31)] and subsequent addition of methacrylic acid. The latter rapidly catalyses reaction (66) and hydroxymethylhydroperoxide is no longer detected [note that the somewhat lower value of hydroxymethylhydroperoxide as compared to that of formaldehyde in the case of acrylic acid (Table 6.4) may be due to the, albeit much lower, buffering effects of acrylic acid. Due to its higher  $\text{p}K_{\text{a}}$  value, methacrylic acid is a better buffer, and thus a more efficient catalyst, than acrylic acid in close to neutral solutions].

The hydroperoxide attributed to 1-hydroperoxypropan-2-one formed in reaction (65) reacts much faster with molybdate-activated iodide ( $k = 0.15 \text{ M}^{-1} \text{ s}^{-1}$ ) than hydroxymethylhydroperoxide ( $k = 3.4 \times 10^{-3} \text{ M}^{-1} \text{ s}^{-1}$ ). Interestingly, the methyl substituent in this hydroperoxide has a marked effect on its decay. Compared to aldehydes, ketones form hydrates (and thus also hydroxyalkylhydroperoxides) less efficiently [in water, formaldehyde is practically fully hydrated,  $\text{CH}_2(\text{OH})_2$ , acetaldehyde  $\sim 50\%$  hydrated, acetone  $< 0.1\%$  hydrated (Bell, 1966)]. Thus, the reaction analogous to reaction (57) will be inefficient, and water elimination occurs instead [reaction (67)]. The buffer properties of methacrylic acid may speed up this reaction. There are other  $\alpha$ -hydroxyalkylhydroperoxides, where water elimination rather than  $\text{H}_2\text{O}_2$  elimination is observed. A case in point is the muconic compound formed in the ozonolysis of phenol (Mvula & von Sonntag, 2003). Reasons for this are as yet not known, but one may recall that  $\text{H}_2\text{O}_2$  elimination is reversible while water elimination is not. A more detailed study of  $\text{H}_2\text{O}_2$  with aldehydes would be required to elucidate this interesting aspect.

The reactions of  $\text{O}_3$  with maleic and fumaric acids in aqueous solution has found some attention (Gilbert, 1977; Leitzke & von Sonntag, 2009; Ramseier & von Gunten, 2009), but mechanistic details were only understood recently (Leitzke & von Sonntag, 2009; Ramseier & von Gunten, 2009). These two isomeric acids are available in high purity. In aqueous solution, *cis*  $\rightleftharpoons$  *trans* isomerisation takes place. This may lead to an artefact, that is, the other isomer increases linearly with the ozone dose, when the work-up of the samples follows the sequence of ozone doses (Leitzke, 2003). It is now clear, that ozone does not induce *cis*  $\rightleftharpoons$  *trans* isomerisation. These two isomers give rise to the same products, but their yields differ remarkably (Table 6.5).

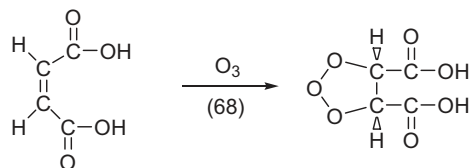
**Table 6.5** Product yields (mol per mol  $\text{O}_3$  consumed) in the reaction of  $\text{O}_3$  with fumaric and maleic acids at pH 5.3 according to Leitzke & von Sonntag (2009)

Product	Fumaric acid	Maleic acid
Formic acid	0.77	0.92
Glyoxylic acid	0.85	1.05
Glyoxal	0.27	0.03
Total peroxide	0.31	ND

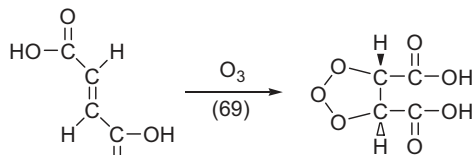
ND = not determined.

With fumaric acid, glyoxal is formed in 27% yield, while with maleic acid it is only 3%. This is a strong indication that these two isomers give rise to two ozonides that differ with respect to their preferred decay routes. This is in line with the concept that ozone addition to the double bond is a concerted reaction

[reactions (68) and (69)]. In any case, a zwitterionic intermediate, if it is an intermediate, must be too short-lived to allow a rotation around the former C–C double bond.

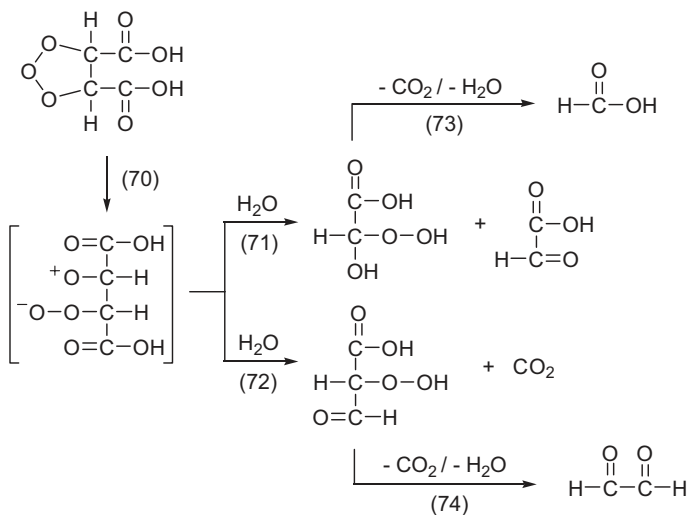


Maleic acid



Fumaric acid

We are not yet in a position to present a mechanistic explanation for this difference, but the general mechanism suggested by reactions (70)–(74) accounts for the observed products.



### 6.6.4 Muconic acids

The ozonolysis of *trans,trans*-muconic acid in aqueous solution has been studied under the conditions of extensive ozonation (Gilbert, 1980). No distinction between primary and secondary products has been made. The primary products and their yields in the ozonolysis of *cis,cis*-muconic acid (Leitzke *et al.*, 2003) are compiled in Table 6.6, and additional information on primary as well as secondary products is also available (Ramseier & von Gunten, 2009) [reactions (75)–(79)].

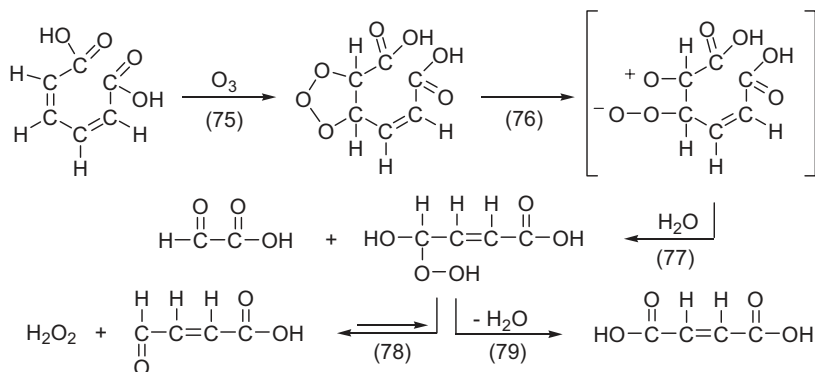


**Table 6.6** Product yields (mol per mol O<sub>3</sub> consumed) in the reaction of O<sub>3</sub> with *cis,cis*-muconic acid according to Leitzke *et al.* (2003)

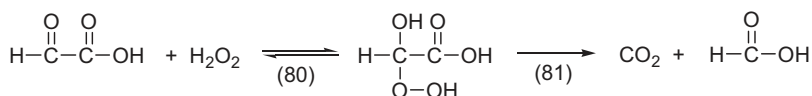
Product	pH 2	pH 8
H <sub>2</sub> O <sub>2</sub>	0.98	0.9
Glyoxylic acid	0.98 <sup>(a)</sup>	0.99 <sup>(a)</sup>
4-Oxobut-2-enoic acid	not quantified <sup>(b)</sup>	not quantified <sup>(b)</sup>
Formic acid	absent	absent

<sup>(a)</sup>Catalase had been added immediately after ozonolysis; <sup>(b)</sup>detected by GC-MS.

There is no organic hydroperoxide detected, and the total peroxide yield is due to H<sub>2</sub>O<sub>2</sub>. The other product is glyoxylic acid. This aldehyde reacts readily with H<sub>2</sub>O<sub>2</sub>, resulting in the subsequent formation of formic acid [reactions (80) and (81)]. For suppressing this secondary reaction by destroying H<sub>2</sub>O<sub>2</sub>, catalase has been added immediately after ozonolysis. Under such conditions, glyoxylic acid matches the H<sub>2</sub>O<sub>2</sub> yield, and formic acid is no longer formed. 4-Oxobut-3-enoic acid has been detected as a major product by GC-MS but was not quantified. Reactions (75)–(79) account for the observed products.

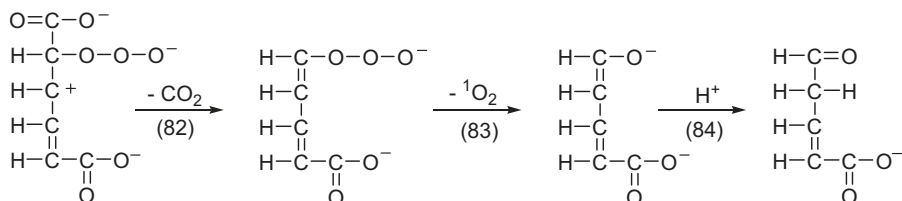


Besides the conversion of glyoxylic acid by hydrogen peroxide into CO<sub>2</sub> and formic acid [reactions (80) and (81)] (for the kinetics of these reactions see (Leitzke *et al.*, 2001), 4-oxobut-3-enoic acid is likely to undergo the analogous reactions (78) and (79). In the absence of catalase, the ensuing products, formic acid and maleic acid, are indeed formed (Ramseier & von Gunten, 2009).



There is the interesting aspect that upon ozonolysis of *cis,cis*-muconic acid, 4% singlet oxygen is formed (Muñoz *et al.*, 2001). This points to an additional pathway for the reaction of muconic acid with ozone. As the formation of the ozonide is exergonic by ~43 kJ mol<sup>-1</sup> (Naumov & von Sonntag, 2009, unpublished) and seems not to decarboxylate readily, an additional pathway in competition to the ozonide formation seems to be of (minor) importance. Approach of ozone to muconic acid may develop a zwitterionic intermediate with the positive charge delocalised over the two conjugated C–C double

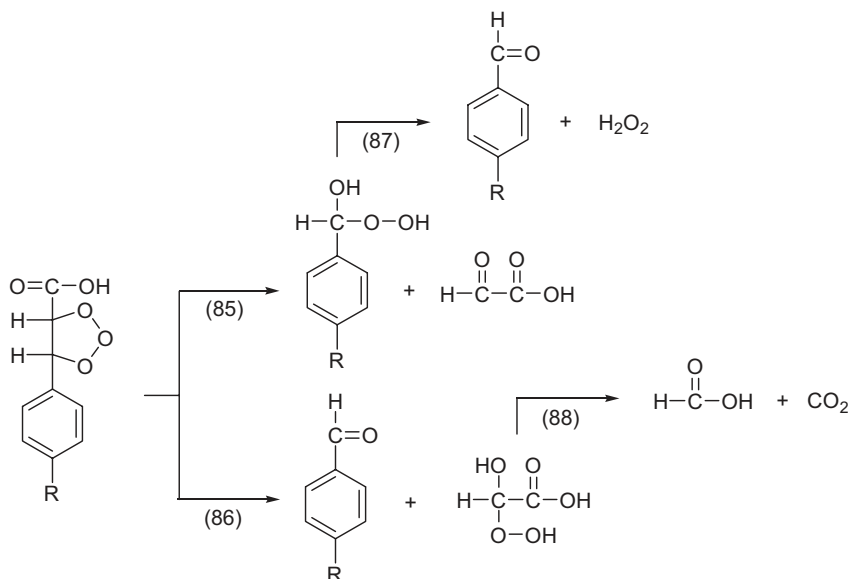
bonds. This is not a stable structure, possibly not even a transition state, but decarboxylation may already occur [reaction (82)] as it tends to develop. Singlet oxygen is subsequently released [reaction (83)].



The standard Gibbs free energy including  $\text{CO}_2$  elimination [reaction (82)] has been calculated at  $-77 \text{ kJ mol}^{-1}$ . At the time when these measurements were made, the implications were not realised, and whether small amounts of 5-oxo-pent-2-enoic acid (or its decarboxylation products) are indeed formed has not been looked at. It seems worth mentioning that with aromatic compounds, where the positive charge of the zwitterionic ozone adduct can be distributed over one more double bond, such adducts are well-defined intermediates (Naumov & von Sonntag, 2010) (Chapter 7).

### 6.6.5 Cinnamic acids

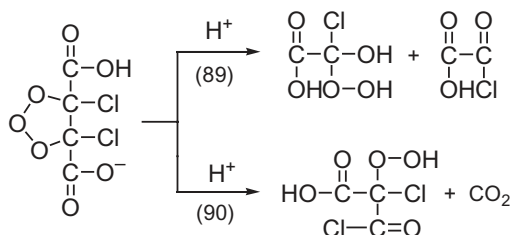
Cinnamic acids contain two potential sites for ozone attack, the olefinic C–C double bond and the aromatic ring. The rate of reaction with the latter is much slower, and thus the site of ozone attack on cinnamic acids is the exocyclic C–C double bond (Leitzke *et al.*, 2001). Electron-donating/electron-withdrawing substituents at the aromatic ring have a much smaller effect on the rate of reaction than one would expect if the site of attack were the aromatic ring (cf. Chapter 7). Although there is only a small effect of methoxy and nitro substituents on the rate of reaction (Table 6.1), there is a marked effect on the decay route of the ozonides [reactions (85)–(88)].



The ozonides of cinnamic acid and its 4-methoxy derivative decay only according to reaction (85), whereas the electron-withdrawing nitro substituent makes it possible that reaction (86) proceeds to 30%. The hydroxyhydroperoxide only eliminates  $\text{H}_2\text{O}_2$  [reaction (87)], and the potentially competing water elimination that would lead to benzoic acid is not observed (<2%).

### 6.6.6 Dichloromaleic acid

With dichloromaleic acid only some preliminary experiments have been carried out (Leitzke & von Sonntag, 2009). These few data are still sufficiently interesting to be reported as they may serve as a basis for future investigations. Ozonation has been carried out at pH 3.1. Under such conditions, the  $\text{Cl}^-$  yield was 3.9 with respect to ozone consumed, much higher than the maximum value of 2.0 for a non-chain reaction, and an acid is formed that has the same retention time as ketomalonic acid (not necessarily a correct assignment). When tertiary butanol (0.26 M), which scavenges reactive free radicals such as  $\cdot\text{Cl}$ , is added in excess, the  $\text{Cl}^-$  yield drops to 1.7, and the unknown acid is no longer formed. This points to a free-radical-induced short chain reaction [reactions (26)–(29)] that runs in parallel to the normal non-radical reaction. The latter may be tentatively described by reactions (89) and (90) and ensuing HCl releasing reactions.

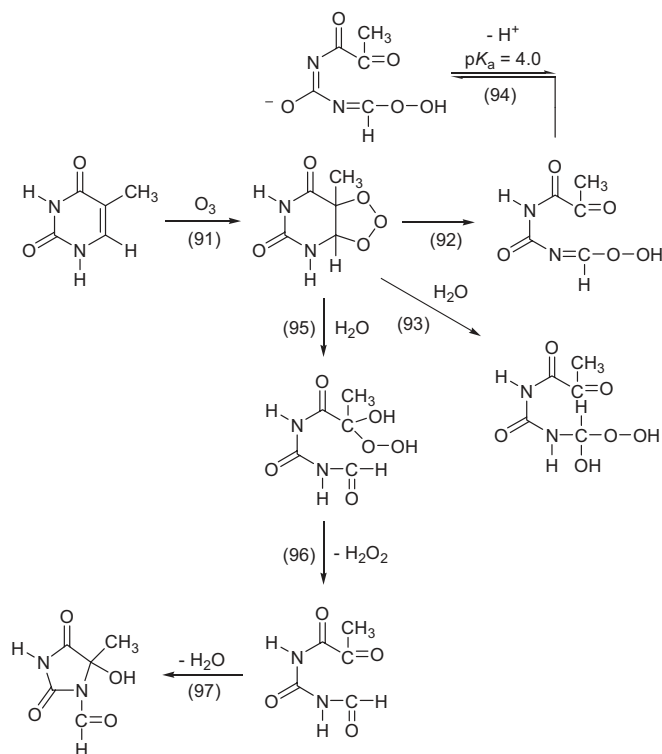


At this point, further suggestions would be mere speculation, as a detailed product study has not yet been carried out, but it is worth mentioning that short chain reactions are common in the peroxy radical chemistry of chlorinated compounds (von Sonntag & Schuchmann, 1997) (cf. Chapter 14).

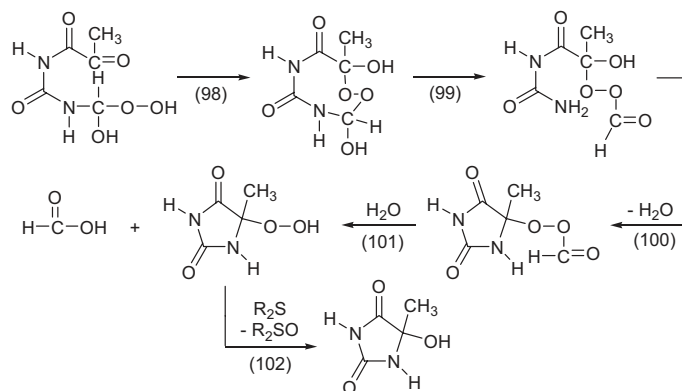
### 6.6.7 Pyrimidine nucleobases

Among the nucleic acid constituents, the pyrimidines react quite readily with ozone (Table 6.1 and Chapter 4). Among these, detailed product studies are only available on thymine and thymidine (Flyunt *et al.*, 2002). Their reactions are governed by the addition of ozone to the C(5)–C(6) double bond. Some key reactions of thymine are shown in reactions (91)–(97). For further details and the reactions of thymidine that are similar but yet markedly different in several aspects the interested reader is referred to the original paper (Flyunt *et al.*, 2002).

The ozonide formed in reaction (91) predominantly (75%) opens the ring in such a way that the positive charge in the virtual zwitterion resides at N(1) giving rise to the acidic [cf. equilibrium (94)] hydroperoxide 1-hydroperoxymethylen-3-(2-oxo-propanoyl)-urea [reaction (92), (34%)] and to its hydrate 1-(hydroperoxy (hydroxy)methyl)-3-(2-oxopropanoyl)urea [reaction (93), (41%)]. The potential intermediate involved in these reactions is not shown.

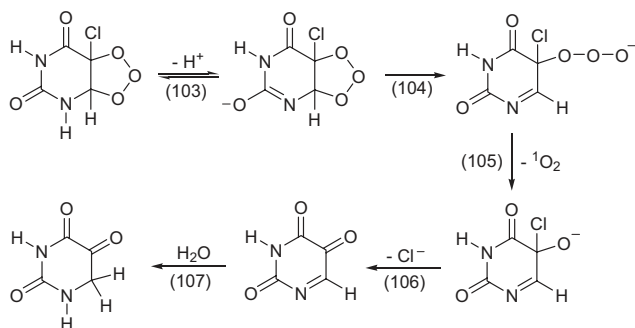


Besides the 75% organic hydroperoxides discussed above, there are 25%  $H_2O_2$  formed in reactions (95)–(97). These hydroperoxides are short-lived and decay largely into 5-hydroperoxy-5-methylhydantoin, which can be reduced by a sulfide into 5-hydroxy-5-methylhydantoin and formic acid [reactions (98)–(102)], while the remaining 1-hydroperoxymethylen-3-(2-oxo-propanoyl)-urea is reduced to *N*-formyl-5-hydroxy-5-methylhydantoin (reaction not shown). Final treatment with base yields 5-hydroxy-5-methylhydantoin and formic acid in 100% yields.



With Thy, singlet oxygen ( $^1O_2$ ) formation, 4% at pH 7 and 8% at pH 8, is marginal but yet a very interesting process. No  $^1O_2$  is detected with the nucleoside, Thyd (Muñoz *et al.*, 2001). This is an

indication that the hydrogen at N1 must be involved. Singlet oxygen formation is much more prominent (45%) with 5-chlorouracil (Table 6.7). For this nucleobase derivative some preliminary data are available (Muñoz *et al.*, 2001) and shed some light on the mechanism. The hydrogen at N1 in the ozonide is most likely acidic [equilibrium (103)].



Subsequent cleavage of the ozonide yielding an isopyrimidine hydrotrioxide [reaction (104)] will be followed by the release of  $^1\text{O}_2$  [reaction (105); for a compilation of  $^1\text{O}_2$  yields in nucleic acid constituents see Table 6.7],  $\text{Cl}^-$  release [reaction (106)] and water addition [reaction (107); for the formation and reactions of isopyrimidines see Al-Sheikhly *et al.* (1984); Schuchmann *et al.* (1984)]. At high pH isodialuric acid and HCl are indeed major products.

**Table 6.7** Singlet oxygen yields (in % of mol  $\text{O}_3$  consumed) in the reaction of ozone with nucleic acid constituents (Muñoz *et al.*, 2001)

Substrate	pH	$^1\text{O}_2$ yield	Molar ratio substrate:ozone
Uracil (Ura)	3.5	No signal	9:1
	7	6	9:1
	11	7	9:1
1,3-Dimethyluracil	3.5	No signal	4:1
	11	No signal	4:1
6-Methyluracil	3.5	No signal	10:1
	7	12	10:1
	10	15	10:1
5-Chlorouracil	3.5	No signal	4:1
	7	45	4:1
	11	43	4:1
Thymine (Thy)	3.5	No signal	4:1
	7	4	4:1
	10	8	4:1
Thymidine (Thyd)	7	No signal	10:1
	10	No signal	4:1

(Continued)

**Table 6.7** Singlet oxygen yields (in % of mol O<sub>3</sub> consumed) in the reaction of ozone with nucleic acid constituents (Muñoz *et al.*, 2001) (*Continued*)

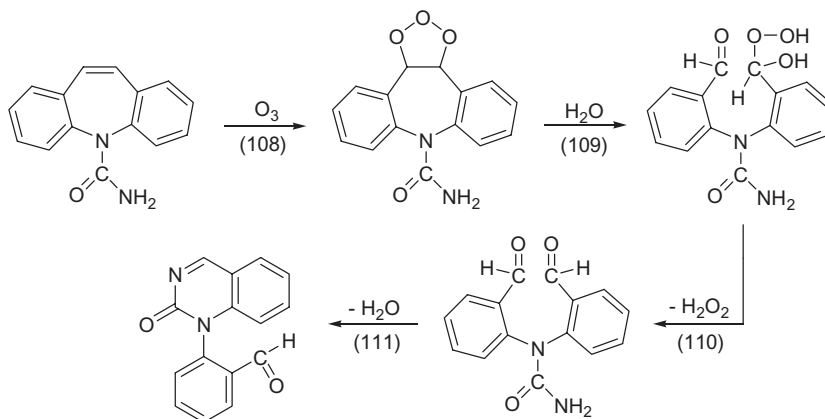
Substrate	pH	<sup>1</sup> O <sub>2</sub> yield	Molar ratio substrate:ozone
Cytosine (Cyt)	7	No signal	16:1
	11	10	16:1
2'-Deoxycytidine (dCyt)	7	No signal	10:1
Cytidine (Cyt)	7	No signal	10:1
2'-Deoxyguanosine (dGuo)	7	40	10:1
Guanosine (Guo)	7	37	1:1
2'-Deoxyadenosine (dAdo)*	7	16	10:1
Adenosine (Ado)*	7	10	1:1
		21	10:1

\*In the presence of tertiary butanol.

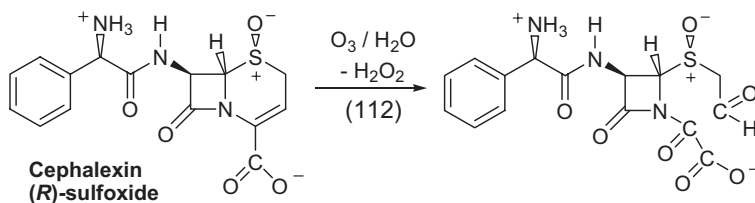
## 6.7 MICROPOLLUTANTS WITH OLEFINIC FUNCTIONS

Chlorinated olefins are abundant micropollutants. Trichloroethene and tetrachloroethene, react too slowly with ozone for an efficient elimination upon ozone treatment (Table 6.1). Their degradation is hence only achieved in DOM containing water by the •OH route (Chapter 3). Mechanistic details are discussed in Chapter 14. Bacterial degradation of the primary chlorinated olefins leads to *cis*-1,2-dichloroethene and to vinyl chloride. In certain ground waters, these secondary pollutants may be of major importance. While *cis*-1,2-dichloroethene also reacts slowly with ozone, vinyl chloride reacts rapidly (Table 6.1), and is degraded by ozone by the pathway shown above.

The high reactivity of the aromatic antiepileptic drug carbamazepine towards ozone (Table 6.1) is due to the reaction of its olefinic C–C double bond [reactions (108)–(111)] (McDowell *et al.*, 2005). In this respect, it shares the cinnamic acids discussed above. The final product, 1-(2-benzaldehyde)-4-hydro(1*H*,3*H*)-quinazoline-2-one reacts only slowly with ozone ( $k = 3 \text{ M}^{-1} \text{ s}^{-1}$ ), and upon ozonation of water and wastewater it is not readily further degraded [for carbamazepine degradation in other water treatment processes such as UV, chlorine dioxide, permanganate and ferrate see Kosiek *et al.* (2009); Hu *et al.* (2009)].



The  $\beta$ -lactam cephalosporin antibiotic cephalixin has two ozone-reactive sites, the sulfide function and a C–C double bond. Both contribute to its ozone-induced degradation. Details are discussed in Chapter 9. The sulfoxides that are formed upon the reaction of ozone continue to react readily with ozone at the C–C double bond, while the sulfoxide function is only of little reactivity (Chapter 9). The reaction of ozone with the cephalixin (*R*)-sulfoxide to the corresponding Criegee product [reaction (112)] takes place to only 30% (Dodd, 2008, 2010).

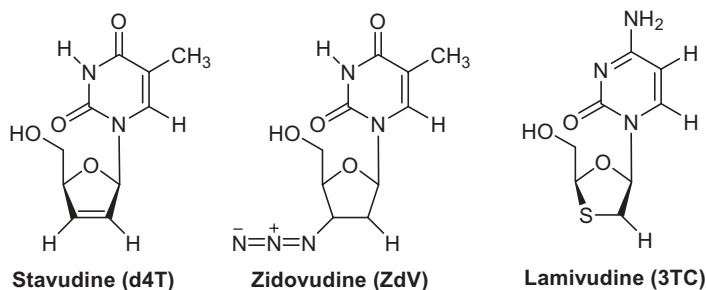


Based on the reactions of acrylic and methacrylic acids discussed above, one would expect that a decarboxylation reaction should occur in competition. The product of this reaction has not yet been identified.

Tylosin, a macrolide antibiotic, has conjugated double bonds and a tertiary amine. The reactivity of the two conjugated C–C double bonds in conjugation with a carbonyl function must be an order of magnitude higher than a single C–C double bond in conjugation with a carbonyl group, as in progesterone, if a comparison of muconic acid with fumaric acid is a good guide (Table 6.1). The reactivity in the pH range relevant for water treatment is mostly controlled by the tertiary amine group (Dodd *et al.*, 2006) and will therefore be discussed in Chapter 8, where the formula of tylosin is also shown.

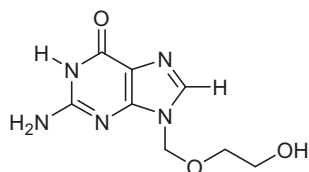
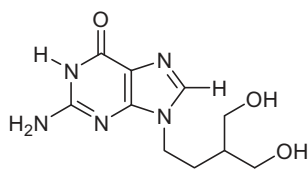
Tetracycline, another antibiotic compound has multiple sites for ozone attack, namely two olefins, a phenolic group and a tertiary amine. In the pH range relevant for water treatment, tetracycline will preferentially react with the phenolic moiety (Dodd *et al.*, 2006a) and will therefore be discussed in Chapter 7, where the formula of tetracycline is also given.

The antiviral drugs stavudine, zidovudine and lamivudine are thymine derivatives. They have been detected in WWTPs (Prasse *et al.*, 2010).

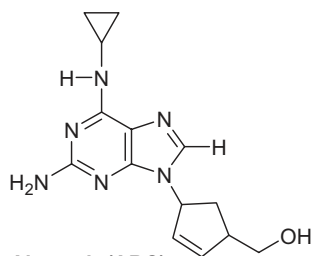


They should be readily eliminated upon ozonation (cf. the rate constant of thymidine in Table 6.1). Stavudine and lamivudine have additional sites for ozone attack, a further C–C double bond and a sulfur, respectively.

The antiviral drugs aciclovir (acyclovir) and penciclovir, also detected in wastewater, belong to the guanine family and with aciclovir ozone rate constants follow closely those of guanine derivatives (Table 6.1). Product formation is due to ozone attack at the C(4)–C(5) double bond (Prasse *et al.*, 2012).

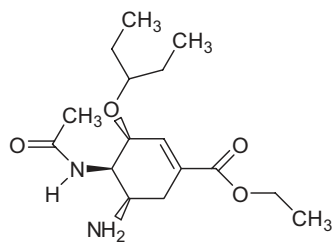
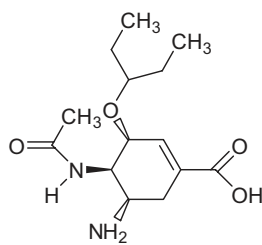
**Aciclovir (AcV)****Penciclovir (PCV)**

The antiviral drug abacavir, also detected in WWTPs (Prasse *et al.*, 2010), belongs to the adenine family.

**Abacavir (ABC)**

Based on this, the ozone reactivity would be poor (cf. the rate constant of adenosine in Table 6.1). But there is also a highly ozone-reactive C–C double bond in the cyclopentene ring, and this guarantees an effective degradation upon ozonation (cf. the rate constant of propene in Table 6.1).

Oseltamivir acid is formed through the human metabolism when Tamiflu<sup>®</sup> (oseltamivir ethylester phosphate) is administered orally. A warning has been expressed that the widespread use of this antiviral drug during an influenza pandemic may lead to an increase in resistance (Singer *et al.*, 2007).

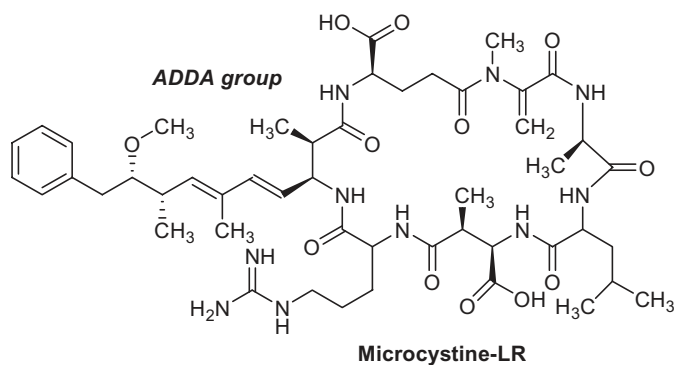
**Oseltamivir****Oseltamivir acid**

The activity of this drug is not markedly decreased in WWTPs (Fick *et al.*, 2007). Its metabolite formed upon hydrolysis of the ester function, oseltamivir acid, is also active and has been detected in WWTP effluents and in rivers during the 2008–09 flu season in Japan (Ghosh *et al.*, 2009). Yet, it is also found in German WWTPs (Prasse *et al.*, 2010). It has been recommended to treat the WWTP effluents with ozone to minimise the risks (Singer *et al.*, 2007). At a wastewater pH of 7–8, oseltamivir acid reacts with ozone mainly at the acrylate function due to its high ozone reactivity (Table 6.1). The nitrogen of the amino group is a second potential site, notably at higher pH. Upon ozonation, antiviral effects disappear proportionally with the degradation of the parent compound. A deviation from this behaviour was observed only for small degrees of transformation (Chapter 4) (Mestankova *et al.*, 2012).

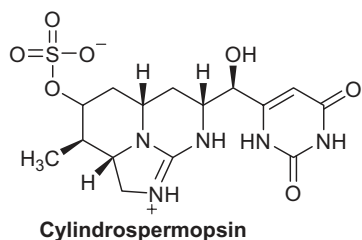
The reactivity of cyanotoxins such as microcystin-LR (MC-LR) is dominated by the ADDA group, a conjugated system of two double bonds (Onstad *et al.*, 2007). When the ADDA group is bonded to the



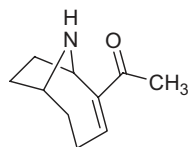
peptidic ring system, it is responsible for the hepatotoxicity of the microcystins. The reaction of ozone with the conjugated double bonds of the ADDA group is fast (Table 6.1). It leads to a cleavage of the ADDA group and hence to a loss of toxicity. In the oxidation of MC-LR by permanganate, the degradation of the parent compound also leads to a loss of its toxicity (Rodríguez *et al.*, 2008). Similar to ozone, it can be assumed from the reactivity of permanganate with olefins that the main site of attack for permanganate is the ADDA group (Waldemer & Tratnyek, 2006; Hu *et al.*, 2009).



Cylindrospermopsin, another cyanotoxin, contains a uracil derivative, which is the active moiety that inhibits protein translation to promote hepatotoxicity or binds to DNA causing strand breakage and genotoxicity (Banker *et al.*, 2001). The main site of attack is the uracil double bond (Onstad *et al.*, 2007), and its ozone chemistry will be similar to that of thymine/thymidine discussed above. Most importantly, the uracil group will be altered significantly which should lead to a loss of the toxic properties of cylindrospermopsin.



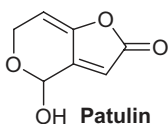
Anatoxin-a is also a cyanotoxin which mimics acetylcholine and over-stimulates muscle cells and may cause paralysis (Carmichael *et al.*, 1979).



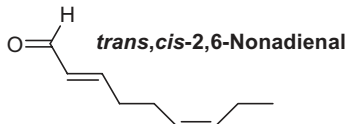
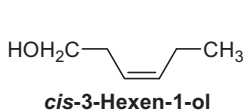
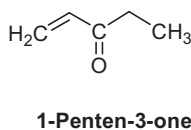
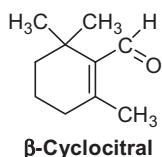
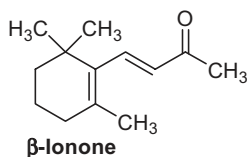
Anatoxin has two functional groups, the amino group and an olefinic function. The reactivity  $pK_a$  of anatoxin-a is 7.88, which means that the olefinic group dominates the reactivity (Table 6.1) for most of

the drinking water relevant pH range (Onstad *et al.*, 2007). The opening of the aliphatic ring caused by a Criegee-type reaction will most likely lead to a loss of anatoxin-a's toxicity.

The mycotoxin patulin is often found in apple juice, and its destruction by ozone has been suggested (Cataldo, 2008). Ozone rate constant and reaction products are as yet not known. The rate constant must be considerably lower than that of  $\beta$ -ionone (Table 6.1), as the carbonyl group in conjugation with the two C–C double bonds withdraws electron density from the sites of ozone attack.

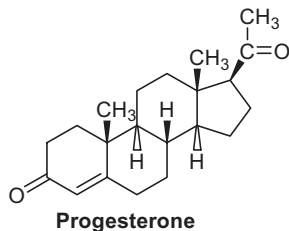
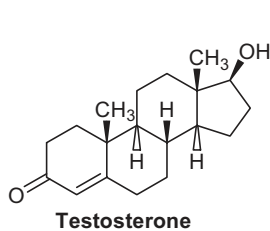


Another class of natural olefin-containing compounds consists of algae derived taste and odour compounds, such as  $\beta$ -ionone,  $\beta$ -cyclocitral, 1-penten-3-one, *cis*-3-hexen-1-ol and *trans,cis*-2,6-nonadienal (for rate constants see Table 6.1; for an overview of taste and odour compounds and their properties see Chapter 5).

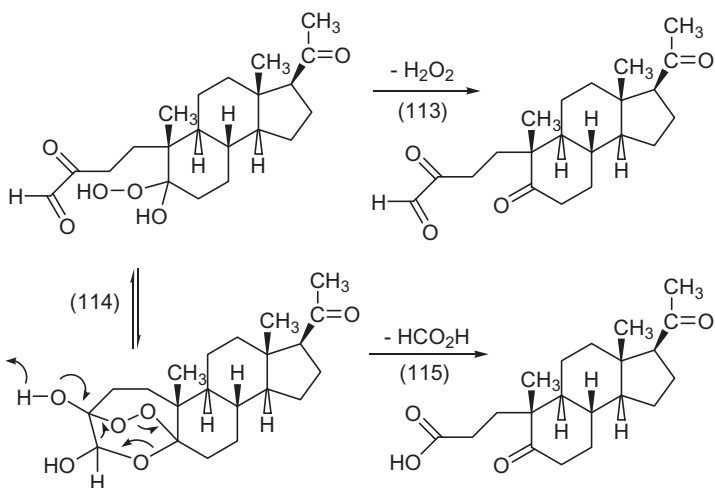


These compounds will react with a Criegee-type reaction, leading to more hydrophilic compounds (Peter & von Gunten, 2007). Since evaporation of these compounds is an important property for their transfer into the cavity of the nose where the odour receptors are, oxidation by ozone is an efficient way to mitigate taste and odour problems caused by olefinic compounds in drinking waters.

The hormones progesterone and testosterone also contain an olefinic group. Progesterone reacts very moderately with ozone (Table 6.1), because of the electron-withdrawing effect of the carbonyl group in conjugation. The reactivity of testosterone is expected to be the same.

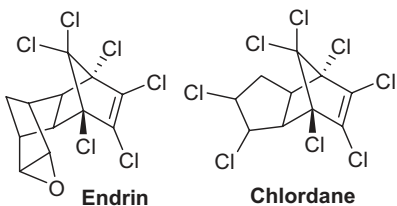


The reaction of ozone leads to a rupture of the 6-membered ring (Barron *et al.*, 2006). This must significantly reduce the biological activity of progesterone and testosterone. Product formation has been studied for progesterone and is shown in reactions (113)–(115) (Barron *et al.*, 2006).



The ozonide (not shown) cleaves the ring leading to aldehyde and hydroxyhydroperoxide functions. The  $\text{H}_2\text{O}_2$  elimination [reaction (113)] is trivial and predominates under the given conditions, but a minor pathway leads to a (well-established) addition of the hydroperoxide to the carbonyl group [equilibrium (114)]. This adduct decomposes after deprotonation of the acidified hydroxyl group [reaction (115)].

The herbicides endrin and chlordane are particularly unreactive towards ozone with respect to its parent *cis*-1,2-dichloroethene (Table 6.1).



This low reactivity has been suggested to be due to a steric hindrance of the C–C double bond on both sides (Yao & Haag, 1991).

# Chapter 7

## Aromatic compounds

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### 7.1 REACTIVITY OF AROMATIC COMPOUNDS

The rate constants of ozone with aromatic compounds vary strongly with the nature of substituents, with ten orders of magnitude between nitrobenzene and phenolate ion (Table 7.1).

**Table 7.1** Compilation of rate constants for the reaction of ozone with aromatic compounds. For nitrogen heterocyclic aromatic compounds and aromatic compounds with nitrogen-containing groups in the side chain see Chapter 8. Published rate constants are rounded to significant figures

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Amidotrizoic acid			<0.8	Huber <i>et al.</i> , 2003
			0.05	Real <i>et al.</i> , 2009
Benzaldehyde			2.5	Hoigné & Bader, 1983b
Benzene			2	Hoigné & Bader, 1983a
Benzenesulfonate			0.23	Yao & Haag, 1991
Benzoate ion			1.2	Hoigné & Bader, 1983b
Bezafibrate			590	Huber <i>et al.</i> , 2003
Bisphenol A	9.6, 10.2		1.7 × 10 <sup>4</sup>	Deborde <i>et al.</i> , 2005
mono-anion			1.1 × 10 <sup>9</sup>	Deborde <i>et al.</i> , 2005
di-anion			1.1 × 10 <sup>9</sup>	Deborde <i>et al.</i> , 2005
Carbofuran			640	Yao & Haag, 1991
Catechol		7	5.2 × 10 <sup>5</sup>	Mvula & von Sonntag, 2003
			3.1 × 10 <sup>5</sup>	Gurol & Nekouinaini, 1984
Chlorobenzene			0.75	Hoigné & Bader, 1983a
2-Chlorophenol	8.3		1100	Hoigné & Bader, 1983b
anion			2 × 10 <sup>8</sup>	Hoigné & Bader, 1983b
4-Chlorophenol	9.2		600	Hoigné & Bader, 1983b
anion			6 × 10 <sup>8</sup>	Hoigné & Bader, 1983b

(Continued)

**Table 7.1** Compilation of rate constants for the reaction of ozone with aromatic compounds. For nitrogen heterocyclic aromatic compounds and aromatic compounds with nitrogen-containing groups in the side chain see Chapter 8. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
2-(4-Chlorophenoxy)-2-methylpropionic acid (Clofibric acid)			<20	Huber <i>et al.</i> , 2005
2-Cresol			1.2 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
3-Cresol			1.3 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
4-Cresol			3 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
1,3-Dichlorobenzene			0.57	Yao & Haag, 1991
1,4-Dichlorobenzene			≪3	Hoigné & Bader, 1983b
2,3-Dichlorophenol	7.7		<2000	Hoigné & Bader, 1983b
2,4-Dichlorophenol	7.8		<1500	Hoigné & Bader, 1983b
anion			~8 × 10 <sup>9</sup>	Hoigné & Bader, 1983b
2,4-Dichlorophenoxyacetic acid (2,4-D)		2	5.3	Xiong & Graham, 1992
Diethyl- <i>o</i> -phthalate			0.1	Yao & Haag, 1991
1,4-Dimethoxybenzene			1.3 × 10 <sup>5</sup>	Muñoz & von Sonntag, 2000a
1,2-Dimethoxytoluene			8.9 × 10 <sup>4</sup>	Ragnar <i>et al.</i> , 1999a
2,3-Dimethylphenol			2.47 × 10 <sup>4</sup>	Gurol & Nekouinaini, 1984
2,4-Dimethylphenol			1.95 × 10 <sup>4</sup>	Gurol & Nekouinaini, 1984
2,6-Dimethylphenol			9.88 × 10 <sup>4</sup>	Gurol & Nekouinaini, 1984
3,4-Dimethylphenol			9.88 × 10 <sup>4</sup>	Gurol & Nekouinaini, 1984
Dimethyl- <i>o</i> -phthalate			0.2	Yao & Haag, 1991
2,6-Di- <i>t</i> -butyl-4-methylphenol (BHT)			7.4 × 10 <sup>4</sup>	Peter & von Gunten, 2007
2,4-Dinitrotoluene		2	<14	Chen <i>et al.</i> , 2008
2,6-Dinitrotoluene		2	<14	Chen <i>et al.</i> , 2008
			5.7	Beltrán <i>et al.</i> , 1998
17 $\alpha$ -Ethinylloestradiol	10.4		1.8 × 10 <sup>5</sup>	Deborde <i>et al.</i> , 2005
anion			3.7 × 10 <sup>9</sup>	Deborde <i>et al.</i> , 2005
			~7 × 10 <sup>9</sup>	Huber <i>et al.</i> , 2003
Ethylbenzene			14	Hoigné & Bader, 1983a
Galaxolide (HHCB)			140	Nöthe <i>et al.</i> , 2007
Gemfibrozil			~2 × 10 <sup>4</sup>	Estimated, see section 7.4
2,2',4,4',5,5'-Hexachlorobiphenyl			<0.9	Yao & Haag, 1991
Hydroquinone		2.6	1.5 × 10 <sup>6</sup>	Gurol & Nekouinaini, 1984
		7	2.3 × 10 <sup>6</sup>	Mvula & von Sonntag, 2003
		3	1.8 × 10 <sup>6</sup>	Mvula & von Sonntag, 2003

(Continued)

**Table 7.1** Compilation of rate constants for the reaction of ozone with aromatic compounds. For nitrogen heterocyclic aromatic compounds and aromatic compounds with nitrogen-containing groups in the side chain see Chapter 8. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Ibuprofen [2-(4-Isobutylphenyl)propionic acid] deprotonated	4.9		7.2	Vel Leitner & Roshani, 2010
			9.6	Huber <i>et al.</i> , 2003
Iomeprol			<0.8	Huber <i>et al.</i> , 2003
Iopamidol			<0.8	Huber <i>et al.</i> , 2003
Iopromide			<0.8	Huber <i>et al.</i> , 2003
Isopropylbenzene			11	Hoigné & Bader, 1983b
Methoxybenzene			290	Hoigné & Bader, 1983a
Methoxychlor			270*	Yao & Haag, 1991
4-Methoxy-1-naphthalenesulfonic acid		7	3.6 × 10 <sup>3</sup>	Benner <i>et al.</i> , 2008
Methylbenzoate			1.1	Hoigné & Bader, 1983b
2-Methyl-4-chlorophenoxyacetic acid (MCPA)		2	11.7	Xiong & Graham, 1992
2-Methyl-4- chlorophenoxypropionic acid (Mecoprop)		2	40	Beltrán <i>et al.</i> , 1994
		7	111	Beltrán <i>et al.</i> , 1994
		2	12.2	Xiong & Graham, 1992
1-Methylnaphthalene			1 × 10 <sup>3</sup>	Legube <i>et al.</i> , 1986
2-Methylphenol	10.2		1.2 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
3-Methylphenol	10.0		1.3 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
Naphthalene			3000 ~1500	Hoigné & Bader, 1983a Legube <i>et al.</i> , 1986
Naproxen			~2 × 10 <sup>5</sup>	Huber <i>et al.</i> , 2005
Nitrobenzene			9 × 10 <sup>-2</sup>	Hoigné & Bader, 1983a
			2.2	Beltrán <i>et al.</i> , 1998
4-Nitrophenol anion	7.2		<50 1.7 × 10 <sup>7</sup>	Hoigné & Bader, 1983b Hoigné & Bader, 1983b
4-N-Nonylphenol	10.7		3.8 × 10 <sup>4</sup>	Deborde <i>et al.</i> , 2005
			3.9 × 10 <sup>4</sup>	Ning <i>et al.</i> , 2007b
anion			6.8 × 10 <sup>9</sup>	Deborde <i>et al.</i> , 2005
4-Octylphenol			4.3 × 10 <sup>4</sup>	Ning <i>et al.</i> , 2007b
17β-Oestradiol	10.4		2.2 × 10 <sup>5</sup>	Deborde <i>et al.</i> , 2005
anion			3.7 × 10 <sup>9</sup>	Deborde <i>et al.</i> , 2005
Oestriol	10.4		1.0 × 10 <sup>5</sup>	Deborde <i>et al.</i> , 2005
anion			3.9 × 10 <sup>9</sup>	Deborde <i>et al.</i> , 2005

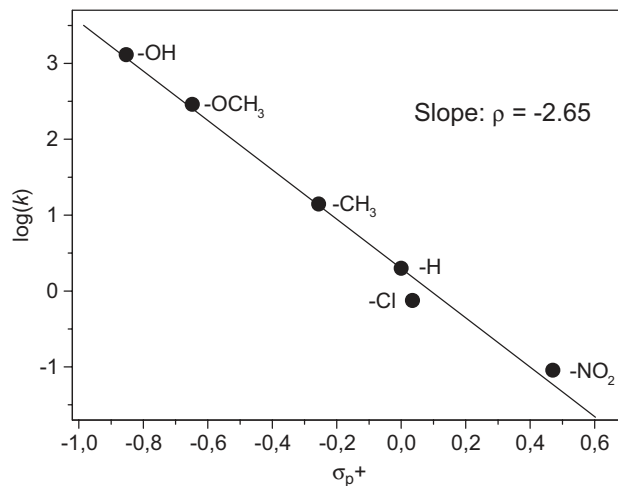
(Continued)

**Table 7.1** Compilation of rate constants for the reaction of ozone with aromatic compounds. For nitrogen heterocyclic aromatic compounds and aromatic compounds with nitrogen-containing groups in the side chain see Chapter 8. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Oestrone	10.4		1.5 × 10 <sup>5</sup>	Deborde <i>et al.</i> , 2005
anion			4.2 × 10 <sup>9</sup>	Deborde <i>et al.</i> , 2005
Paracetamol		2.0	1.4 × 10 <sup>3</sup>	Andreozzi <i>et al.</i> , 2003
		5.5	1.3 × 10 <sup>5</sup>	Andreozzi <i>et al.</i> , 2003
Pentabromophenol anion			1.7 × 10 <sup>6</sup>	Mvula & von Sonntag, 2003
2,3,3',5,6-Pentachlorobiphenyl			<0.05	Yao & Haag, 1991
Pentachlorophenol	4.7			
anion		2	>3 × 10 <sup>5</sup>	Hoigné & Bader, 1983b
			1.2 × 10 <sup>6</sup>	Mvula & von Sonntag, 2003
Phenol	9.9		1300	Hoigné & Bader, 1983b
anion			1.4 × 10 <sup>9</sup>	Hoigné & Bader, 1983b
1-Phenoxy-2-propanol			320	Benner <i>et al.</i> , 2008
Resorcinol	9.8	2	>3 × 10 <sup>5</sup>	Hoigné & Bader, 1983b
Salicylic acid	3.0,13.4		<500	Hoigné & Bader, 1983b
anion			2.8 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
Tetracycline		7	1.9 × 10 <sup>6</sup>	Dodd, 2008
Toluene			14	Hoigné & Bader, 1983a
Tonalide (AHTN)			8	Nöthe <i>et al.</i> , 2007
2,4,6-Tribromoanisole			0.02	Peter & von Gunten, 2007
2,4,6-Trichloroanisole			0.06	Peter & von Gunten, 2007
1,2,3-Trichlorobenzene			<0.06	Yao & Haag, 1991
2,4,5-Trichlorophenol	6.9		<3000	Hoigné & Bader, 1983b
anion			>1 × 10 <sup>9</sup>	Hoigné & Bader, 1983b
2,4,6-Trichlorophenol	6.1		<1 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
anion			>1 × 10 <sup>8</sup>	Hoigné & Bader, 1983b
Triclosan	8.1		1.3 × 10 <sup>3</sup>	Suarez <i>et al.</i> , 2007
		7	3.8 × 10 <sup>7</sup>	Suarez <i>et al.</i> , 2007
anion			5.1 × 10 <sup>8</sup>	Suarez <i>et al.</i> , 2007
2,4,6-Triiodophenol anion			6.8 × 10 <sup>6</sup>	Mvula & von Sonntag, 2003
1,3,5-Trimethoxybenzene			9.4 × 10 <sup>5</sup>	Muñoz & von Sonntag, 2000
3,4,5-Trimethoxytoluene			2.8 × 10 <sup>5</sup>	Dodd <i>et al.</i> , 2006a
1,2,4-Trimethylbenzene			400	Hoigné & Bader, 1983b
1,3,5-Trimethylbenzene			700	Hoigné & Bader, 1983b
Vancomycin		7	6.1 × 10 <sup>5</sup>	Dodd, 2008
<i>m</i> -Xylene			94	Hoigné & Bader, 1983b
<i>o</i> -Xylene			90	Hoigné & Bader, 1983b
<i>p</i> -Xylene			140	Hoigné & Bader, 1983b

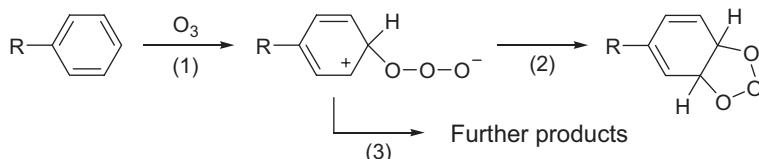
\*Consumption of substrate

In their pioneering work, Hoigné and Bader have shown that the logarithm of the rate constant for the reaction of ozone with substituted benzenes correlates linearly with the  $\sigma_p^+$  values of the substituents (Hoigné & Bader, 1983a). As the  $\rho$  value (slope) of this Hammett-type plot was negative ( $\rho = -3.14$ ), they concluded that in its reaction with benzene and its derivatives, ozone must act as an electrophilic agent. A similar plot with another set of  $\sigma_p^+$  values also including the strongly electron-withdrawing  $\text{NO}_2$  substituent is shown in Figure 7.1 (Naumov & von Sonntag, 2010). Here, the slope ( $\rho = -2.65$ ) is slightly less negative, but such variations are common when using different sets of  $\sigma$  values.



**Figure 7.1** Hammett-type plot for ozone reactions with benzene and its derivatives according to Naumov & von Sonntag, 2010 with permission. Logarithm of the rate constant vs. the  $\sigma_p^+$  values taken from Gordon & Ford, 1972.

The first step in the reaction of ozone with aromatic compounds is the formation of an adduct [reaction (1)].

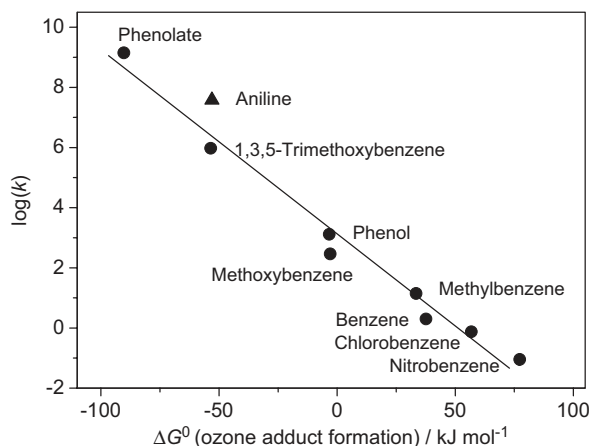


Hammett type plots are based on free energy relationships ( $\Delta G^0 = -\ln K \times RT$ ), and thus the standard Gibbs free energy of the formation of ozone adducts that can be calculated by quantum chemistry (Naumov & von Sonntag, 2010) must also correlate with the logarithm of the rate constant when the transition state is close to the adduct. This is apparently the case (Figure 7.2).

In the case of alkenes and alkynes, the ozone reaction seems to proceed via a concerted cycloaddition to the ozonide and ozone adducts cannot be calculated as intermediates (Chapter 6). In aromatic systems, however, the positive charge that develops upon formation of the ozone adduct [reaction (1)] is distributed over the whole aromatic ring, and a collapse to the ozonide [reaction (2)] is sufficiently retarded to allow an ozone adduct to become a distinct chemical entity (intermediate). This explains why

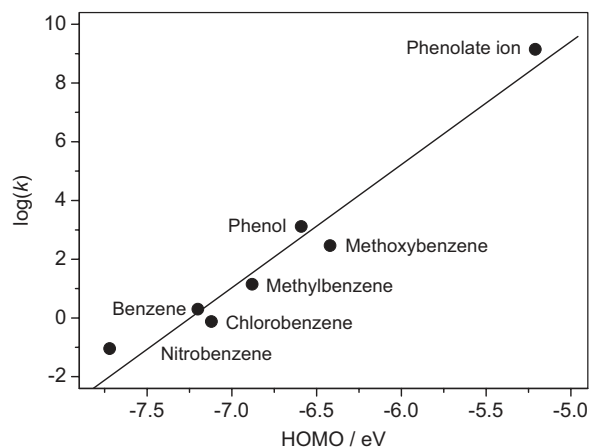


in aromatic compounds there are further reaction pathways [reaction (3)], and the formation of the ozonide [reaction (2)] and its subsequent decay is only one of them.



**Figure 7.2** The logarithm of the rate constant for the reaction of ozone with benzene derivatives vs. the calculated standard Gibbs free energy of adduct formation. Adapted from Naumov & von Sonntag, 2010. The aniline rate constant, possibly somewhat too high, is taken from Tekle-Röttering *et al.*, 2011, the corresponding standard Gibbs free energy was calculated by S. Naumov.

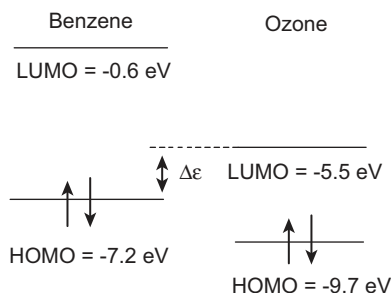
Several correlations with properties of the aromatic compound and the logarithm of the rate constant have been attempted, that is, properties that favour the formation of the adduct. The correlation with the energy of the highest occupied orbital (HOMO, Figure 7.3) comes out best.



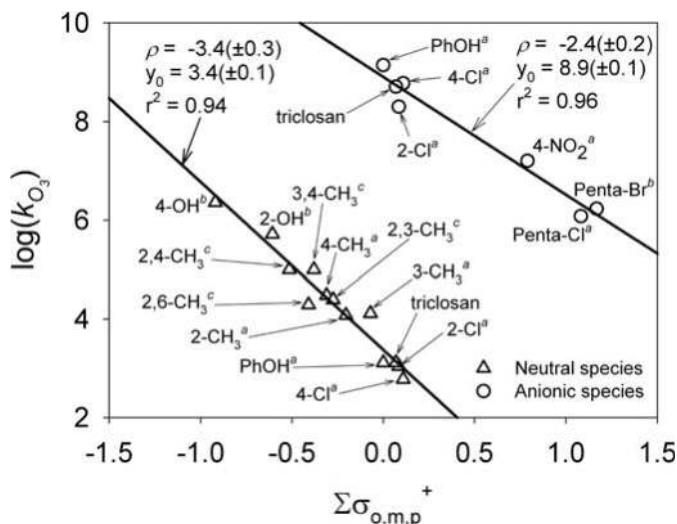
**Figure 7.3** Correlation of the logarithm of the rate constant with the energy of the HOMO. Adapted from Naumov & von Sonntag, 2010, with permission.

According to the chemical reactivity theory of Klopman and Salem (Klopman, 1968; Salem, 1968; Fleming, 2002), the reaction between the reaction partners proceeds in a way to produce the most

favourable interaction energy. This is controlled by two factors, an electrostatic interaction approximated by atomic charges and a frontier orbital interaction. The frontier orbital interaction is the interaction between occupied and unoccupied orbitals on the two interacting molecules. The frontier orbital theory contains the additional assumption that the reaction depends mostly on the interaction between the highest occupied molecular orbital (HOMO) of one reaction partner and the lowest unoccupied molecular orbital (LUMO) of the other (as shown in Figure 7.4 for the interaction of ozone with benzene). The smaller the energy separation ( $\Delta\epsilon$ ) between the HOMO of the donor and the LUMO of the acceptor the larger the interaction between reaction partners should be. With aromatic compounds, the most favourable interaction occurs between the HOMO of aromatic compounds (electron donor) and the LUMO of ozone as the electron acceptor.



**Figure 7.4** MO scheme [B3LYP/6-311G + (d)] of the frontier orbital interaction of benzene with ozone. Due to the small energy difference  $\Delta\epsilon$ , the most favourable interaction takes place between the HOMO of benzene and the LUMO of ozone. This interaction has charge transfer character and leads to a strong shift of negative charge from benzene to ozone (about 0.8 e) according to Naumov & von Sonntag, 2010, with permission.



**Figure 7.5** Correlation of the logarithm of the second order rate constants for the reaction of various phenols and triclosan with ozone with the Hammett coefficients. According to Suarez *et al.*, 2007, with permission.

Aniline has also been included in Figure 7.1. Apparently, its ozone chemistry, as poorly as it is understood at present (Chapter 8), seems to be largely governed by an ozone addition to the ring. The yields of products that require an ozone addition to nitrogen are very minor.

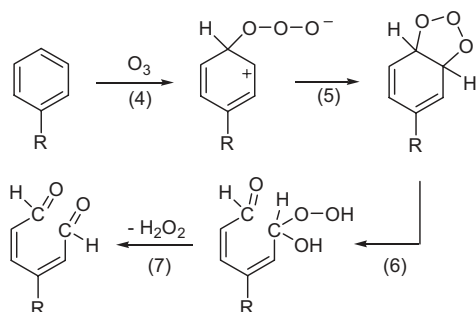
Hammett plots are not only of academic interest; they are of high predictive value since  $\sigma$  values are additive and this allows the estimation of an unknown rate constant. Figure 7.5 demonstrates that the second order rate constant for triclosan (for structure see Paragraph 7.4) could be derived by a Hammett-type correlation with substituted phenols for both the neutral and anionic form. The measured values correspond nicely with the predictions.

In another study, it has been shown for two musk fragrances, with the same molecular weight but different structure, galaxolide and tonalide (for their structures see Paragraph 7.4), that this approach can be successful within a factor of two (Nöthe *et al.*, 2007). While galaxolide has only electron-donating substituents, tonalide also has an electron-withdrawing one, the acetyl group. As a consequence, the ozone reactivity of the latter is much lower (Table 7.1).

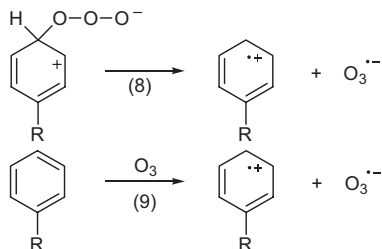
## 7.2 DECAY OF OZONE ADDUCTS

The rate constants for the reaction of benzene and all its mono-substituted derivatives with ozone is  $< 2 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ . Muconic products that arise from the breakdown of the ozonide [cf. reaction (6)] react with rate constants near  $10^4 \text{ M}^{-1} \text{ s}^{-1}$  (Chapter 6). Thus, a detailed study of the primary products is not feasible. Although phenol has a rate constant of only  $1.3 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ , the presence of low phenolate equilibrium concentrations [ $\text{p}K_{\text{a}}(\text{phenol}) = 9.9$ ,  $k(\text{phenolate} + \text{O}_3) = 1.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ] results in the observed rate constant of  $> 1 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$  at pH 7 (for the 'reactivity  $\text{p}K'$ ' see Chapter 2, Figure 2.3). Thus, phenols are good candidates for product studies. Upon substitution with two or more alkoxy groups, the ozone rate constant is also enhanced to an extent, that a study of the primary products can be successful. Thus, our knowledge of the ozonolysis of aromatic compounds can be based only on electron-rich benzene derivatives, phenol (Mvula & von Sonntag, 2003; Ramseier & von Gunten, 2009), and di- and trimethoxybenzenes (Mvula *et al.*, 2009). Here, it must be noted that in these compounds the high electron density in the benzene ring will allow reactions to occur that are not as likely to take place in the parent benzene and in benzene derivatives with electron-withdrawing substituents. With this *caveat* in mind, the ozone chemistry of aromatic compounds is discussed. The key reactions that were observed with such electron-rich aromatic compounds are presented here in general terms and will be substantiated below when discussing real systems.

A reaction that always occurs with aromatic compounds, and is well-documented in the reactions of olefins with ozone, is the formation of an ozonide and its breakdown [reactions (4)–(7)].



This reaction is generally exergonic and will be given by all aromatic compounds. In competition, the ozone adduct may dissociate into a radical cation and an ozonide radical anion [reaction (8)]. This reaction may also proceed directly via an outer sphere electron transfer [reaction (9)].

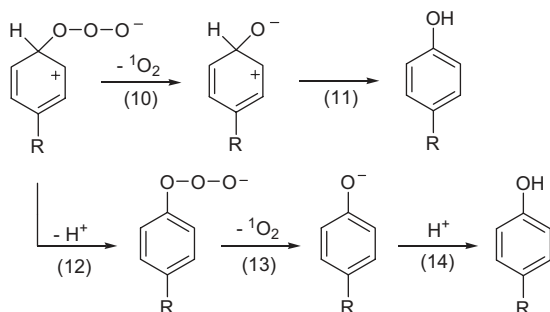


Which of the two processes will dominate depends on the influence of the substituents on the energetics of reactions (4), (8) and (9). For benzene, all these reactions are markedly endergonic (Table 7.2), and no  $\text{O}_3^{\bullet-}$  is expected to be formed. With methoxybenzene, all reactions are exergonic, and the observed formation of  $\bullet\text{OH}$  (via  $\text{O}_3^{\bullet-}$ ) is possible by reaction (4) followed by (8) but also by direct electron transfer [reaction (9)]. With 1,3,5-trimethoxybenzene, reactions (4) and (9) are both exergonic but reaction (8) is endergonic. Here, direct electron transfer [reaction (9)] will be the process resulting in  $\bullet\text{OH}$  formation.

**Table 7.2** Standard Gibbs free energies ( $\text{kJ mol}^{-1}$ ) for the formation of the ozone adduct, its decay into the radical cation and the ozonide radical anion, and the direct electron transfer for benzene, methoxybenzene and 1,3,5-trimethoxybenzene [Naumov and von Sonntag (2009), unpublished]

Starting material	Starting material $\rightarrow$ radical cation + $\text{O}_3^{\bullet-}$	Starting material $\rightarrow$ ozone adduct	Ozone adduct $\rightarrow$ radical cation + $\text{O}_3^{\bullet-}$
Benzene	+58 $\text{kJ mol}^{-1}$	+38 $\text{kJ mol}^{-1}$	+20 $\text{kJ mol}^{-1}$
Methoxybenzene	-12 $\text{kJ mol}^{-1}$	-3 $\text{kJ mol}^{-1}$	-9 $\text{kJ mol}^{-1}$
1,3,5-Trimethoxybenzene	-36 $\text{kJ mol}^{-1}$	-54 $\text{kJ mol}^{-1}$	+18 $\text{kJ mol}^{-1}$

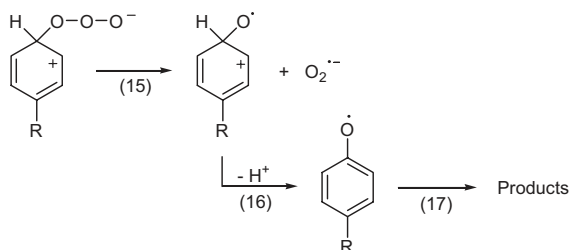
Another process that always occurs is the hydroxylation of the starting material. It may be due to the release of oxygen from the ozone adduct followed by a hydrogen shift [reactions (10) and (11)] or by a re-aromatisation of the zwitterionic ozone adduct by proton loss [reaction (12)]. This aromatic hydrotrioxide anion would then have to lose oxygen [reaction (13)] followed by protonation of the phenolate ion [reaction (14)]. The spin conservation rule demands that oxygen is released in its excited singlet state,  $\text{O}_2(^1\Delta_g)$ , which lies 95.5  $\text{kJ mol}^{-1}$  above the triplet ground state,  $\text{O}_2(^3\Sigma_g^-)$ . For a compilation of singlet oxygen yields in ozone reactions of aromatic compounds see Table 7.3.



**Table 7.3** Singlet oxygen yields in percentage of consumed ozone from the reaction of ozone with aromatic compounds according to (Muñoz *et al.*, 2001). Aniline derivatives, discussed in Chapter 8, are included

Compound	Singlet oxygen yield/%
Phenol pH 1.8	Nil
Phenol pH 7	6
Phenol pH 9	9
Tyrosine pH 7	9
2,4,6-Trimethylphenol pH 9	17
Pentachlorophenol pH 8	58
Pentabromophenol pH 8	48
2,4,6-Triiodophenol pH 9	19
1,4-Dimethoxybenzene	6
1,3,5-Trimethoxybenzene	30
<i>N, N</i> -Dimethylaniline pH 8.5	7
<i>N, N, N', N'</i> -Tetramethylphenylenediamine pH 3.5	9
<i>N, N, N', N'</i> -Tetramethylphenylenediamine pH 6	6

The decay of the ozone adduct into superoxide and phenoxy radicals has also been suggested [reactions (15) and (16)] (Ragnar *et al.*, 1999a, b).



$\text{O}_3^{\cdot-}$  and  $\text{O}_2^{\cdot-}$  are the precursors of  $\cdot\text{OH}$ , which may be formed in substantial yields in ozone reactions with aromatic compounds. Here,  $\text{O}_2^{\cdot-}$  seems to be of a minor importance (see below). The  $\cdot\text{OH}$  radical yield (with respect to ozone consumption) formed in the ozone treatment of wastewater will also arise mainly from such reactions (Chapter 3). Moreover, the hydroxylation process generates further electron-rich aromatic compounds, a requirement for a continuation of  $\cdot\text{OH}$  production at high ozone doses.

Phenols react very rapidly with ozone (Table 7.1), and in the reactions of ozone with aromatic compounds of relatively low reactivity (see above) they can build up to only very low steady-state concentrations and their formation may be difficult to detect.

## 7.3 OZONE REACTIONS OF AROMATIC COMPOUNDS – PRODUCTS AND REACTIONS OF REACTIVE INTERMEDIATES

### 7.3.1 Methoxylated benzenes

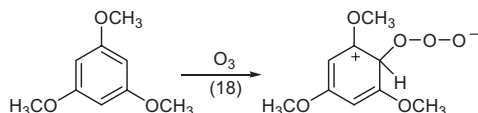
The products and yields formed upon ozonolysis of anisole, 1,2-dimethoxybenzene, 1,4-dimethoxybenzene and 1,3,5-trimethoxybenzene are compiled in Table 7.4. The structures of the products are shown in Figure 7.6.

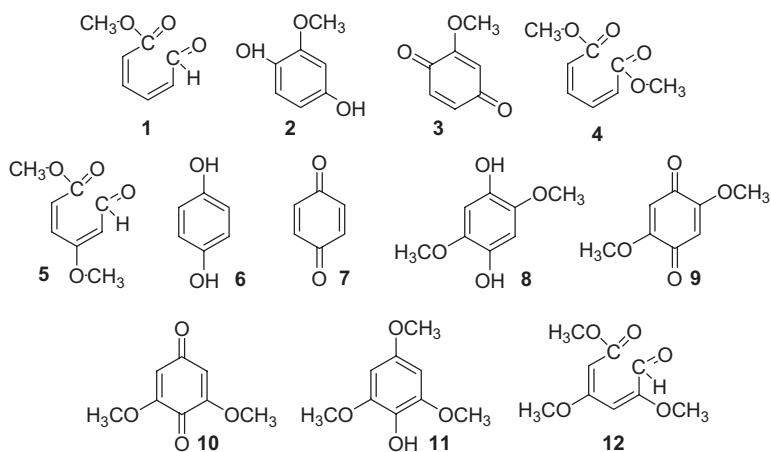
**Table 7.4** Ozonolysis of anisole, 1,2-dimethoxybenzene, 1,4-dimethoxybenzene and 1,3,5-trimethoxybenzene. Products and their yields in percentage of ozone consumed according to Mvula *et al.* (2009). Nitroform anion yields were determined in the presence of tetranitromethane and are an upper limit for  $O_2^{\bullet-}$  yields

Starting material/product	Yield/%
<b>Anisole</b>	
Methyl(2Z,4Z)-6-oxohexa-2,4-dienoate <b>1</b>	identified
2-Methoxyhydroquinone <b>2</b> and/or 2-methoxy-1,4-benzoquinone <b>3</b>	identified
Hydrogen peroxide	23
$\bullet OH$ (estimated)	~8
<b>1,2-Dimethoxybenzene</b>	
Dimethyl-(2Z,4Z)-hexa-2,4-diendioate <b>4</b>	25
Singlet oxygen (Muñoz <i>et al.</i> , 2001)	9
Hydrogen peroxide	27
$\bullet OH$ (estimated)	~14
Nitroform anion	4
<b>1,4-Dimethoxybenzene</b>	
Methyl(2Z,4E)-4-methoxy-6-oxo-hexa-2,4-dienoate <b>5</b>	52
Hydroquinone <b>6</b>	2
1,4-Benzoquinone <b>7</b>	8
2,5-Dimethoxyhydroquinone <b>8</b>	identified
2,5-Dimethoxy-1,4-benzoquinone <b>9</b>	identified
Singlet oxygen (Muñoz <i>et al.</i> , 2001)	6
Hydrogen peroxide	56
$\bullet OH$ (estimated)	~17
Nitroform anion	9
<b>1,3,5-Trimethoxybenzene</b>	
2,6-Dimethoxy-1,4-benzoquinone <b>10</b>	20
2,4,6-Trimethoxyphenol <b>11</b>	identified
(2E,4E)-methyl-3,5-dimethoxy-6-oxohexa-2,4-dienoate <b>12</b>	identified
Singlet oxygen (Muñoz <i>et al.</i> , 2001)	22
Hydrogen peroxide	(6.5)*
$\bullet OH$ (estimated)	~15
Nitroform anion	10

\*see text

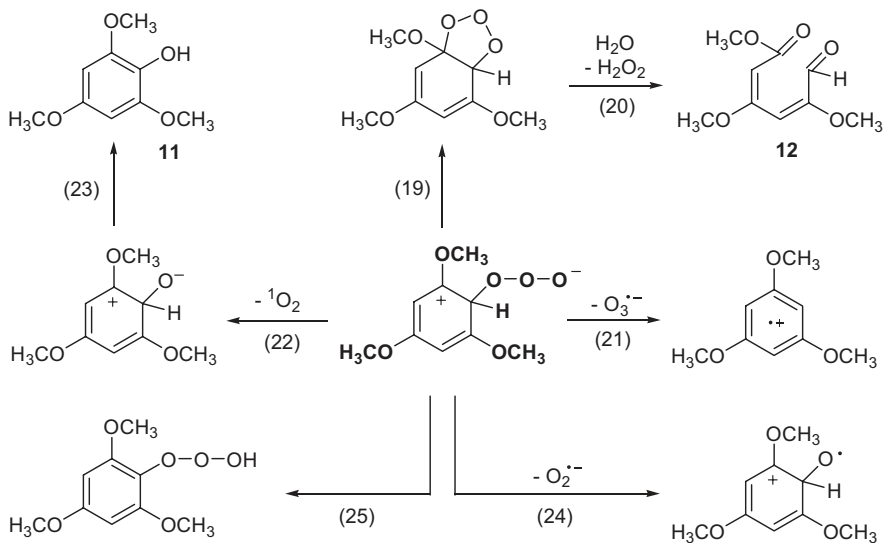
In 1,3,5-trimethoxybenzene, the 2-, 4- and 6-positions are strongly activated, and hence one has to consider practically only one ozone adduct [reaction (18)].



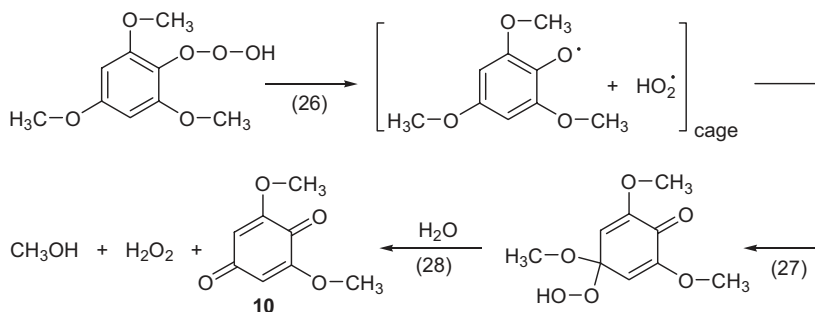


**Figure 7.6** Structures identified in the ozonolysis of anisole (1–3), 1,2-dimethoxybenzene (4), 1,4-dimethoxybenzene (5–9) and 1,3,5-trimethoxybenzene (10–12).

Its ensuing decay routes are discussed in some detail in Mvula *et al.* (2009). Here it suffices to show only the essentials [reactions (19)–(25)], that is, neglecting acid/base equilibria. As in olefins, there is decay into the ozonide [reaction (19)]. This is the precursor of muconic compound **12** [reaction (20)]. In competition, the adduct may release  $O_3^{\bullet-}$  [reaction (21)], the origin of the relatively high  $\bullet OH$  yield ( $O_3^{\bullet-} + H_2O \rightarrow \bullet OH + O_2 + OH^-$ , details in Chapter 11). The release of singlet oxygen [reaction (22)], is connected with a hydroxylation of the aromatic ring [formation of **11**, reaction (23)]. Reaction (24) gives rise to  $O_2^{\bullet-}$  and reaction (25) to a hydrotrioxide.



A major product is quinone **10** (Table 7.4). It has been suggested that it is mainly formed upon the decay of the hydrotrioxide [reactions (26)–(28)]. For the reaction of  $HO_2^{\bullet}/O_2^{\bullet-}$  with phenoxyl radicals [cf. reaction (27)] see Jin *et al.* (1993).



### 7.3.2 Phenols

Phenols react moderately rapidly with ozone, but the reaction of their anions is close to diffusion controlled (Table 7.1). With  $\text{p}K_a(\text{phenol}) = 9.9$ , the rate of reaction observed at pH 7 is hence determined by the reaction of the phenolate anion in equilibrium (Chapter 2). Nevertheless, the product yields listed in Table 7.5 for pH 6–7 and for pH 10 are markedly different in many cases and must be due to different decay routes of the primary ozone adduct at these two different pH conditions.

**Table 7.5** Ozonolysis of phenol. Products and their yields in percentage of ozone consumed. In several experiments, tertiary butanol (tBuOH) was added for scavenging  $\bullet\text{OH}$  radicals. When more than one value is given, further runs at four or five different ozone concentrations were carried out Mvula & von Sonntag (2003)

Product (Scavenger)	$\leq \text{pH } 3$	pH 6–7	pH 10
Hydroquinone	1.6/1.1 <sup>(a)</sup>	13.3/16	0.8
Hydroquinone (tBuOH)	ND	<1	ND
Catechol	4.8/1.8 <sup>(a)</sup>	13.6	20
Catechol (tBuOH)	ND	2	ND
1,4-Benzoquinone	9.6/10.4/6.1 <sup>(a)</sup>	4.6/4.6	32
1,4-Benzoquinone (tBuOH)	ND	13	ND
<i>cis,cis</i> -Muconic acid	4.8/4.0/3 <sup>(a)</sup>	2.8	1
<i>cis,cis</i> -Muconic acid (tBuOH)	ND	2.0	ND
4,4'-Dihydroxybiphenyl	ND	ND	~1
2,4'-Dihydroxybiphenyl	ND	ND	~1
Singlet dioxygen	absent	5.6	8
$\bullet\text{OH}$ (estimated)	20/22	28/26/24	22
Nitroform anion (TNM)	3	ND	ND
Organic (hydro)peroxide	ND	absent	ND
Organic (hydro)peroxide (tBuOH)	ND	2.6	ND
Hydrogen peroxide	8.5	4.8	2
Hydrogen peroxide (tBuOH)	ND	16	ND
Hydrogen peroxide (DMSO)	ND	13	ND
Phenol consumption	33 <sup>(a)</sup>	48 <sup>(a)</sup>	59 <sup>(a)</sup>
Phenol consumption (tBuOH)	ND	42 <sup>(a)</sup>	ND

<sup>(a)</sup>[Phenol] =  $2.5 \times 10^{-4}$  M, ND = not determined, TNM = tetranitromethane, DMSO = dimethyl sulfoxide.

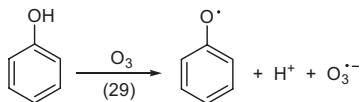


There is further study on phenol ozonolysis (Table 7.6) (Ramseier & von Gunten, 2009). There, product yields were given in percentage of phenol consumed, while in Table 7.5 product yields are based on ozone consumed.

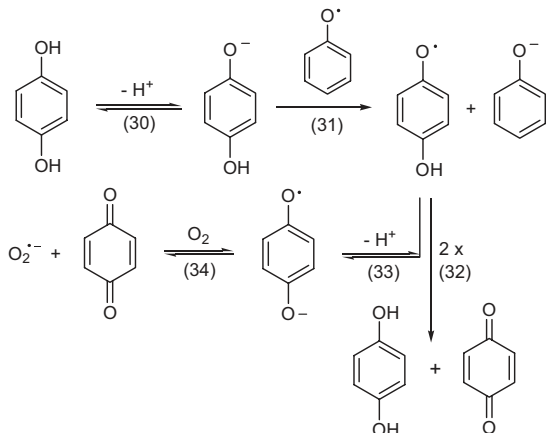
**Table 7.6** Ozonolysis of phenol (200  $\mu\text{M}$ ). Products and their yields in percentage of phenol consumed. Reactions of  $\cdot\text{OH}$  were suppressed by tBuOH addition. According to Ramseier & von Gunten (2009)

Product	pH 3	pH 7
1,4-Benzoquinone	17/18	40/35
Hydroquinone	4/7	0/2
Catechol	0/1	27/33
<i>cis,cis</i> -Muconic acid	2/3	5/6

The values in Table 7.6 are necessarily higher than those of Table 7.5, since phenol consumption by ozone is substantially lower than unity (Table 7.5). This effect is also pH dependent. Moreover, for the presence of tBuOH, data are partially missing in Table 7.5 to allow a detailed comparison of the two data sets. The contribution of  $\cdot\text{OH}$  in these ozone-induced reactions cannot be neglected as its yield is near 20–25% (Table 7.5). The formation of  $\cdot\text{OH}$  (via  $\text{O}_3^{\cdot-}$ ) is balanced by an equivalent amount of phenoxyl radicals [reaction (29)].



The reduction potential of phenol at pH 7 is 860 mV (Wardman, 1989). This may be compared with the corresponding reduction potentials of hydroquinone (549 mV) and catechol (530 mV). Hydroquinone and catechol are formed in hydroxylation reactions such as those depicted in reactions (10)–(14). The reduction potential of the peroxy radical derived from tBuOH must be near 800 mV under such conditions (Chapter 14). Thus, notably hydroquinone is further oxidised in an ensuing electron transfer reaction [reactions (30) and (31)] and subsequent disproportionation [reaction (32)]. An electron transfer to  $\text{O}_2$  is endergonic [reduction potential of 1,4-benzoquinone is 400 mV (Wardman, 1989), for  $\text{O}_2^{\cdot-}$  see Chapter 2]. Yet, when  $\text{O}_2^{\cdot-}$  is drawn out of equilibrium (34) the reaction may proceed nevertheless.



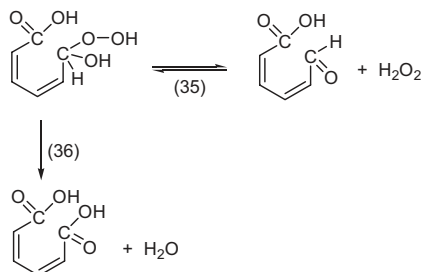
With hydroquinone as substrate, the yield of 1,4-benzoquinone is markedly enhanced in the presence of tBuOH and the data shown in Table 7.7 are supported by the study of Ramseier & von Gunten (2009), which gives a hydroquinone consumption related value of 83% at pH 7 and 52–61% at pH 3. The corresponding oxidation product of catechol, 1,2-benzoquinone, is unstable and would escape detection (cf. Table 7.8).

**Table 7.7** Ozonolysis of hydroquinone (1 mM). Products and their yields in percentage of ozone consumed in absence and presence of tBuOH, added for scavenging  $\cdot\text{OH}$  (Mvula & von Sonntag, 2003)

Product	Yield
1,4-Benzoquinone	13/12
1,4-Benzoquinone (t-BuOH)	36/32
1,4-Benzoquinone (DMSO)	30
2-Hydroxy-1,4-benzoquinone	11
2-Hydroxy-1,4-benzoquinone (tBuOH)	<1
2-Hydroxy-1,4-benzoquinone (DMSO)	<1
1,2,4-Trihydroxybenzene	absent
Singlet dioxygen	16
Hydrogen peroxide	5.6
Hydrogen peroxide (tBuOH)	14
Hydrogen peroxide (DMSO)	10.4
Organic (hydro)peroxides	absent
Organic (hydro)peroxides (tBuOH)	1.9
Formaldehyde	absent
Formaldehyde (tBuOH)	21/20
2-Hydroxy-2-methylpropionaldehyde	absent
2-Hydroxy-2-methylpropionaldehyde (tBuOH)	23
Methanesulfinic acid (DMSO)	6
Methanesulfonic acid (DMSO)	27
Hydroquinone consumption	47 <sup>(a)</sup>
Hydroquinone consumption (tBuOH)	48 <sup>(a)</sup>

<sup>(a)</sup>[Hydroquinone] =  $2.5 \times 10^{-4}$  M, TNM = tetranitromethane, DMSO = dimethyl sulfoxide.

*cis,cis*-Muconic acid is formed via the ozonide [cf. reaction (4)–(6)]. The hydroxyhydroperoxide that must be the intermediate typically loses  $\text{H}_2\text{O}_2$  [reaction (35)], but here a water elimination is observed [reaction (36)]. This has been attributed to the fact that reaction (35) is reversible, while reaction (36) is not (Mvula & von Sonntag, 2003).



**Table 7.8** Ozonolysis of catechol (1 mM). Products and their yields in % of ozone consumed (Mvula & von Sonntag, 2003)

Product	Yield
2-Hydroxy-1,4-benzoquinone	7.4
1,2,4-Trihydroxybenzene	absent
<i>cis,cis</i> -Muconic acid	7/10
Singlet dioxygen	14
Hydrogen peroxide	5.1
Hydrogen peroxide (DMSO)	7.2
Organic (hydro)peroxides	absent
Formaldehyde	absent
Formaldehyde (tBuOH)	11
Methanesulfinic acid (DMSO)	absent
Methanesulfonic acid (DMSO)	22
Catechol consumption	47 <sup>(a)</sup>

<sup>(a)</sup>[Catechol] =  $2.5 \times 10^{-4}$  M, TNM = tetranitromethane, DMSO = dimethyl sulfoxide.

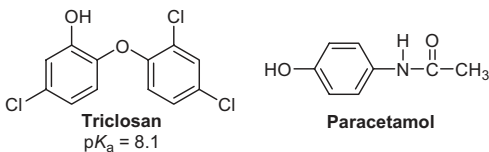
This implies that other  $\alpha$ -hydroxyalkylhydroperoxides may also show water elimination, albeit on a much longer time scale. The efficiency of such a process will depend on the relative rates of such reactions.

## 7.4 MICROPOLLUTANTS WITH AROMATIC FUNCTIONS

Many micropollutants contain a benzene ring. This may be the site of ozone attack, but as most aromatic compounds react only slowly with ozone unless substituted by –OH and –OR functions, other ozone-reactive sites may dominate the reaction. Here, we deal only with those micropollutants whose reactivity is dominated by the aromatic ring. The aromatic micropollutant may contain an olefinic side chain, a nitrogen or a sulfur (even aniline derivatives) and these are discussed in Chapters, 6, 8 and 9, respectively.

Micropollutants that contain a phenolic function react very rapidly with ozone, because these phenols are in equilibrium with the phenolate which has a very high ozone rate constant, and it is the phenolate in equilibrium that determines their rate of degradation, notably in drinking water and wastewater which typically has a pH between 7 and 8.

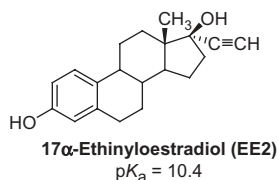
Triclosan is widely applied in personal care products such as soaps and toothpastes due to its antibacterial properties. Paracetamol is a common painkiller.



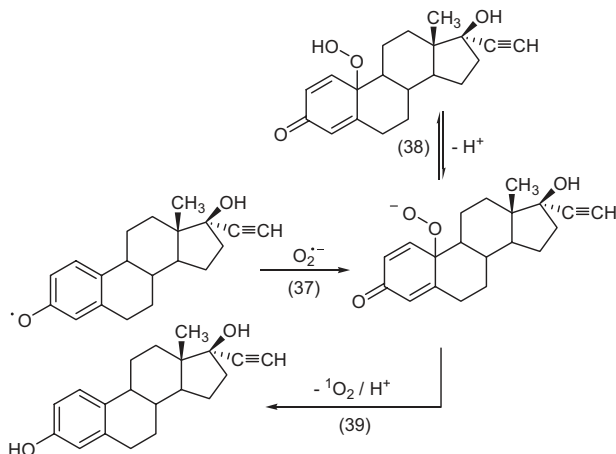
Triclosan can be found in wastewater effluents in concentrations of up to  $200 \text{ ng L}^{-1}$  (Singer *et al.*, 2002). Its high second-order rate constant at pH 7 (Table 7.1) is due to the lower  $pK_a$  value of the phenol as compared to unsubstituted phenol. With the parent phenol (see above), triclosan shares a low consumption per ozone reacted (0.41) (Suarez *et al.*, 2007). Its reaction with ozone leads to a complete loss of its antibacterial properties (Chapter 4). For paracetamol, a series of degradation products are

reported that are in line with the discussed mechanisms for the reaction of ozone with phenols (Andreozzi *et al.*, 2003).

17 $\alpha$ -Ethinylestradiol is an artificial oestrogen, and, due to its abundant use as contraceptive, it can be found in the effluents of many WWTPs (Chapter 4).

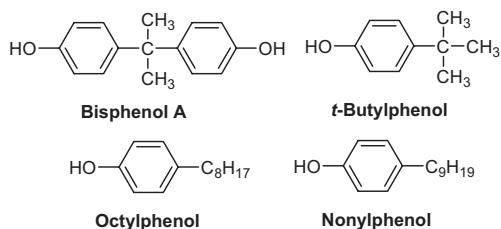


Its ozonolysis has been investigated in some detail (Huber *et al.*, 2004), and the observation has been made that some time after the ozone treatment about 3% of the 17 $\alpha$ -ethinylestradiol destroyed is regenerated. In ozone reactions, phenoxyl radicals and O<sub>2</sub><sup>-</sup> can be generated side by side (see above), and cage recombination can lead to a hydroperoxide (d'Alessandro *et al.*, 2000) [reactions (37) and (38)].



This must be far less ozone reactive than the phenol/phenolate system and escapes subsequent ozonolysis at moderate ozone doses. Out of equilibrium (38), <sup>1</sup>O<sub>2</sub> is slowly eliminated [reaction (39)] regenerating the starting material. Complete mineralisation of 17 $\alpha$ -ethinylestradiol as discussed by Beltrán *et al.*, (2009) is not required for elimination of its oestrogenic activity (Chapter 4).

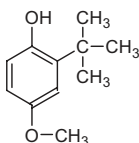
Most common phenolic micropollutants are bisphenol A, *t*-butylphenol as well as octyl- and nonylphenols (cf. Chapter 4).



Most of the bisphenol A is used for the production of polycarbonate and epoxy resins, flame retardants and other speciality products (Staples *et al.*, 1998). Bisphenol A is often detected in surface waters (Kolpin

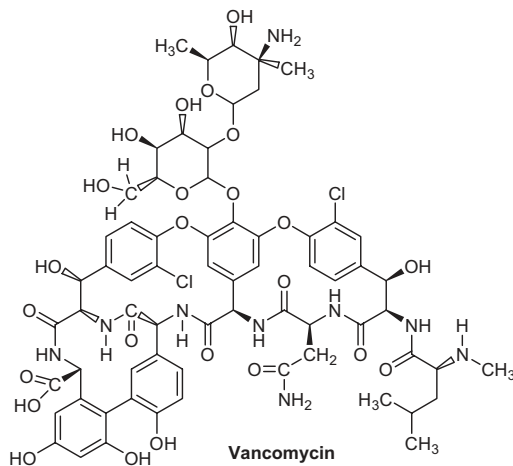
*et al.*, 2002). The transformation of bisphenol A by ozone leads to the expected products as described by the ozone-phenol reactions discussed above (Deborde *et al.*, 2008). Alkyl phenols are degradation products of the alkylphenolethoxylates. These tensides are produced worldwide at 650,000 t/a, 90% of which are nonylphenolethoxylates. The technical product is a mixture of many isomers the distribution of which depends on the manufacturing process (Günther, 2002) (see also Chapter 4).

2-*t*-Butyl-4-methoxyphenol (“butylated hydroxyanisol”) (Lau *et al.*, 2007) is a commonly used antioxidant additive in food. It has some endocrine properties and has been found in river waters in Italy as the most abundant phenolic compound (Davi & Gnudi, 1999). Its degradation by ozone has found some attention (Lau *et al.*, 2007).



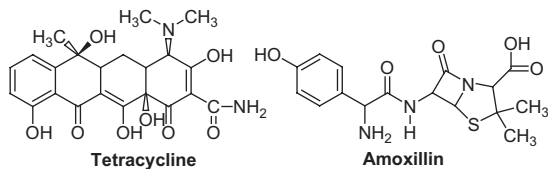
**2-*t*-Butyl-4-methoxyphenol**

The ozone chemistry of the antibiotic vancomycin may be largely governed by an attack at the phenolic moieties, but there is also a secondary amino group that can serve as an additional site of ozone attack (for a rate constant see Table 7.1). A single ozone attack destroys its biological activity (Dodd, 2008).



**Vancomycin**

There are further antibiotics containing a phenolic function, tetracycline and amoxillin (for rate constants see Table 7.1). Their biological activity is destroyed by a single ozone attack (Dodd, 2008) (Chapter 4).



**Tetracycline**

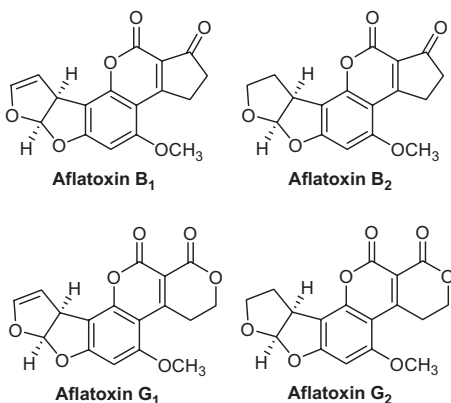
**Amoxillin**

Tetracycline has several ozone-reactive sites, namely a phenolic ring, enolic functions and an exocyclic tertiary amino group. The  $pK_a$  values for the tertiary amine and the phenol groups are at 7.7 and 9.7,

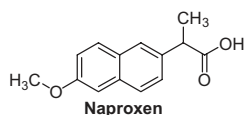
respectively. Details of the preferred sites of attack as a function of pH are not fully established, but these functions and the enolic groups are obvious candidates.

Amoxicillin has three ozone-reactive sites, the phenol, amine and sulfide groups. It has  $pK_a$  values at 2.68 (carboxylic acid), 7.49 (amine) and 9.68 (phenol). Rate constants as a function of pH have not been reported, but it is most likely that at the pH values relevant for water ozonation, amoxicillin degradation by ozone is largely governed by reactions with the deprotonated phenol site in equilibrium (Andreozzi *et al.*, 2005). The amine (Chapter 8) and sulfide (Chapter 9) sites would react more slowly.

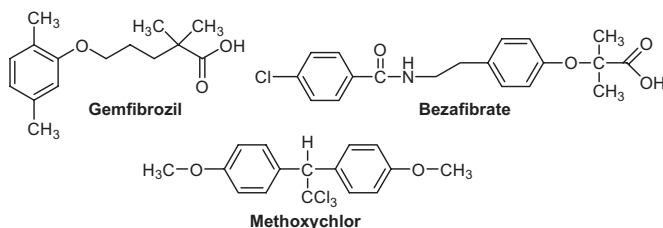
Aflatoxins belong to the group of mycotoxins which are produced by a number of fungi such as *Aspergillus*, *Penicillium* and *Fusarium*. The structures of the most abundant ones are shown below. Their aromatic rings carry strongly electron-donating substituents, that is, their rate constants toward ozone must be high, most likely close to that of 1,3,5-trimethoxybenzene (Table 7.1). As a consequence, they are readily degraded (detoxified) by ozone (McKenzie *et al.*, 1997). Their olefinic functions are all deactivated by electron-withdrawing substituents (Chapter 6), and thus their contributions to detoxifications by ozone are expected to be minor.



Naphthalene sulfonic acid derivatives are used as textile auxiliaries. Some aspects of their degradation by ozone have been addressed (Babuna *et al.*, 2009). The reaction of ozone with such compounds is moderately fast, near  $10^3 \text{ M}^{-1} \text{ s}^{-1}$ , if the parent, naphthalene, is a good guide (Table 7.1). Naxopren is an antiphlogistic pharmaceutical with a naphthalene moiety, additionally activated by a methoxy and an alkyl group. This leads to a marked enhancement of the rate constant (Table 7.1) (Huber *et al.*, 2005).

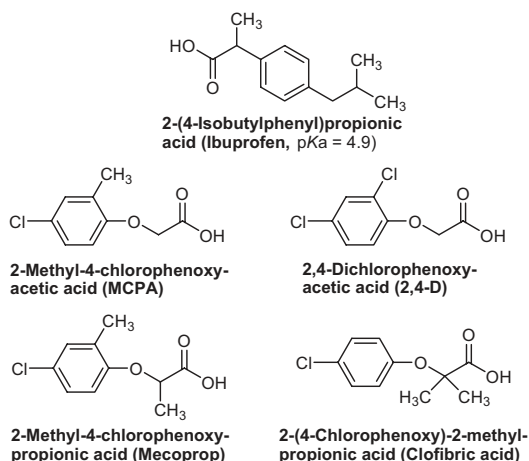


The lipid-lowering drug gemfibrozil contains a benzene ring that is activated by two alkyl and one alkoxy groups. Its ozone rate constant has been estimated to  $\sim 2 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ , by quantitative structure–activity relationship (QSAR) (Lee & von Gunten, 2012), which lies between naxopren and bezafibrate (Table 7.1). The herbicide methoxychlor also belongs to the group of aromatic compounds activated by alkoxy groups.



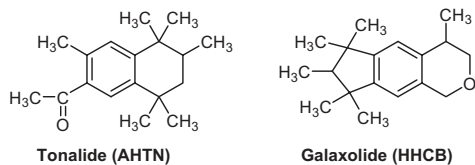
Bezafibrate has two aromatic rings. One carries one alkyl and one alkoxy group, while the other is deactivated by the chlorine and amide substituents. The ozone attack is expected to occur preferentially on the alkyl-/alkoxy-activated benzene ring. There is a host of products; muconic and hydroxylated ones seem to dominate (Dantas *et al.*, 2007).

When the number of activating substituents is decreased and/or deactivating substituents such as chlorine are present, the rate of reactions drops substantially (Paragraph 7.1). The analgesic ibuprofen reacts very slowly indeed as do the herbicides MCPA, 2,4-D, mecoprop and clofibric acid (Table 7.1) [for reviews on the degradation of herbicides by ozone and AOPs see Ikehata & El-Din (2005a); Ikehata & El-Din (2005b)].



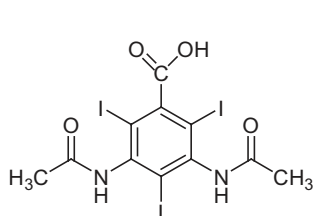
With clofibrate, the chloride yield is near 40% of ozone consumption [Sein *et al.*, (2006), unpublished results]. Ozone-refractory chlorinated products do not seem to be uncommon, as with 4-chlorophenol incomplete chloride release is also observed (Andreozzi & Marotta, 1999).

The musk fragrances galaxolide and tonalide have the same molecular weight but differ markedly in their ozone rate constants (Table 7.1).

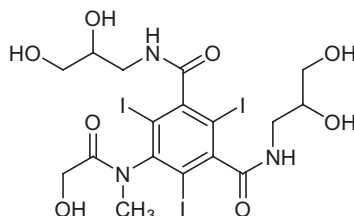


The reason for this has been discussed above. In a bubble column, the disappearance of the less reactive one, tonalide, is partly due to stripping effects (Nöthe *et al.*, 2007).

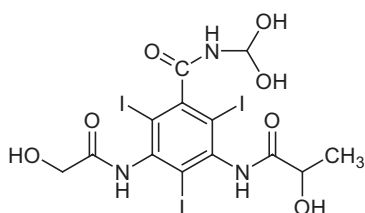
X-ray contrast media such as amidotrizoic acid, iomeprol, iopamidol and iopromide are abundant micropollutants (Schulz *et al.*, 2008). All contain a benzene ring with three iodine substituents to provide the x-ray response and further hydrophilic substituents to guarantee high water solubility.



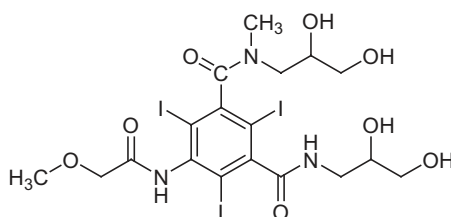
Amidotrizoic acid



Iomeprol



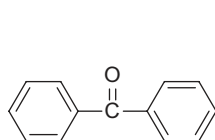
Iopamidol



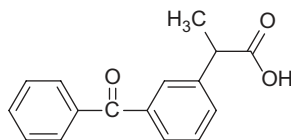
Iopromide

All substituents are electron-withdrawing, and thus their ozone rate constants are all  $<0.8 \text{ M}^{-1} \text{ s}^{-1}$  (Table 7.1). This agrees with a more recent iomeprol study (Seitz *et al.*, 2006). Upon ozone treatment of wastewater, they are only eliminated via the  $\bullet\text{OH}$  route. Therefore high doses of ozone are required for their elimination (Chapter 3). They share this problem with activated carbon. Here, a high dosage of powdered activated carbon is required for the adsorption of these highly water-soluble compounds (Nowotny *et al.*, 2007) (for GAC data see (Seitz *et al.*, 2006).

Benzophenone is used for protection against UV radiation in perfumes, soaps, colours and plastic packaging material. Its ozone rate constant must be similarly low as that of the structurally related analgesic ketoprofen [ $k = 0.4 \text{ M}^{-1} \text{ s}^{-1}$ , Real *et al.* (2009)].

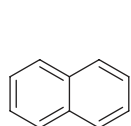


Benzophenone

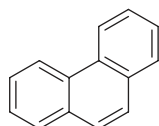


Ketoprofen

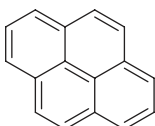
Polycyclic aromatic compounds are poorly soluble in water (Schwarzenbach *et al.*, 2010) and are not expected to play a major role as contaminants in water. Typical examples are naphthalene (Legube *et al.*, 1983, 1986), phenanthrene, pyrene, benzo[a]pyrene and the chlorinated biphenyls.



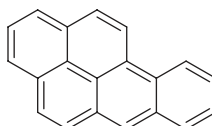
Naphthalene



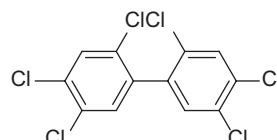
Phenanthrene



Pyrene



Benzo[a]pyrene

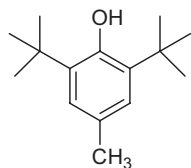


2,2',4,4',5,5'-Hexachloro-biphenyl

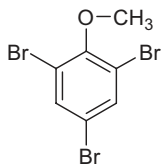


Ozone rate constants with polycyclic aromatic compounds are high [for naphthalene see Table 7.1; missing in this table are the rate constants for phenanthrene ( $k = 1.5 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ), pyrene ( $k = 4 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ ) and benzo[a]pyrene ( $k = 6 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ ) reported by Butković *et al.* (1983)].

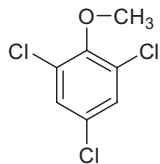
Of the aromatic taste and odour compounds (Peter & von Gunten, 2007), only 2,6-di-*t*-butyl-4-methylphenol (BHT), leached from polyethylene pipes, reacts rapidly with ozone, while 2,4,6-tribromoanisole and 2,4,6-trichloroanisole, derived by methylation from the corresponding phenols by micro-organisms, are practically ozone-refractory (Table 7.1).



**2,6-Di-*t*-butyl-4-methylphenol (BHT)**



**2,4,6-Tribromoanisole (TBA)**



**2,4,6-Trichloroanisole (TCA)**

For their taste and odour properties see Chapter 5.

# Chapter 8

## Nitrogen-containing compounds

### 8.1 REACTIVITY OF NITROGEN-CONTAINING COMPOUNDS

For aliphatic amines to be ozone-reactive, the lone electron pair at nitrogen has to be accessible. Protonation of aliphatic amines or complexation of the nitrogens as in Fe(III)–EDTA or Fe(III)–DTPA eliminates the ozone reactivity or at least strongly reduces it (Table 8.1).

**Table 8.1** Compilation of ozone rate constants of nitrogen-containing compounds in aqueous solution. Rate constants for sulfur-containing amino acids are given in Chapter 9. Published rate constants are rounded to significant figures

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Acebutolol	9.2		2.9 × 10 <sup>5</sup>	Benner <i>et al.</i> , 2008
		7	1.9 × 10 <sup>3</sup>	Benner <i>et al.</i> , 2008
protonated			60	Benner <i>et al.</i> , 2008
N-Acetylglycine		3.7	0.3	Pryor <i>et al.</i> , 1984
N-α-Acetylhistidine	7.3		8.4 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
N-α-Acetyllysine	10.5		1.0 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
N-ε-Acetyllysine	9.46		2.4 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
protonated			no reaction	Pryor <i>et al.</i> , 1984
N-(4)-Acetylsulfamethoxazole	5.5		260	Dodd <i>et al.</i> , 2006a
protonated			20	Dodd <i>et al.</i> , 2006a
Alachlor			3.4	de Laat <i>et al.</i> , 1996
Alanine	9.87		6.4 × 10 <sup>4</sup>	Hoigné & Bader, 1983b
			7.6 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
			2.8 × 10 <sup>4</sup>	Muñoz & von Sonntag, 2000b
protonated			no reaction	Pryor <i>et al.</i> , 1984
			~3 × 10 <sup>-3</sup>	Hoigné & Bader, 1983b
β-Alanine			6.2 × 10 <sup>4</sup>	Hoigné & Bader, 1983b

(Continued)

**Table 8.1** Compilation of ozone rate constants of nitrogen-containing compounds in aqueous solution. Rate constants for sulfur-containing amino acids are given in Chapter 9. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Amikacin	6.7, 8.4 8.4, 9.7	7	1.8 × 10 <sup>3</sup>	Dodd, 2008
4-Aminophenylmethyl sulfone			4.7 × 10 <sup>4</sup>	Dodd <i>et al.</i> , 2006a
Ammonia	9.24		20	Hoigné & Bader, 1983b
			44	Garland <i>et al.</i> , 1980
protonated			no reaction	Hoigné & Bader, 1983b
Aniline	4.63		9.0 × 10 <sup>7</sup>	Hoigné & Bader, 1983
			3.8 × 10 <sup>7</sup>	Tekle-Röttering <i>et al.</i> , 2011
		6.5	1.4 × 10 <sup>7</sup>	Pierpoint <i>et al.</i> , 2001
		1.5	5.9 × 10 <sup>4</sup>	Pierpoint <i>et al.</i> , 2001
Arginine	8.99		5.7 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
Asparagine monoanion	2.0, 8.8		4.2 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
Aspartate ion	9.82		4.1 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
protonated			1.0	Pryor <i>et al.</i> , 1984
Atenolol	9.6		6.3 × 10 <sup>5</sup>	Benner <i>et al.</i> , 2008
protonated			110	Benner <i>et al.</i> , 2008
Atrazine		2	24	Yao & Haag, 1991
			2.3	Xiong & Graham, 1992
			5.65	de Laat <i>et al.</i> , 1996
			6.0	Acero <i>et al.</i> , 2000
Azithromycin	8.7, 9.5	7	1.1 × 10 <sup>5</sup>	Dodd <i>et al.</i> , 2006a
Azobenzene		2	220	Yao & Haag, 1991
1-(2-Benzaldehyde)-4-hydro(1 <i>H</i> ,3 <i>H</i> )-quinazoline-2-one			3.0	Kosjek <i>et al.</i> , 2009
Benzotriazole	1.6, 8.2		35	Lutze <i>et al.</i> , 2011a
			36	Vel Leitner & Roshani, 2010
anion			2650	Lutze <i>et al.</i> , 2011a
Benzylamine	9.33		6.3 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
Butylamine	10.77		1.2 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
			1.7 × 10 <sup>5</sup>	Hoigné & Bader, 1983b
protonated			≤ 0.1	Pryor <i>et al.</i> , 1984
s-Butylamine	10.83		5.2 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
protonated			no reaction	Pryor <i>et al.</i> , 1984
3-Chloroaniline		6	7.84 × 10 <sup>6</sup>	Pierpoint <i>et al.</i> , 2001
4-Chloroaniline		6	1.04 × 10 <sup>7</sup>	Pierpoint <i>et al.</i> , 2001
5-Chlorobenzotriazole	-0.04, 7.5		13	Lutze <i>et al.</i> , 2011a
anion			630	Lutze <i>et al.</i> , 2011a

(Continued)

**Table 8.1** Compilation of ozone rate constants of nitrogen-containing compounds in aqueous solution. Rate constants for sulfur-containing amino acids are given in Chapter 9. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Chlorotoluron			50.5 394	de Laat <i>et al.</i> , 1996 Benitez <i>et al.</i> , 2007
Ciprofloxacin monoprotonated	6.2, 8.8		9 × 10 <sup>5</sup> 7.5 × 10 <sup>3</sup>	Dodd <i>et al.</i> , 2006a Dodd <i>et al.</i> , 2006a
Clarithromycin		7	4 × 10 <sup>4</sup>	Lange <i>et al.</i> , 2006
Creatine		2	~0.5	Hoigné & Bader, 1983b
Creatinine		6	~2	Hoigné & Bader, 1983b
Cyclohexanemethylamine protonated	10.3		7.1 × 10 <sup>4</sup> <1	Dodd <i>et al.</i> , 2006a Dodd <i>et al.</i> , 2006a
Cyclohexylamine protonated	10.6		4.9 × 10 <sup>4</sup> <1	Dodd <i>et al.</i> , 2006a Dodd <i>et al.</i> , 2006a
Cyclophosphamide			2.27 3.0	Fernández <i>et al.</i> , 2010 Garcia-Ac <i>et al.</i> , 2010
Deethylatrazine		2	0.18	Acero <i>et al.</i> , 2000
Deethyldeisopropylatrazine		2	<0.1	Acero <i>et al.</i> , 2000
Deisopropylatrazine		2	3.1	Acero <i>et al.</i> , 2000
2,4-Diamino-5-methylpyrimidine monoprotonated	3.2, 7.1		1.3 × 10 <sup>6</sup> 2.9 × 10 <sup>3</sup>	Dodd <i>et al.</i> , 2006a Dodd <i>et al.</i> , 2006a
diprotonated			5.0 × 10 <sup>2</sup>	Dodd <i>et al.</i> , 2006a
1,4-Diazabicyclo[2.2.2]octane (DABCO) monoprotonated	3.0, 8.2		3.2 × 10 <sup>6</sup> 3.5 × 10 <sup>3</sup>	Muñoz & von Sonntag, 2000b Muñoz & von Sonntag, 2000b
Diazepam			0.75	Huber <i>et al.</i> , 2003
Dichloramine			1.3	Haag & Hoigné, 1983b
Diclofenac			1.8 × 10 <sup>4</sup> 6.8 × 10 <sup>5</sup> ~10 <sup>6</sup>	Vogna <i>et al.</i> , 2004 Sein <i>et al.</i> , 2008 Huber <i>et al.</i> , 2003
Diethylamine protonated	10.49		6.2 × 10 <sup>5</sup> 9.1 × 10 <sup>5</sup> 11 ± 6	Pryor <i>et al.</i> , 1984 Muñoz & von Sonntag, 2000b Pryor <i>et al.</i> , 1984
Diethylenetriaminepentaacetic acid (DTPA)	-0.1, 0.7 1.6, 2.0 2.6, 4.3 8.6, 10.5			
CaDTPA <sup>3-</sup>			6200	Stemmler <i>et al.</i> , 2001
Fe(III)DTPA <sup>2-</sup>			<10	Stemmler <i>et al.</i> , 2001
Fe(III)(OH)DTPA <sup>3-</sup>			2.4 × 10 <sup>5</sup>	Stemmler <i>et al.</i> , 2001

(Continued)

**Table 8.1** Compilation of ozone rate constants of nitrogen-containing compounds in aqueous solution. Rate constants for sulfur-containing amino acids are given in Chapter 9. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
ZnDTPA <sup>3-</sup>			3500	Stemmler <i>et al.</i> , 2001
<i>N,N</i> -Dimethylacetamide		7	0.7	Pryor <i>et al.</i> , 1984
Dimethylamine	11		1.2 × 10 <sup>7</sup>	Hoigné & Bader, 1983b
protonated			<0.1	Hoigné & Bader, 1983b
4-Dimethylaminoantipyrine	5.1		1.7 × 10 <sup>8</sup>	Lee <i>et al.</i> , 2007a
protonated			1.7 × 10 <sup>5</sup>	Lee <i>et al.</i> , 2007a
3-(Dimethylaminomethyl) indole	10.0		2 × 10 <sup>9</sup>	Lee <i>et al.</i> , 2007a
protonated			2.4 × 10 <sup>6</sup>	Lee <i>et al.</i> , 2007a
Dimethylaniline	5.1		2 × 10 <sup>9</sup>	Lee <i>et al.</i> , 2007a
5,6-Dimethylbenzotriazole	~2		880	Lutze <i>et al.</i> , 2011a
anion	~9.28		3.3 × 10 <sup>4</sup>	Lutze <i>et al.</i> , 2011a
Dimethylchloramine			1.9 × 10 <sup>3</sup>	Haag & Hoigné, 1983b
<i>N,N</i> -Dimethylcyclohexylamine	10.7		3.7 × 10 <sup>6</sup>	Dodd <i>et al.</i> , 2006a
protonated			<1	Dodd <i>et al.</i> , 2006a
Dimethylethanolamine	9.2		1.1 × 10 <sup>7</sup>	Lee <i>et al.</i> , 2007a
protonated			<0.2	Lee <i>et al.</i> , 2007a
Dimethylformamide			0.24	Lee <i>et al.</i> , 2007a
3,5-Dimethylisoxazole			5.4 × 10 <sup>1</sup>	Dodd <i>et al.</i> , 2006a
Dimethylsulfamide (DMS)		7	~20	von Gunten <i>et al.</i> , 2010
Diuron			14.7	de Laat <i>et al.</i> , 1996
			16.5	Benitez <i>et al.</i> , 2007
		2.4	13.3	Chen <i>et al.</i> , 2008
Enrofloxacin	6.1, 7.7	7	1.5 × 10 <sup>5</sup>	Dodd <i>et al.</i> , 2006a
Ethylenediaminetetraacetic acid (EDTA)	0.26, 0.96, 2.0, 2.7, 6.2, 10.2		3.3 × 10 <sup>6</sup>	Muñoz & von Sonntag, 2000b
monoprotonated (HEDTA)			1.6 × 10 <sup>5</sup>	Muñoz & von Sonntag, 2000b
CaEDTA <sup>4-</sup>		6	~1 × 10 <sup>5</sup>	Muñoz & von Sonntag, 2000b
Fe(III)EDTA <sup>3-</sup>		6	320	Muñoz & von Sonntag, 2000b
Ethyl <i>N</i> -piperazine-carboxylate	8.3		1.1 × 10 <sup>6</sup>	Dodd <i>et al.</i> , 2006a
protonated			<1	Dodd <i>et al.</i> , 2006a
2-Fluoroaniline		6	7.3 × 10 <sup>6</sup>	Pierpoint <i>et al.</i> , 2001
3-Fluoroaniline		6	8.1 × 10 <sup>6</sup>	Pierpoint <i>et al.</i> , 2001
4-Fluoroaniline		6	1.2 × 10 <sup>7</sup>	Pierpoint <i>et al.</i> , 2001
Glutamate ion	9.47		2.6 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
protonated			0.2	Pryor <i>et al.</i> , 1984
Glycine	9.78		1.3 × 10 <sup>5</sup>	Hoigné & Bader, 1983b

(Continued)

**Table 8.1** Compilation of ozone rate constants of nitrogen-containing compounds in aqueous solution. Rate constants for sulfur-containing amino acids are given in Chapter 9. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
			2.1 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
			2.1 × 10 <sup>5</sup>	Muñoz & von Sonntag, 2000b
protonated			0.05	Hoigné & Bader, 1983b
Hexahydro-1,3,5-trinitro-1,3,5-triazin (RDX)		2.4	0.97	Chen <i>et al.</i> , 2008
Histidine	6.0		2.1 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
Hydroxylamine	6.0		2 × 10 <sup>4</sup>	Hoigné <i>et al.</i> , 1985
Imidazole	6.95		2.4 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
protonated			4 × 10 <sup>5</sup>	Hoigné & Bader, 1983b
			22	Hoigné & Bader, 1983b
Iminodiacetic acid	9.12		2.8 × 10 <sup>6</sup>	Muñoz & von Sonntag, 2000b
3-Iodoaniline		6	7.4 × 10 <sup>6</sup>	Pierpoint <i>et al.</i> , 2001
4-Iodoaniline		6	9.2 × 10 <sup>6</sup>	Pierpoint <i>et al.</i> , 2001
Isoleucine	9.76		5.6 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
2-Isopropyl-3-methoxypyrazine (IPMP)			50	Peter & von Gunten, 2007
Isoproturon			141	de Laat <i>et al.</i> , 1996
			2218	Benitez <i>et al.</i> , 2007
Leucine	9.74		5.3 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
Lincomycin	7.79		2.8 × 10 <sup>6</sup>	Qiang <i>et al.</i> , 2004
protonated			3.3 × 10 <sup>5</sup>	Qiang <i>et al.</i> , 2004
Linuron	2.4		3	de Laat <i>et al.</i> , 1996
			1.9	Benitez <i>et al.</i> , 2007
			2.6	Chen <i>et al.</i> , 2008
protonated			no reaction	Pryor <i>et al.</i> , 1984
Lysine	9.18		3.1 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
Methotrexate			>10 <sup>4</sup>	Garcia-Ac <i>et al.</i> , 2010
2-Methoxyaniline		6	1.7 × 10 <sup>7</sup>	Pierpoint <i>et al.</i> , 2001
N-Methylacetamide			0.6	Pryor <i>et al.</i> , 1984
Methylamine	10.6		<1 × 10 <sup>5</sup>	Hoigné & Bader, 1983b
3-Methylaniline		6	1.9 × 10 <sup>7</sup>	Pierpoint <i>et al.</i> , 2001
5-Methylbenzotriazole	~1.65, ~8.5		164	Lutze <i>et al.</i> , 2011a
anion			1.0 × 10 <sup>4</sup>	Lutze <i>et al.</i> , 2011a
Methylchloramine			810	Haag & Hoigné, 1983a
Methyldichloramine			<1 × 10 <sup>-2</sup>	Haag & Hoigné, 1983a
4-Methylimidazole	7.52		3.1 × 10 <sup>6</sup>	Pryor <i>et al.</i> , 1984

(Continued)

**Table 8.1** Compilation of ozone rate constants of nitrogen-containing compounds in aqueous solution. Rate constants for sulfur-containing amino acids are given in Chapter 9. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
1-Methylpyrrolidine	10.2		2.0 × 10 <sup>6</sup>	Dodd <i>et al.</i> , 2006a
protonated			<1	Dodd <i>et al.</i> , 2006a
4-Methylsulfonylaniline		6	4.7 × 10 <sup>4</sup>	Pierpoint <i>et al.</i> , 2001
Metolachlor			3	de Laat <i>et al.</i> , 1996
Metoprolol	9.7		8.6 × 10 <sup>5</sup>	Benner <i>et al.</i> , 2008
protonated			330	Benner <i>et al.</i> , 2008
		7	2.0 × 10 <sup>3</sup>	Benner <i>et al.</i> , 2008
Monobromamine			40	Haag <i>et al.</i> , 1984
Monochloramine			26*	Haag & Hoigné, 1983
Morpholine	8.36		1.8 × 10 <sup>5</sup>	Tekle-Röttering <i>et al.</i> , 2011
Nitritotriacetic acid (NTA)	1.65, 2.94		9.8 × 10 <sup>5</sup>	Muñoz & von Sonntag, 2000b
	10.33			
		2	830	Games & Staubach, 1980
3-Nitroaniline		6	2.4 × 10 <sup>6</sup>	Pierpoint <i>et al.</i> , 2001
4-Nitroaniline		6	1.4 × 10 <sup>5</sup>	Pierpoint <i>et al.</i> , 2001
Nitroform anion			1.4 × 10 <sup>4</sup>	Flyunt <i>et al.</i> , 2003a
N-Nitrosodimethylamine			~10	Hoigné & Bader, 1983a
			0.052	Lee <i>et al.</i> , 2007b
1-Phenoxy-3-propanol		7	320	Benner <i>et al.</i> , 2008
Phenylalanine	9.24		3.8 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
Proline	10.6		4.3 × 10 <sup>6</sup>	Pryor <i>et al.</i> , 1984
Prometon	4.3	3	~2	Chen <i>et al.</i> , 2008
		7.5	<12	Chen <i>et al.</i> , 2008
Propachlor			0.94	de Laat <i>et al.</i> , 1996
Propranolol	9.5		~1 × 10 <sup>5</sup>	Benner <i>et al.</i> , 2008
protonated			~1 × 10 <sup>5</sup>	Benner <i>et al.</i> , 2008
Propylamine		2	≤ 1 × 10 <sup>-2</sup>	Hoigné & Bader, 1983b
Pyridine	5.14		~3	Hoigné & Bader, 1983b
			2.0	Andreozzi <i>et al.</i> , 1991
protonated			0.01	Hoigné & Bader, 1983b
Quinoline			51	Wang <i>et al.</i> , 2004
Roxithromycin	9.2	7	6.3 × 10 <sup>4</sup>	Dodd <i>et al.</i> , 2006a
Serine	9.21		1.29 × 10 <sup>5</sup>	Pryor <i>et al.</i> , 1984
protonated			7 ± 4	Pryor <i>et al.</i> , 1984
Simazine		4.3	4.8	Yao & Haag, 1991
		2	3.3	Xiong & Graham, 1992
Spectinomycin	6.8, 8.8		1.3 × 10 <sup>6</sup>	Qiang <i>et al.</i> , 2004

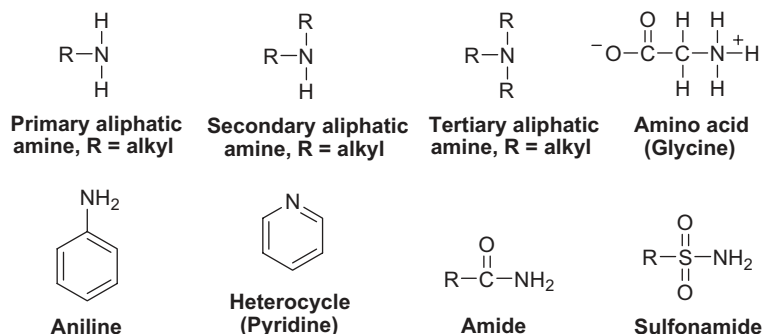
(Continued)

**Table 8.1** Compilation of ozone rate constants of nitrogen-containing compounds in aqueous solution. Rate constants for sulfur-containing amino acids are given in Chapter 9. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
protonated			3.3 × 10 <sup>5</sup>	Qiang <i>et al.</i> , 2004
Sulfamethoxazole	5.6		4.7 × 10 <sup>4</sup>	Dodd <i>et al.</i> , 2006a
conjugate base			5.7 × 10 <sup>5</sup>	Dodd <i>et al.</i> , 2006a
Tetranitromethane			10	Flyunt <i>et al.</i> , 2003a
Threonine	9.11		4.6 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
Tramadol	9.4		1.0 × 10 <sup>6</sup>	Zimmermann <i>et al.</i> , 2012
protonated			7.7 × 10 <sup>4</sup>	Zimmermann <i>et al.</i> , 2012
Triethylamine	11.01		2.1 × 10 <sup>6</sup>	Pryor <i>et al.</i> , 1984
			4.1 × 10 <sup>6</sup>	Muñoz & von Sonntag, 2000b
protonated			5 ± 4	Pryor <i>et al.</i> , 1984
Trimethoprim	3.2, 7.1	7	2.7 × 10 <sup>5</sup>	Dodd <i>et al.</i> , 2006a
Trimethylamine	9.76		4.1 × 10 <sup>6</sup>	Hoigné & Bader, 1983b
			5.1 × 10 <sup>6</sup>	Muñoz & von Sonntag, 2000b
Tryptophan	9.38		7 × 10 <sup>6</sup>	Pryor <i>et al.</i> , 1984
Tylosin	7.7	7	5.1 × 10 <sup>5</sup>	Dodd <i>et al.</i> , 2006a
Valine	9.72		6.8 × 10 <sup>4</sup>	Pryor <i>et al.</i> , 1984
protonated			≤ 3	Pryor <i>et al.</i> , 1984

\*a rate constant of 7 M<sup>-1</sup>s<sup>-1</sup> was determined for substrate decrease

For aromatic amines (cf. Figure 8.1), the aromatic ring is a second potential site of ozone attack.

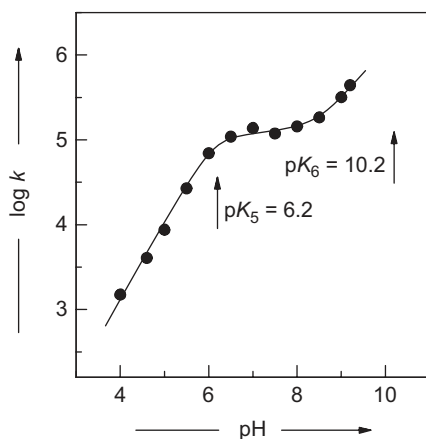
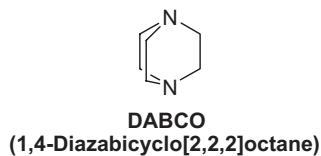


**Figure 8.1** Nitrogen-containing compounds.

The reactivity of the nitrogen in aromatic heterocycles is low (cf. pyridine). In amides, the free electron pair is drawn towards the electron-withdrawing carbonyl function with the effect that amides show



extremely low rate constants, e.g. *N*-methylacetamide (Table 8.1). In sulfonamides, the electron-withdrawing effect of the neighbouring SO<sub>2</sub> group is so strong that they become weak acids [e.g. p*K*<sub>a</sub>(sulfamethoxazole) = 5.7 (Huber *et al.*, 2005)]. With compounds that carry two amino groups such as EDTA (for structure see below) and DABCO, the rate constants are high, when both amino groups are deprotonated, but drops by three orders of magnitude when one of them is protonated (cf. Table 8.1 and Figure 8.2). Apparently, protonation of one of the nitrogens also affects the electron density of the other, thereby reducing its reactivity towards ozone.

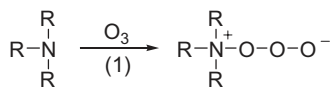


**Figure 8.2** Logarithm of the ozone rate constant of ethylenediaminetetraacetic acid (EDTA) as a function of pH according to Muñoz & von Sonntag, 2000b, with permission. For structure of EDTA see Section 8.3.

## 8.2 GENERAL MECHANISTIC CONSIDERATIONS

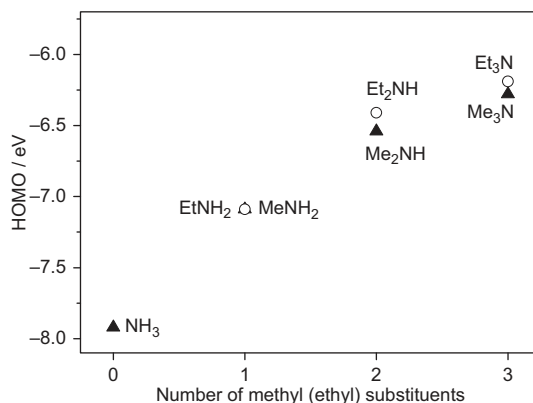
### 8.2.1 Aliphatic amines

Ozone reacts with aliphatic amines and amino acids by adding to the lone pair at nitrogen [reaction (1)].



Ammonia, the parent of the amines, reacts only very slowly with ozone (Table 8.1; for a catalysis by Br<sup>-</sup> see Chapter 11). Alkylamines react several orders of magnitude faster. Electron-donating alkyl groups

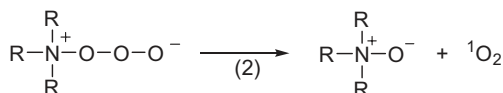
enhance the electron density at nitrogen allowing the electrophilic ozone to undergo the addition reaction (1) more readily. This increase in electron density can be seen from the dependence of the HOMO as a function of the number of alkyl substituents (Figure 8.3).



**Figure 8.3** Energy of the HOMO of ammonia and its methyl and ethyl derivatives vs. the number of methyl (ethyl) substituents (Naumov & von Sonntag, 2009, unpublished).

An increase in the electron density at nitrogen should correlate with a decrease of the standard Gibbs free energy of reaction (1), and it would be tempting to correlate the rate constants of the reaction of ozone with the standard Gibbs free energy of adduct formation, reaction (1), as has been successfully done in the case of the addition of ozone to aromatic compounds (Chapter 7). A major problem in arriving at reliable data is, however, the fact that a water molecule hydrogen bonded to the nitrogen is replaced by ozone and the loss of this hydrogen bond (ca. 25 kJ mol<sup>-1</sup>) may have to be taken into account (note that this problem does not arise with aromatic compounds, Chapter 7). Moreover, steric effects seem to play an important role. This is apparent from the drop in the p*K*<sub>a</sub> value on going from the (protonated) dimethylamine (p*K*<sub>a</sub> = 10.64) to trimethylamine (p*K*<sub>a</sub> = 9.8) despite the fact that the nitrogen in trimethylamine has a higher electron density (Figure 8.3).

The ozone adducts to amines may lose O<sub>2</sub> [reaction (2)].



Since the ozone adduct in its ground state is in its singlet state, the overall spin multiplicity of the products must also be a singlet (spin conservation rule). As a consequence, O<sub>2</sub> is released in its (excited) singlet state [<sup>1</sup>O<sub>2</sub>, O<sub>2</sub>(<sup>1</sup>Δ<sub>g</sub>)], which lies 95.5 kJ mol<sup>-1</sup> above the (triplet) ground state of O<sub>2</sub> [<sup>3</sup>O<sub>2</sub>, O<sub>2</sub>(<sup>3</sup>Σ<sub>g</sub><sup>-</sup>)]. The singlet oxygen yields in ozone reactions are typically high (Table 8.2).

With tertiary amines, this reaction results in the formation of *N*-oxides [reaction (2)] (Muñoz & von Sonntag, 2000b; Lange *et al.*, 2006; Zimmermann *et al.*, 2012) (Table 8.3). For trimethylamine,

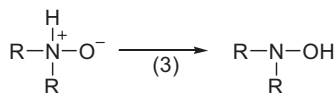
quantum-chemical calculations indicate that reactions (1) and (2) are both exergonic [ $\Delta G^0 = -48 \text{ kJ mol}^{-1}$  and  $-63 \text{ kJ mol}^{-1}$ , respectively; Naumov & von Sonntag (2010, unpublished)].

**Table 8.2** Singlet oxygen ( $^1\text{O}_2$ ) yields (in mol % of mol ozone consumed) in the reaction of ozone with amines at different pH values. The ratio of substrate concentration to ozone concentration is given in parentheses. According to Muñoz *et al.* (2001)

Substrate	pH	$^1\text{O}_2$ yield/% ([substrate] : [ozone])
Trimethylamine	7	63 (10:1)
	9.5	60 (10:1), 69 (100:1)
Triethylamine	7	No signal (1:1), 42 (10:1), 72 (10:1)
	8	No signal (1:1), 63 (10:1), 80 (100:1)
	9.5	52 (1:1), 73 (10:1), 85 (100:1)
	10.5	59 (1:1)
	11.5	78 (100:1)
DABCO	7	70 (1:1), 80 (10:1)
	9	90 (10:1)
Ethylenediaminetetraacetic acid (EDTA)	4.5	No signal (1:1), 19 (10:1)
	5.5	No signal (1:1), 40 (10:1), 39 (100:1)
	7	39 (1:1), 59 (10:1), 43 (100:1)
	9.5	31 (1:1), 33 (10:1), 37 (100:1)
EDTA/ $\text{Ca}^{2+}$	$\sim 3$	15 (10:1)
EDTA/ $\text{Fe}^{3+}$	$\sim 3$	No signal (1:1), No signal (10:1)
Nitrilotriacetic acid (NTA)	7	No signal (1:1), 18 (10:1)
	9.5	22 (1:1), 21 (10:1)
Diethylamine	9	20 (1:1)
	10.5	24 (1:1), 20 (10:1)
	9	17 (1:1)
Iminodiacetic acid (IDA)	9	17 (1:1)
	10.5	20 (1:1), 18 (10:1)
Ethylamine	9	No signal (1:1)
	10.5	11 (1:1), 17 (10:1)
Glycine	7	No signal (1:1), (10:1)
	10.5	4 (10:1)
<i>N,N</i> -Diethylaniline	8.5	7 (17:1)
<i>N,N,N,N</i> -Tetramethylphenylenediamine	3.5	9 (3:1)
	6	4 (3:1)

Detailed data on primary and secondary amines are not yet available, but for dimethylamine quantum-chemical calculations indicate that reactions (1) and (2) are also both exergonic ( $\Delta G^0 = -41 \text{ kJ mol}^{-1}$  and  $-74 \text{ kJ mol}^{-1}$ , respectively) and that the corresponding *N*-oxide is only a short-lived

intermediate and rearranges into the isomeric hydroxylamine [reaction (3);  $\Delta G^0 = -20 \text{ kJ mol}^{-1}$ ; Naumov & von Sonntag (2010, unpublished)].



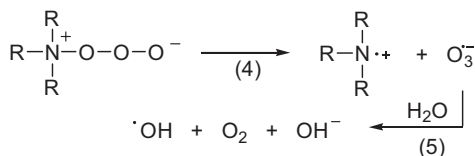
**Table 8.3** Products of the reaction of ozone with trimethylamine, triethylamine and 1,4-diazabicyclo[2.2.2]octane (DABCO) in % of ozone consumed (Muñoz & von Sonntag, 2000b)

Product	Trimethylamine	Triethylamine	DABCO
Aminoxide	93	85	90
Singlet oxygen	69	85	90
Secondary amine	Not determined	15 (7) <sup>(a)</sup>	Not observed
Aldehyde	9	19	Not observed

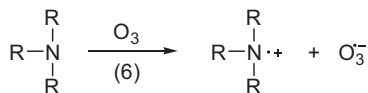
<sup>(a)</sup>in the presence of tertiary butanol

In the case of propranolol, the hydroxylamine has been identified (Benner & Ternes, 2009b).

In competition with  $^1\text{O}_2$  elimination [reaction (2)], the ozone adduct may also cleave heterolytically, thereby forming an amine radical cation and an ozonide radical anion,  $\text{O}_3^{\cdot-}$  [reaction (4)]. The latter reacts with water giving rise to  $\cdot\text{OH}$  [reaction (5), for details see Chapter 11].

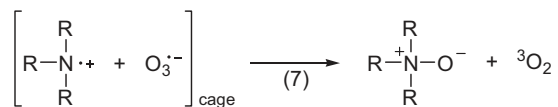


In principle, this reaction could also proceed via a direct electron transfer without an adduct as intermediate [reaction (6)].



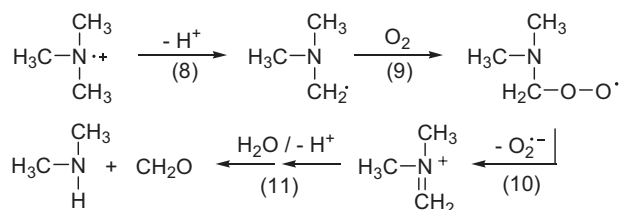
In reactions (4) and (6), two radicals are formed. Whenever two radicals are formed side by side, they are held together by the solvent for a short period of time. If they react with one another at diffusion-controlled rates there is a given chance that they will react within the solvent cage in competition with diffusing out of the cage. The importance of such cage reactions was first addressed by Rabinowitch (Rabinowitch & Wood, 1936; Rabinowitch, 1937). The kinetics for diffusion-controlled reactions were discussed by Noyes (Noyes, 1954). A typical example is the photodecomposition of  $\text{H}_2\text{O}_2$ . In the gas phase, two  $\cdot\text{OH}$  are formed per photodissociation event. In water, however, there is a 50% probability of the two  $\cdot\text{OH}$  formed recombining within the solvent cage to  $\text{H}_2\text{O}_2$ . Thus in water, the yield of free  $\cdot\text{OH}$  is only 50% with respect to the primary  $\cdot\text{OH}$  yield. Viscosity is one parameter that has a substantial effect on the yield of the cage product and so is temperature [for examples of cage effects in free-radical reactions see (Barrett

*et al.*, 1968; Chuang *et al.*, 1974; Mark *et al.*, 1996; Goldstein *et al.*, 2005)]. In the given trialkylamine case, this may lead to the formation of the *N*-oxide [reaction (7)].



In contrast to reaction (2), triplet (ground state)  $\text{O}_2$  can be formed, as radicals have a doublet spin multiplicity, and their disproportionation can lead to one molecule in the singlet state (here: the *N*-oxide) and one molecule in the triplet state (here:  ${}^3\text{O}_2$ ). This can explain why in the trialkylamines singlet oxygen yields are below *N*-oxide yields. Such a gap between the yields of singlet oxygen and O-transfer products is not observed with sulfides, but sulfides do not give rise to free-radicals in their reactions with ozone (Chapter 9).

Besides reactions (4) and (5),  $\cdot\text{OH}$  radicals can also be formed via  $\text{O}_2^{\cdot-}$  ( $\text{O}_2^{\cdot-} + \text{O}_3 \rightarrow \text{O}_2 + \text{O}_3^{\cdot-}$ , cf. Chapter 13). This ozone-reactive intermediate is formed in the course of the decay of aliphatic amine radical cations [reactions (8)–(11)].



Details of the kinetics of reactions (8)–(11), including the rate constants of all individual steps (not shown here), have been elucidated with the help of the pulse radiolysis technique (Das & von Sonntag, 1986; Das *et al.*, 1987) (for a potential role of these reactions in contributing to  $\cdot\text{OH}$  formation in the reaction of ozone with DOM see Chapter 3). The  $\cdot\text{OH}$  yields in the reaction of ozone with some amines are compiled in Table 8.4.

**Table 8.4** Compilation of  $\cdot\text{OH}$  yields in % of ozone consumed (mol  $\cdot\text{OH}$  per mol ozone) in the reaction of ozone with amines

Amine	$\cdot\text{OH}$ yield/%	Reference
Adenosine	43	Flyunt <i>et al.</i> , 2003a
Aniline	27	Tekle-Röttering <i>et al.</i> , 2011
Benzotriazole anion	~32	Lutze <i>et al.</i> , 2011a
Diclofenac	30	Sein <i>et al.</i> , 2008
<i>N,N</i> -Diethylaniline	28	Flyunt <i>et al.</i> , 2003a
<i>N,N</i> -Diethyl- <i>p</i> -phenylenediamine <sup>(a)</sup>	23	Jarocki, 2011, unpublished
5,6-Dimethylbenzotriazole anion	~20	Lutze <i>et al.</i> , 2011a
5-Methylbenzotriazole anion	~28	Lutze <i>et al.</i> , 2011a
Morpholine	33	Tekle-Röttering <i>et al.</i> , 2011

(Continued)

**Table 8.4** Compilation of  $\cdot\text{OH}$  yields in % of ozone consumed (mol  $\cdot\text{OH}$  per mol ozone) in the reaction of ozone with amines (*Continued*)

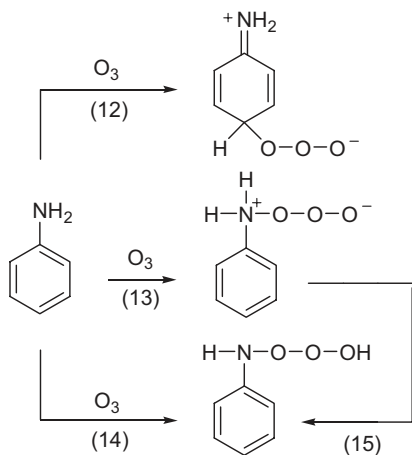
Amine	$\cdot\text{OH}$ yield/%	Reference
o-Phenylenediamine	30	Flyunt <i>et al.</i> , 2003a
<i>N,N,N,N</i> -Tetramethylphenylenediamine	68 <sup>(b)</sup>	Flyunt <i>et al.</i> , 2003a
Trimethylamine	15	Flyunt <i>et al.</i> , 2003a

<sup>(a)</sup>see Chapter 2, <sup>(b)</sup>for a *caveat* see Flyunt *et al.* (2003)

In the reaction of ozone with activated carbon,  $\cdot\text{OH}$  radicals are formed (Jans & Hoigné, 1998). This reaction has been attributed to the presence of nitrogen-containing sites in the activated carbon (Sánchez-Polo *et al.*, 2005), and when these sites are oxidised by ozone,  $\cdot\text{OH}$  production ceases (Chapter 3).

## 8.2.2 Aromatic amines (anilines)

The reaction of ozone with aniline is very fast (Table 8.1). The rate constant determined by competition with buten-3-ol ( $k = 3.8 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ ) may still be somewhat too high, because  $<0.5$  mol aniline are destroyed per mol ozone consumed. Aniline shares this phenomenon with diclofenac, and a potential explanation of this has been made below. A rate constant just above  $10^7 \text{ M}^{-1} \text{ s}^{-1}$  would be compatible with an addition to the strongly activated aromatic ring [Chapter 7, e.g. reaction (12)], but an addition to the nitrogen must also be envisaged [reactions (13)–(15)].

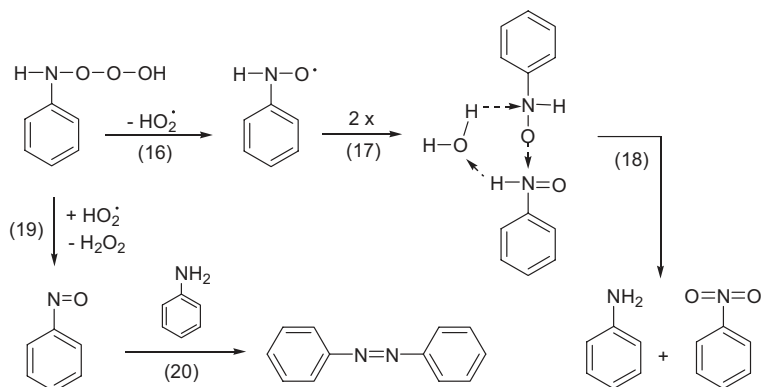


Quantum-chemical calculations indicate that addition to the ring is markedly exergonic [reaction (12),  $\Delta G^0 = -53 \text{ kJ mol}^{-1}$ , Naumov & von Sonntag (2009, unpublished)]. This value and the above rate constant fall reasonably well on the plot of calculated standard Gibbs free energies vs. the logarithm of the rate constant such as shown in Figure 7.2 (Chapter 7) (Tekle-Röttering *et al.*, 2011). An addition to the nitrogen is slightly endergonic [reaction (13),  $\Delta G^0 = +15 \text{ kJ mol}^{-1}$ ]. However, it cannot be excluded that an addition to nitrogen is accompanied with a concomitant proton transfer (in analogy to the well-documented proton transfer coupled electron transfer) [reaction (14),  $\Delta G^0 = -77 \text{ kJ mol}^{-1}$ ]. Thus, a reaction at nitrogen, possibly competing with an addition to the ring, is not unlikely.

Despite the considerable number of papers that deal with the ozone chemistry of aniline (Gilbert & Zinecker, 1980; Dore *et al.*, 1980; Turhan & Uzman, 2007; Caprio & Insola, 1985), a material balance is still missing. Products that are evidently due to an attack at nitrogen are nitrosobenzene, nitrobenzene and azobenzene (after completion of the nitrosobenzene plus aniline reaction). With respect to ozone consumption, their yields are very low ( $\sim 0.5\%$ ,  $\sim 0.7\%$  and  $\sim 0.02\%$ , respectively; Tekle-Röttering, private communication). This indicates that ozone attack at nitrogen is a very minor reaction.

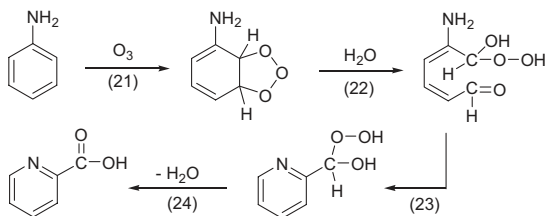
Concerning the mechanism of their formation, one has to take into account that nitrobenzene is a primary product despite the fact that it requires two oxidation equivalents.

The NO–OO<sup>−</sup> bond length in the species formed in reaction (13) is long (1.812 Å), and this intermediate would readily release O<sub>2</sub><sup>•−</sup>. Once protonated [cf. reactions (14) and (15)], the intermediate becomes so unstable that upon optimisation of the structure it releases HO<sub>2</sub><sup>•</sup> [reaction (16)]. A bimolecular decay of the nitroxyl radical, assisted by water [reaction (17)] giving rise to aniline and nitrobenzene is energetically feasible [reaction (18),  $\Delta G^0 = -83 \text{ kJ mol}^{-1}$ ].

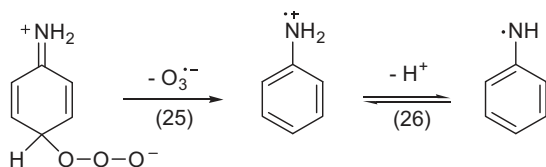


Nitrosobenzene may be formed in the disproportionation of the nitroxyl radical with HO<sub>2</sub><sup>•</sup> [reaction (19), e.g. in the cage]. The reaction of nitrosobenzene with aniline to form azobenzene [reaction (20)] is a slow postozonation process. The kinetics of this reaction is well documented (Yunes *et al.*, 1975; Dalmagro *et al.*, 1994).

The reactions at nitrogen, although quite interesting as such, are of little importance in comparison to an addition at the ring. Here most product escaped detection, except pyridine-2-carboxylic acid which seems to be derived from the ozonide formed upon closing of the *ortho* ozone adduct (not shown, cf. Chapter 7) [reactions (21)–(24)].



Ozone addition to the ring may be followed by a release of O<sub>3</sub><sup>•−</sup> [e.g. reaction (25)].

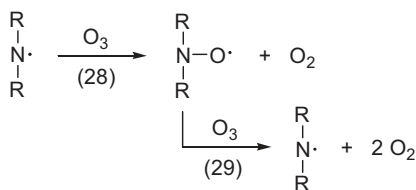


The high  $\cdot\text{OH}$  yield (precursor:  $\text{O}_3^{\cdot-}$ ) given in Table 8.4 must be due to this reaction. Aromatic radical cations are in equilibrium with the corresponding radicals. The  $\text{p}K_a$  value of the aniline radical cation is 7.05. As expected, substituents experience a strong effect of the  $\text{p}K_a$  values expressed as a free-energy relationship (27) (Jonsson *et al.*, 1994, 1995).

$$\text{p}K_a = 7.09 - 3.17 \sum_{i=2}^6 \sigma_i^+ \quad (27)$$

Aniline radical cations are also formed upon  $\cdot\text{OH}$  attack on aniline (Qin *et al.*, 1985), and products observed there may also be of some relevance for aniline ozonolysis. Beyond those mentioned above, there are no further products at the level of low-molecular-weight compounds, and, most likely, the major products are hidden in the oligomer fraction (condensation products with aniline), which is not yet fully elucidated.

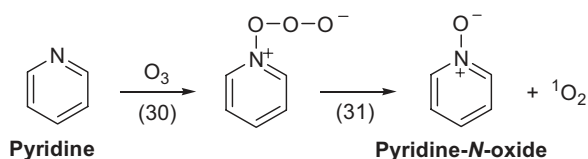
Deficits in the material balance between ozone and amine consumption have been reported for diclofenac, and it has been suggested that there may be a chain reaction that destroys ozone in competition with its reaction with amines (Sein *et al.*, 2008) [reactions (28) and (29)] (see also Chapter 13).



Quantum chemical calculations were carried out with morpholine as a model system. They show that both reactions are exergonic ( $\Delta G^\circ = -77 \text{ kcal mol}^{-1}$  and  $-23 \text{ kcal mol}^{-1}$ , respectively, Naumov & von Sonntag, 2011, unpublished). A stable nitroxyl radical, TEMPO, reacts indeed very fast with ozone ( $k = 1.3 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ ) (Muñoz & von Sonntag, 2000a).

### 8.2.3 Nitrogen-containing heterocyclic compounds

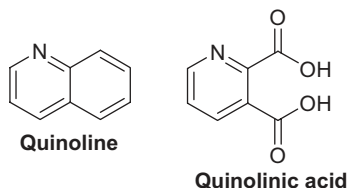
Pyridine reacts with ozone (Table 8.1) about as fast as benzene ( $k = 2 \text{ M}^{-1} \text{ s}^{-1}$ , Table 7.1), many orders of magnitude slower than most other nitrogen-containing compounds. In the presence of tBuOH as  $\cdot\text{OH}$  scavenger, which substantially protects pyridine from getting additionally degraded, the major product (ca. 80% of pyridine degraded) is the *N*-oxide (Andreozzi *et al.*, 1991) [reactions (30) and (31)]. This indicates that the major primary site of ozone attack is the nitrogen.





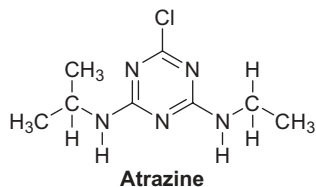
According to quantum-chemical calculations, *N*-adduct formation [reaction (30)] is exergonic ( $\Delta G^0 = -49 \text{ kJ mol}^{-1}$ ) and the NO–OO bond in the adduct is very long (2.085 Å, Naumov & von Sonntag 2011, unpublished). Thus, the subsequent release of  $^1\text{O}_2$  is already preformed in the adduct [reaction (31),  $\Delta G^0 = -81 \text{ kJ mol}^{-1}$ ]. The low rate constant despite the high driving force for this reaction is analogous to the reaction of ozone with dimethyl sulfoxide (Chapter 9), but is not yet fully understood and may be due to a coulombic repulsion of ozone and the pyridine nitrogen resulting in substantial activation energy of this reaction. A reaction by addition to the ring seems unlikely as the standard Gibbs free energy for addition is too positive ( $\Delta G^0 > +158 \text{ kJ mol}^{-1}$ ) to account for the observed rate constant (cf. Chapter 7).

Quinoline reacts much faster than pyridine (Table 8.1). Oxidation of intermediates with  $\text{H}_2\text{O}_2$  after ozonation leads to quinolinic acid as the major product (Andreozzi *et al.*, 1992).



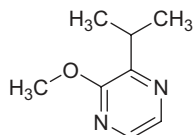
This indicates a change in mechanism. It is now the benzene ring that is mainly attacked (note the high ozone rate constant of naphthalene (Chapter 7, Table 7.1). It seems that the formation of quinoline-*N*-oxide has not been looked for. Thus, to what extent an attack at nitrogen also takes place is as yet not known.

With atrazine, the ozone rate constant is low (Table 8.1). Ozone attack at the ring can be excluded (cf. pyridine) and ozone attack must be at the nitrogens.



There are two types of nitrogens, and data are not yet available for deciding the preferred site.

2-Isopropyl-3-methoxypyrazine (IPMP) is a potent taste and odour compound (Chapter 5). Similarly to atrazine, ozone attack will probably occur at the nitrogens. An activation by the methoxy group leads to a higher rate constant.



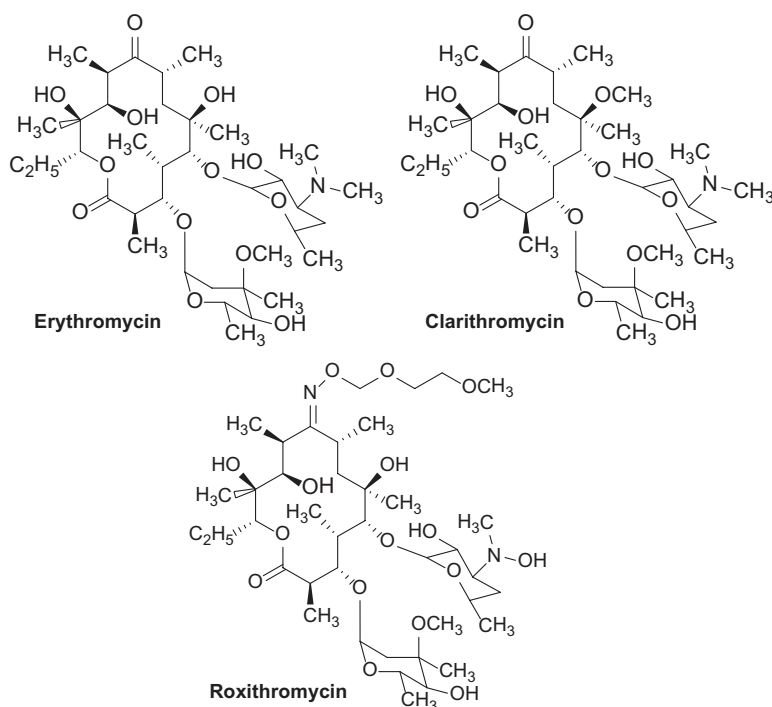
**2-Isopropyl-3-methoxy-  
pyrazine (IPMP)**

### 8.3 MICROPOLLUTANTS WITH NITROGEN-CONTAINING FUNCTIONS

Ammonia is oxidised by ozone to nitrate (Hoigné & Bader, 1978). The reaction of ammonia with ozone is very slow (Table 8.1), and *en route* to nitrate several oxidation steps are required. Assuming O-transfer

reactions, these must be hydroxylamine ( $\text{H}_2\text{NOH}$ ), hyponitrous acid ( $\text{HNO}$  and its dimer) and nitrite ( $\text{NO}_2^-$ ). Of these intermediates, it is known that hydroxylamine (Table 8.1) and nitrite (Chapter 11) react many orders of magnitude faster with ozone than ammonia itself, and thus these products can only attain very low steady states in the course of the reaction. Moreover,  $\text{HNO}$  is unstable. It decays bimolecularly to  $\text{N}_2\text{O}$ , and to what extent this reaction can be intercepted by ozone and the corresponding ozone rate constant are unknown. In general, mechanistic details of systems that react only slowly with ozone are not readily accessible.

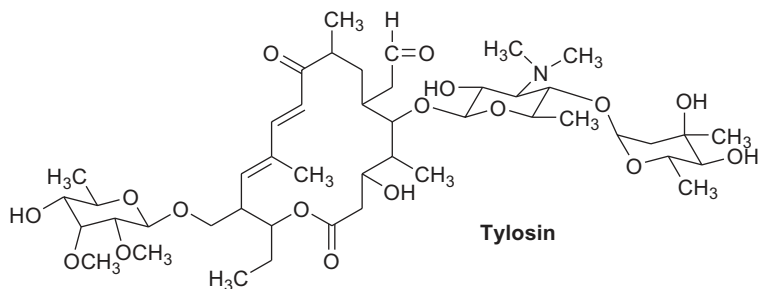
Many pharmaceuticals have amino groups as essential functional groups. Cases in point are the macrolide antibiotics such as erythromycin, clarithromycin, roxithromycin and tylosin. They are not fully degraded upon biological wastewater treatment. For the occurrence of macrolide antibiotics in the aquatic environment see Chapter 4.



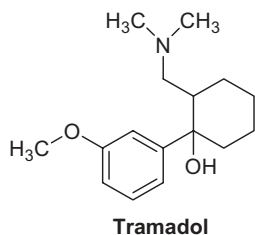
Their site of ozone attack is the tertiary amino group. A product study has been carried out with clarithromycin, and it has been found that the major product is the *N*-oxide [ $> 90\%$ , cf. reaction (2)], and as a minor route, demethylation and formaldehyde formation occurs [cf. reactions (8)–(11)] (Lange *et al.*, 2006). Since the tertiary amino group is essential for the antibacterial activity of these drugs (Goldman *et al.*, 1990; Schlünzen *et al.*, 2001), its conversion to the *N*-oxide or demethylation eliminates the biological activity (Chapter 4) (Lange *et al.*, 2006).

Demethylation has also been reported for roxithromycin, but the expected *N*-oxide formation escaped detection (Radjenovic *et al.*, 2009). Further degradation requires the action of  $\cdot\text{OH}$  (Radjenovic *et al.*, 2009). Among others, the elimination of a sugar moiety was observed. Scission of the glycosidic linkage induced by  $\cdot\text{OH}$  is common in carbohydrate chemistry (von Sonntag, 1980).

The macrolide drug tylosin has two ozone-reactive sites, the tertiary amino group and the dienone function. Their contribution to degradation of tylosin by ozone is pH dependent. The degradation above pH ~5 is controlled by the tertiary amino group (Dodd *et al.*, 2006a).

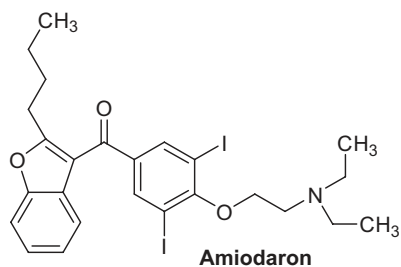


Tramadol is an opioid which is frequently prescribed in case of moderate to severe acute and chronic pain.



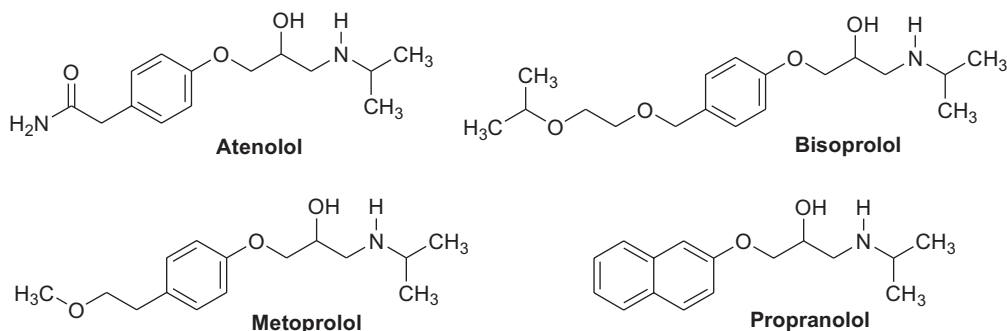
About 10–30% of the tramadol is excreted unchanged via urine and concentrations of up to 97 µg/L and 6 µg/L were reported in secondary effluent and surface waters, respectively (Kasprzyk-Hordern *et al.*, 2009). As expected from the above, the main ozone product of tramadol is its *N*-oxide (ca. 90%) and a minor one, *N*-dealkylated tramadol (<10%) (Zimmermann *et al.*, 2012).

Amiodaron, a commonly used drug against cardiac arrhythmia, also contains a tertiary amine function, and its ozone chemistry, as yet not studied, must be analogous to that of the other tertiary amines.



Beta blockers, for example, atenolol, metoprolol, bisoprolol or propranolol, which are commonly observed as micropollutants in wastewater (Huggett *et al.*, 2003), [for their fate in wastewater see

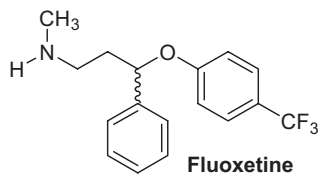
Wick *et al.* (2009)] contain secondary aliphatic amino groups, and this side group seems to be required for the biological response.



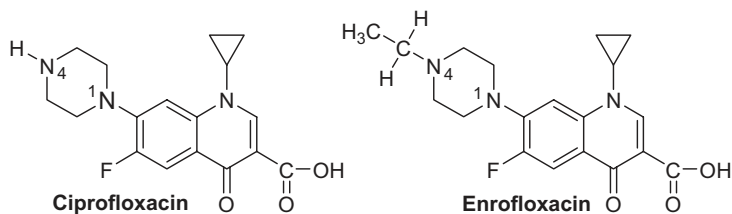
At a wastewater pH of 7–8, the reaction of ozone with these beta blockers is largely determined by the reaction of the free amine in equilibrium (cf. Chapter 2) with the exception of propranolol, in which ozone attack at the more reactive naphthalene ring also takes place (Benner & Ternes, 2009b).

This was confirmed in a product study on metoprolol (Benner & Ternes, 2009a) in which the product from amine oxidation (hydroxylamine) has been detected. The chemistry is complex as substantial amounts of  $\cdot\text{OH}$  are also formed (Sein *et al.*, 2009).

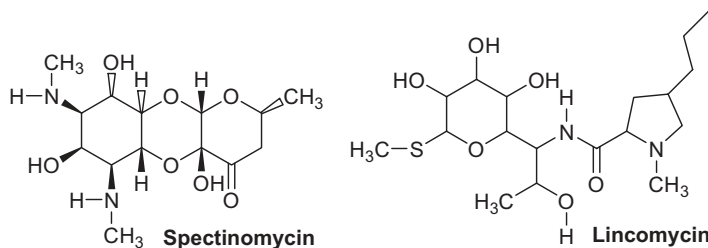
The ozone-reactive site of the psychotropic drug fluoxetine is also the secondary amine in the side group. The aromatic rings are of comparatively little ozone reactivity.



For the antibiotics ciprofloxacin and enrofloxacin (for rate constants see Table 8.1), sites of ozone attack are the nitrogens at N1 and N4. The reason for the higher reactivity of enrofloxacin at pH 7 compared to that of ciprofloxacin is most likely due to the differences of the  $pK_a$  values at N4, reported as 7.7 and 8.8, respectively (Dodd *et al.*, 2006a).

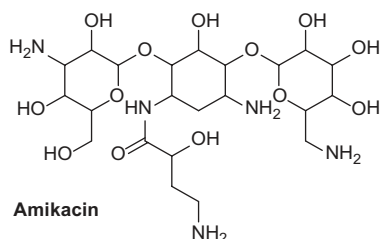


The sites of ozone attack at the antibiotic spectinomycin are the secondary nitrogens (Qiang *et al.*, 2004).

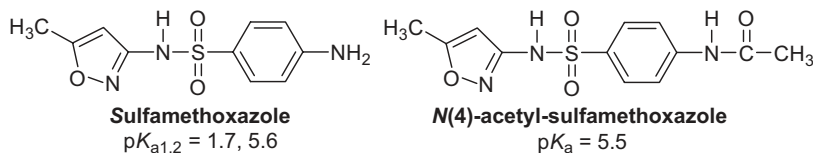


In lincomycin, the tertiary nitrogen in the five-membered ring and the sulfur in the sulfide group are competing sites for ozone attack (Qiang *et al.*, 2004; Dodd, 2008). The pH dependence of the ozone rate constant showed that at pH < 5 the sulfur group is the reactive moiety, whereas at higher pH values the tertiary amine becomes dominant.

The antibiotic amikacin has four primary amino groups, which are the ozone-reactive sites (Dodd, 2008).



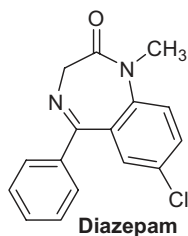
The sulfonamide sulfamethoxazole has two  $pK_a$  values; the one at 1.7 is due to protonation at the aniline group (note that the model compound 4-aminophenyl methylsulfone has a  $pK_a$  value of 1.5). The strong electron-withdrawing sulfonamide function is the reason for this low value.



*N*-Acetylation, as in *N*(4)-acetyl-sulfamethoxazole, shows that the  $pK_a$  at 5.5 must be due to a deprotonation at the sulfonamide nitrogen. At a pH where the sulfonamide function is deprotonated, the sulfamethoxazole rate constant is an order of magnitude higher than with the neutral molecule (Table 8.1) (Dodd *et al.*, 2006a). The model compound 4-aminophenyl methyl sulfone has a rate constant of  $4.7 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ , while *N*(4)-acetyl-sulfamethoxazole displays rate constants of  $260 \text{ M}^{-1} \text{ s}^{-1}$  (deprotonated) and  $20 \text{ M}^{-1} \text{ s}^{-1}$  (neutral). The latter observation excludes the sulfonamide nitrogen as the ozone-reactive site, although its deprotonation increases the rate of reaction by adding further electron density into the ring.

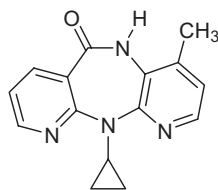
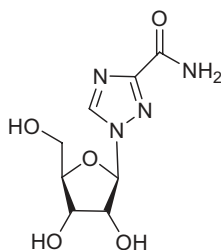
These data point to the nitrogen at the anilino group and/or the now activated aromatic ring in sulfamethoxazole as the major site of attack. The slow reaction found for neutral *N*(4)-acetyl-sulfamethoxazole may be attributed to an addition to the C–C double bond on the oxazole ring. This reaction would become faster upon deprotonation of the sulfonamide function, which channels electron density into the oxazole ring.

The psychotropic drug diazepam has two nitrogens. One is an amide nitrogen and certainly of negligible ozone reactivity. The other is an enamine nitrogen with the double bond conjugated into the aromatic ring.

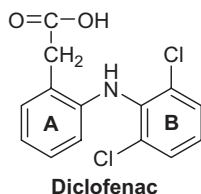


The rate constant is so low (Table 8.1, below that of benzene, Chapter 7, Table 7.1) that ozone addition may take place at the aromatic rings (one deactivated by chlorine, the other deactivated by the conjugated enamine that could act like a carbonyl function).

The metabolite of the antiviral drug Tamiflu<sup>®</sup>, oseltamivir carboxylate has been discussed in Chapter 6, because at the pH of wastewaters its ozone reactivity will be largely dominated by the C–C double bond and not by its amino group. Further nitrogen-containing antiviral drugs found in WWTP effluents are ribavirin, and nevirapine (Prasse *et al.*, 2010). For other antiviral drugs, besides Tamiflu<sup>®</sup>, see Chapter 6.



An abundant micropollutant is the nonsteroidal anti-inflammatory drug diclofenac. It is highly toxic (Henschel *et al.*, 1997) to aquatic life such as fish (Schwaiger *et al.*, 2004), but also to birds, and the dramatic decline in the vulture population on the Indian subcontinent has been attributed to diclofenac poisoning (Oaks *et al.*, 2004; Shultz *et al.*, 2004).



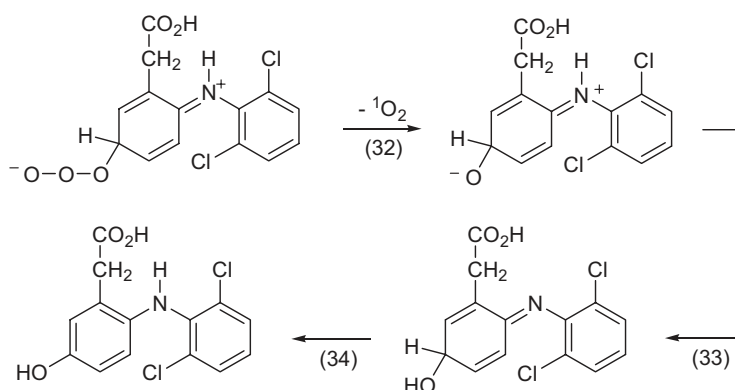
It reacts fast with ozone (Table 8.1) and is thus readily eliminated from drinking water and wastewater upon ozonation. Its ozone chemistry has found considerable attention (Vogna *et al.*, 2004; Sein *et al.*, 2008, 2009). Potential sites of ozone attack are the nitrogen but also the aromatic ring **A**. Both rings are activated by the imino group (cf. aniline), but ring **B** is deactivated by the two chlorines (Chapter 7). Amines and electron-rich aromatic compounds give rise to  $O_3^{\cdot-}$  and thus to  $\cdot OH$  radicals, and this is also observed

with diclofenac (Sein *et al.*, 2008) (Table 8.4). In the original paper, it has been suggested that it arises from the ozone adduct at nitrogen, but ozone attack at ring A would give the same result [cf. reaction (25)].

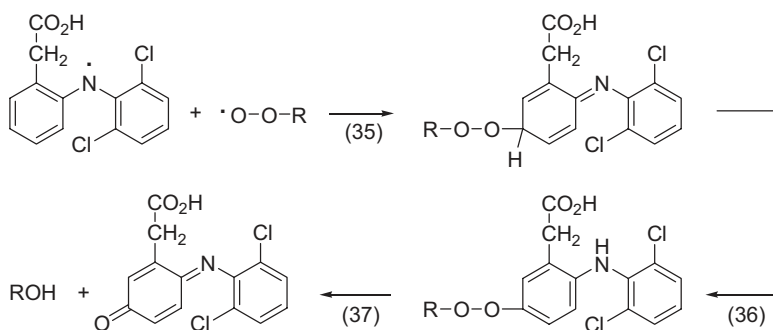
In absence of other  $\cdot\text{OH}$  scavengers,  $\cdot\text{OH}$  radicals will react with diclofenac. These reactions have been discussed (Sein *et al.*, 2008), but under wastewater or drinking water conditions they are scavenged by the water matrix (Chapter 3), and these reactions must then largely fall away.

The diclofenac radical cation is in equilibrium with the corresponding aminyl radicals [cf. equilibrium (26); for  $\text{p}K_{\text{a}}$  values of such intermediates see above], and these may interact with other radicals, notably peroxy radicals, present.

In competition with  $\text{O}_3^{\cdot-}$  elimination, the adduct can undergo  $^1\text{O}_2$  elimination [reaction (32)], and this leads to the formation of hydroxylated products [reactions (33) and (34)].

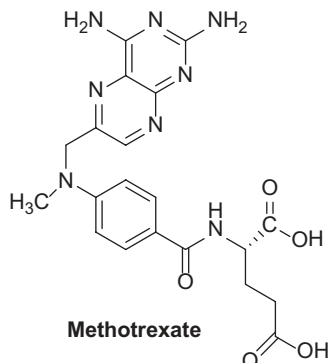


The reaction of the aminyl radical with peroxy radicals yields 1,5-diclofenaciminoquinone [reactions (35)–(37)].

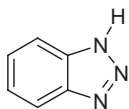


The consumption of diclofenac by ozone is rather low, and it has been suggested that this might be due to an ozone-consuming chain reaction that gives rise to no other products but  $\text{O}_2$  [cf. reactions (28) and (29)] (Sein *et al.*, 2009) (for the reactions of radicals with ozone see Chapter 13).

The cytostatic drug methotrexate also reacts rapidly with ozone (Table 8.1) and poses no problem in detoxifying waters with ozone (Garcia-Ac *et al.*, 2010).



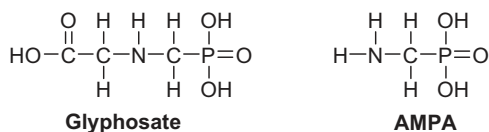
Benzotriazoles are widespread micropollutants (Cancilla *et al.*, 2003; Janna *et al.*, 2011). In Switzerland, they are, after EDTA, the second most abundant individual contaminants in many natural waters (Cancilla *et al.*, 2003; Voutsas *et al.*, 2006). Among other applications, benzotriazoles are used as corrosion inhibitors in dishwasher detergents and for de-icing of aircraft (Hart *et al.*, 2004; Weiss *et al.*, 2006). Benzotriazole acts as an inhibitor of the nitrification process (Callender & Davis, 2002). There are some studies on its reaction with ozone (Legube *et al.*, 1987; Vel Leitner & Roshani, 2010; Lutze *et al.*, 2011a; Müller *et al.* 2012). Its protonated form dominates below pH 1.6 and its deprotonated form above pH 8.2. The ozone rate constants strongly depend on its protonation state (Table 8.1).



**Benzotriazole**  
p*K*<sub>a</sub> = 1.6, 8.2

Similarly to the more simple aromatic compounds (Chapter 7), there is a good correlation of the standard Gibbs free energy of formation of ozone adducts to the ring with the logarithm of the rate constants on benzotriazole, its derivatives and their anions (Lutze *et al.*, 2011). The electron rich anions give rise to <sup>•</sup>OH (Table 8.4).

The herbicide glyphosate is an amine containing three acidic groups (one carboxylate and two phosphonate groups).

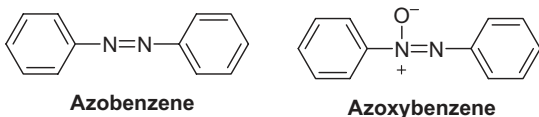


Thus, it is largely present as a zwitterion. Protonation at nitrogen must prevent a rapid reaction at pH 6.5, where it is degraded only slowly (Assalin *et al.*, 2010). AMPA is one of the ensuing products. At pH 10, degradation is more efficient and AMPA is also degraded in the course of reaction.

The triazine herbicide atrazine has been mentioned above. Due to its low ozone rate constant, atrazine is mainly degraded in DOM-containing water via the <sup>•</sup>OH route. These <sup>•</sup>OH-induced reactions are discussed in some detail in Chapter 14. For reviews on the degradation of herbicides by ozone and AOPs see (Ikehata & El-Din, 2005a, b).

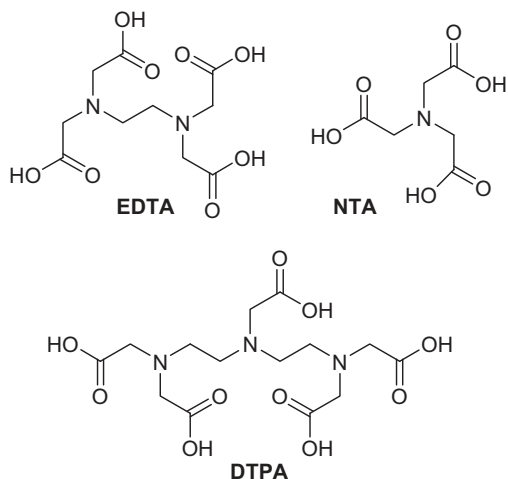
Azobenzene is a building block of azo dyes. It has a moderate reactivity with ozone (Table 8.1).





In its reactions with ozone, it gives rise to azoxybenzene (von Sonntag, unpublished). Azoxybenzene still retains some absorption in the visible region, and this may have to be taken into account when the discoloration of azo dyes by ozone is attempted (López-López *et al.*, 2007). For the oxidation of azo dyes by ozone in industrial wastewaters see Khadhraoui *et al.* (2009); Konsowa *et al.* (2010); Tabrizi *et al.* (2011) and references cited therein.

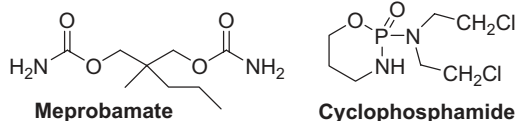
Abundant nitrogen-containing micropollutants are the complexing agents EDTA, NTA and DTPA.



Whenever the lone electron pair at nitrogen is not available for ozone attack by protonation or by complexation to a transition metal ion, the reactivity drops dramatically. A case in point is EDTA. It has  $pK_a$  values at 0.26, 0.96, 2.0, 2.7, 6.2 and 10.2. The latter two are relevant to protonation at nitrogen and this is reflected in the rate of ozone reaction (Figure 8.2). When both amino groups are free, the rate constant is  $3.2 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$  and it drops to  $1.6 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  when EDTA is monoprotonated. Further lowering the pH results in a drop of a factor of ten in the rate constant per pH unit. That is, the remaining ozone reactivity is only due to the concentration of free amine in equilibrium and fully protonated amines are practically non-reactive towards ozone. Complexation of EDTA by  $\text{Ca}^{2+}$  has only a small effect ( $k = 10^5 \text{ M}^{-1} \text{ s}^{-1}$  at pH 6), as  $\text{Ca}^{2+}$  is largely complexed by the carboxyl groups of EDTA [for a review on stability constants see Smith & Martell (1987); for the mechanism of the degradation of EDTA by  $\cdot\text{OH}$  see Höbel & von Sonntag (1998)]. In contrast, complexation by Fe(III), which involves also the lone electron pairs at the nitrogens, lowers the rate constant to  $330 \text{ M}^{-1} \text{ s}^{-1}$  at the same pH 6 (Muñoz & von Sonntag, 2000b). A similar effect was observed for the kinetics of the oxidation of DTPA. Complexation of DTPA with Fe(III) leads to a dramatic decrease of the ozone reaction rate constant relative to the free DTPA (Stemmler *et al.*, 2001). However, when the Fe(III)-hydroxo-DTPA complex is formed at  $\text{pH} > 6$  there is an increase in the rate of DTPA oxidation (Table 8.1). Therefore, DTPA can be quite readily degraded in the pH-range 7–8 of drinking and wastewaters.

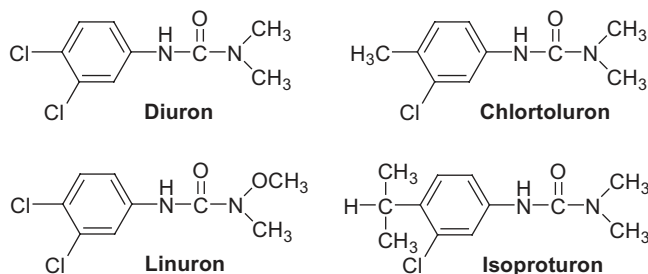
It has been mentioned above that the nitrogen in amides is not a target for ozone attack. Hence urethane-based micropollutants such as the sedative meprobamate and the cytostatic drug

cyclophosphamide are practically ozone-refractory (for cyclophosphamide see Table 8.1) and can only be eliminated by the  $\cdot\text{OH}$  route (cf. Chapters 3 and 14).



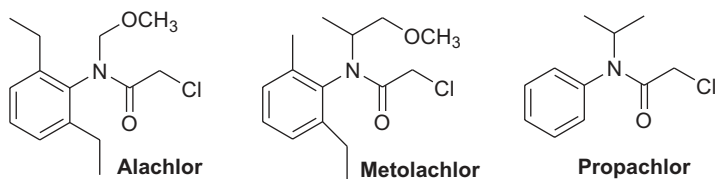
The ozone chemistry of the antibiotics tetracycline and vancomycin may be largely governed by an attack at the phenolic moieties and is discussed in Chapter 7, but there is also a secondary amino group that can serve as an additional site of ozone attack. Anatoxin-A and cylindrospermopsin contain a C–C double bond besides a secondary amine function and have been discussed in Chapter 6.

The phenylurea-derived herbicides diuron, chlortoluron, linuron and isoproturon react from slowly to moderately fast with ozone (Table 8.1; note the poor agreement among the reported rate constants). The nitrogens at the urea functions are non-reactive and, ozone addition to the aromatic ring (Chapter 7) is slow due to the chlorine functions at the ring.



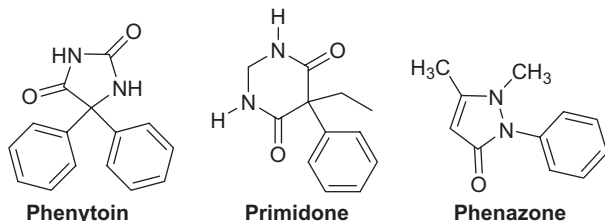
Although in wastewater diuron will be mainly degraded by the  $\cdot\text{OH}$  route, direct action of ozone also eliminates its toxicity. Some products have been determined, and their toxicity towards algae has been assessed (Mestankova *et al.*, 2011). The toxicity of diuron towards algae is completely eliminated by ozone and  $\cdot\text{OH}$  (Mestankova *et al.*, 2011).

In the acetamide-derived herbicides, alachlor, metolachlor and propachlor, the same principle governs their ozone reactivity (Table 8.1) as discussed for the phenylureas. For relative efficiencies of the degradation of herbicides by ozone see Ormad *et al.* (2010).



Amoxicillin ozonolysis is determined by its phenol group and discussed in Chapter 7.

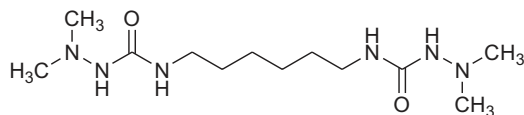
Further abundant micropollutants in wastewater are the antiepileptic drug phenytoin, the anticonvulsant primidone and the analgesic phenazone.



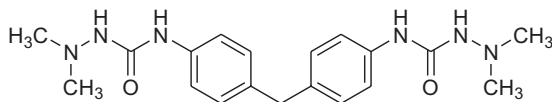
Primidone [ $k = 1.0 \text{ M}^{-1} \text{ s}^{-1}$ , Real *et al.* (2009)] and phenytoin have very low ozone reactivity (Lee & von Gunten, 2012). This has been demonstrated in the relative resistance of primidone to ozone degradation during full-scale wastewater treatment (Hollender *et al.*, 2009). For phenazone, a high reactivity with ozone can be expected due to the structural similarity to 4-dimethylaminoantipyrene (Table 8.1).

### 8.3.1 The *N*-Nitrosodimethylamine (NDMA) puzzle

*N*-Nitrosodimethylamine is a disinfection by-product, notably observed after chloramine disinfection (Mitch *et al.*, 2003; Choi & Valentine, 2002; Gerecke & Sedlak, 2003). In wastewater ozonation, the antiyellowing agents HDMS and TMDS have been recognised as NDMA precursors (Kosaka *et al.*, 2009).



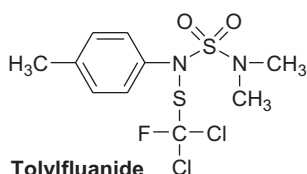
4,4'-Hexamethylenebis (1,1-dimethylsemicarbazide) (HDMS)



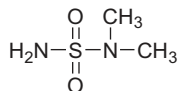
1,1,1',1'-Tetramethyl-4,4'-(methylene-di-*p*-phenylene)-disemicarbazide (TMDS)

For this suspected human carcinogen, a notification level of 10 ng/L has been published by the California Department of Public Health (NDMA, 2009). The standard for an excess lifetime cancer risk of  $10^{-5}$  for drinking waters was calculated to be 100 ng/L (WHO, 2004). For the same risk, bromate, another known ozonation by-product was calculated to be 3000 ng/L and bromoform, a known chlorination by-product 100,000 ng/L (WHO, 2004).

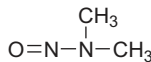
Also with ozone disinfection, NDMA can be a disinfection by-product. The fungicide tolylfluanide is hydrolytically and biologically degraded at pH 7 with a half-life of two days into dimethylsulfamide (DMS).



Tolylfluanide



Dimethylsulfamide (DMS)

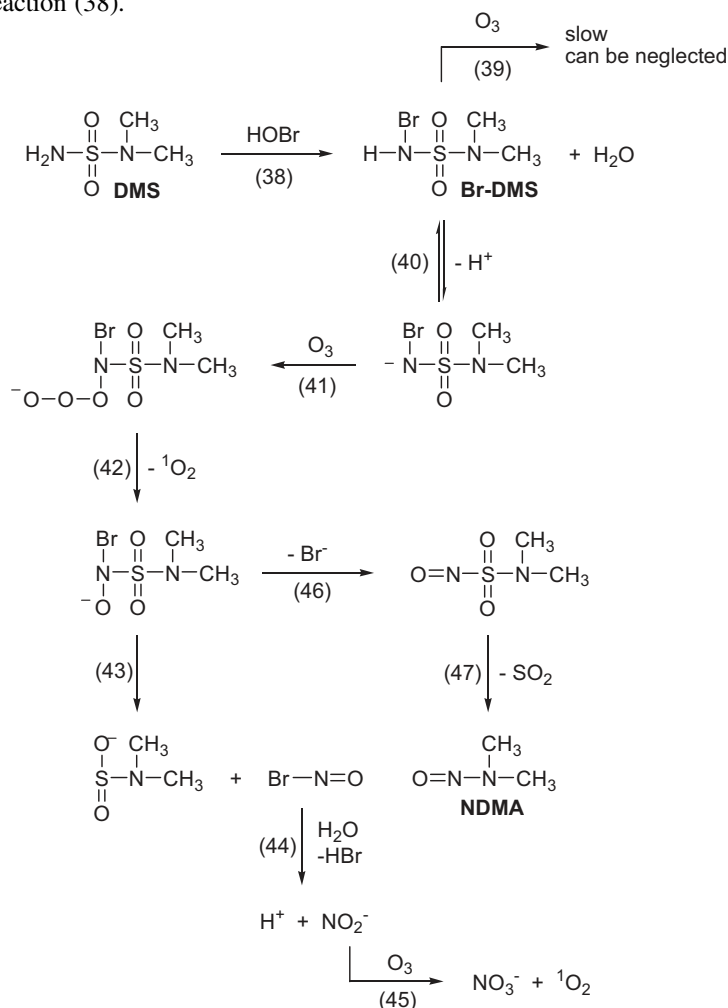


*N*-Nitrosodimethylamine (NDMA)

Due to its short half-life, tolylfluanide as such poses no problem, but its degradation product DMS has a much longer half-life, 50–70 days. In Germany for example, DMS concentrations of 100–1000 ng L<sup>-1</sup> and 50–90 ng L<sup>-1</sup> were detected in ground waters and surface waters, respectively. Its elimination by typical water treatment processes such as riverbank filtration, activated carbon filtration, treatment with permanganate, chlorine dioxide or UV-radiation proved to be ineffective (Schmidt & Brauch, 2008). DMS as such does not pose a problem. Ozonation of waters taken from areas where tolylfluanide had been used as fungicide in, e.g. strawberry cultivation led, however, to high NDMA levels (Schmidt & Brauch, 2008). This shows that NDMA, even though typically formed in small yields only, has to be monitored carefully. It is noteworthy that in most European countries the use of tolylfluanide is no longer allowed.

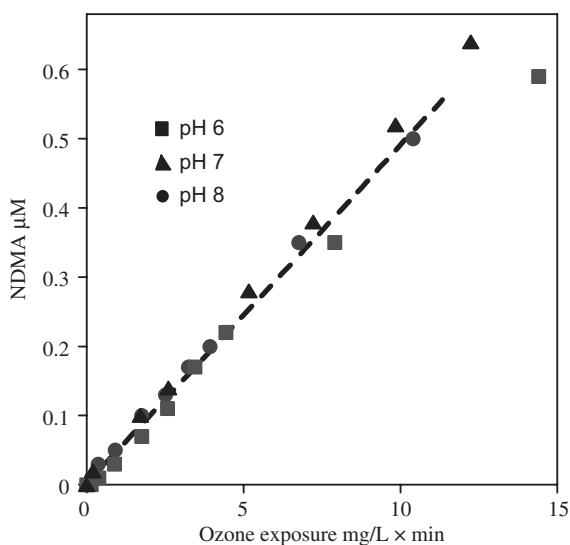
The reaction of ozone with DMS in distilled water does not yield NDMA. Br<sup>-</sup>, present in trace amounts in practically all waters, catalyses the formation of NDMA from DMS during ozonation (von Gunten *et al.*, 2010). Below, the present mechanistic concept of NDMA formation is discussed.

In the reaction of ozone with Br<sup>-</sup>, HOBr is formed (Chapter 11). This reacts with DMS according to reaction (38).



Brominated DMS (Br–DMS) reacts in its deprotonated form with ozone to an adduct [reactions (40) and (41)], and this loses singlet oxygen [reaction (42)]. The ensuing unstable intermediate can either lose nitroxyl bromide [reaction (43)] or, in competition, give rise to  $\text{Br}^-$  plus nitrosodimethylsulfamide [reaction (46)]. Nitroxyl bromide hydrolyses to nitric acid which is quickly oxidised to nitrate [reactions (44) and (45)]. Nitrosodimethylsulfamide undergoes an intramolecular rearrangement forming NDMA by  $\text{SO}_2$  extrusion [reaction (47)].

HOBr formation is the rate-limiting step in NDMA production (von Gunten *et al.*, 2010). Already  $\text{Br}^-$  concentrations in the order of  $10 \mu\text{g/L}$  are sufficient to catalyse this reaction. The formation of NDMA from DMS as a function of ozone exposure during ozonation of  $\text{Br}^-$ -containing waters is shown in Figure 8.4.

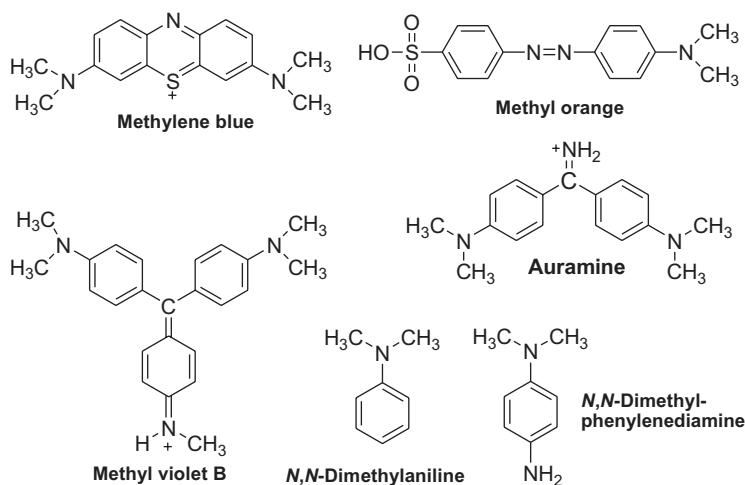


**Figure 8.4** NDMA formation upon ozonation of DMS- and  $\text{Br}^-$ -containing ultrapure water in the presence of 5 mM tBuOH as a function of the ozone exposure at pH 6 (squares), 7 (triangles), and 8 (circles). The ozone dose was 1 mg/L (20  $\mu\text{M}$ ), initial DMS and  $\text{Br}^-$  concentrations were 2.5 and 0.5  $\mu\text{M}$ , respectively. The dashed line is a kinetic simulation for the cumulative HOBr formation during ozonation at pH 8. Reprinted with permission from von Gunten *et al.* (2010). Copyright (2010) American Chemical Society.

In the pH range 6–8, NDMA formation is independent of pH in agreement with the ozone/ $\text{Br}^-$  reaction. The dashed line in Figure 8.4 shows the calculated rate of HOBr formation confirming that oxidation of  $\text{Br}^-$  is the rate-limiting step.

NDMA is also formed during ozonation of DMS in presence of HOCl with a lower yield of 20–30% (von Gunten *et al.*, 2010). This is, however, not a catalytic process, because  $\text{Cl}^-$ , which is released in the reaction of Cl–DMS with ozone, is only re-oxidised to a non-measurable extent to HOCl upon ozonation (Chapter 11).

DMS is not the only potential precursor of NDMA formation upon ozonation. In fact, some dyes that contain a dimethylamino function were reported to yield NDMA upon ozonation (Oya *et al.*, 2008).



The chemical yield of NDMA (in percentage of the target molecule consumed at excessive ozonation as it seems) were low, although the NDMA yields are sufficiently high to be of potential relevance (Table 8.5).

**Table 8.5** NDMA formation in the ozonation of some *N*-dimethyl groups containing compounds (0.5 mM) (Oya *et al.*, 2008)

Target compound	NDMA/ngL <sup>-1</sup>	Chemical yield/%
Methylene blue	310	$8.3 \times 10^{-3}$
Methyl orange	270	$7.2 \times 10^{-3}$
Methyl violet B	460	$1.2 \times 10^{-2}$
Auramine	480	$1.3 \times 10^{-2}$
Brilliant green	<5	$<1 \times 10^{-4}$
<i>N,N</i> -Dimethylformamide	13	$3.5 \times 10^{-4}$
<i>N,N</i> -Dimethylaniline	240	$6.4 \times 10^{-3}$
<i>N,N</i> -Dimethylphenylenediamine	1600	$4.3 \times 10^{-2}$

Dimethylamine can also yield NDMA upon ozonation (Yang *et al.*, 2009; Andrzejewski *et al.*, 2008). Also in this case, NDMA yields are extremely low (<0.01% at pH 7.5, ozone dose 66 mg/L). For such low chemical yields, mechanistic suggestions cannot be made, especially since NDMA cannot be a primary product. This raises the question as to how relevant these data are for ozone treatment of wastewaters containing dyes that have *N*-dimethylamino groups, but they are a most useful *caveat* to make one aware of the potential formation of NDMA.

# Chapter 9

## Reactions of sulfur-containing compounds

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### 9.1 REACTIVITY OF SULFUR-CONTAINING COMPOUNDS

Ozone reacts with sulfur compounds in their low oxidation states such as bisulfide/dihydrogen sulfide ( $\text{HS}^-/\text{H}_2\text{S}$ ) (Chapter 11), thiols (RSH) sulfides (RSR), disulfides (RSSR), sulfoxides ( $\text{R}_2\text{SO}$ ), sulfinic acids [ $\text{RS}(\text{O})\text{OH}$ ] and sulfite [ $\text{HOS}(\text{O})\text{O}^-$ ] (Chapter 11). All sulfur(VI) compounds (e.g. sulfate ion, organic sulfates and sulfonic acids) do not react with ozone. Reported rate constants are compiled in Table 9.1.

**Table 9.1** Compilation of ozone rate constants and singlet oxygen yields in percentage of ozone consumption (Muñoz *et al.*, 2001) of some organic sulfur-containing compounds. For inorganic sulfur-containing compounds see Chapter 11. For cephalixin see Chapter 6, for lincomycin see Chapter 8. Published rate constants are rounded to significant figures

Compound	pH	Rate constant $\text{M}^{-1} \text{s}^{-1}$	Singlet oxygen yield	Reference
Aldicarb	2.1	$4.4 \times 10^4$		Yao & Haag, 1991
	7.0	$4.3 \times 10^5$		
Cysteine		$4.2 \times 10^4$		Pryor <i>et al.</i> , 1984
		$3.0 \times 10^4$		Hoigné & Bader, 1983b
		$3.0 \times 10^4$		Hoigné & Bader, 1983b
anion		$2.4 \times 10^6$		Pryor <i>et al.</i> , 1984
Cystine	1	555		Hoigné & Bader, 1983b
	3.1	$1 \times 10^3$		
Dimethyl sulfoxide		8		Pryor <i>et al.</i> , 1984 Reisz <sup>(a)</sup>
		1.8 at 20 °C <sup>(a)</sup>		
<i>trans</i> -1,2-Dithiane-4,5-diol		$2.1 \times 10^5$	105	Muñoz <i>et al.</i> , 2001
1,4-Dithiothreitol	4.8		46	Muñoz <i>et al.</i> , 2001
	9		17	

(Continued)

**Table 9.1** Compilation of ozone rate constants and singlet oxygen yields in percentage of ozone consumption (Muñoz *et al.*, 2001) of some organic sulfur-containing compounds. For inorganic sulfur-containing compounds see Chapter 11. For cephalixin see Chapter 6, for lincomycin see Chapter 8. Published rate constants are rounded to significant figures (*Continued*)

Compound	pH	Rate constant $M^{-1} s^{-1}$	Singlet oxygen yield	Reference
EPTC (S-ethyl-N,N-dipropylthiocarbamate)		500 <sup>(b)</sup>		Chen <i>et al.</i> , 2008
Glutathione		$4 \times 10^6$		Pryor <i>et al.</i> , 1984
protonated, $pK_a = 8.75$		$2 \times 10^4$		Pryor <i>et al.</i> , 1984
bis(2-Hydroxyethyl) disulfide		$1.7 \times 10^5$		Muñoz <i>et al.</i> , 2001
Methanesulfinate		$2 \times 10^6$	96	Flyunt <i>et al.</i> , 2001a
Methionine		$1.8 \times 10^6$	104	Pryor <i>et al.</i> , 1984
Molinate		500 <sup>(b)</sup>		Chen <i>et al.</i> , 2008
Penicillin G	7	$4.8 \times 10^3$		Dodd <i>et al.</i> , 2010
Vydate (Oxamyl)	2–7	620		Yao & Haag, 1991

<sup>(a)</sup>  $\log A = 11.5$ ,  $E_a = 63 \text{ kJ mol}^{-1}$  [Reisz & von Sonntag (2011), unpublished results], <sup>(b)</sup> Estimated.

For thiols, rate constants increase upon deprotonation (cf. cysteine), and this is expected, as the higher electron density in the anion favours the attack by the electrophilic ozone. This effect is even more pronounced in the  $HS^-/H_2S$  system (Chapter 11). The reaction of sulfides is also very fast (cf. methionine). The rate constants for the reactions of uncharged disulfides such as *trans*-1,2-dithiane-4,5-diol bis(2-hydroxyethyl) disulfide are about  $2 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$ . Positively charged neighbouring groups such as in cystine at pH 3.1 and pH 1 dramatically reduce the rate of reaction. The rate constants of sulfoxides (cf. dimethyl sulfoxide) are low and this is of major importance for the elimination of the biological activity of penicillin G upon ozonation of wastewater (see below). In contrast to dimethyl sulfoxide, methylsulfinate reacts very fast with ozone.

Only some ozone adducts that are likely intermediates in the (dominating)  $^1O_2$  elimination reactions (for yields see Table 9.1) are sufficiently stable to calculate the Gibbs energy of adduct formation (see below). This prevents us from presenting a similar correlation of Gibbs energies of adduct formation with the logarithm of the rate constant as has been found for aromatic compounds (Chapter 7).

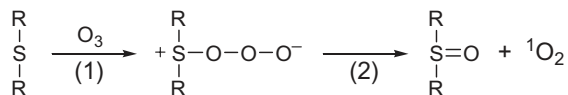
## 9.2 THIOLS

There is very little information as to the ozone reactions of thiols. In contrast to other sulfur-containing compounds that show singlet oxygen ( $^1O_2$ ) yields near 100% (Table 9.1), it is only near 50% for thiols and even less for thiolate ions (cf. 1,4-dithiothreitol, Table 9.1). In this respect, there is an analogy to  $HS^-/H_2S$  (Chapter 11). The understanding of the mechanism of the  $HS^-$  reaction increased considerably by quantum-chemical calculations, and it became apparent, that the ozone adduct can rearrange readily by transferring an O-atom in competition with the release of  $^1O_2$  (Mark *et al.*, 2011). If such a reaction were to proceed in thiols, sulfinic peracids would be the primary reaction products. Thus far, this is only speculation, and detailed studies would be required for substantiating this hypothesis.



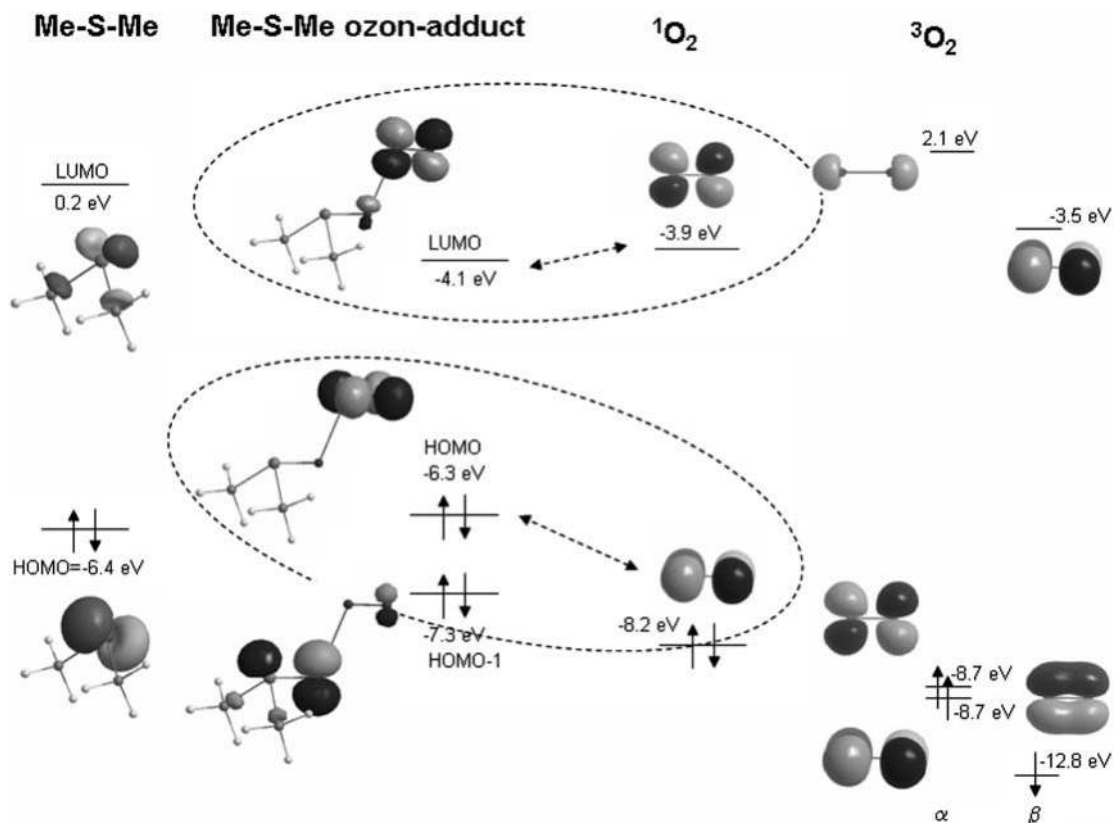
### 9.3 SULFIDES, DISULFIDES AND SULFINIC ACIDS

For sulfides, disulfides and sulfinic acids the singlet oxygen ( $^1\text{O}_2$ ) yield is unity (Table 9.1). This points to O-transfer as the only reaction, as shown in reactions (1) and (2) for a sulfide as an example.



With sulfides, the sulfoxide yield equals that of singlet oxygen, as has been shown for methionine (Muñoz *et al.*, 2001). With the disulfides *trans*-1,2-dithiane-4,5-diol disulfide and bis(2-hydroxyethyl) disulfide, the *S*-alkylsulfonates are the corresponding products (Mvula, 2002), and with methanesulfinic acid, methanesulfonic acid is also formed with a yield of unity (Flyunt *et al.*, 2001a). In the case of an electron transfer occurring as well, a chain reaction would set in (Flyunt *et al.*, 2001a). This is not observed.

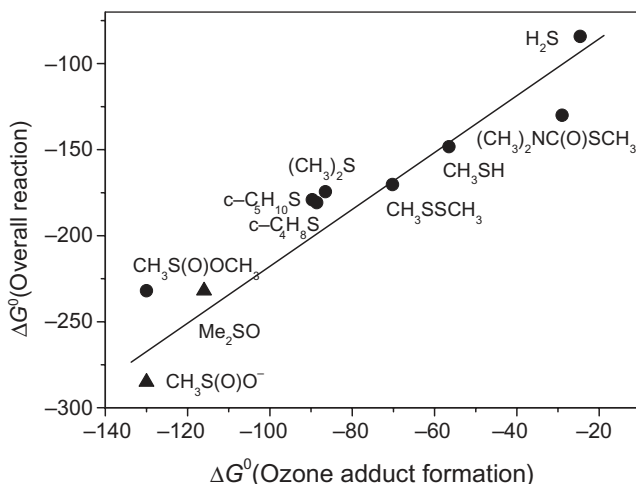
In DFT calculations [Naumov & von Sonntag (2010), unpublished results], ozone adducts were stable only for  $\text{H}_2\text{S}$ , methanethiol, the sulfides and dimethyl disulfide.



**Figure 9.1** Molecular orbitals of dimethyl sulfide, its ozone adduct, of singlet oxygen ( $^1\text{O}_2$ ) and triplet (ground state) oxygen ( $^3\text{O}_2$ ) according to Naumov & von Sonntag (2010), unpublished.

Some data for dimethyl sulfide are shown in Figure 9.1. The orbital of highest energy (HOMO, Highest Occupied Molecular Orbital) is at sulfur. This is the position where ozone adds to the molecule. In this adduct, the SO–OO bond is already very long (2.18 Å), and  $^1\text{O}_2$  is practically preformed. This can be seen from orbitals of the two outer oxygens (HOMO and LUMO, Lowest Unoccupied Molecular Orbital) that already have the symmetry and spin distribution of  $^1\text{O}_2$ . This differs substantially from that of  $^3\text{O}_2$  given for comparison. Moreover, the O–O bond length in  $^1\text{O}_2$  (1.205 Å) is very close to the SOO–O bond length in the adduct (1.233 Å), while the S–OOO bond length in the adduct is only marginally longer (1.558 Å) than that of the final product dimethyl sulfoxide (1.549 Å).

With dimethyl sulfoxide and methanesulfinate ion, the ozone adducts even decomposed on the way to optimising their structures, but shortly before this occurred single-point values indicated that their standard Gibbs free energies of adduct formation must be near  $-116 \text{ kJ mol}^{-1}$  and  $-178 \text{ kJ mol}^{-1}$ , respectively. With methyl methanesulfinate the adduct was also practically decomposed but the standard Gibbs free energy of adduct formation could still be calculated. There seems to be a correlation between the standard Gibbs free energy of the overall reaction and the standard Gibbs free energy of adduct formation (Figure 9.2). The value for the ozone adduct to  $\text{HS}^-$  has not been included, as the adduct is generally unstable and the value obtained was only a local minimum. In fact, O-transfer is only of minor importance, and the reaction proceeds in several directions, which are discussed in Chapter 11.



**Figure 9.2** Correlation of the standard Gibbs free energy of ozone adduct formation with the standard Gibbs free energy of the overall O-transfer reaction. Dimethyl sulfoxide and methylsulfinate ion (triangles) do not form stable adducts and the standard Gibbs free energy of adduct formation has been estimated by single-point calculations [Naumov & von Sonntag (2011), unpublished results].

Thus, in these reactions the adduct is often not a real intermediate but rather a transition state. This may happen, when the standard Gibbs free energy of the overall reaction exceeds about  $200 \text{ kJ mol}^{-1}$ .

It is tempting to speculate that in benzene and its derivatives the transition state in the formation of the adduct is very close to the adduct, and thus we observe an excellent correlation of the standard Gibbs free energy of adduct formation with the logarithm of the rate constant (Chapter 7). In the sulfur compounds, in contrast, we may have an early transition state, and the overall energetics as expressed by the standard Gibbs

free energy does not correlate with the rate of reaction. This is not without precedence. In the H-abstraction of alkyl radicals from thiols ( $R^\bullet + R'SH \rightarrow RH + R'S^\bullet$ ), the rate constant of reaction *increases with decreasing* energy gain of product formation (Reid *et al.*, 2002). This intriguing observation has been rationalised by a detailed quantum mechanical analysis of the reaction path, and it has been concluded that there must be an early transition state and that charge polarisation effects dominate the rate of reaction.

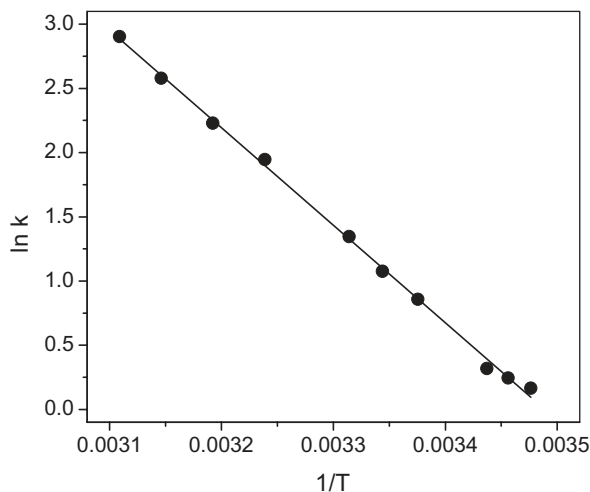
Dimethyl sulfoxide reacts only very slowly with ozone (Table 9.1) despite the high exergonicity of the overall reaction (Figure 9.2). An adduct sufficiently stable to account as an intermediate cannot be calculated (see above). It may be speculated that the oxygen withdraws much of the electron density at sulfur and the zwitterionic adduct with a positive charge at sulfur cannot be established.

## 9.4 SULFOXIDES

Sulfoxides react very slowly with ozone (Table 9.1). Thus as far as micropollutant abatement is concerned, these typical products of the reactions of sulfides must be considered as ozone-refractory. With dimethyl sulfoxide (DMSO), dimethyl sulfone is the only product detectable by  $^1\text{H}$  NMR analysis [Jarocki & von Sonntag (2011), unpublished results]. Quantum-chemical calculations indicate that there is indeed a high likelihood for this reaction [Naumov & von Sonntag (2010), unpublished results].

Due to its low ozone rate constant and its high  $\bullet\text{OH}$  rate constant, dimethyl sulfoxide (DMSO) can be used to detect and quantify  $\bullet\text{OH}$  yields in ozone reactions (Chapter 14).

Because, for the determination of  $\bullet\text{OH}$  in ozone reaction, the rate constant of ozone with DMSO is crucial for setting up adequate competition conditions, its ozone rate constant has been re-determined [Reisz & von Sonntag (2011), unpublished results]. According to the new data, the earlier value ( $8 \text{ M}^{-1}\text{s}^{-1}$ , Table 9.1) seems to be on the high side. In Figure 9.3, an Arrhenius plot for the reaction of ozone with DMSO is given.



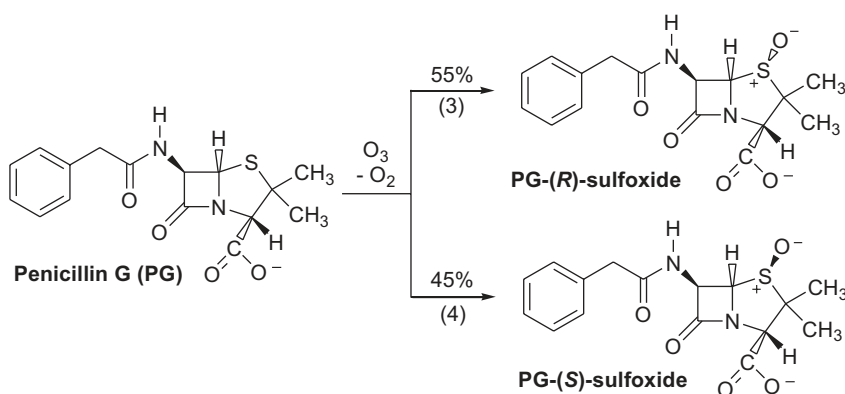
**Figure 9.3** Arrhenius plot for the reaction of ozone with dimethyl sulfoxide according to Reisz & von Sonntag (2011), unpublished results.

This yields  $k = 1.8$  at  $20^\circ\text{C}$  ( $\log A = 11.5$ ,  $E_a = 62 \text{ kJ mol}^{-1}$ ). The Hammond–Leffler postulate assumes early transition states for strongly exergonic reactions, and data shown in Figure 9.2 indicate that this situation may be met in the DMSO/ozone reaction. The fact that the reaction is nevertheless slow is due

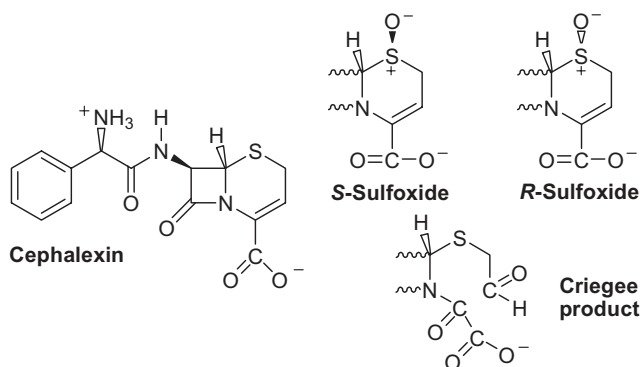
to the high activation energy. Similarly high activation energies are observed in ozone reactions with C–H functions (Chapter 10).

## 9.5 MICROPOLLUTANTS CONTAINING AN OZONE-REACTIVE SULFUR

The ozone-reactive site in the antibacterial agent penicillin G is its sulfide function. Adequately substituted sulfoxides are chiral, and with penicillin G two enantiomeric sulfoxides are formed, the *R*-isomer dominating over the *S*-isomer in a 55/45 ratio [reactions (3) and (4)]. The *R*-isomer is the energetically preferred product (Naumov & von Sonntag, 2012, unpublished quantum-chemical calculations). Practically no other products are formed (Dodd *et al.*, 2010).



Similarly, the main products of cephalexin, which belongs to the group of cephalosporin antibiotics are the *R*- and *S*-sulfoxides.

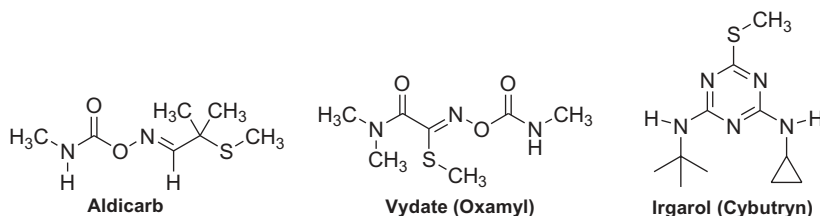


However, the C–C double bond is another site of attack, and thus the Criegee product (Chapter 6) is also of importance here. In principle, the amino group could also be a third site of ozone attack, but at pH 7, where these experiments were carried out, it is largely protonated. At a higher pH, the amino group must be another site of attack (for the pH dependence of different ozone-reactive groups see Chapter 2). At pH 7,  $k_{obs}$  is reported as  $8.7 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$ , and at this pH amines would react an order of magnitude more slowly (Chapter 8). A material balance of the initially formed products shows that the *R*-sulfoxide dominates ( $\sim 34\%$ ) over the *S*-sulfoxide ( $\sim 18\%$ ). The Criegee product ( $\geq 28\%$ ) plus a hydrolysed Criegee product

(~5%) are formed in a somewhat lower but comparable yield. This indicates that the observed rate constant must be due to about equal contributions of the reactivity of the sulfide function and the C–C double bond.

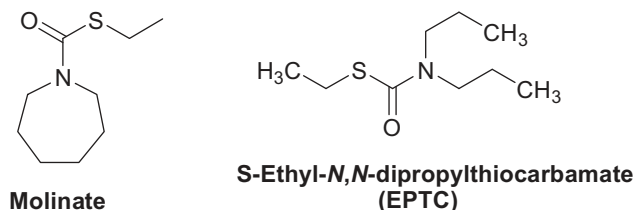
With penicillin G,  $k_{obs}$  is only  $4.8 \times 10^3 \text{ M}^{-1}\text{s}^{-1}$  at pH 7. One would thus have to conclude that the sulfide function in the five-membered ring is less reactive than in the six-membered ring.

The insecticides aldicarb and vydate and the antifouling agent (algicide) irgarol have sulfide groups which are the primary sites of ozone attack (Table 9.1). It is expected that mainly the corresponding sulfoxides are formed in these reactions.



The antibiotic lincomycin has two potential sites of ozone attack, a sulfide group and the tertiary nitrogen in the five-membered ring. Because the reaction rate is largely controlled by the tertiary amine at near-neutral pH, lincomycin ozonolysis is discussed in Chapter 8. The antibiotic amoxicillin contains a sulfide function, but also amine and phenolic groups. It is the ozone chemistry of the latter that dominates its degradation (Chapter 7).

The thiocarbamate herbicides molinate and EPTC have been estimated to react moderately fast with ozone (Table 9.1).



The reaction may lead by O-transfer to the corresponding sulfinylamides. Details are as yet not known.

# Chapter 10

## Compounds with C–H functions as ozone-reactive sites

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### 10.1 REACTIVITY OF COMPOUNDS WITH C–H FUNCTIONS AS OZONE-REACTIVE SITES

The title compounds react generally so slowly with ozone that in pollutant abatement they are typically called “ozone refractory”. Yet, within this generally low reactivity there is a spread in their ozone rate constants of seven orders of magnitude (Table 10.1).

**Table 10.1** Compilation of ozone rate constants of compounds containing only C–H functions as reactive sites. Published rate constants are rounded to significant figures

Compound	pKa	pH	$k/M^{-1} s^{-1}$	Reference
Acetate ion			$<3 \times 10^{-5}$	Hoigné & Bader, 1983b
Acetic acid	4.75		$\leq 3 \times 10^{-5}$ $<1 \times 10^{-6}$	Hoigné & Bader, 1983b Sehested et al., 1992
Acetone			$3.2 \times 10^{-2}$	Hoigné & Bader, 1983a
Bromoform			$\leq 2 \times 10^{-2}$	Hoigné & Bader, 1983a
1-Butanol		2	0.6	Pryor <i>et al.</i> , 1984
2-Butanone		2	0.7	Hoigné & Bader, 1983a
Butyrate ion			$\leq 6 \times 10^{-3}$	Hoigné & Bader, 1983b
Butyric acid	4.8		$\leq 6 \times 10^{-3}$	Hoigné & Bader, 1983b
Carbon tetrachloride			$<5 \times 10^{-3}$	Hoigné & Bader, 1983a
Chloroform			$\leq 0.1$	Hoigné & Bader, 1983a
Cyclopentanol		2	2.0	Hoigné & Bader, 1983a
Dichloromethane			$\leq 0.1$	Hoigné & Bader, 1983a
Diethyl ether		2	1.1	Hoigné & Bader, 1983a
Diethyl malonate		2	0.06	Hoigné & Bader, 1983a
1,4-Dioxane			0.32	Hoigné & Bader, 1983a
Ethanol			0.45	Pryor <i>et al.</i> , 1984
			0.37	Hoigné & Bader, 1983a

(Continued)

**Table 10.1** Compilation of ozone rate constants of compounds containing only C–H functions as reactive sites. Published rate constants are rounded to significant figures (*Continued*)

Compound	pKa	pH	$k/M^{-1} s^{-1}$	Reference
Formaldehyde			0.1	Hoigné & Bader, 1983a
Formate ion <sup>(a)</sup>			$100 \pm 20$	Hoigné & Bader, 1983b
no additive <sup>(b)</sup>			82	Reisz & von Sonntag, 2011
with tBuOH <sup>(c)</sup>			46	Reisz & von Sonntag, 2011
Formic acid	3.75		very low	Hoigné & Bader, 1983b
Geosmin			0.1	Peter & von Gunten, 2007
Glucose		2	0.45	Hoigné & Bader, 1983a
Glutarate ion			$(8 \pm 2) \times 10^{-3}$	Hoigné & Bader, 1983b
Glutaric acid	4.3, 5.4		$< 8 \times 10^{-3}$	Hoigné & Bader, 1983b
Glyoxylate ion			$1.9 \pm 0.2$	Hoigné & Bader, 1983b
Glyoxylic acid	3.2		$0.17 \pm 0.4$	Hoigné & Bader, 1983b
Malonate ion			$7 \pm 2$	Hoigné & Bader, 1983b
Malonic acid	2.8, 5.7		$< 4$	Hoigné & Bader, 1983b
Methanol			$\sim 0.02$	Hoigné & Bader, 1983a
2-Methylisoborneol			0.35	Peter & von Gunten, 2007
2-Methyl-2-propanol (tertiary Butanol)			$\sim 3 \times 10^{-3}$	Hoigné & Bader, 1983a
			$1.1 \times 10^{-3(d)}$	Reisz & von Sonntag, 2011
Octanal			$8 \pm 0.8$	Hoigné & Bader, 1983a
1-Octanol			$\leq 0.8$	Hoigné & Bader, 1983a
Oxalate dianion (Oxalic acid)	1.2, 4.2		$\leq 4 \times 10^{-2}$	Hoigné & Bader, 1983b
2-Pentanone			$\sim 0.02$	Hoigné & Bader, 1983a
Pivalate ion			$2 \times 10^{-3}$	Pryor <i>et al.</i> , 1984
Pivalic acid	5.03		$< 1 \times 10^{-3}$	Pryor <i>et al.</i> , 1984
Propanal			2.5	Hoigné & Bader, 1983a
1-Propanol			0.37	Hoigné & Bader, 1983a
2-Propanol			1.9	Hoigné & Bader, 1983a
			1.9	Pryor <i>et al.</i> , 1984
			$0.83^{(e)}$	Reisz & von Sonntag, 2011
Propionate ion			$(1 \pm 0.5) \times 10^{-3}$	Hoigné & Bader, 1983b
Propionic acid	4.9		$< 4 \times 10^{-4}$	Hoigné & Bader, 1983b
Propyl acetate			0.03	Hoigné & Bader, 1983a
Succinate ion			$(3 \pm 1) \times 10^{-2}$	Hoigné & Bader, 1983b
Succinic acid	4.2, 5.6		$< 3$	Hoigné & Bader, 1983b
Sucrose			0.012	Hoigné & Bader, 1983a
			0.05	Pryor <i>et al.</i> , 1984
Tetrahydrofuran			6.1	Pryor <i>et al.</i> , 1984

<sup>(a)</sup>In the presence of 2-propanol as •OH scavenger, <sup>(b)</sup>at 20°C,  $\log A = 10.88$ ,  $E_a = 50.3 \text{ kJ mol}^{-1}$ , <sup>(c)</sup>tBuOH as •OH scavenger, at 20°C,  $\log A = 11.36$ ,  $E_a = 54.6 \text{ kJ mol}^{-1}$ , <sup>(d)</sup>at 20°C,  $\log A = 9.30$ ,  $E_a = 68.7 \text{ kJ mol}^{-1}$ , <sup>(e)</sup>at 20°C,  $\log A = 12.51$ ,  $E_a = 70.7 \text{ kJ mol}^{-1}$ .

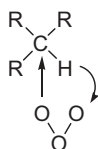
For the ozone reactions of formate ion, 2-propanol and tertiary butanol (2-methyl-2-propanol, tBuOH) A factors and activation energies have been determined (Table 10.1). For formate ion, data in the presence of tBuOH show that scavenging  $\bullet\text{OH}$  radicals not only lowers the observed rate constant, but also enhances the activation energy (Section 10.3). The importance of  $\bullet\text{OH}$  radicals in such systems is discussed below, but similar effects are expected for other compounds such as alcohols and ethers, but information is more difficult to obtain for these because of their lower rate constants (unfavourable competition conditions).

## 10.2 GENERAL MECHANISTIC CONSIDERATIONS

For the reaction of ozone with compounds that have only C–H functions as reactive sites, such as methane, three primary reactions have been considered: (i) H-abstraction [reaction (1)], (ii) hydride transfer [reaction (2)], and (iii) insertion [reaction (3)] (Nangia & Benson, 1980; Giamalva *et al.*, 1986). For aqueous solutions, one may even add electron transfer [reaction (4)].

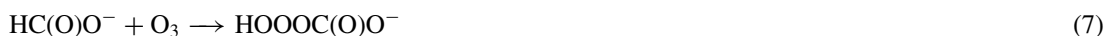


With methane as a model substrate that must react very slowly with ozone (rate constant not available, but may be similar to or lower than tertiary butanol, Table 11.1), quantum chemical reactions have been carried out [Naumov & von Sonntag, (2011), unpublished]. H-abstraction [reaction (1)], is mildly endergonic ( $\Delta G^0 = +20 \text{ kJ mol}^{-1}$ ). Hydride transfer [reaction (2)] is markedly endergonic ( $\Delta G^0 = +150 \text{ kJ mol}^{-1}$ ) as is electron transfer [reaction (4),  $\Delta G^0 = +254 \text{ kJ mol}^{-1}$ ]. While reactions (1), (2) and (4) are mechanistically straightforward, insertion, reaction (3), is somewhat problematic. In the transition state (cf. Figure 10.1), the carbon has to become pentavalent, and the transfer of the hydrogen is related to the H-abstraction reaction (1). Although reaction (3) is the most exergonic of these reactions,  $\Delta G^0 = -168 \text{ kJ mol}^{-1}$ , there may be a considerable activation energy that would make this reaction slow. This may generally hold for insertion reactions which are all highly exergonic,



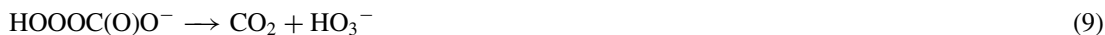
**Figure 10.1** Likely transition state in the insertion reaction.

The formate ion reacts fastest within this group of compounds, and here one may write reactions (5)–(8).





Compared to methane, the calculated energetics are now very different. For the H-abstraction reaction (5), a standard Gibbs free energy of  $-32 \text{ kJ mol}^{-1}$  has been calculated. Hydride transfer is now highly exergonic [reaction (6),  $\Delta G^0 = -249 \text{ kJ mol}^{-1}$ ]. The insertion reaction (7) continues to be exergonic [ $\Delta G^0 = -239 \text{ kJ mol}^{-1}$ ]. An electron transfer remains endergonic [reaction (8),  $\Delta G^0 = +43 \text{ kJ mol}^{-1}$ ], but is no longer dramatically so when compared to methane [reaction (4)]. Interestingly, the insertion product is sufficiently stable to account as an intermediate. Its decay into the final products [reaction (9),  $\Delta G^0 = -61 \text{ kJ mol}^{-1}$ ] is exergonic, as expected.



These calculations indicate that it will not be possible for this group of compounds to come up with a uniform reaction mechanism for the primary step as in the case of olefins and, at least to a large extent, for aromatic compounds (Chapters 6 and 7). H-abstraction and electron transfer [cf. reactions (1), (4), (5) and (8) give rise to  $\text{HO}_3^*/\text{O}_3^{*-}$  and hence to  $\bullet\text{OH}$  (Chapter 11)]. There are ways of quantifying  $\bullet\text{OH}$  in ozone reactions (Chapter 14), and use has been made of this for addressing the importance of these radical-forming processes.

Hydride transfer [cf. reactions (2) and (5)] has been favoured by Benson (Nangia & Benson, 1980), while the Plesnicar and Pryor groups (Plesnicar *et al.*, 1998; Giamalva *et al.*, 1986) suggest that H-abstraction [cf. reactions (1) and (5)] dominates. It will be shown below that both processes seem to contribute to varying extents based on the few preliminary data that are available at present (formate ion, 2-propanol and tertiary butanol). As long as H-abstraction contributes to a significant extent, the observed rate constant must correlate with the C–H bond dissociation energy (BDE). Such a correlation can inherently not be perfect, as the contribution of H-abstraction varies from compound to compound, but at least the order of magnitude will be approximately correct.

A plot of the logarithm of the rate constant vs. the standard Gibbs free energies ( $\Delta G^0$ ) for H-transfer should then give a straight line. For this plot, formate ion, 2-propanol, ethanol, methanol and tertiary butanol (tBuOH) have been selected (Table 10.2 and Figure 10.2).

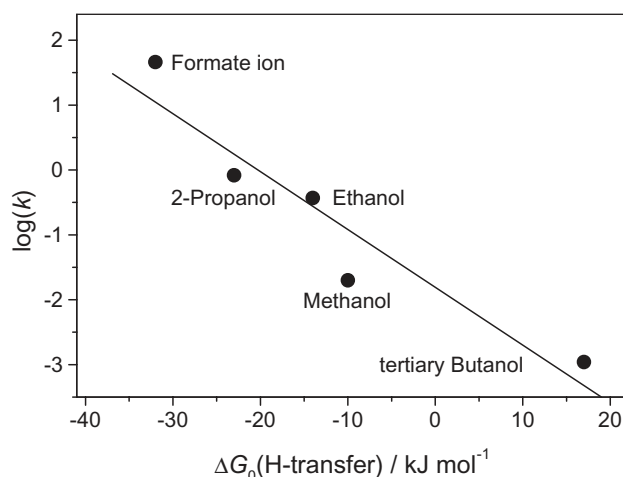
**Table 10.2** Rate constants of ozone with some saturated alcohols and the formate ion (Table 10.1) and calculated standard Gibbs free energies for H-abstraction by ozone [Naumov & von Sonntag (2011), unpublished] as well as some available BDEs (von Sonntag, 2006) of the relevant C–H bonds

Compound	$k/\text{M}^{-1} \text{ s}^{-1}$	$\Delta G^0$ (H-abstraction)/ $\text{kJ mol}^{-1}$	BDE $\text{kJ mol}^{-1}$
H–C(O)O <sup>−</sup>	46	−32	
H–C(CH <sub>3</sub> ) <sub>2</sub> OH	0.83	−23	393
H–C(CH <sub>3</sub> ,H)OH	0.4	−14	396
H–CH <sub>2</sub> OH	0.02	−10	402
H–CH <sub>2</sub> C(CH <sub>3</sub> ) <sub>2</sub> OH	0.001	+17	423 <sup>a</sup>

<sup>a</sup>Taken from the value for ethane.

If it is correct that H-abstraction and hydride transfer are the main competing ozone reactions for C–H compounds in aqueous solution, their rate constants must be similar and, as a consequence, kinetic parameters that determine H-abstraction seem to also determine hydride transfer to a similar extent. These ideas are presented here to elicit further research. Quite obviously, the approach outlined above is

an oversimplification. For example, the acetate ion reacts much slower with ozone than tBuOH (Table 10.1) although the C–H BDE (calculated at  $\Delta G^0 = +14 \text{ kJ mol}^{-1}$ ) is lower (consider mesomeric stabilisation of the ensuing radical) than that of tBuOH. Yet, in this respect, ozone shares this surprising effect with the much more reactive  $\bullet\text{OH}$  radical [ $k(\bullet\text{OH} + \text{acetate}) = 8 \times 10^7 \text{ M}^{-1}\text{s}^{-1}$ ,  $k(\bullet\text{OH} + \text{tBuOH}) = 6 \times 10^8 \text{ M}^{-1}\text{s}^{-1}$  (Buxton *et al.*, 1988)]. Thus, factors beyond mere BDEs play a role in H-abstraction reactions.

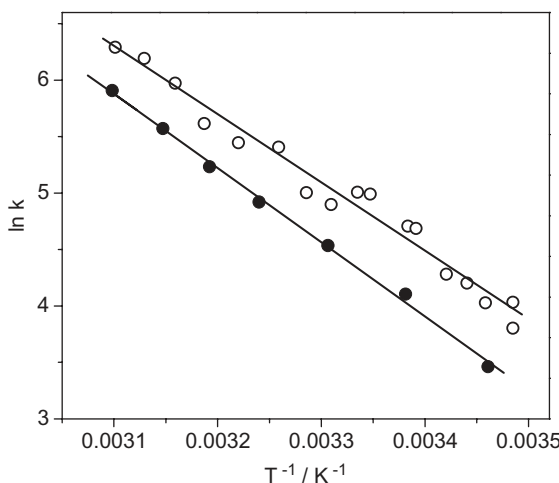


**Figure 10.2** Plot of the logarithm of the rate constants for the reactions of ozone with formate ion, 2-propanol, ethanol, methanol and tertiary butanol vs. the calculated standard Gibbs free energy for H-transfer from the substrate to ozone.

There is a host of data regarding the products in the reactions of ozone with neat substrates or in carbon tetrachloride solutions (Bailey, 1982; Plesnicar *et al.*, 1976, 1991, 1998, 2000; Cerkovnik & Plesnicar, 1983, 1993, 2005; Koller *et al.*, 1990; Koller & Plesnicar, 1996; Kovac & Plesnicar, 1979; Murray *et al.*, 1970), but the information regarding their reactions in aqueous solution is meagre. Presently, information on the ozone chemistry of compounds containing only C–H functions as ozone reactive sites (carboxylic acids, alcohols, carbonyl compounds) is very limited, and data using excessive ozonation (Niki *et al.*, 1983) cannot be used for elucidating mechanistic aspects. One may be tempted to transfer mechanistic concepts derived in non-polar environments to aqueous solutions, but, as will be shown, the presence of water has a dramatic effect on the rates of some reactions. To this point, one of us (CvS) together with two younger colleagues (Erika Reisz and Alexandra Jarocki) has carried out some experiments on the formate ion, 2-propanol and tertiary butanol and these, as yet unpublished, data now allow us to put the ozone chemistry of C–H reactive sites into perspective.

### 10.3 FORMATE ION

Of all C–H reactive compounds, ozone reacts fastest with the formate ion (Table 10.1). Upon addition of the  $\bullet\text{OH}$  scavenger tBuOH,  $k_{\text{obs}}$  is lowered (Table 10.1), and the observed activation energy is higher ( $54.6 \text{ kJ mol}^{-1}$ ) than in the absence of tBuOH ( $50.3 \text{ kJ mol}^{-1}$ ) (Table 10.1 and Figure 10.3).



**Figure 10.3** Arrhenius plot for the reaction of ozone with the formate ion (open circles) and in the presence of the  $\bullet\text{OH}$  scavenger tBuOH (closed circles, [formate ion] = 10–100  $\mu\text{M}$ , [tBuOH] = 0.2 M) [Reisz & von Sonntag (2011) unpublished results].

The yield of free  $\bullet\text{OH}$  is near 40% (Reisz *et al.*, 2012a). There are two conceivable reactions that could lead to  $\bullet\text{OH}$  radicals, that is, to their precursors  $\text{HO}_3^\bullet/\text{O}_3^\bullet$  [reactions (5) and (8)]. For the H-abstraction reaction (5), a standard Gibbs free energy of  $-32 \text{ kJ mol}^{-1}$  has been calculated, while electron transfer (8) is endergonic,  $\Delta G^0 = +43 \text{ kJ mol}^{-1}$ . Of these two conceivable reactions, the exergonic reaction is favoured here. H-abstraction reactions may be connected with considerable activation energies, and it is not surprising that reaction (5) is slow despite the exergonicity of the reaction.

Cage recombination (reaction of  $\text{CO}_2^{\bullet-}$  with  $\text{HO}_3^\bullet$ ) will lower the free  $\bullet\text{OH}$  yield. The efficiency of cage recombination depends on the recombination rate constants of the radicals involved. With  $\bullet\text{OH}$ , for example, it is high ( $k = 5.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ), while for  $\text{SO}_4^{\bullet-}$  it is much lower ( $k = 8 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ). As a consequence, the free  $\bullet\text{OH}$  yield in the photolysis of  $\text{H}_2\text{O}_2$  is 1.0 at room temperature (Legrini *et al.*, 1993), while in the photolysis of peroxodisulfate the free  $\text{SO}_4^{\bullet-}$  yield is 1.4 (Mark *et al.*, 1990). Upon increasing the temperature, the viscosity of water is lowered, the  $\text{SO}_4^{\bullet-}$  radicals diffuse even more freely into the bulk solution, and at  $50^\circ\text{C}$  the quantum yield of free  $\text{SO}_4^{\bullet-}$  approaches the maximum value of 2.0. With respect to the radicals formed in reactions (5) and (8), one has to consider that the competing reactions (10) and (11) occur on the  $10^{-12} \text{ s}$  timescale [cf.  $\text{p}K_a(\text{HO}_3^\bullet) = -2.0$ , Chapter 13], while the timescale of cage reactions is in the order of  $10^{-9} \text{ s}$ .



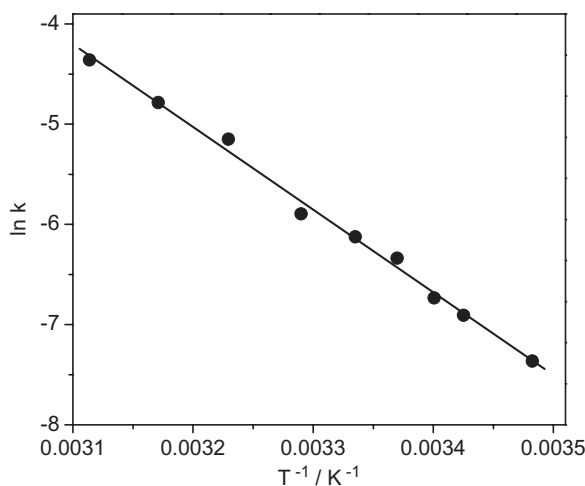
Reactions  $\text{O}_3^{\bullet-} + \text{O}_3^{\bullet-}$  ( $k = 9 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ) and  $\text{CO}_2^{\bullet-} + \text{CO}_2^{\bullet-}$  ( $k = 5 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ) are relatively slow, and  $k(\text{O}_3^{\bullet-} + \text{CO}_2^{\bullet-})$  may be similar, while the reaction  $\bullet\text{OH} + \text{CO}_2^{\bullet-}$  may be as fast as  $\bullet\text{OH} + \bullet\text{OH}$ . Thus, cage recombination efficiency may be close to or even less than that of  $\text{S}_2\text{O}_8^{2-}$  photolysis. Based on this, the free  $\bullet\text{OH}$  yield is not far from 57% for total radical formation if one assumes the same cage escape efficiency as in  $\text{S}_2\text{O}_8^{2-}$  photolysis (Reisz *et al.*, 2012a).

With this, the free-radical generating reactions (5) [plus (8)] are important processes, but certainly not the only ones. There must be non-radical processes such as (6) and (7) that contribute about as much to the primary reaction

as the free-radical reactions. Neglecting the insertion reaction (7), leaves hydride transfer (6) as the competing reaction. The hydride transfer is highly exergonic ( $\Delta G^0 = -249 \text{ kJ mol}^{-1}$ ), yet the observed reaction is slow. This can be reconciled considering that in the transition state the strong solvation of the formate ion disappears while that of  $\text{HO}_3^-$  has to build up. As far as products are concerned, hydride transfer and insertion are indistinguishable. With tertiary butanol, however, these two processes give rise to very different products, and hydride transfer has been shown to be by far the dominating process (see below). In analogy, it is also favoured here.

## 10.4 2-METHYL-2-PROPANOL (TERTIARY BUTANOL)

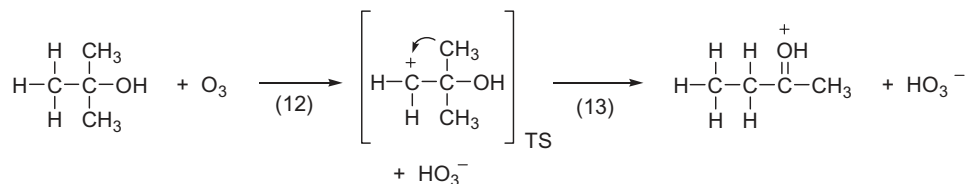
Tertiary butanol (tBuOH) reacts with ozone nearly five orders of magnitudes more slowly than the formate ion (Table 10.1). From the data in Figure 10.4, an activation energy of  $E_a = 68.7 \text{ kJ mol}^{-1}$  is calculated.



**Figure 10.4** Arrhenius plot for the reaction of ozone with tertiary butanol (1 M) (Reisz *et al.*, 2012a).

At a tBuOH concentration of 1 M, formaldehyde (7%), acetone (9%) and methyl ethyl ketone (92%) have been quantified (Reisz *et al.*, 2012a). While formaldehyde and acetone are typical  $\bullet\text{OH}$ -induced products (Chapter 14), methyl ethyl ketone is not formed via free-radical reactions.

Upon trying to calculate the standard Gibbs free energy for hydride transfer, the quantum-chemical calculations proceeded automatically to protonated methyl ethyl ketone by a methyl shift [reaction (12)/(13)]. The carbocation depicted in reaction (12) is not an intermediate in this reaction. It is a transition state, at the best, *en route* to the products [reaction (13);  $\Delta G^0(12)/(13) = -114 \text{ kJ mol}^{-1}$ ].



Protonated ketones are very strong acids, the  $\text{p}K_a$  value of protonated acetone is given as  $-3.06$  (Bagno *et al.*, 1995), and protonated methyl ethyl ketone is also only a very short-lived intermediate. Insertion of ozone into tBuOH yielding  $\text{HOOCH}_2\text{C}(\text{CH}_3)_2\text{OH}$  is strongly exergonic ( $\Delta G^0 = -145 \text{ kJ mol}^{-1}$ ). This

potential intermediate would most likely decay into  $\text{HO}_2^\bullet$  and  $^\bullet\text{OCH}_2\text{C}(\text{CH}_3)_2\text{OH}$  ( $\Delta G^0 = -17 \text{ kJ mol}^{-1}$ ) rather than release of  $\text{HO}_3^-$  ( $\Delta G^0 = +31 \text{ kJ mol}^{-1}$ ). This renders insertion as a route to methyl ethyl ketone unlikely.

Compared to hydride transfer, H-abstraction is minor [reaction (14),  $\Delta G^0 = +17 \text{ kJ mol}^{-1}$ ].



As  $\text{HO}_3^\bullet$  is converted to  $^\bullet\text{OH}$  that again abstracts a hydrogen from tBuOH, two  $^\bullet\text{CH}_2\text{C}(\text{CH}_3)_2\text{OH}$  radicals are generated by one primary event (for details of the ensuing chemistry see Chapter 14). This closes the product balance (ozone vs. products) shown above, which is only seemingly above 100%.

## 10.5 2-PROPANOL

Detailed information on the ozonolysis of 2-propanol in organic solvents is available, and data in aqueous solution have recently been obtained [Reisz *et al.* (2011), unpublished results]. The difference between product yields in organic solvents and in water is remarkable, and first the results of studies in an organic solvent are discussed.

With 2-propanol in acetone- $d_6$ ,  $\text{H}_2\text{O}_3$  and the  $\alpha$ -hydroxyalkylhydrotrioxide were detected by low-temperature  $^{17}\text{O}$ -NMR (Table 10.3) in a 1:2 ratio (Plesnicar *et al.*, 1998). The final products (1 M in methyl-*t*-butyl ether) are compiled in Table 10.4.

**Table 10.3**  $^{17}\text{O}$ -NMR shifts ( $\delta$ ) of  $(\text{CH}_3)_2\text{C}(\text{OH})\text{OOOH}$ ,  $\text{H}_2\text{O}_3$  and  $\text{H}_2\text{O}_2$  in acetone- $d_6$  at  $-10^\circ\text{C}$ .  $\delta$  Values in ppm downfield of the internal standard  $\text{H}_2^{17}\text{O}$ . According to Plesnicar *et al.* (1998)

Compound	$\delta\text{O}^1$	$\delta\text{O}^2$	$\delta\text{O}^3$
$(\text{CH}_3)_2\text{C}(\text{OH})\text{O}^1-\text{O}^2-\text{O}^3-\text{H}$	368	445	305
$\text{H}-\text{O}^1-\text{O}^2-\text{O}^3-\text{H}$	305	421	305
$\text{H}-\text{O}^1-\text{O}^2-\text{H}$	187	187	

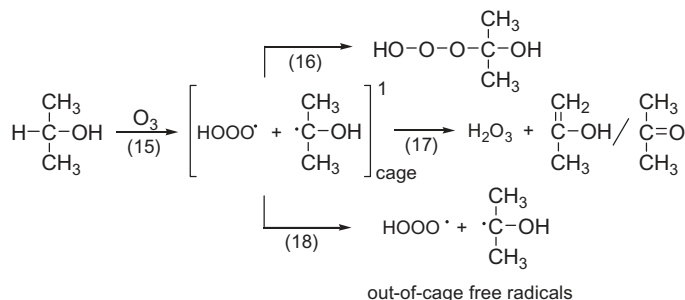
**Table 10.4** Ozonolysis of 2-propanol (1 M in methyl-*t*-butyl ether) at  $-78^\circ\text{C}$ . Product determination after warming. Material balance as by GC/MS and NMR (sum of all products = 100%) (Plesnicar *et al.*, 1998) and in aqueous solution [Jarocki *et al.* (2011), preliminary unpublished results]. Material balance based on ozone consumed

Product	Organic solvent	Water
Acetone	$37 \pm 5$	88
Acetic acid	$39 \pm 5$	3.6
Acetic peracid	$11 \pm 2$	
Formic acid	$7 \pm 2$	
Formaldehyde (as hemiacetal)	$5 \pm 1$	
Formaldehyde		3.9
$\text{H}_2\text{O}_2$	$11 \pm 3$	n.d.

n.d.: not determined

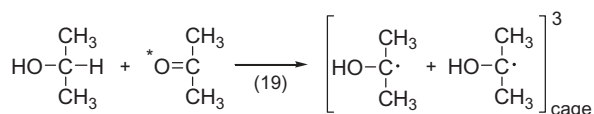
In the organic solvent, there is, however, a major material balance deficit of one-carbon compounds (formaldehydeispropylacetal plus formic acid, 12%) vs. two-carbon products (acetic acid plus acetic peracid, 50%). This could be due to the fact that GC without derivatisation is not a reliable method for determining formaldehyde. Assuming that the missing one-carbon compound is formaldehyde, one may follow the proposed mechanistic suggestions (Plesnicar *et al.*, 2000) with some additions.

It has been suggested that ozone reacts as an H-abstracter. This would create a radical pair that is held together for a short time by the solvent cage, where it can react by combination or disproportionation. Such reactions are shown here for the 2-propanol system [reactions (15)–(18)].

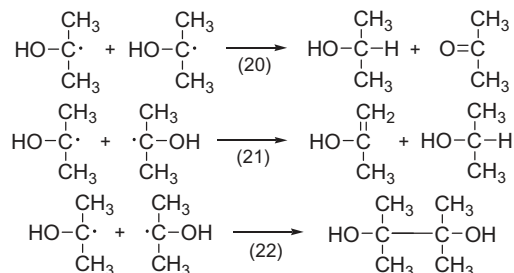


Evidence for the formation of the enol of acetone (2-hydroxypropene) is obtained from experiments with 2-propanol deuterated at methyl, where deuterium is incorporated into the  $\text{H}_2\text{O}_3$  formed.

Preferred H-transfer from the methyl groups as compared to the OH group is typical for the disproportionation of the 2-hydroxymethyl radical (von Sonntag, 1969; Blank *et al.*, 1975). This is an amusing reaction in so far as it follows, as so often in free-radical chemistry, Ostwald's step rule, that is, the thermodynamically less favoured product, here the enol of acetone, is formed preferentially [ $\Delta G^0(2\text{-hydroxypropene} \rightarrow \text{acetone}) = -69 \text{ kJ mol}^{-1}$ , Naumov, private communication]. In the photolysis of acetone in the presence of 2-propanol, two 2-hydroxyprop-2-yl radicals are formed within the solvent cage [reaction (19)].

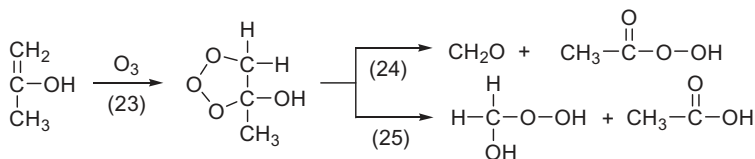


As this reaction is caused by triplet acetone, the multiplicity of the ensuing radical pair is also triplet. This prevents a ready recombination/disproportionation in the cage, as activation energy is required for their reaction as the crossing over point triplet  $\rightarrow$  singlet is at higher energies. Thus most radicals will diffuse out of the cage, and it is mainly the reaction of the free radicals that accounts for the products [reactions (20)–(22)].



An analysis of the data using 2-propanol- $d_6$  as a reactant indicated that  $k_{\text{CH}}/k_{\text{OH}} = 3.3$  and  $k_{\text{CH}}/k_{\text{recomb}} = 3.4$  (Blank *et al.*, 1975).

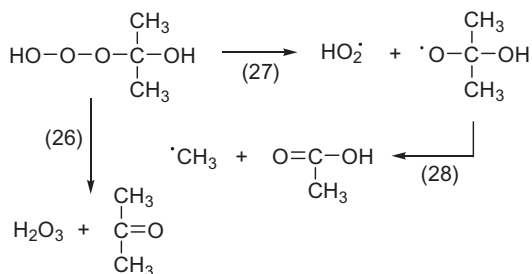
In the above ozone plus 2-propanol reaction (15), the radical pair has singlet multiplicity, and compared to the excited acetone plus 2-propanol reaction (19), there is no barrier for the cage reaction. Thus, enol (2-hydroxypropene) formation is most likely a cage reaction [cf. reaction (17)]. In the ozonolysis of 2-propanol in an organic solvent, ozonolysis of 2-hydroxypropene is believed to compete with the transformation of enol-acetone (2-hydroxypropene) to acetone (Plesnicar *et al.*, 1998), and it has been suggested that acetic peracid and formic acid may result from this reaction (Plesnicar *et al.*, 2000). Based on what has been reported in Chapter 6 for aqueous solutions, one may suggest reactions (23)–(25).



The electron-withdrawing OH substituent at the C–C double bond will drive the reaction preferentially toward reaction (25) if vinyl chloride (Chapter 6) is a good guide, that is, acetic acid will be favoured over acetic peracid, as observed (Table 10.4).

Formic acid is not accounted for in this scheme. Yet, formic acid may result from the reaction of acetic peracid with formaldehyde considering the reaction of acetic peracid with acetaldehyde (Schuchmann & von Sonntag, 1988).

In competition, the radicals may diffuse out of the cage [reaction (18)]. Here, the viscosity of the solvent is of major importance, and at low temperatures, where the solvent is more viscous, cage reactions will be strongly favoured. In these reactions, the above-mentioned products would be formed. The  $\alpha$ -hydroxyalkylhydrotrioxide, in analogy to hemiacetals and the  $\alpha$ -hydroxyalkylhydroperoxides mentioned in Chapter 6, may decompose into  $\text{H}_2\text{O}_3$  plus acetone [reaction (26)].



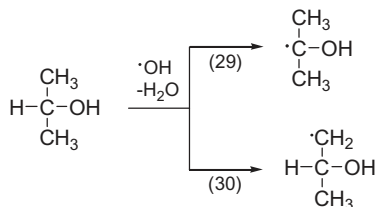
For this reaction, there is low-temperature NMR evidence (Plesnicar *et al.*, 1998). In competition, in analogy to tetroxides (von Sonntag & Schuchmann, 1997; von Sonntag, 2006), the  $\alpha$ -hydroxyalkylhydrotrioxide may undergo homolytic cleavage into  $\text{HO}_2\cdot/\text{O}_2^{\cdot-} + \text{H}^+$  and an oxyl radical [reaction (27)]. In accordance with this, a standard Gibbs free energy of  $\Delta G^0 = +9 \text{ kJ mol}^{-1}$  has been calculated for the decay of  $\text{CH}_3\text{OOOH}$  into  $\text{CH}_3\text{O}\cdot + \text{HO}_2\cdot$  (O–O bond length  $1.438\text{\AA}$ ), while the competing decay into  $\text{CH}_3\text{OO}\cdot + \cdot\text{OH}$  (O–O bond length  $1.427\text{\AA}$ ) is considerably more endergonic ( $\Delta G^0 = +48 \text{ kJ mol}^{-1}$  (Naumov & von Sonntag 2011, unpublished). The ensuing  $\beta$ -fragmentation [reaction (28)] will be very fast, cf. Chapter 14.

This reaction would also account for acetic acid and formaldehyde. The latter is a major product in the reaction of the methyl radical with  $\text{O}_2$  (Schuchmann & von Sonntag, 1984) (note that formic acid is also a minor product). The decay of the  $\alpha$ -hydroxyalkylhydrotrioxide into acetone and  $\text{H}_2\text{O}_3$  is sped-up in the

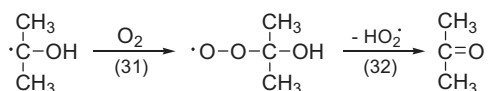
presence of water, and it is conceivable that oxyl radical formation is minor in water compared to 2-propanol in an organic solvent, as  $\text{H}_2\text{O}_3$  elimination [reaction (26)] and oxyl radical formation followed by  $\beta$ -fragmentation [reactions (27) and (28)] are competing reactions (note that  $\beta$ -fragmentation products are not observed with D-glucose, see below).

According to this mechanistic concept, one of the primary products is the  $\text{HO}_2^\bullet$  radical [reaction (18)]. It readily decomposes into  $\bullet\text{OH}$  plus  $\text{O}_2$  [reaction (11)] (for details see Chapter 13).

Thus, any  $\text{HO}_2^\bullet$  that escapes the cage will induce  $\bullet\text{OH}$  reactions. For 2-propanol, they are well documented. Reaction (29) is preferred over reaction (30) in a 4:1 ratio (Asmus *et al.*, 1973).



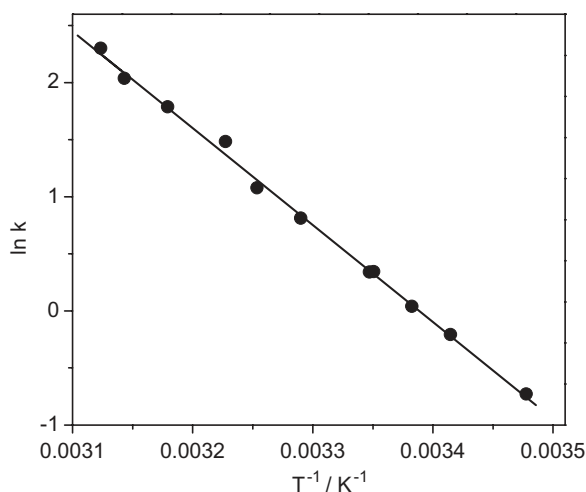
Both radicals thus formed react rapidly with  $\text{O}_2$  [e.g. reaction (31)].



The  $\alpha$ -hydroxyalkylperoxyl radical eliminates (in water)  $\text{HO}_2^\bullet$  [reaction (32),  $k = 650 \text{ s}^{-1}$  (Bothe *et al.*, 1977)]. The  $\text{OH}^-$ -induced  $\text{O}_2^{\bullet-}$  elimination is diffusion-controlled ( $k = 10^{10} \text{ M}^{-1}\text{s}^{-1}$ ). The other 2-propanol-derived peroxyl radical decays bimolecularly (for details see Chapter 14).

The question now arises as to what extent the above reactions also dominate the ozonolysis of 2-propanol in water.

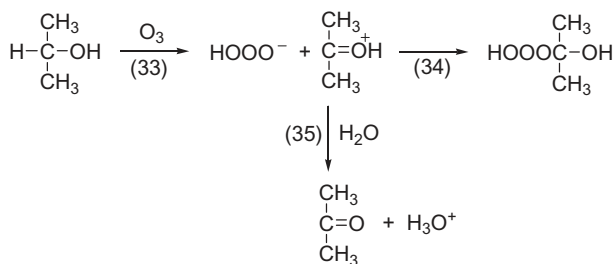
The reaction of ozone with 2-propanol in water requires an activation energy of  $E_a = 70.7 \text{ kJ mol}^{-1}$  ( $\log A = 12.51$ , for an Arrhenius plot see Figure 10.5).



**Figure 10.5** Arrhenius plot for the reaction of ozone with 2-propanol in water [Reisz & von Sonntag, 2011, unpublished results].



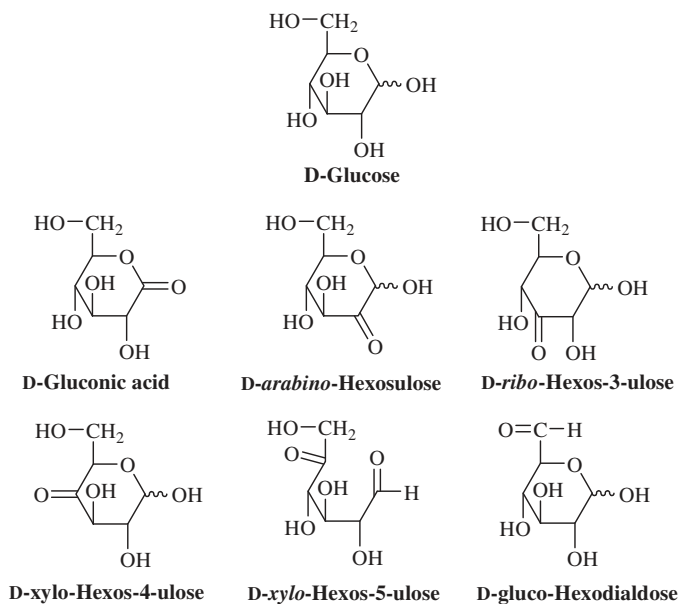
The formaldehyde yield is low, 3.9% with respect to ozone consumption, and is enhanced to 5.4 in the presence of an excess of tBuOH, that is, when  $\bullet\text{OH}$  radicals are scavenged by tBuOH ([2-propanol] = 0.1 M, [tBuOH] = 1 M; efficiency of  $\bullet\text{OH}$  scavenging by tBuOH = 75%; efficiency of ozone scavenging by tBuOH = 1%). The difference of 1.7% points to a free  $\bullet\text{OH}$  yield of 3.4% (for a discussion of the use of tBuOH in the determination of  $\bullet\text{OH}$  in ozone reactions see Chapter 14). This is the minimum value of H-abstraction in this system. It could double if the cage recombination product [cf. reaction (16)] would decompose homolytically [reaction (27)] rather than eliminate  $\text{H}_2\text{O}_3$  according to reaction (26). Note, that the liberation of  $\text{HO}_2\bullet$  would give rise to  $\text{O}_2^{\bullet-}$ , which would react with ozone yielding  $\bullet\text{OH}$  (for details see Chapters 11 and 13). Thus in aqueous solution, H-abstraction can be  $\sim 7\%$  at the most. This is now in agreement with the formate and tBuOH systems where other, non-radical processes compete (formate, tBuOH) or even dominate (tBuOH). With tBuOH, insertion could be excluded, and all data would be compatible with a hydride transfer. For 2-propanol, one would then write reactions (33)–(35).



In reaction (33) an intimate ion pair is formed that, in principle, could recombine [reaction (34)]. Protonated acetone formed in reaction (33) is, however, a very strong acid [ $\text{p}K_{\text{a}} = -3.06$  (Bagno *et al.*, 1995)], and deprotonation (35) must compete very effectively. Reaction (33) is very exergonic ( $\Delta G^0 = -160 \text{ kJ mol}^{-1}$ ). The energy difference between acetone and its enol is  $-69 \text{ kJ mol}^{-1}$ . This leaves ample room for the enol being formed as well in analogy with what has been discussed for H-abstraction [cf. reaction (17)]. The formaldehyde yield is matched by that of acetic acid. As discussed above, their formation could be due to an ozonolysis of the enol [reaction (23)], or a decomposition of the hydrotrioxide [reaction (27) and subsequent reactions]. In the presence of  $\text{OH}^-$ , the enol lifetime is reduced and thus its ozonolysis suppressed. Indeed, the acetate yield drops to 10% of its former value when ozonolysis is carried out at pH 10. As  $\text{OH}^-$  would also enhance the rate of hydrolysis of the hydrotrioxide into  $\text{H}_2\text{O}_3$  and acetone [reaction (25)], a distinction between these two mechanistic possibilities cannot be made. Assuming that additional ozone is required for the ozonolysis of the acetone enol, the material balance is fair ( $\sim 96\%$ ).

## 10.6 CARBOHYDRATES

In the reaction with D-glucose, ozone attacks all six C–H sites leading to the corresponding two-electron oxidised products (Schuchmann & von Sonntag, 1989). Their structures are shown in Figure 10.6, and their yields are compiled in Table 10.5.

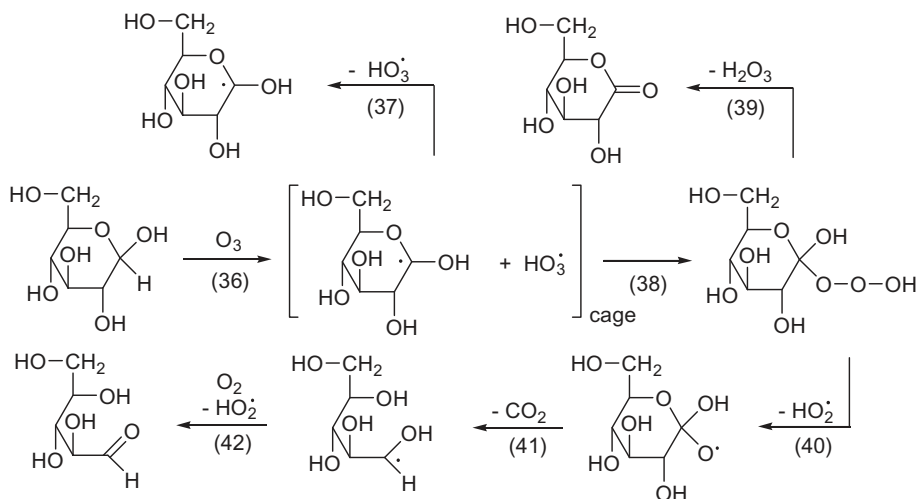


**Figure 10.6** Glucose and its ozone products.

**Table 10.5** Products and their yields (in percent age of ozone/ $\cdot\text{OH}$  radicals) of the reaction of D-glucose ( $4 \times 10^{-3}$  M) with ozone and  $\cdot\text{OH}$  radicals ( $\gamma$ -radiolysis in  $\text{N}_2\text{O}/\text{O}_2$ -saturated solution) at pH 6.5. Tertiary butanol (tBuOH, 0.1 M) has been added in one set of experiments for scavenging 90% of the  $\cdot\text{OH}$  radicals (Schuchmann & von Sonntag, 1989)

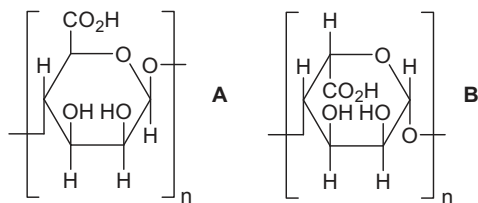
Product	Ozone	Ozone/tBuOH	$\cdot\text{OH}$ Radicals
D-Gluconic acid	30	67	21
D-arabino-Hexosulose	17	12	17
D-ribo-Hexos-3-ulose	9	7	11
D-xylo-Hexos-4-ulose	9	5	10
D-xylo-Hexos-5-ulose	5	2	8
D-gluco-Hexodialdose	30	6	32
Sum	93	65	90

Addition of tBuOH, which scavenges 90% of the  $\cdot\text{OH}$  radicals formed in these reactions, lowers the total yield of carbohydrate products from 93% to 65%. The effect of  $\cdot\text{OH}$  can be read from the data obtained by  $\gamma$ -radiolysis in  $\text{N}_2\text{O}/\text{O}_2$ -saturated solution. One notices that these radicals are not very selective as far as the C–H sites are concerned, and the relatively high yield of D-gluco-hexodialdose is largely due to the fact that C6 carries two hydrogens. In contrast, the distribution in the  $\cdot\text{OH}$ -scavenged system shows a marked preponderance with respect to an attack at C1, which carries the weakest bound hydrogen. D-Arabinose is not among the products, and other carbohydrates containing five carbon atoms are also not formed. This indicates that oxyl radicals and ensuing  $\beta$ -fragmentations [cf. reactions (40)–(42)] do not occur.



The release of H<sub>2</sub>O<sub>3</sub> [cf. reaction (39)] terminates the reaction as H<sub>2</sub>O<sub>3</sub> decomposes into H<sub>2</sub>O and O<sub>2</sub> without giving rise to free radicals (see below). Reaction (37), however, yields an •OH radical, and this reacts rapidly with glucose. The glucose radicals react with O<sub>2</sub> and the peroxy radicals thus formed release HO<sub>2</sub>•/O<sub>2</sub>•<sup>-</sup> [for the kinetics see Bothe *et al.* (1978)]. As O<sub>2</sub>•<sup>-</sup> reacts rapidly with O<sub>3</sub> yielding further radicals, a chain reaction is induced (note the similarities of product distribution of ozone without a scavenger and  $\gamma$ -radiolysis). The scavenging data do not lead to a firm conclusion as to the primary •OH yield for reactions such as reaction (37), but 15% may be a good guess. Based on more recent information, the original interpretation of the glucose data (Schuchmann & von Sonntag, 1989) had to be somewhat modified as shown above. Based on the above, competing reactions could be analogous to those discussed above for formate ion and for 2-propanol.

Alginic acids are polysaccharides consisting mainly of 1,4-linked  $\beta$ -D-manuronic acid (**A**) and varying amounts of 1,4-linked  $\alpha$ -L-guluronic acid (**B**).



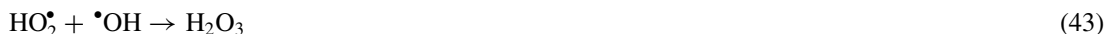
Upon reacting with ozone, chain breaks are formed with an efficiency of 18% (Akhlaq *et al.*, 1990). This is mainly due to the formation of •OH (see above). With alginic acid, radiolytically generated •OH causes chain breakage with an efficiency of 22% and O<sub>2</sub>•<sup>-</sup> release with an efficiency of 73%. The reactions of carbohydrates with •OH have been reviewed (von Sonntag, 1980; von Sonntag & Schuchmann, 2001).

## 10.7 DIHYDROGEN TRIOXIDE – PROPERTIES OF A SHORT-LIVED INTERMEDIATE

In the above reactions, dihydrogen trioxide, H<sub>2</sub>O<sub>3</sub>, is an important, albeit short-lived, product. It has also been quoted as a reactive intermediate in other contexts (Wentworth Jr *et al.*, 2001, 2003; Czapski &

Bielski, 1963, 1970; Xu & Goddard III, 2002; Fujii *et al.*, 1997; Engdahl & Nelander, 2002; Lesko *et al.*, 2004), hence it seems worthwhile to report what is known thus far about this interesting intermediate, notably its fate in aqueous solution.

In water [“slightly acidic”, as acids are formed (Plesnicar *et al.*, 2000)], the lifetime of  $\text{H}_2\text{O}_3$  is much shorter (estimated at 20 ms) than in organic solvents (16 min) (Plesnicar, 2005). More detailed information for the reactions of  $\text{H}_2\text{O}_3$  in aqueous solution, is available from pulse radiolysis experiments (Czapski & Bielski, 1963; Bielski, 1970).  $\text{H}_2\text{O}_3$  has been generated in acidic,  $\text{O}_2$ -saturated solutions. Under such conditions  $\text{HO}_2^\bullet$  and  $^\bullet\text{OH}$  are generated in a 1 : 0.8 ratio. Their bimolecular reaction gives rise to  $\text{H}_2\text{O}_3$  [reaction (43)].



This short-lived intermediate decays  $\text{H}^+$ -catalysed [reaction (44),  $k = 6 \text{ M}^{-1}\text{s}^{-1}$ ] and as anion,  $\text{HO}_3^-$ , in equilibrium [reaction (45)].

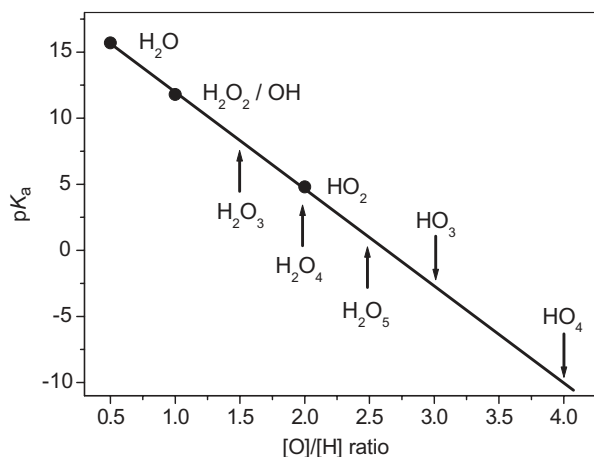


The  $\text{p}K_a$  value of  $\text{H}_2\text{O}_3$  [reaction (45)] can be estimated from relationship (47) (Bielski & Schwarz, 1968).

$$\text{p}K_a(\text{H}_x\text{O}_y) = 19 - 7([\text{O}]/[\text{H}]) \quad (47)$$

The decay of  $\text{HO}_3^-$  according to reaction (46), that is, even with the release of  ${}^1\text{O}_2$  is exergonic [ $\Delta G^0 = -51 \text{ kJ mol}^{-1}$ ,  $\text{HO}-\text{OO}^-$  distance 1.482 Å,  $\text{HOO}-\text{O}^-$  distance 1.402 Å, Naumov and von Sonntag (2011), unpublished results]. The much higher solvation energy of  $\text{OH}^-$  as compared to  $\text{HO}_3^-$  will contribute substantially to the exergonicity of this reaction.

From relationship (47), the  $\text{p}K_a$  value of  $\text{H}_2\text{O}_3$  is calculated as 8.5. A plot of this relationship is shown in Figure 10.7.



**Figure 10.7** Plot of  $\text{p}K_a$  values of  $\text{H}_x\text{O}_y$  compounds as a function of the H/O ratio according to relationship (47). The  $\text{p}K_a$  values of  $\text{H}_2\text{O}$ ,  $^\bullet\text{OH}$ ,  $\text{H}_2\text{O}_2$  and  $\text{HO}_2^\bullet$  are experimental values. From Merényi *et al.*, 2010b. Copyright Wiley-VCH Verlag. Reproduced with permission.

It allows one to also estimate the  $pK_a$  values of other  $H_xO_y$  intermediates such as  $HO_3^*$ ,  $H_2O_4$ , and so on that are of interest in the chemistry of ozone in aqueous solution. The validity of this plot has been confirmed by calculating the  $pK_a$  of  $HO_3^*$  using a thermodynamic cycle (Naumov & von Sonntag, 2011b).

The ratio of  $k_{-45}/k_{45}$  has been given as  $1720 M^{-1}$  (Czapski & Bielski, 1963), and taking  $k_{-45} = 10^{10} M^{-1}s^{-1}$  (Eigen, 1963), the intrinsic decay rate of  $HO_3^-$  must be near  $6 \times 10^6 s^{-1}$ . This rather long lifetime has been taken as a hint that reaction (46) may even give rise to triplet (ground state)  $O_2$ , that is, a spin conversion without a heavy atom effect may take place (Sein *et al.*, 2007). This suggestion was based on the report that in the ozonolysis of 2-propanol in water (note that 2-propanol is likely to also give rise to  $H_2O_3$  in water) no singlet oxygen signal could be recorded (Muñoz *et al.*, 2001). Inspection of these data shows that the 2-propanol concentration chosen, although 500 times the ozone concentration, was possibly too low for arriving at a firm conclusion. At an ozone concentration of  $1 \times 10^{-4} M$ , the 2-propanol concentration would have been  $5 \times 10^{-2} M$ . With  $k(2\text{-propanol} + O_3) = 0.83 M^{-1}s^{-1}$ , this would have resulted in a half-life of 14 seconds. Strong signals with half-lives of 1 s were successfully detected, but it may well be possible that a weaker 2-propanol signal might have come out too broad and thus too low for adequate detection. Thus, this reference is not a proof for the absence of singlet oxygen in the aqueous 2-propanol system, and the option that reaction (46) proceeds in the spin-allowed mode, that is, under the release of singlet oxygen, is not ruled out.

The chemical reactivity of  $H_2O_3$  is low. It seems that its reaction is somewhat similar to that of  $H_2O_2$ . It does not react with alcohols or  $I^-$ , and 1.6 M  $Fe^{2+}$  were required for its reduction within its short lifetime in aqueous solution (Czapski & Bielski, 1963).

## 10.8 SATURATED MICROPOLLUTANTS LACKING OZONE-REACTIVE HETEROATOMS

All saturated compounds lacking ozone-reactive heteroatoms react so slowly with ozone (Table 10.1) that the direct reaction of ozone in removing such micropollutants is not efficient. They mostly react, however, rapidly with  $\bullet OH$ . Their reactions with  $\bullet OH$  are discussed in Chapter 14. In DOM-containing waters such as wastewater and drinking water, the reaction of ozone with the water matrix leads to  $\bullet OH$  formation, and by this route ozone-refractory compounds are eliminated (Chapter 3).

# Chapter 11

## Inorganic anions and the peroxone process

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### 11.1 INTRODUCTORY REMARKS

Inorganic anions are negatively charged, and thus react much faster than their conjugate acids, for example,  $\text{HS}^-/\text{H}_2\text{S}$  (Table 11.1).

**Table 11.1** Compilation of ozone rate constants of inorganic anions (for metal-derived anions see Chapter 12). Published rate constants are rounded to significant figures;  $\text{p}K_{\text{a}}$  values of conjugate acids

Compound	$\text{p}K_{\text{a}}$	$k / \text{M}^{-1} \text{s}^{-1}$	Reference
Azide ion	9.4	$4 \times 10^6$	Hoigné <i>et al.</i> , 1985
protonated		$<4 \times 10^3$	Hoigné <i>et al.</i> , 1985
Borate ion protonated		$<6 \times 10^{-2}$	Hoigné <i>et al.</i> , 1985
diprotated		$<4 \times 10^{-3}$	Hoigné <i>et al.</i> , 1985
Bromate ion		$1 \times 10^{-3}$	Hoigné <i>et al.</i> , 1985
Bromide ion		160 at 20 °C 258 at 25 °C	Haag & Hoigné, 1983a Liu <i>et al.</i> , 2001
Bromite ion		$>1 \times 10^5$ $8.9 \times 10^4$	Hoigné <i>et al.</i> , 1985 Nicoson <i>et al.</i> , 2002
Carbonate ion	10.3, 6.3	$<0.1$	Hoigné <i>et al.</i> , 1985
Bicarbonate ion		$\ll 0.01$	Hoigné <i>et al.</i> , 1985
Chlorate ion		$\ll 1 \times 10^{-4}$	Hoigné <i>et al.</i> , 1985
Chloride ion		$<3 \times 10^{-3}$ $6 \times 10^{-4}$ at 9.5 °C, $E_{\text{a}} = 74 \text{ kJ mol}^{-1}$	Hoigné <i>et al.</i> , 1985 Yeatts & Taube, 1949
Chlorite ion		$4 \times 10^6$ $8.2 \times 10^6$	Kläning <i>et al.</i> , 1985 Nicoson <i>et al.</i> , 2002
Cyanate ion	3.9	$\leq 10^{-2}$	Hoigné <i>et al.</i> , 1985

(Continued)

**Table 11.1** Compilation of ozone rate constants of inorganic anions (for metal-derived anions see Chapter 12). Published rate constants are rounded to significant figures;  $pK_a$  values of conjugate acids (*Continued*)

Compound	$pK_a$	$k / M^{-1} s^{-1}$	Reference
Cyanide ion	9.1	$1 \times 10^3$ $2.6 \times 10^3$	Hoigné <i>et al.</i> , 1985 Gurol & Bremen, 1985
protonated		$\leq 10^{-3}$	Hoigné <i>et al.</i> , 1985
Hydroperoxide ion	using 11.6	$5.5 \times 10^6$	Staehelin & Hoigné, 1982
protonated	using 11.8	$9.6 \times 10^6$ <0.01 0.065**	Sein <i>et al.</i> , 2007 Staehelin & Hoigné, 1982 Sehested <i>et al.</i> , 1992
Hydroxide ion		48 70	Forni <i>et al.</i> , 1982 Staehelin & Hoigné, 1982
protonated (water)		$< 1 \times 10^{-7}$	Hoigné <i>et al.</i> , 1985
Hypobromite ion	8.8	430 at 25 °C	Haag & Hoigné, 1983a
protonated		$\leq 1 \times 10^{-2}$	Haag & Hoigné, 1983a
Hypochlorite ion	7.5	170*	Haag & Hoigné, 1983b
Hypoiodite ion	10.4	$1.6 \times 10^6$ $3.6 \times 10^4$	Bichsel & von Gunten, 1999b
Iodate ion		$< 10^{-4}$	Hoigné <i>et al.</i> , 1985
Iodide ion		$2 \times 10^9$ $1.2 \times 10^9$	Garland <i>et al.</i> , 1980 Liu <i>et al.</i> , 2001
Nitrate ion		$< 10^{-4}$	Hoigné <i>et al.</i> , 1985
Nitrite ion	3.29	$5.83 \times 10^5$ $1.8 \times 10^5$	Liu <i>et al.</i> , 2001 Hoigné <i>et al.</i> , 1985
protonated		<500	Hoigné <i>et al.</i> , 1985
Perchlorate ion		$\ll 2 \times 10^{-5}$	Hoigné <i>et al.</i> , 1985
Periodate ion		<0.01	Hoigné <i>et al.</i> , 1985
Phosphate ion protonated	2.1, 7.2, 12.3	$< 2 \times 10^{-4}$	Hoigné <i>et al.</i> , 1985
diprotated		<0.02	Hoigné <i>et al.</i> , 1985
Sulfate ion protonated	2	$< 10^{-4}$	Hoigné <i>et al.</i> , 1985
Sulfide ion protonated	6.9	$3 \times 10^9$	Hoigné <i>et al.</i> , 1985
diprotated		$\sim 3 \times 10^4$	Hoigné <i>et al.</i> , 1985
Sulfite ion	7	$1.5 \times 10^9$ $1.3 \times 10^9$	Hoffmann, 1986 Liu <i>et al.</i> , 2001
protonated		$3.7 \times 10^5$ $8 \times 10^5$ $8.6 \times 10^5$	Hoffmann, 1986 Liu <i>et al.</i> , 2001 Erickson <i>et al.</i> , 1977
Sulfur dioxide		$2 \times 10^6$ $2.4 \times 10^4$	Nahir & Dawson 1987 Neta <i>et al.</i> , 1988 based on Hoffmann, 1986
		$< 10^4$	Erickson <i>et al.</i> , 1977
Thiosulfate ion		$2.2 \times 10^8$ $(0.7-2.2) \times 10^8$	Utter <i>et al.</i> , 1992 Kanofsky & Sima, 1995

\* For the decay of ozone; for the decay of  $ClO^-$ , the rate constant is  $140 M^{-1} s^{-1}$ .

\*\* At 31 °C.

Water does not react with ozone, but its conjugate base,  $\text{OH}^-$ , reacts with ozone, albeit slowly (Table 11.1). In all these reactions, O-transfer reactions dominate, and an ozone adduct must be the first intermediate or is at least a transition state as in the reaction of  $\text{NO}_2^-$  with ozone (see below). In other cases, the standard Gibbs free energies of adduct formation can be calculated by quantum chemistry. When this reaction is slightly endergonic, adduct formation is not only slow but the reaction is also reversible. A case in point is the reaction with  $\text{Br}^-$ . There may be also other faster decay routes of the adduct, and then no reversibility is observed (as in  $\text{OH}^-$ ). Since the substrate anion ( $\text{A}^-$ ) and ozone are in their singlet ground states, the spin conservation rule demands that the multiplicities of the adducts and their products must be singlets as well [reactions (1) and (2)]. Thus, the oxygen that is released in reaction (2) must be in its excited singlet state,  $^1\text{O}_2$  [ $\text{O}_2(^1\Delta_g)$ ]. The excited state of oxygen ( $^1\text{O}_2$ ) lies  $95.5 \text{ kJ mol}^{-1}$  above its ground state [ $^3\text{O}_2$ ,  $\text{O}_2(^3\Sigma_g^-)$ ]. This is of major importance when the energetics of such O-transfer reactions is assessed.



The heavy atom effect can enhance the rate of singlet  $\rightarrow$  triplet conversion by spin-orbit coupling, and this is the reason why the  $^1\text{O}_2$  yield in the reaction of ozone with  $\text{Br}^-$  and  $\text{I}^-$  is lowered to 54% and 14%, respectively (see below). These low  $^1\text{O}_2$  yields are a further indication for a certain lifetime of these adducts.

Nitrite is sometimes used as a competitor for the determination of ozone rate constants because nitrate, the main product, can be readily quantified. The authors of the higher and later value, state that their value has been measured with special care (Liu *et al.*, 2001), and this value may be used for such competition studies.

## 11.2 HYDROXIDE ION

The reaction of ozone with  $\text{OH}^-$  gives rise to  $\cdot\text{OH}$  radicals (Staelin & Hoigné, 1982). As far as the mechanism is concerned, it has been suggested that an O-transfer may occur [reaction (3)] and  $\text{HO}_2^-$  thus formed may induce the peroxone process.



A recent thermokinetic analysis comes to the conclusion that in the first step an adduct is formed [reaction (4),  $\Delta G^\circ = 3.5 \text{ kJ mol}^{-1}$ ] (Merényi *et al.*, 2010b).



This decays into  $\text{HO}_2^\bullet$  plus  $\text{O}_2^{\bullet-}$  [equilibrium (5),  $\Delta G^\circ = 14.8 \text{ kJ mol}^{-1}$ ].



In the absence of  $\text{O}_3$ , these radicals eventually decay by H-transfer [reaction (6),  $k = 9.7 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$  (Bielski *et al.*, 1985)], about 50 times more slowly than the reverse of reaction (5).



$\text{HO}_2^\bullet$  is in equilibrium with  $\text{O}_2^{\bullet-}$  [equilibrium (7),  $\text{p}K_a(\text{HO}_2^\bullet) = 4.8$  (Bielski *et al.*, 1985)].





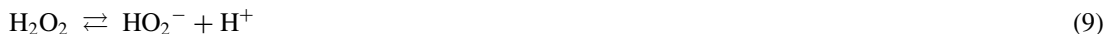
With ozone,  $O_2^{\bullet-}$  gives rise to  $O_3^{\bullet-}$  [reaction (8),  $k = 1.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Sehested *et al.*, 1983),  $1.6 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Bühler *et al.*, 1984)] that is the precursor of  $\bullet\text{OH}$  (for details see Chapter 13).



In the literature, the reaction of ozone with  $\text{OH}^-$  is often wrongly cited as the source for  $\bullet\text{OH}$  in a given system. This reaction has a very low rate constant (Table 11.1) and can only play a role at very high pH. An example may show this. Even at pH 8, the upper end for pH values for drinking waters and wastewaters, the reaction is so slow ( $k_{\text{obs}} = [\text{OH}^-] \times k_4 = 7 \times 10^{-5} \text{ s}^{-1}$ ;  $t_{1/2} = 10.000 \text{ s} = 2.8 \text{ h}$ ) that it must be neglected as other ozone reactions that occur in competition are typically much faster [for example, the reaction of ozone with DOM (Chapter 3)].

### 11.3 HYDROPEROXIDE ION – PEROXONE PROCESS

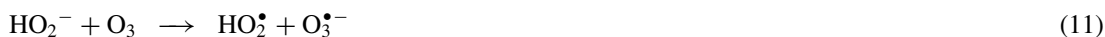
The combination of ozone with  $\text{H}_2\text{O}_2$  for water treatment is often called the “peroxone process”. It gives rise to  $\bullet\text{OH}$  and is one of the most common AOPs. It was first described in a brilliant paper by (Staehelin & Hoigné, 1982). There, it has been shown that the rate constant for the reaction of ozone with  $\text{H}_2\text{O}_2$  is very low (Table 11.1) and that the observed reaction is due to its anion,  $\text{HO}_2^-$ , present in equilibrium [equilibrium (9)].



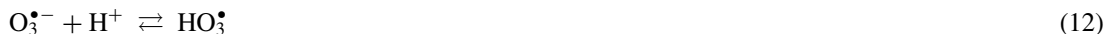
The rate of reaction at a pH below the  $\text{p}K_a$  of  $\text{H}_2\text{O}_2$ ,  $k_{\text{obs}}$ , is thus given by equation (10). In the original paper, a  $\text{p}K_a(\text{H}_2\text{O}_2) = 11.6$  was taken (Staehelin & Hoigné, 1982). A more recent paper uses  $\text{p}K_a(\text{H}_2\text{O}_2) = 11.8$  (Sein *et al.*, 2008), and subsequent discussions are based on this higher  $\text{p}K_a$  value. This has an effect on  $k$  but not on the experimentally observed  $k_{\text{obs}}$ .

$$k_{\text{obs}} = k(\text{HO}_2^- + \text{O}_3) \times 10^{(\text{pH} - \text{p}K_a)} \quad (10)$$

It has been suggested (Staehelin & Hoigné, 1982) that the reaction proceeds by electron transfer [reaction (11)].



It has been proposed that the  $\text{O}_3^{\bullet-}$  radical becomes protonated [reaction (12)] and the ensuing  $\text{HO}_3^{\bullet}$  radical decomposes into  $\bullet\text{OH}$  and  $\text{O}_2$  [reaction (13),  $\text{p}K_a(\text{HO}_3^{\bullet}) = 8.2$  (Bühler *et al.*, 1984)].



The  $\text{HO}_2^{\bullet}$  is in equilibrium with  $\text{O}_2^{\bullet-}$  [equilibrium (14)], and this undergoes electron transfer to ozone [reaction (15)].



The overall stoichiometry has been concluded to be  $\text{H}_2\text{O}_2 + 2\text{O}_3 \rightarrow 2\bullet\text{OH} + 3\text{O}_2$ . In fact, the efficiency of  $\bullet\text{OH}$  formation is only half of this (von Sonntag, 2008; Jarocki *et al.*, 2012), and this calls for a revision of this mechanism. Before discussing details, a completely different view of the peroxone process must be mentioned. Based on the observed kinetic isotope effect, it has been suggested that in the primary step a hydride is transferred ( $\text{HO}_2^- + \text{O}_3 \rightarrow \text{O}_2 + \text{HO}_3^-$ ), and the ensuing chemistry has

been attributed to the reaction of  $\text{H}_2\text{O}_3$  (Lesko *et al.*, 2004) [for formation and decay of  $\text{H}_2\text{O}_3$  see Chapter 10]. Since it has been shown that this observed kinetic isotope effect was due to a kind of experimental artefact (Sein *et al.*, 2007), this mechanism must be disregarded, and the earlier concept of  $\bullet\text{OH}$  formation continues to be valid, although it requires modifications (Merényi *et al.*, 2010a).

As the first step, one must assume the formation of an adduct [reaction (16),  $\Delta G^\circ = -39.8 \text{ kJ mol}^{-1}$  (Merényi *et al.*, 2010a)].



This reaction is slightly more exergonic than the electron transfer [reaction (11),  $\Delta G^\circ = -26.6 \text{ kJ mol}^{-1}$ ]. The adduct may decompose in two directions [reactions (17),  $\Delta G^\circ = 13.2 \text{ kJ mol}^{-1}$ , and (18),  $\Delta G^\circ = -197 \text{ kJ mol}^{-1}$ ].



The experimental observation that the efficiency of  $\bullet\text{OH}$  formation is only 50% can be rationalised if these reactions occur to about the same extent. At first sight, it may be surprising that  $k_{18}$  is not significantly larger than  $k_{17}$ . However, a reaction involving making or breaking of a single bond is inherently much faster than a reaction in which several bonds are simultaneously rearranged. Thus, the closeness of the two rate constants makes sense.

The ozonide radical anion,  $\text{O}_3^{\bullet-}$ , is in rapid equilibrium with  $\text{O}_2$  and  $\text{O}^{\bullet-}$  [equilibrium (19);  $k_{19} = 1.4 \times 10^3 \text{ s}^{-1}$ ,  $k_{-19} = 3.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Elliot & McCracken, 1989)], and  $\text{O}^{\bullet-}$  is in equilibrium with its conjugate acid,  $\bullet\text{OH}$  [equilibrium (20);  $\text{p}K_a(\bullet\text{OH}) = 11.8$ ].



Since only  $\text{O}^{\bullet-}$  but not  $\bullet\text{OH}$  reacts with  $\text{O}_2$ , these equilibria drive  $\text{O}_3^{\bullet-}$  into  $\bullet\text{OH}$  and  $\text{O}_2$  (except at very high pH, where these equilibria stabilise  $\text{O}_3^{\bullet-}$ ). This mechanistic concept replaces the current one, where  $\text{O}_3^{\bullet-}$  is protonated and  $\text{HO}_3^\bullet$  decomposes into  $\bullet\text{OH}$  and  $\text{O}_2$  [reaction (13)]. The reported  $\text{p}K_a(\text{HO}_3^\bullet) = 6.15$  (revised at 8.2, Bühler, private communication) must be a kinetic artefact (so-called “reactivity  $\text{p}K$ ”, see Chapter 2) (Merényi *et al.*, 2010a). It is now clear that it must be rather near  $-2$  (Merényi *et al.*, 2010a; Naumov & von Sonntag, 2011b). In this context, it may be mentioned that the decay of  $\text{HO}_3^\bullet$  in the gas phase [reaction (13)] has been calculated at a high level of theory [CCSD(T)/6-311++G\*\*] and found to be slightly endothermic ( $\Delta H = 21 \text{ kJ mol}^{-1}$  for the *trans* form and  $20 \text{ kJ mol}^{-1}$  for the *cis* form) (Plesnicar *et al.*, 2000). In water, the decay of  $\text{HO}_3^\bullet$  is markedly exergonic,  $\Delta G^\circ = -47 \text{ kJ mol}^{-1}$  (Naumov & von Sonntag, 2011b).

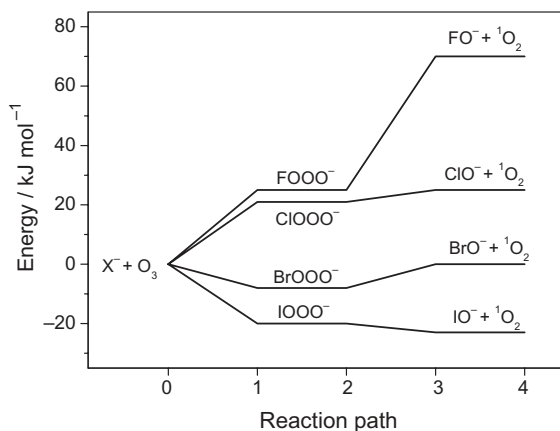
## 11.4 FLUORIDE

There are no reports on the reaction of the  $\text{F}^-$  with ozone. It seems not to react with ozone, and this is fairly well understood considering that both adduct formation and subsequent oxygen release as  $^1\text{O}_2$  as required by the spin conservation rule are endergonic (Table 11.2).

On top of the endergonicities of these reactions, there must be substantial activation energies, and this must be the reason for the low reactivity, if any, of the fluoride ion.

**Table 11.2** Reactions of ozone with halide ions. Standard Gibbs free energies ( $\Delta G^0/\text{kJ mol}^{-1}$ ) for the formation of ozone adducts and their decay by oxygen release according to Naumov & von Sonntag (2010) unpublished

Halide ion	$\Delta G^0$ (Adduct formation)	$\Delta G^0$ (Oxygen release)	State of $\text{O}_2$
Fluoride	+25	+45	$^1\text{O}_2$ , spin allowed
		-50	$^3\text{O}_2$ , spin forbidden
Chloride	+21	+4	$^1\text{O}_2$ , spin allowed
		-92	$^3\text{O}_2$ , spin forbidden
Bromide	-8	+8	$^1\text{O}_2$ , spin allowed
		-86	$^3\text{O}_2$ , spin forbidden
Iodide	-20	-3	$^1\text{O}_2$ , spin allowed
		-98	$^3\text{O}_2$ , spin forbidden



**Figure 11.1** Energetics of the reaction of ozone with halide ions along the reaction path according to Naumov & von Sonntag, 2010, unpublished. For  $\text{Br}^-$  and  $\text{I}^-$ , there is also a competing release of ground state  $\text{O}_2$  ( $^3\text{O}_2$ ). The latter makes the last step much more exergonic (Table 11.2).

In Figure 11.1, the data in Table 11.2 are visualised. With  $\text{F}^-$  and  $\text{Cl}^-$ , all steps along the reaction path are endergonic, with  $\text{Br}^-$  there is reversibility of the adduct, and with  $\text{I}^-$  reactions are exergonic throughout, as will be discussed below.

## 11.5 CHLORIDE

For  $\text{Cl}^-$ , the situation is similar in so far as the addition reaction is also noticeably endergonic, and a substantial activation energy of  $74 \text{ kJ mol}^{-1}$  has been reported (Yeatts & Taube, 1949). The ensuing release of  $^1\text{O}_2$  from an adduct is weakly endergonic (Table 11.2), and there may be an additional barrier for the release of  $^1\text{O}_2$  potentially favouring the reverse of adduct formation. Altogether, this may result in a very slow reaction (Table 11.1). It has been suggested that hypochlorite and oxygen are formed

(Yeatts & Taube, 1949). Since the potential product hypochlorite [ $pK_a(\text{HOCl}) = 7.5$ ] has a comparatively high rate constant (Table 11.1), product interference with the reaction of ozone plus  $\text{Cl}^-$  is likely.

The reaction of ozone with  $\text{Cl}^-$  can be typically neglected. Even in seawater ( $[\text{Cl}^-] \approx 0.5 \text{ M}$  in the Atlantic) the reaction of ozone with chloride will be largely overrun by competing reactions (e.g. by a reaction with  $\text{Br}^-$ ,  $[\text{Br}^-] \approx 1 \text{ mM}$ ).

## 11.6 HYPOCHLORITE

In aqueous solution, chlorine,  $\text{Cl}_2$ , is in equilibrium with  $\text{HOCl}$ ,  $\text{OCl}^-$  and  $\text{Cl}_3^-$  [reactions (21)–(23)].



UV–Vis absorption maxima and equilibrium constants are compiled in Table 11.3.

Hypochlorous acid ( $\text{HOCl}$ ) does not react with ozone which slows down the reaction towards chlorate at circum-neutral pH. Hypochlorite reacts moderately rapidly with ozone (Table 11.1). It gives rise to  $\text{Cl}^-$  and  $\text{ClO}_2^-$  in a 3.4:1 ratio (Haag & Hoigné, 1983b). This is an indication that there are two competing reactions [reactions (24)  $k_{24} = 30 \text{ M}^{-1} \text{ s}^{-1}$  and (25)  $k_{25} = 110 \text{ M}^{-1} \text{ s}^{-1}$ ].



**Table 11.3** UV–Vis absorption maxima and equilibrium constants of halogen-derived species in water (20–25°C)

Compound	$\lambda_{\text{max}}/\text{nm}$	$\epsilon/\text{M}^{-1} \text{ cm}^{-1}$	$K$	Reference
$\text{Cl}_2$	323	68	$K_{\text{Hydrolysis}} = 4 \times 10^{-4} \text{ M}^2$	Soulard <i>et al.</i> , 1981
$\text{HOCl}$	233	97	$K_a = 4 \times 10^{-8} \text{ M}^{-1}$ $pK_a = 7.5$	Soulard <i>et al.</i> , 1981 Morris, 1966
$\text{ClO}^-$	292	350		Soulard <i>et al.</i> , 1981
$\text{Cl}_3^-$	233	18 500		Soulard <i>et al.</i> , 1981
	325	85		Soulard <i>et al.</i> , 1981
			$K(\text{Cl}^- + \text{Cl}_2) = 0.18 \text{ M}^{-1}$	Eigen & Kustin, 1962
$\text{Br}_2$	392	175	$K_{\text{Hydrolysis}} = 7.2 \times 10^{-9} \text{ M}^2$ $K_{\text{Hydrolysis}} = 3.5\text{--}6 \times 10^{-9} \text{ M}^2$	Soulard <i>et al.</i> , 1981 Beckwith <i>et al.</i> , 1996
$\text{HOBr}$	260	160	$K_a = 1.8 \times 10^{-9} \text{ M}^{-1}$ $pK_a = 8.74$ $pK_a = 8.8$	Soulard <i>et al.</i> , 1981 Haag & Hoigné, 1983a
$\text{BrO}^-$	329	345		Soulard <i>et al.</i> , 1981
$\text{Br}_3^-$	266	35 000		Soulard <i>et al.</i> , 1981
		40 900		Beckwith <i>et al.</i> , 1996

(Continued)

**Table 11.3** UV–Vis absorption maxima and equilibrium constants of halogen-derived species in water (20–25°C) (*Continued*)

Compound	$\lambda_{\max}/\text{nm}$	$\epsilon/\text{M}^{-1}\text{cm}^{-1}$	$K$	Reference
$\text{I}_2$			$K(\text{Br}^- + \text{Br}_2) = 17\text{ M}^{-1}$	Eigen & Kustin, 1962
			$K_{\text{Hydrolysis}} = 5.44 \times 10^{-13}\text{ M}^2$	Burger & Liebhafsky, 1973
HOI			$K_{\text{a}} = 4 \times 10^{-11}\text{ M}^{-1}$	Bichsel & von Gunten, 2000b
			$pK_{\text{a}} = 10.4 \pm 0.1$	
$\text{I}_3^-$	350	25 500	$pK_{\text{a}} = 10.6 \pm 0.8$	Chia, 1958
			351	25 700
$\text{I}_3^-$	350	25 500	$K(\text{I}^- + \text{I}_2) = 725\text{ M}^{-1}$	Burger & Liebhafsky, 1973
			351	25 700

The mechanisms of these reactions must be analogous to the reactions of  $\text{BrO}^-$  with ozone, discussed in more detail below, in that adducts are the most likely intermediates. Reaction (25) is one of the examples, where ozone acts as a reducing agent.

## 11.7 CHLORITE

Chlorite,  $\text{ClO}_2^-$ , reacts rapidly with ozone (Table 11.1). Since chlorate was found to be the final product, it has been suggested that ozone reacts with  $\text{ClO}_2^-$  by O-transfer (Haag & Hoigné, 1983b). However, more recently it has been shown that this reaction proceeds by electron transfer (Klänning *et al.*, 1985) [reaction (26),  $\Delta G^0 = -43\text{ kJ mol}^{-1}$  (Naumov & von Sonntag, 2011b, SI)].



The subsequent reactions of ozone with  $\text{ClO}_2^\bullet$  are discussed in Chapter 13. Although it has been stated that perchlorate is not a product in the reaction of  $\text{ClO}_2^-$  with ozone (Haag & Hoigné, 1983b), traces of perchlorate (in the order of 1% of chlorate) are also formed (Rao *et al.*, 2010).  $\text{Cl}_x\text{O}_y$  radicals are potential intermediates (Rao *et al.*, 2010).

## 11.8 BROMIDE

The reaction of ozone with  $\text{Br}^-$  is of major interest, as the final oxidation product is bromate,  $\text{BrO}_3^-$ , which is classified as a potential human carcinogen with a drinking water standard of 10  $\mu\text{g/l}$  (WHO, 2004). This system has been widely studied (Haag *et al.*, 1982; Haag & Hoigné, 1983a; von Gunten & Hoigné, 1992, 1994, 1996 von Gunten *et al.*, 1995; Liu *et al.*, 2001; Naumov & von Sonntag, 2008b). The oxidation of  $\text{Br}^-$  to bromate is a multi-stage process. Hypobromite and bromite are intermediates. In the first step, an adduct is formed [reactions (27) and (28)].



This reaction is slow (Table 11.1) and reversible (Liu *et al.*, 2001). Quantum-chemical calculations support this experimental observation [ $\Delta G^0 = +6\text{ kJ mol}^{-1}$  (Naumov & von Sonntag, 2008b), cf. Table 11.4].

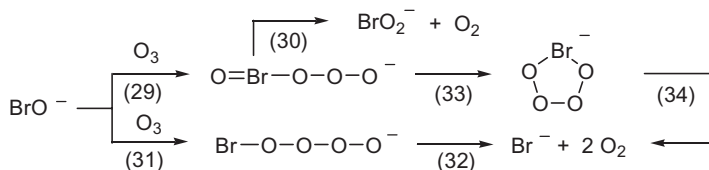
**Table 11.4** Calculated Gibbs energies ( $\Delta G$ ) taking the solvent water into account (B3LYP/6-311+G(d)/SCRF=COSMO) according to Naumov & von Sonntag (2008b)

Reaction	$\Delta G/\text{kJ mol}^{-1}$
$\text{Br}^- + \text{O}_3 \rightarrow \text{BrOOO}^-$	+6
$\text{BrOOO}^- \rightarrow \text{BrO}^- + \text{O}_2(^1\Delta_g)$ spin allowed	+13
$\text{BrOOO}^- \rightarrow \text{BrO}^- + \text{O}_2(^3\Sigma_g^-)$ spin forbidden	-81
$\text{Br}^- + \text{O}_3 \rightarrow \text{BrOOO}^- \rightarrow \text{BrO}^- + \text{O}_2(^1\Delta_g)$ spin allowed	+19
$\text{Br}^- + \text{O}_3 \rightarrow \text{BrOOO}^- \rightarrow \text{BrO}^- + \text{O}_2(^3\Sigma_g^-)$ spin forbidden	-75
$\text{BrO}^- + \text{O}_3 \rightarrow \text{Adduct} \rightarrow \text{BrO}_2^- + \text{O}_2(^1\Delta_g)$ spin allowed	-36
$\text{BrO}^- + \text{O}_3 \rightarrow \text{Adduct} \rightarrow \text{BrO}_2^- + \text{O}_2(^3\Sigma_g^-)$ spin forbidden	-130
$\text{BrO}^- + \text{O}_3 \rightarrow \text{Adduct} \rightarrow \text{Br}^- + 2 \text{O}_2(^3\Sigma_g^-)$ spin allowed	-347
$\text{BrO}_2^- + \text{O}_3 \rightarrow \text{Adduct} \rightarrow \text{BrO}_3^- + \text{O}_2(^3\Sigma_g^-)$ spin allowed	-93
$\text{BrO}_2^- + \text{O}_3 \rightarrow \text{Adduct} \rightarrow \text{BrO}_3^- + \text{O}_2(^3\Sigma_g^-)$ spin forbidden	-187

In competition with the reverse of reaction (1), the adduct loses  $\text{O}_2$  [reaction (2)]. The spin conservation rule demands that  $\text{O}_2$  must be released in its excited singlet state,  $^1\text{O}_2$  [ $\text{O}_2(^1\Delta_g)$ ], because ozone,  $\text{Br}^-$  and  $\text{BrOOO}^-$  are all in their singlet ground states. The adduct is, however, sufficiently long-lived that the heavy atom effect exerted by the bromine in the adduct also allows, by spin orbit coupling, the release of (triplet) ground-state  $\text{O}_2$  [ $^3\text{O}_2$ ,  $\text{O}_2(^3\Sigma_g^-)$ ]. This route is energetically more favourable as the excited state ( $^1\text{O}_2$ ) lies  $95.5 \text{ kJ mol}^{-1}$  above the ground state ( $^3\text{O}_2$ ). The  $^1\text{O}_2$  yield in this system is only 54% (Muñoz *et al.*, 2001).

## 11.9 HYPOBROMITE

The reaction of ozone with  $\text{BrO}^-$  gives rise to two products,  $\text{BrO}_2^-$  plus  $\text{O}_2$ , the trivial and *oxidative* pathway [reactions (29) and (30);  $k_{\text{obs}} = 100 \text{ M}^{-1} \text{ s}^{-1}$  (Haag & Hoigné, 1983a);  $\Delta G^0 = -36 \text{ kJ mol}^{-1}$  for the spin-allowed reaction, formation of  $^1\text{O}_2$  (Naumov & von Sonntag, 2008b)], but there is also a *reductive* pathway leading to  $\text{Br}^-$  plus  $2 \text{O}_2$  [reactions (31) and (32) or reactions (29), (33) and (34);  $k_{\text{obs}} = 330 \text{ M}^{-1} \text{ s}^{-1}$  (Haag & Hoigné, 1983a);  $\Delta G^0 = -347 \text{ kJ mol}^{-1}$  (Naumov & von Sonntag, 2008b)].

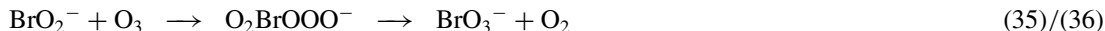


For the two pathways, one may assume two different adducts [reactions (29) vs. (31)]. The alternative, one common adduct [reaction (29)] followed by reactions (33) and (34) for the reductive pathway has, however, been favoured as  $\text{BrO}^-$  is more negative at oxygen (86% of excess electron density) than at bromine (14%) (Naumov & von Sonntag, 2008b). The electronic structure of  $\text{O}_3$  is largely bipolar with negative charges at the outer oxygens. An addition to oxygen as compared to bromine may be disfavoured by charge repulsion despite the fact that  $\text{O}_3$  is electrophilic.

The interesting reductive pathway finds its analogy in the reactions of ozone with  $\text{ClO}^-$  (see above) and  $\text{Mn}^{2+}$  *en route* to  $\text{MnO}_4^-$  (Reisz *et al.*, 2008) (Chapter 12).

### 11.10 BROMITE

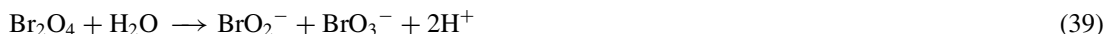
The fast reaction of  $\text{BrO}^-$  with ozone was originally suggested to be an O-transfer [reactions (35) and (36)] (Hoigné *et al.*, 1985).



This reaction is energetically feasible [ $\Delta G^0 = -93 \text{ kJ mol}^{-1}$  for the spin allowed reaction (Naumov & von Sonntag, 2008b)]. Yet, it has been shown that the reaction is dominated by an electron transfer [reaction (37);  $\Delta G^0 = -64 \text{ kJ mol}^{-1}$  (Naumov & von Sonntag, 2011a, SI)] (Nicoson *et al.*, 2002).



In the reaction of ozone with  $\text{Br}^-$  en route to bromate,  $\bullet\text{OH}$  radicals (precursor:  $\text{O}_3^{\bullet-}$ ) have indeed been detected [Jarocki & von Sonntag (2011), unpublished results]. The ensuing rapid bimolecular decay [equilibrium (38)] and reaction of the dimer with water and a faster reaction with  $\text{OH}^-$  [cf. reaction (39)] give rise to bromate (Buxton & Dainton, 1968; Field & Försterling, 1986).



The forward rate constant of  $k_{38} = 1.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  and also the equilibrium constant  $K_{38}$  given by Buxton & Dainton (1968) are somewhat in doubt (Buxton & von Sonntag, 2010, unpublished). Yet, the error in  $k_{38}$  may not be high, as radical-radical recombination reactions are typically close to diffusion controlled. When the value of  $k_{38} = 1.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  is assumed,  $k_{-38} = 7.4 \times 10^4 \text{ s}^{-1}$  is obtained (Field & Försterling, 1986).

Overall, bromite is quickly and quantitatively transformed into bromate during typical ozonation conditions in water treatment. In real waters, ozone reactions with the DOM give rise to  $\bullet\text{OH}$  and DOM also serves as  $\bullet\text{OH}$  scavenger (Chapter 3). As  $\bullet\text{OH}$  contributes significantly to bromate formation, its generation during ozonation of  $\text{Br}^-$ -containing waters is a highly non-linear process for which predictions are very difficult. Some aspects are discussed below and in Chapter 14.

It is noteworthy that the reaction stops at bromate and does not continue up to perbromate. The reason for this is the high endothermicity of the reaction [spin allowed:  $\Delta G^0(\text{BrO}_3^- + \text{O}_3 \rightarrow \text{BrO}_4^- + {}^1\text{O}_2) = +144 \text{ kJ mol}^{-1}$ ; spin forbidden:  $\Delta G^0(\text{BrO}_3^- + \text{O}_3 \rightarrow \text{BrO}_4^- + {}^3\text{O}_2) = +47 \text{ kJ mol}^{-1}$ , Naumov & von Sonntag (2011), unpublished results].

### 11.11 IODIDE

Ozone reacts very rapidly with  $\text{I}^-$  (Table 11.1). The reaction proceeds by O-transfer with an adduct as an intermediate [reactions (40) and (41)] (Muñoz *et al.*, 2001).



Both steps are exergonic (Table 11.2), but, in contrast to  $\text{Br}^-$ , the first step is not reversible. Yet, the second step is only slightly exergonic and the adduct must have a certain lifetime. Evidence for this comes from the low yield of  ${}^1\text{O}_2$  (14%) (Muñoz *et al.*, 2001). As with  $\text{Br}^-$ , this low  ${}^1\text{O}_2$  yield is due to the heavy atom effect (see discussion in Section 11.1).

In slightly acidic solution and with some excess of  $I^-$ , the final product is  $I_3^-$ . Several equilibria have to be taken into account [equilibria (42)–(44), for equilibrium constants see Table 11.3].



The situation is even more complex, as in both neutral and basic solutions major amounts of iodate ( $IO_3^-$ ) are present in equilibrium. In the concentration range of typical drinking waters, this is, however, negligible.

$HOI/IO^-$  can be formed by ozonation but also in chlorination and chloramination processes. It reacts with DOM to form iodo-organic compounds (Krasner *et al.*, 2006; Bichsel & von Gunten, 1999b; Bichsel & von Gunten, 2000a). In drinking water or bottled water, some of the low molecular weight iodo-organic compounds can cause taste and odour problems [e.g. iodoform (Bichsel & von Gunten, 2000a; Bruchet, Duguet, 2004)] or are even of toxicological concern. Some of the iodo-organic compounds are substantially more toxic than the chloro- or bromo-analogues (Richardson *et al.*, 2008). The chance of forming iodo-organic compounds increases in the order  $O_3 < HOCl \ll NH_2Cl$ , because the rate of the subsequent  $HOI/IO^-$  reactions decreases in this order. This means that during chloramination,  $HOI/IO^-$  has the longest lifetime and can react with DOM moieties (Bichsel & von Gunten, 1999b).

During ozonation,  $IO^-/HOI$  is quickly (Table 11.1) further oxidised to iodate in two steps, similar to the case of hypobromite, with a first step to iodite [reactions (45) and (46)] and a second step to iodate [reaction (47)].

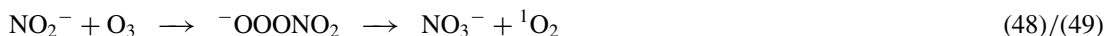


In contrast to  $HOCl$  and  $HOBr$ ,  $HOI$  is quickly oxidised by ozone. Due to the high  $pK_a$  of  $HOI$  [ $pK_a = 10.4$ , (Bichsel & von Gunten, 2000b)], the reaction of ozone with  $HOI$  is the main pathway for its further oxidation towards iodate in the pH range relevant for water treatment. This oxidation has been tentatively written as an O-transfer, although, in analogy to the reactions of  $ClO_2^-$  [reaction (26)] and  $BrO_2^-$  [reaction (37)], an electron transfer is also conceivable. In contrast to bromate, iodate is not problematic from a human toxicological point of view. Iodate is even added to table salt as a food supplement for iodine in iodine-deficient areas such as Switzerland (Bürigi *et al.*, 2001).

The rate constant for the oxidation of iodite with ozone is not known, however, it is faster than the preceding reactions and therefore not rate limiting. Since the reactions of  $I^-$  and its follow-up products with ozone are so fast,  $\bullet OH$  radical reactions can be neglected (in contrast to  $Cl^-/Br^-$  plus ozone systems). For the same reason, pre-ozonation provides an excellent opportunity to mitigate iodine-derived problems in water supply systems (for an example see Section 11.18).

## 11.12 NITRITE

Ozone reacts rapidly with nitrite (Table 11.1). The main product is nitrate. The O-transfer requires an adduct as an intermediate, and the released oxygen must be in its singlet state [reactions (48) and (49)]. Indeed, the  $^1O_2$  yield has been found at 96% (Muñoz *et al.*, 2001).





The reaction seems to be complex. The structure of the first adduct ( $\Delta G^\circ = -5 \text{ kJ mol}^{-1}$ ) is far away from that of the final products, nitrate and  $^1\text{O}_2$ . It has to rearrange into a second adduct ( $\Delta G^\circ = -105 \text{ kJ mol}^{-1}$ ) the structure of which is now very close to the final products to which it decays ( $\Delta G^\circ = -78 \text{ kJ mol}^{-1}$ ) (Naumov *et al.*, 2010).

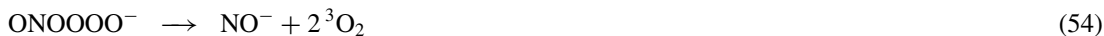
Ozone can also add to one of the oxygens [reaction (50),  $\Delta G^\circ = +58 \text{ kJ mol}^{-1}$ ] leading to peroxyxynitrite [reactions (51),  $\Delta G^\circ = -65 \text{ kJ mol}^{-1}$  and (52),  $\Delta G^\circ = -128 \text{ kJ mol}^{-1}$ ], a product that is formed with a 2.6% yield (Naumov *et al.*, 2010).



Reaction (52) is followed by a recombination of the two radicals [reaction (53),  $\Delta G^\circ = -28 \text{ kJ mol}^{-1}$ ].



An alternative route [reaction (54),  $\Delta G^\circ = +90 \text{ kJ mol}^{-1}$ ] that would be analogous to one of the decay routes of the adduct formed in the peroxone process [reaction (18)] is markedly endergonic and thus excluded.



Of the two processes that lead to peroxyxynitrite, reaction (53) is not only favoured energetically but also produces  $^3\text{O}_2$ , in agreement with the observation that the  $^1\text{O}_2$  yield is slightly below unity. For the reaction to peroxyxynitrite to be able to compete with the reactions to nitrate, there must be a substantial barrier to the first intermediate. The fact that the reaction of ozone with nitrite is four orders below diffusion controlled (Table 11.1) supports this conclusion.

In addition to these reactions,  $\bullet\text{OH}$  is also formed, which is likely to occur by electron transfer [reaction (55)]. The precursor of  $\bullet\text{OH}$  is  $\text{O}_3^{\bullet-}$  (see section 11.3).

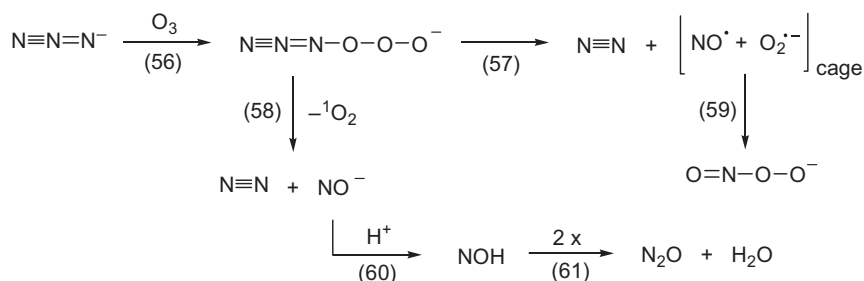


The  $\bullet\text{OH}$  yield is near 4% (Naumov *et al.*, 2010).

### 11.13 AZIDE

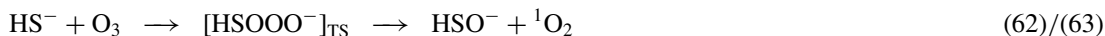
The interest in the reaction of ozone with azide in aqueous solution dates back to 1929 (Gleu & Roell, 1929). The formation of a yellow compound that decomposed during the attempt to isolate it was reported. Upon heating such yellow solutions, gas evolved consisting of  $\text{N}_2$ ,  $\text{N}_2\text{O}$  and  $\text{O}_2$  in approximately equal concentrations. Arsenite and other reducing compounds were oxidised in these mildly alkaline solutions. A reaction with formaldehyde was also noticed. An excess of alkali prevented the formation of the yellow colour and also reduced the release of  $\text{N}_2$  and  $\text{N}_2\text{O}$ . Much later, the formation of  $\text{N}_2\text{O}$  was confirmed and the oxidising species identified as peroxyxynitrite (Uppu *et al.*, 1996).  $\text{N}_2$  was, however, not found among the reaction products. Singlet oxygen is formed in 17% yield (after correction for quenching) (Muñoz *et al.*, 2001). At this stage, it seems to be premature to come up with a well-founded mechanism, as reaction conditions seem to strongly influence the chemistry. Here, the complex chemistry of peroxyxynitrite (Mark *et al.*, 1996; Goldstein *et al.*, 2005) could be one of the reasons. The

mechanistic suggestions depicted in reactions (56)–(61) are written to trigger new experiments *en route* to a better understanding of this interesting system.



### 11.14 HYDROGEN SULFIDE

Bisulfide,  $\text{HS}^-$ , reacts five orders of magnitude faster with ozone than  $\text{H}_2\text{S}$  [ $\text{p}K_a(\text{H}_2\text{S}) = 7.0$ ] (Table 11.1). Thus, except at very low pH, the reaction of ozone is governed by  $\text{HS}^-$ . At 16%, the yield of singlet oxygen ( $^1\text{O}_2$ ) is low (Muñoz *et al.*, 2001). This is in contrast to many organic sulfur compounds, where yields of 100% are common (with the exception of 1,4-dithiothreitol) (Table 9.1). This points to a complex chemistry. Formation of  $^1\text{O}_2$  demands that an adduct is formed in the first step [reactions (62) and (63)].



Sulfuric acid is formed as the only detectable final product, and 2.3 mol of ozone are required for the formation of 1 mol of sulfuric acid (Overbeck, 1995), and this surprisingly low value has been confirmed as 2.4 (Mark *et al.*, 2011). In the case where ozone would only react by O-transfer, a stoichiometry of 4 mol would be required. Thus, further oxidation equivalents must be provided in these reactions to account for the observed stoichiometry. There is the possibility that free-radical reactions are induced and the additional oxidation equivalents are provided by the dissolved  $\text{O}_2$ . Yet, there is also another possibility.

The overall reaction (62)/(63) is exergonic with  $\Delta G^0 = -136 \text{ kJ mol}^{-1}$  (Mark *et al.*, 2011). The product of reaction (62), the ozone adduct, is not a stable intermediate. It rather must be considered as a transition state (TS). In one of the calculations its structure and standard Gibbs free energy of formation has been obtained as a local minimum ( $\Delta G^0 = -111 \text{ kJ mol}^{-1}$ ). Avoiding this local minimum, the reaction proceeds in the calculations by internal cyclisation and O-transfer giving rise to the anion of sulfinic peracid,  $\text{HS(O)OO}^-$  [reaction (64)].

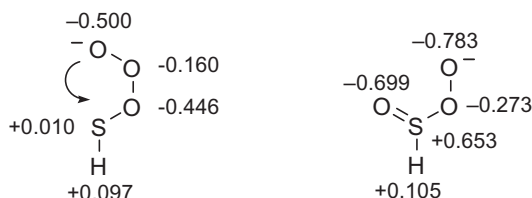


This reaction is much more exergonic ( $\Delta G^0 = -244 \text{ kJ mol}^{-1}$ ) than the formation of  $^1\text{O}_2$ . Reaction (64) is facilitated by the positive charge at sulfur (Figure 11.2).

The identification of sulfinic peracid as a likely intermediate in the reaction of ozone with  $\text{HS}^-$  can now explain, why the stoichiometry of oxidation of  $\text{HS}^-/\text{H}_2\text{S}$  by ozone is only  $\sim 2.4$  rather than 4.0 if a series of simple O-transfer reactions were to occur [for a detailed discussion see Mark *et al.* (2011)].

An ozone treatment has been proposed for the remediation of  $\text{H}_2\text{S}/\text{HS}^-$ -containing waters (Overbeck, 1995; Solisio *et al.*, 1999). Ozonation is quite frequently applied in the mineral water industry for the mitigation of sulfide-induced odour problems (another example is shown below for  $\text{I}^-$ -induced odour

problems). Because the ozone plus  $\text{HS}^-$  reaction is so fast,  $\text{HS}^-$  is rapidly consumed even considering ozone reactions with the water matrix, that is, only low ozone doses are required and formation of by-products such as bromate is not a problem. This, together with the fact that sulfuric acid is the only product, makes ozonation feasible both from an economic and human health point of view.



**Figure 11.2** Charge distributions in the transition state of the reaction of ozone with  $\text{HS}^-$  as taken from a local minimum and its cyclisation product. The arrow indicates the direction of the O-transfer.

### 11.15 HYDROGEN SULFITE

In aqueous solution,  $\text{SO}_2$  is in equilibrium with  $\text{H}_2\text{SO}_3$  [ $\text{p}K_a(\text{H}_2\text{SO}_3) = 1.9$ ],  $\text{HSO}_3^-$  [ $\text{p}K_a(\text{HSO}_3^-) = 7.0$ ] and  $\text{SO}_3^{2-}$ . Compared to the reactions of sulfite and bisulfite (Table 11.1), the reaction of  $\text{SO}_2$  must be very slow (Erickson *et al.*, 1977), and thus  $\text{HSO}_3^-$  and  $\text{SO}_3^{2-}$  are the targets for the ozone reaction. Details of the reaction mechanisms are not known.

### 11.16 BROMATE FORMATION AND MITIGATION IN WATER TREATMENT

Bromate is the most relevant oxidation/disinfection by-product formed upon ozonation because of its toxicological relevance (see above). The low drinking water standard may not be fully justified according to some preliminary experiments on the fate of bromate in gastric juices (Keith *et al.*, 2006a, b; Cotruvo *et al.*, 2010). This, however, does not alter the situation in which this low value must not be exceeded in drinking water treatment using ozone.

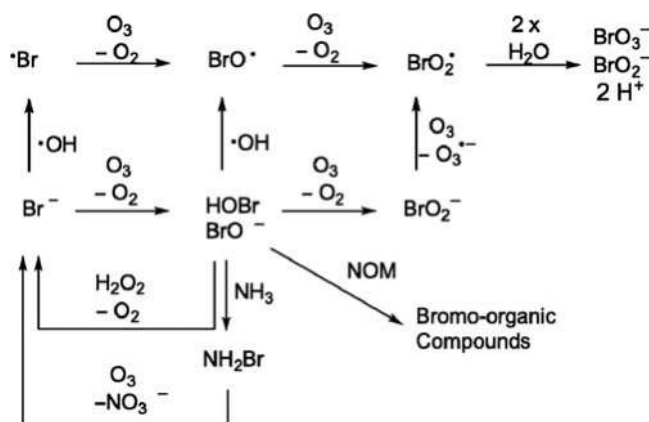
Bromate is formed in  $\text{Br}^-$ -containing waters through a complicated mechanism including both ozone and  $\bullet\text{OH}$  reactions (Haag & Hoigné, 1983a; von Gunten & Hoigné, 1994; von Gunten *et al.*, 1996; von Gunten & Oliveras, 1998; Westerhoff *et al.*, 1998a, b; Song *et al.*, 1996) (Chapters 11 and 14).  $\text{HOBr}/\text{BrO}^-$  is a crucial intermediate, because its further transformation is relatively slow. Therefore, its lifetime is sufficiently long for it to undergo various side reactions, which are summarised in Figure 11.3.

In presence of ammonia, it can form monobromamine which is only slowly oxidised by ozone (Chapter 8) to nitrate and bromide (see below). Therefore, the transient monobromamine concentration is significant and allows reduction of the rate of bromate formation. In fact, ammonia addition is one of the proposed methods for bromate minimisation (Song *et al.*, 1997; Hofmann & Andrews, 2001; Pinkernell & von Gunten, 2001).

Another important sink for the  $\text{HOBr}$  intermediate is its reaction with  $\text{H}_2\text{O}_2$ . It may occur in  $\text{H}_2\text{O}_2$ -based AOPs [reaction (65),  $k = 7.6 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ] (von Gunten & Oliveras, 1997).



Due to this reaction, bromate formation is lower in AOPs such as  $O_3/H_2O_2$  compared to the conventional ozonation process. However, even in the presence of  $H_2O_2$ , bromate cannot be entirely suppressed during ozonation (von Gunten & Oliveras, 1998). In contrast, it is completely suppressed in the AOP  $UV/H_2O_2$ . From  $\gamma$ -radiolytic experiments, it has been concluded that HOBr is a key intermediate towards bromate formation even if  $\cdot OH$  is the only oxidant (von Gunten & Oliveras, 1998) (see also Chapter 14).



**Figure 11.3** Simplified bromate formation mechanism during ozonation of bromide containing waters. The possible reactions of HOBr with ammonia, hydrogen peroxide and NOM are also shown. Adapted from von Gunten & Hoigné, 1996.

Finally, DOM also has an important influence on bromate formation. Its main role is related to its effect on ozone chemistry and  $\cdot OH$  formation during ozonation (Chapter 3), but it is also important because the reaction of HOBr with NOM moieties leads to bromo-organic compounds.

Bromate removal, once formed, has been investigated with several processes such as activated carbon filtration, Fe(II) addition, UV treatment, photocatalytic and biological processes (Hijnen *et al.*, 1995; Siddiqui *et al.*, 1994, 1996; Mills *et al.*, 1996; Asami *et al.*, 1999; Bao *et al.*, 1999; Gordon *et al.*, 2002; Peldszus *et al.*, 2004; van Ginkel *et al.*, 2005; Kirisits *et al.*, 2000, 2001). Activated carbon which is often in place after ozonation is only efficient when fresh. Initially, a chemical bromate reduction occurs. Thereafter, bromate is only reduced biologically under anaerobic conditions. However, such conditions are not easily met in the oxygen-rich environment after ozonation. UV-based processes for bromate removal are typically very energy intensive and chemical reduction is highly inefficient. Therefore up until now, no bromate reduction processes have been implemented in full-scale water treatment systems. The focus of mitigation is on the minimisation of its formation during ozonation. Based on the mechanistic understanding of bromate formation (Figure 11.3, Chapters 11, 14), various minimisation methods are available today and are summarised in Table 11.5 (Krasner *et al.*, 1993; Kruithof *et al.*, 1993; Galey *et al.*, 2000; Song *et al.*, 1997; Pinkernell & von Gunten, 2001; Hofmann & Andrews, 2001; Buffle *et al.*, 2004; Neemann *et al.*, 2004).

The chlorine–ammonia process is particularly interesting and is the result of the empirical observation that bromate formation can be substantially reduced in systems in which a pre-chlorination is followed by ammonia addition and by ozonation (Neemann *et al.*, 2004). The mechanism of this process has been explained by the following reaction mechanism (Buffle *et al.*, 2004) [reaction (66),  $k = 1.55 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$

(Kumar & Margerum, 1987); reaction (67),  $k = 8 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$  (Haag *et al.*, 1984); reaction (68),  $k = 40 \text{ M}^{-1} \text{ s}^{-1}$  (Haag *et al.*, 1984); reaction (69),  $k \gg 40 \text{ M}^{-1} \text{ s}^{-1}$  (Haag *et al.*, 1984)].



**Table 11.5** Bromate mitigation strategies

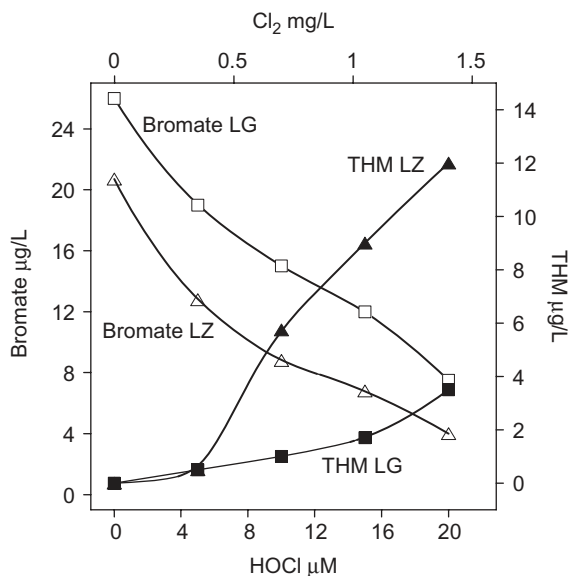
Method	Reduction of $\text{BrO}_3^-$ formation compared to conventional ozonation	Problems
pH depression	~Factor of 2	High alkalinity waters
Ammonia addition	~Factor of 2	Residual ammonia has to be removed in biological filtration, ammonia addition to drinking waters is forbidden in many European countries
Chlorine–ammonia process	~Factor of 10	Residual ammonia, ammonia addition to drinking waters is forbidden in many European countries, formation of halo-organic compounds in pre-chlorination
Peroxone process	Depends largely on point of $\text{H}_2\text{O}_2$ addition	Disinfection efficiency might be significantly reduced; mostly suited for bromate minimisation in oxidation processes when disinfection is not intended

The advantage of this process is the efficient masking of bromide as monobromamine ( $\text{NH}_2\text{Br}$ ) prior to ozonation.  $\text{NH}_2\text{Br}$  only reacts slowly with ozone (Chapter 8) and releases bromide (Figure 11.3). Therefore, especially during the initial phase of ozonation for which the  $\bullet\text{OH}$  radical impact is high, bromide is not available for the oxidation towards bromate. Due to the acid–base speciation of  $\text{HOCl}$ , the rate of reaction (66) is pH-dependent (only  $\text{HOCl}$  reacts with bromide,  $\text{p}K_a(\text{HOCl}) = 7.5$ ). Furthermore, the reaction of  $\text{HOCl}$  with DOM may lead to chloro-organic compounds. Therefore, the free chlorine contact time has to be optimised for maximum bromide oxidation and acceptable formation of chloro-/bromo-organics. Figure 11.4 shows an example of the application of the chlorine–ammonia process in Lake Zurich and Lake Greifensee water and the trade-off between bromate minimisation and trihalomethane (THM) formation.

In these experiments, both waters were buffered at pH 8, spiked with  $590 \mu\text{g/L Br}^-$ , pre-chlorinated for 5 min, followed by the addition of  $300 \mu\text{g/L NH}_3$  and analysed 60 min after ozone addition ( $1.5 \text{ mg/L}$  ozone, Lake Zurich water;  $3 \text{ mg/L}$  ozone, Lake Greifensee water). Exact ozone exposures were not determined for each data point but preliminary experiments showed that the above doses correspond to similar ozone exposures of  $(10 \pm 1.5) \text{ mg min L}^{-1}$  in both waters.

In ammonia-containing raw waters, chlorine is consumed quickly by ammonia [ $k(\text{HOCl} + \text{NH}_3) \approx 3 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$  (Deborde & von Gunten, 2008)], and the  $\text{NH}_2\text{Cl}$  formed in this reaction only oxidizes  $\text{Br}^-$  slowly to  $\text{HOBr}$  [ $k(\text{NH}_2\text{Cl} + \text{Br}^-) = 0.28 \text{ M}^{-1} \text{ s}^{-1}$  at pH 7 (Trofe *et al.*, 1980)]. Nevertheless,

bromate formation can be reduced by the chlorine–ammonia process. An additional mechanism has been suggested, namely the reaction of chlorine with organic amines leading to the corresponding chloramines. They seem to have a lower  $\bullet\text{OH}$  yield in their reaction with ozone during post-ozonation (Buffle & von Gunten, 2006). For a given ozone exposure, the corresponding  $\bullet\text{OH}$  exposure will thus be lower than in conventional ozonation, and hence less bromate will be formed.

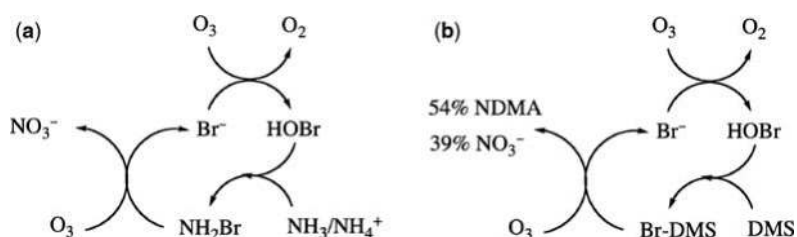


**Figure 11.4** Bromate minimisation and sum of trihalomethane (THM) formation for the chlorine–ammonia process for various pre-chlorination doses in Lake Zurich (LZ) and Lake Greifensee (LG) water. Reprinted (adapted) with permission from Buffle *et al.*, 2004. Copyright (2004) American Chemical Society.

Bromate minimisation in the peroxone process has been optimised by the HiPOx<sup>®</sup> process (Bowman, 2005) in which ozone is added in small portions dosed at various points along the hydraulic pathway through a reactor to reduce residual ozone concentrations to very low levels. In excess of  $\text{H}_2\text{O}_2$ , HOBr, which now becomes a decisive intermediate, is reduced back to  $\text{Br}^-$ . However, this process is only applicable for oxidation and not for disinfection, because ozone concentrations are kept at a minimum.

## 11.17 BROMIDE-CATALYSED REACTIONS

The first reported case of a  $\text{Br}^-$ -catalysis during ozonation is an improved ammonia oxidation which is shown in Figure 11.5a (Haag *et al.*, 1984). At circum-neutral pH, acceleration of ammonia oxidation is caused by the difference of the apparent second-order rate constant for the reaction of ozone with  $\text{NH}_3/\text{NH}_4^+$  ( $k_{\text{app}} \approx 0.025 \text{ M}^{-1} \text{ s}^{-1}$ ) and  $\text{NH}_2\text{Br}$  ( $k = 40 \text{ M}^{-1} \text{ s}^{-1}$ ) (Haag *et al.*, 1984). Since the formation of HOBr from the oxidation of  $\text{Br}^-$  is reasonably fast ( $k = 160 \text{ M}^{-1} \text{ s}^{-1}$ , see above) and the reaction of HOBr with  $\text{NH}_3/\text{NH}_4^+$  is very fast ( $k = 8 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ , see above), the oxidation of  $\text{NH}_2\text{Br}$  by ozone is the rate-limiting step in ammonia oxidation. Compared to the direct oxidation of  $\text{NH}_3/\text{NH}_4^+$  by ozone (Chapter 8), the  $\text{Br}^-$ -catalysed process is several orders of magnitude faster. Another  $\text{Br}^-$ -catalysed reaction is the formation of *N*-nitrosodimethylamine (NDMA) during ozonation of dimethylsulfamide (DMS)-containing waters (Figure 11.5b). This is discussed in more detail in Chapter 8.



**Figure 11.5** Bromide-catalysed oxidation of (a) ammonia and (b) dimethylsulfamide (DMS) during ozonation. Adapted from von Gunten *et al.*, 2010 with permission.

### 11.18 MITIGATION OF IODIDE-RELATED PROBLEMS

Typical I<sup>-</sup> concentrations in water resources are fairly low ( $\leq 10 \mu\text{g/L}$ ) meaning that iodide is not a problem generally. However in special geological formations or in coastal areas, I<sup>-</sup> concentrations can be elevated and depending on the oxidative treatment, problems with iodo-organic compounds can arise from the reaction of HOI/OI<sup>-</sup> with DOM. Because the reaction of I<sup>-</sup> to iodate with ozone is a fast process with a very short lifetime of HOI (see above), pre-ozonation provides an excellent opportunity to mitigate I<sup>-</sup>-derived problems in the distribution system. The following example will illustrate this in more detail.

In a Swiss mineral water ([I<sup>-</sup>] = 30  $\mu\text{g/L}$ ), occasionally iodine-derived taste and odour problems were observed which led to massive consumer complaints. In addition to I<sup>-</sup>, the same water also contains relatively high Br<sup>-</sup> concentrations ( $\geq 100 \mu\text{g/L}$ ). To mitigate this problem, introduction of an ozonation step into the process line was proposed for transforming I<sup>-</sup> to iodate. However, the ozone dose had to be adjusted for a complete transformation of I<sup>-</sup> to iodate without any significant bromate formation. Iodate is a stable sink of iodine which hinders the formation of iodo-organic compounds. Based on the reaction kinetics shown above and in Chapter 14, bromate formation during ozonation is several orders of magnitude slower than iodate formation. This shows the high selectivity of ozone for I<sup>-</sup> oxidation. Therefore, based on laboratory experiments, a plug-flow reactor with a residence time of 30 s and an ozone residual concentration of  $\leq 0.15 \text{ mg/L}$  at the effluent was selected. The residual ozone was quenched in an activated carbon filter.

Table 11.6 shows the results of the full-scale treatment train for iodide, iodate, bromide and bromate concentrations, from raw water to bottled water.

**Table 11.6** Ozonation of a Swiss mineral water for mitigation of iodide-derived taste and odour problems. Bromide and iodide concentrations in the raw water and resulting iodate levels ( $\mu\text{g/L}$ ) in the bottled water (Bichsel & von Gunten, 1999a; Salhi & von Gunten, 1999)

Anion	Raw water	Ozonated water	Bottled water
Bromide	101	102	101
Bromate	< d.l.	< d.l.	< d.l.
Iodide	32	n.d.	n.d.
Iodate	< d.l.	46	46

d.l.: detection limit (bromate, iodate: 0.1  $\mu\text{g/L}$ ), n.d.: not detected.

It is evident that  $\text{I}^-$  is completely oxidised to iodate, while the  $\text{Br}^-$  concentration remains constant. In the bottled water samples, bromate levels were always  $< 2 \mu\text{g/L}$  and iodate was stable for several months. This process is a promising approach for solving  $\text{I}^-$ -derived drinking water problems. It could be applied as a pre-treatment step in drinking waters containing elevated  $\text{I}^-$  levels to avoid formation of iodo-organic compounds in post-disinfection processes such as chlorination and chloramination.



# Chapter 12

## Reactions with metal ions

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### 12.1 REACTIVITY OF METAL IONS

The first detailed report on the reactivity of ozone towards metals and metal ions was by *Schönbein* (Schönbein, 1854), and this early report is still worthwhile reading. Reported rate constants are compiled in Table 12.1.

**Table 12.1** Compilation of ozone rate constants with metal ions. Published rate constants are rounded to significant figures

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Ag <sup>+</sup>			0.035	Noyes <i>et al.</i> , 1937
			0.04	Reisz <i>et al.</i> , 2012b
As(OH) <sub>3</sub>	9.2		5.5 × 10 <sup>5</sup>	Dodd <i>et al.</i> , 2006b
AsO(OH) <sub>2</sub> <sup>-</sup>	12.2		1.5 × 10 <sup>8</sup>	Dodd <i>et al.</i> , 2006b
Co <sup>2+</sup>			0.62	Hill, 1949
			0.66 at 0°C	Yeatts & Taube, 1949
Cu <sup>2+</sup>			no reaction	Yeatts & Taube, 1949
Fe <sup>2+</sup>		0–2	8.2 × 10 <sup>5</sup>	Lögager <i>et al.</i> , 1992
		0–3	8.5 × 10 <sup>5</sup>	Jacobsen <i>et al.</i> , 1997
Fe(CN) <sub>6</sub> <sup>4-</sup>			1.2 × 10 <sup>6</sup>	Flyunt <i>et al.</i> , 2003a
Mn <sup>2+</sup>			1.5 × 10 <sup>3</sup>	Jacobsen <i>et al.</i> , 1998a
			1.8 × 10 <sup>3</sup>	Jacobsen <i>et al.</i> , 1998a
			3.9 × 10 <sup>3</sup>	Tyupalo & Yakobi, 1980
		7	1.3 × 10 <sup>3</sup>	Reisz <i>et al.</i> , 2008
		7	1.0 × 10 <sup>3</sup>	Reisz <i>et al.</i> , 2008
Mn(II)oxalate			760	Reisz <i>et al.</i> , 2008
Mn(II)polyphosphate			1.4 × 10 <sup>4</sup>	Reisz <i>et al.</i> , 2008

(Continued)

**Table 12.1** Compilation of ozone rate constants with metal ions. Published rate constants are rounded to significant figures (*Continued*)

Compound	pK <sub>a</sub>	pH	k/M <sup>-1</sup> s <sup>-1</sup>	Reference
Pb <sup>2+</sup>			no reaction	Reisz & von Sonntag, unpublished
Pb(OH) <sup>+</sup>			slow	Reisz & von Sonntag, unpublished
Pb(OH) <sub>2</sub>			~1 × 10 <sup>3</sup>	Reisz & von Sonntag, unpublished
SeO(OH) <sub>2</sub>	2.8		negligible	von Gunten & Jaeggi, unpublished
SeO <sub>2</sub> (OH) <sup>-</sup>	8.5		~0.5	von Gunten & Jaeggi, unpublished
SeO <sub>3</sub> <sup>2-</sup>			1.7 × 10 <sup>4</sup>	von Gunten & Jaeggi, unpublished
Sn <sup>2+</sup>			2 × 10 <sup>9</sup>	Utter <i>et al.</i> , 1992
Sn(butyl) <sub>3</sub> Cl			4–6	Sein <i>et al.</i> , 2009
Sn(butyl) <sub>3</sub> OSn(butyl) <sub>3</sub>			7	Sein <i>et al.</i> , 2009
Sn(butyl) <sub>2</sub> Cl <sub>2</sub>			0.5–0.7	Sein <i>et al.</i> , 2009

The kinetics of the reactions of ozone with metal ions in their low oxidation states have been largely studied with As(III), Fe(II) and Mn(II). These reactions are governed by O-transfer reactions and ozone adducts are likely intermediates. With As(III), which can be present as As(OH)<sub>3</sub> and As(OH)<sub>2</sub><sup>-</sup> in the near neutral pH range, the monoanion reacts faster by nearly three orders of magnitude, and this reflects the general behaviour of electrophilic ozone. For Fe<sup>2+</sup>, the rate constant has only been measured in acid solutions, and based on the above one may speculate that, in analogy to the oxidation with oxygen (King, 1998), the rate may go up in less acidic and neutral solutions where contributions of Fe(OH)<sup>+</sup> and Fe(OH)<sub>2</sub> dominate. Complexation has a marked effect on the rate of reaction, as shown for Mn(II). The iron complex Fe(CN)<sub>6</sub><sup>4-</sup> does not exchange its ligands readily, and there is no free site for ozone to add on. Thus, Fe(II) has to undergo a one-electron transfer reaction.

## 12.2 ARSENIC

In neutral solution As(III) is largely undissociated [equilibria (1) and (2), pK<sub>a</sub>(As(OH)<sub>3</sub>) = 9.2; pK<sub>a</sub>(AsO(OH)<sub>2</sub><sup>-</sup>) = 12.2].



As(III) is readily oxidised by ozone, whereas As(OH)<sub>3</sub> reacts much more slowly [reaction (3)] than the monoanion, AsO(OH)<sub>2</sub><sup>-</sup> [reaction (4), cf. Table 12.1].



Arsenic acid [As<sup>V</sup>O(OH)<sub>3</sub>] is a stronger acid than arsenous acid [pK<sub>a1</sub> = 2.2, pK<sub>a2</sub> = 6.9 and pK<sub>a3</sub> = 11.5]. These pK<sub>a</sub> values are very similar to those of the related phosphoric acid. The oxidation of As(III) and the concomitant formation of deprotonated arsenic acid species are desired in water treatment because As(V) adsorbs much better on iron(III)(hydr)oxide-containing filters than As(III) (Ruhland *et al.*, 2003a, b; Roberts *et al.*, 2004; Voegelin *et al.*, 2010). Therefore, the combination of

ozonation with iron(III)(hydr)oxide filtration is a powerful tool for arsenic mitigation in drinking and mineral waters.

### 12.3 COBALT

Cobalt has two oxidation states, Co(II) and Co(III). The lower oxidation state reacts with ozone (Table 12.1). It has been suggested that in this slow reaction  $\bullet\text{OH}$  radicals are generated (Hill, 1949). As the reduction potential  $E_0(\text{Co}^{3+}/\text{Co}^{2+}) = 1.8 \text{ V}$  is considerably higher than  $E_0(\text{O}_3/\text{O}_3^{\bullet-}) = 1.03 \text{ V}$  (Chapter 2), this suggestion has to be put on a better footing. Techniques are now available for doing this (Chapter 14).

### 12.4 COPPER

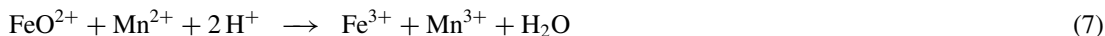
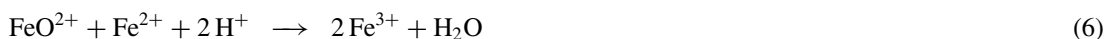
A reaction of  $\text{Cu}^{2+}$  with ozone is not observed (Yeatts & Taube, 1949), although there is a higher oxidation state, Cu(III) (Asmus *et al.*, 1978; Ulanski & von Sonntag, 2000).

### 12.5 IRON

Originally, it was thought that  $\text{Fe}^{2+}$  reacts with ozone by electron transfer (Tyupalo & Dneprovskii, 1981), but this view has since been corrected in favour of an O-transfer [reaction (5)] (Lögager *et al.*, 1992; Jacobsen *et al.*, 1997)].



The Fe(IV) species that is formed in reaction (5) is a strong oxidant and reacts rapidly with  $\text{Fe}^{2+}$  [reaction (6),  $k = 7.2 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  (Jacobsen *et al.*, 1997),  $1.4 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  (Lögager *et al.*, 1992)] and  $\text{Mn}^{2+}$  [reaction (7),  $k = 1 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  (Jacobsen *et al.*, 1998b)].



The latter reaction is of relevance for the further oxidation of manganese to  $\text{MnO}_4^-$  in the ozonation of drinking waters and wastewaters that contain both  $\text{Fe}^{2+}$  and  $\text{Mn}^{2+}$  (see below).

Reliable rate constants are only available for acid solutions (Table 12.1). Due to a higher electron density at iron,  $\text{Fe}(\text{OH})^+$  is expected to react more rapidly than  $\text{Fe}^{2+}$  and hence dominates the Fe(II) oxidation kinetics in such waters. In the case of oxidation of iron(II) by  $\text{O}_2$ , the rate of its oxidation at circum-neutral pH is largely controlled by the  $\text{Fe}(\text{OH})_2$  species [ $k(\text{O}_2 + \text{Fe}^{2+}) = 5.5 \times 10^{-5} \text{ M}^{-1} \text{ s}^{-1}$ ,  $k[\text{O}_2 + \text{Fe}(\text{OH})^+] = 4.2 \times 10^2 \text{ M}^{-1} \text{ s}^{-1}$ ,  $k[\text{O}_2 + \text{Fe}(\text{OH})_2] = 5.2 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$  (King, 1998)]. In carbonate-containing waters, carbonate and hydroxo-carbonate complexes also play an important role (King, 1998).

In  $\text{Fe}(\text{CN})_6^{4-}$ , iron is fully complexed by tightly-bound cyano ligands, and ozone can no longer form an adduct. Thus, ozone has to react by one-electron transfer [reaction (8)] (Flyunt *et al.*, 2003a).

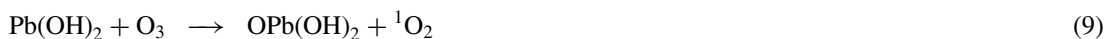


The  $\bullet\text{OH}$  yield is only about 70% (note that  $\text{O}_3^{\bullet-}$  gives rise to  $\bullet\text{OH}$ , Chapter 11), and it has been tentatively suggested that in competition with electron transfer, ozone may also react with the ligands.

## 12.6 LEAD

The browning of paper strips soaked with basic lead acetate was used by *Schönbein* for detecting ozone (Schönbein, 1854). Yet, only very recently [Reisz & von Sonntag (2011), unpublished] this reaction has found some further attention. Depending on pH, Pb(II) is present as  $\text{Pb}^{2+}$ ,  $\text{Pb}(\text{OH})^+$ ,  $\text{Pb}(\text{OH})_2$  or  $\text{Pb}(\text{OH})_3^-$  (Carell & Olin, 1960). In acid solution, where  $\text{Pb}^{2+}$  dominates, barely any reaction is observed overnight [Reisz, Naumov & von Sonntag, 2011, unpublished results]. Even at pH 9, where  $\text{Pb}(\text{OH})^+$  and  $\text{Pb}(\text{OH})_2$  dominate,  $k_{\text{obs}} \approx 330 \text{ M}^{-1} \text{ s}^{-1}$  (Table 12.1) is still low. Based on the data on As(III), one has to conclude that the reaction is mainly given by the less positively charged species. Under such conditions  $\alpha[\text{Pb}(\text{OH})_2]$  is near 30%, and we conclude that  $\text{Pb}(\text{OH})^+$ , like  $\text{Pb}^{2+}$ , is of little reactivity and that  $k[\text{Pb}(\text{OH})_2 + \text{O}_3]$  must be near  $10^3 \text{ M}^{-1} \text{ s}^{-1}$ .

In this context, some quantum-chemical calculations have been carried out. According to these, addition of ozone to  $\text{Pb}^{2+}$  is endergonic ( $\Delta G^0 = +22 \text{ kJ mol}^{-1}$ ) and the Pb–O bond in this adduct is extremely long (2.61 Å). For  $\text{Pb}(\text{OH})^+$ , no stable ozone adduct could be calculated, and in these preliminary calculations, triplet (ground-state)  $\text{O}_2$  was released in an endergonic reaction ( $\Delta G^0 = +13 \text{ kJ mol}^{-1}$ ). Only when one proceeds to  $\text{Pb}(\text{OH})_2$ , does the overall reaction also become exergonic for the spin-allowed formation of singlet oxygen [reaction (9),  $\Delta G^0 = -11 \text{ kJ mol}^{-1}$ ].



These calculations reflect the experimental observations well.

## 12.7 MANGANESE

Ozone reacts markedly slower (Table 12.1) with  $\text{Mn}^{2+}$  than with  $\text{Fe}^{2+}$  [reaction (10)]. Complexation of  $\text{Mn}^{2+}$  by polyphosphate or oxalate markedly influences the rate of reaction (Table 12.1).



The  $\text{MnO}^{2+}$  species reacts rapidly with water [reaction (11),  $k > 5 \text{ s}^{-1}$  (Reisz *et al.*, 2008)] yielding a colloidal  $\text{MnO}_2$  solution. This prevents a ready further oxidation by ozone to  $\text{MnO}_4^-$ .



As a consequence, in distilled water and in neutral solutions, only small amounts of  $\text{MnO}_4^-$  are formed. In acid solution or when  $\text{Mn}^{2+}$  is complexed, however, the reaction proceeds to  $\text{MnO}_4^-$  when ozone is in large excess. Otherwise and with an excess of  $\text{Mn}^{2+}$ , Mn(III) is the final product [reaction (12)].



Oxidation to  $\text{MnO}_4^-$  is most interesting, since as much as four times more ozone is required than the stoichiometry suggests. The reason for this is that ozone may also act as a reductant with some of the high oxidation states of manganese. To visualise this, the highly exergonic ( $\Delta G^0 = -200 \text{ kJ mol}^{-1}$ ) reaction (13) may be drawn. There may be other intermediates that could react similarly.



A reaction where ozone acts as a reductant has also been observed in reactions with hypobromite ( $\text{BrO}^- + \text{O}_3 \rightarrow \text{Br}^- + 2\text{O}_2$  in competition with  $\text{BrO}^- + \text{O}_3 \rightarrow \text{BrO}_2^- + \text{O}_2$ ) and with hypochlorite (Chapter 11). Another example seems to be the reaction of ozone with Ag(II) (see below).

In drinking water and in wastewater, the formation of substantial amounts of  $\text{MnO}_4^-$  may be observed (quite noticeable when such waters turn pink upon ozonation). Under such conditions, it cannot be the acidic environment or large amounts of complexing agents which cause the substantial formation of  $\text{MnO}_4^-$  (bicarbonate buffer induces  $\text{MnO}_4^-$  formation only at elevated concentrations), and thus there must be an additional route. Waters that contain Mn(II) typically also contain Fe(II). Fe(II) reacts rapidly with ozone and the fraction of Fe(IV) that is not scavenged by Fe(II) then oxidises Mn(II) [reaction (7)]. The Mn(III) thus formed can be more readily oxidised to  $\text{MnO}_4^-$  than the very short-lived  $\text{MnO}^{2+}$  intermediate (Reisz *et al.*, 2008).

Colloidal  $\text{MnO}_2$  has very interesting properties. It is a much stronger oxidant than ground technical  $\text{MnO}_2$  (birnesite). It reacts most rapidly with  $\text{H}_2\text{O}_2$  under violent  $\text{O}_2$  formation, a reaction not given by birnesite (von Sonntag, unpublished results). The most complex reaction involves, in the first step, the activation of the  $\text{MnO}_2$  solution by forming Mn(III) centres ( $k = 700 \text{ M}^{-1} \text{ s}^{-1}$ ) (Baral *et al.*, 1985). This activated solution catalyses the further decomposition of  $\text{H}_2\text{O}_2$  without being much consumed. The  $\text{MnO}_2$  solution also bleaches indigotrisulfonic acid ( $k > 10^7 \text{ M}^{-1} \text{ s}^{-1}$ ) while permanganate reacts much more slowly ( $k = 1.3 \times 10^3 \text{ M}^{-1} \text{ s}^{-1}$ ) (Reisz *et al.*, 2008). For further studies on the formation and reactivity of  $\text{MnO}_2$  colloids see Baral *et al.* (1986) and Lume-Pereira *et al.* (1985).

## 12.8 SELENIUM

In aquatic environmental systems, selenium is present as selenite ( $\text{Se}^{\text{IV}}\text{O}_3^{2-}$ ) or selenate ( $\text{Se}^{\text{VI}}\text{O}_4^{2-}$ ). Selenite reacts stoichiometrically with ozone by O-transfer to selenate [reaction (14)].



The reaction is highly pH-dependent because only  $\text{SeO}_3^{2-}$  reacts rapidly with ozone, whereas  $\text{SeO}_2(\text{OH})^-$  reacts rather slowly and  $\text{SeO}(\text{OH})_2$  practically not at all (Table 12.1).

The oxidation of selenite to selenate by ozone is of interest for selenite-containing mineral waters. Selenite can be slowly (within several weeks) transformed by micro-organisms to selenium-organic compounds which cause taste and odour problems. Once selenium is present in its higher oxidised form, selenium-organic compounds are no longer formed.

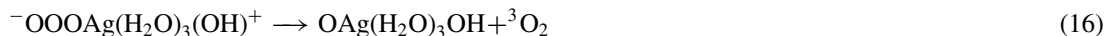
## 12.9 SILVER

In water, silver can exist in four oxidation states: Ag(0) (colloidal silver) Ag(I), Ag(II) and Ag(III). Over the whole pH range of interest Ag(I) is present as  $\text{Ag}^+$ . Ag(II) dominated only below pH 5.35 by  $\text{Ag}^{2+}$  and at pH > 8.35  $\text{Ag}(\text{OH})_2$  dominates (Asmus *et al.*, 1978).  $\text{Ag}^{2+}$  is a strong oxidant ( $E^0 = +2.0 \text{ V}$ ) (Blumberger *et al.*, 2004), but the other Ag(II) species must be less oxidising. When Ag(II) is generated by pulse radiolysis at pH 7, the species decays by second-order kinetics, and it has been assumed that Ag(II) disproportionates into  $\text{Ag}^+$  and Ag(III) (Pukies *et al.*, 1968). As further details are not known, it is also conceivable that Ag(II) forms a dimer that would be equivalent to an Ag(I)/Ag(III) binuclear complex.

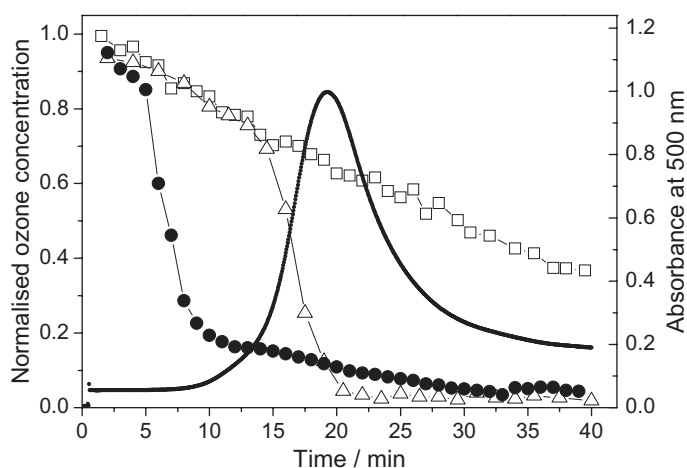
The reaction of ozone with  $\text{Ag}^+$  is slow (Table 12.1) and complex (Reisz *et al.*, 2012b). Generally, the positive charges (low electron density at the site of reaction) impede the formation of an adduct by the electrophilic ozone. Concomitant proton release from the hydration shell [four water molecules in the case of  $\text{Ag}^+$  (Blumberger *et al.*, 2004)] may facilitate the process [reaction (15)].



For releasing singlet  $O_2$  in a spin-allowed reaction, the energetics are often very unfavourable. Silver, as a heavy atom, can mediate the release of (triplet) ground state  $O_2$  [e.g. reaction (16)].



As the slow reaction of  $Ag^+$  with ozone proceeds, the kinetics continue at the slow rate of the initial reaction (Figure 12.1, squares) or suddenly accelerate as in the majority of experiments (Figure 12.1, triangles). Concomitant with the sudden acceleration, colloidal  $Ag(0)$  is formed, which can be monitored at 500 nm [cf. (Stamplecoskie & Scaiano, 2010)] (Reisz *et al.*, 2012b). The decomposition of ozone on  $Ag(0)$  nanoparticles has been reported (Morozov *et al.*, 2011).



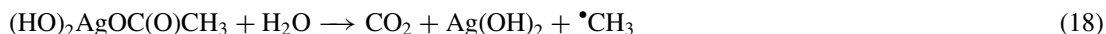
**Figure 12.1** Decay of ozone (close to  $100 \mu M$  in the various experiments), followed by titrating remaining ozone with 3-butenol (open squares and triangles). The solid line indicates  $Ag(0)$  formation measured at 500 nm and relates to the ozone decay shown in triangles. Data in closed circles have been obtained in the presence of 1 mM acetate. According to Reisz *et al.*, 2012b.

The precursor of  $Ag(0)$  has been considered to be  $Ag(II)$  [in equilibrium with  $Ag^+$  and  $Ag(III)$ ], for example, the exergonic reaction (17) (Reisz *et al.*, 2012b).



In this reaction, ozone acts as a reducing agent. Such a reaction is not without precedent (cf. Section 12.7 and Chapter 11).

$Ag(0)$  formation is accelerated by the addition of acetate. Here,  $Ag(II)$  formation is favoured by the intramolecular electron transfer reaction (18).



Oxalate also accelerates the ozone plus  $\text{Ag}^+$  reactions, but without giving rise to  $\text{Ag}(0)$ .  $\text{Ag}(\text{III})$  oxalate decomposes by intramolecular electron transfer to  $\text{Ag}^+$  without  $\text{Ag}(\text{II})$  as an intermediate [reaction (19)].



A well-documented intramolecular electron transfer process of a transition metal ion oxalate in its high oxidation state is  $\text{Mn}(\text{III})$  (Taube, 1947, 1948a, b).

## 12.10 TIN

The reaction of ozone with  $\text{Sn}^{2+}$  is close to diffusion controlled, much faster than any other transition metal ion (Table 12.1). In an organic solvent, this reaction gives rise to  $^1\text{O}_2$  in high yields (Emsenhuber *et al.*, 2003). This is a strong indication of an adduct being formed in the first step as depicted in reaction (20).



One may assume that  $\text{OSn}^{2+}$  formed in reaction (21) subsequently hydrolyses giving rise to  $\text{SnO}_2$ . Experiments confirming this point have not been carried out.

Tributyltin reacts somewhat faster with ozone (Table 12.1) than 2-propanol (Table 10.1). Somehow, tin must be involved in its reactivity as has been proposed for tetrabutyl tin in carbon tetrachloride solutions (Alexandrov *et al.*, 1971). In tributyltin, the electron density at tin is lower. This is not a favourable situation for a reaction of an electrophilic agent such as ozone. Indeed, dibutyltin whose electron density at tin is even lower reacts an order of magnitude more slowly [ $k = 0.5 - 0.7 \text{ M}^{-1} \text{ s}^{-1}$  (Sein *et al.*, 2009)].

Tributyl tin chloride gives rise to dibutyl tin chloride as the main product. Further products are formaldehyde, acetaldehyde, propanal and butanal (Sein *et al.*, 2009).

## 12.11 METAL IONS AS MICROPOLLUTANTS

Worldwide, about 50 million people suffer from high levels of arsenic in their drinking water, in some severe cases exceeding the limiting permissible value of  $10 \mu\text{g}/\text{l}$  by a factor of 100. Countries most affected are Bangladesh, India (West Bengal), Vietnam, China, Taiwan, Argentina, Chile, Mexico and the West of the USA (Smedley & Kiniburgh, 2002). Some suggestions as to the potential reasons for the toxicity of arsenic have been made (Hughes, 2002). Arsenic remediation typically involves an oxidation of  $\text{As}(\text{III})$  to  $\text{As}(\text{V})$  and adsorption of the latter on iron hydroxides (e.g. in flocculation with  $\text{FeCl}_3$ ) (Katsoyiannis *et al.*, 2008; Karcher *et al.*, 1999) or on iron(III)(hydr)oxide-based adsorbents (Driehaus, 2002). In the oxidation of  $\text{As}(\text{III})$  to  $\text{As}(\text{V})$ , ozone may be of some advantage as the reaction is very fast (Table 12.1). Nevertheless, this solution is only applicable in industrialised countries. In developing countries pre-chlorination is a feasible alternative, since  $\text{As}(\text{III})$  is quickly oxidised by chlorine [pH 7:  $k_{\text{app}}(\text{As}(\text{III}) + \text{chlorine}) = 2.6 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  (Dodd *et al.*, 2006b)].

Iron(II) and manganese(II) are common water contaminants in reduced source waters. Iron(II) is mainly an aesthetic problem, whereas manganese has also been discussed in relation to its neurotoxicity especially for children (WHO, 2004; Bouchard *et al.*, 2011). Iron(II) and manganese(II) removal is carried out by oxidation followed by precipitation and separation of the  $\text{Fe}(\text{III})$  and  $\text{Mn}(\text{III,IV})$  (hydr)oxides. Oxidation is mostly performed with oxygen in abiotic or microbiologically mediated processes (Mouchet, 1992). These processes are often sufficiently fast for iron(II) (Stumm & Lee, 1961). At low pH or in the presence of organic matter forming strong complexes with iron(II), however, a stronger oxidant such as ozone may be needed (Theis & Singer, 1974). At circum-neutral pH, abiotic  $\text{Mn}(\text{II})$  oxidation with oxygen is very slow (Morgan, 2005) and therefore, other oxidants such as ozone must be applied. In this

case, permanganate may be formed (see above) which has to be removed by a post-filtration step containing activated carbon or another reducing material (Singer, 1990).

Organotin compounds such as tributyltin have been widely used as an anti-fouling agent in ship paints and as biocides in wood preservatives and in textiles. The use of these substances has not been allowed since the late 1990s in most European and North American countries (Chau *et al.*, 1997), but they are still observed in effluents of WWTPs (European Commission, 2000). Their biodegradation is very slow and thus they persist in the environment [for their detection see Takeuchi *et al.*, (2000)]. They have endocrinic properties and their effect on aquatic life is dramatic (Duft *et al.*, 2003a) (Chapter 4). As their rate of reaction with ozone is low (Table 12.1), a direct reaction with ozone is ineffective in their elimination from contaminated waters and only the  $\bullet\text{OH}$  route can reduce their levels (Chapter 14).



# Chapter 13

## Reactions with free radicals

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### 13.1 REACTIVITY OF RADICALS

Ozone reacts fast with most free radicals, in some cases close to diffusion-controlled. The rate constants reported thus far are compiled in Table 13.1.

**Table 13.1** Compilation of ozone rate constants with free radicals. Published rate constants are rounded to significant figures

Radical	$k/M^{-1} s^{-1}$	Reference
Bromine atom ( $\cdot Br$ )	$1.5 \times 10^8$ <sup>(a)</sup>	von Gunten & Oliveras, 1998
Carboxymethyl radical ion (1-) ( $\cdot CH_2C(O)O^-$ )	$2 \times 10^9$	Sehested <i>et al.</i> , 1987
Chlorine dioxide ( $ClO_2$ )	$1.05 \times 10^3$ $1.1 \times 10^3$	Kläning <i>et al.</i> , 1985 Hoigné <i>et al.</i> , 1985
Dichloro radical anion ( $Cl_2^{\cdot -}$ )	$9 \times 10^7$	Bielski, 1993
(Dioxido)trioxidosulfate(dot-) ( $^-O_3SOO\cdot$ )	$1.6 \times 10^5$	Lind <i>et al.</i> , 2003
Hydrated electron ( $e_{aq}^-$ )	$3.6 \times 10^{10}$ $3.6 \times 10^{10}$	Bahnemann & Hart, 1982 Sehested <i>et al.</i> , 1983
Hydrogen atom ( $\cdot H$ )	$2 \times 10^{10}$	Sehested <i>et al.</i> , 1983
Hydroxyl ( $\cdot OH$ )	$3 \times 10^9$ $1.1 \times 10^8$	Bahnemann & Hart, 1982 Sehested <i>et al.</i> , 1984
2-Hydroxy-2-methylpropylperoxy ( $\cdot OOCCH_2C(CH_3)_2OH$ )	$1.8 \times 10^4$	Lind <i>et al.</i> , 2003
2-Peroxyacetic acid ( $HOC(O)CH_2OO\cdot$ )	$\geq 2.7 \times 10^4$	Lind <i>et al.</i> , 2003
2-Peroxyacetate $^-OC(O)CH_2OO\cdot$	$7.8 \times 10^3$	Lind <i>et al.</i> , 2003
2-Peroxychloroacetate ( $^-OC(O)CHClOO\cdot$ )	$1.6 \times 10^4$	Lind <i>et al.</i> , 2003
1-Peroxypropan-2-one ( $CH_3C(O)CH_2OO\cdot$ )	$\geq 7.3 \times 10^4$	Lind <i>et al.</i> , 2003
Superoxide ( $O_2^{\cdot -}$ )	$1.5 \times 10^9$ $1.6 \times 10^9$	Sehested <i>et al.</i> , 1983 Bühler <i>et al.</i> , 1984
TEMPO	$10^7$	Muñoz & von Sonntag, 2000a

<sup>(a)</sup>Estimated by kinetic modelling.

For a considerable number of radicals, standard Gibbs free energies of their reactions with ozone have been calculated (Naumov & von Sonntag, 2011a). In several cases, radicals react with ozone by giving rise to adducts. Only the adduct of the hydrated electron to ozone,  $O_3^{\bullet-}$ , is sufficiently long-lived to become detectable on the microsecond time scale, that is, by pulse radiolysis (Elliot & McCracken, 1989). For more short-lived adducts, evidence for their formation can be obtained by quantum-mechanical calculations as potential minima on the reaction path. In the majority of cases, however, no such potential minimum is obtained. "Adducts" are then, at best, bona-fide transition states *en route* to the products. The outcome of these calculations is compiled in Tables 13.2–13.5. In its reaction with free radicals, ozone has to compete with  $O_2$ , a well-known free-radical scavenger. Yet, as will be discussed below,  $O_2$  reacts only with very limited radical types rapidly and irreversibly. Thus, ozone reacts with many free radicals effectively, despite the fact that  $O_2$  is typically present in large excess over ozone.

### 13.2 OZONE REACTIONS WITH REDUCING RADICALS

The reduction potentials of  $e_{aq}^-$ ,  $H^\bullet$ ,  $CO_2^{\bullet-}$  and  $O_2^{\bullet-}$  at pH 7 are  $-2.78$  V,  $-2.4$  V,  $-1.8$  V and  $-0.33$  V ( $-0.18$  V, correcting for  $O_2$  solubility, cf. Chapter 2), respectively, while ozone has a reduction potential of  $+1.1$  V (Wardman, 1989). Thus, there is a substantial driving force for an electron transfer. With the hydrated electron, ozone reacts at a diffusion-controlled rate by addition [reaction (1)].



In water,  $O_3^{\bullet-}$  is relatively long-lived (Elliot & McCracken, 1989), and dissociative electron transfer ( $O_3 + e_{aq}^- \rightarrow O^{\bullet-} + O_2$ ) can be excluded as an alternative reaction path. The subsequent decay of  $O_3^{\bullet-}$ , an abundant precursor of  $\bullet OH$  in ozone reactions, is discussed in Chapter 11.

$H^\bullet$  also reacts by addition [reaction (2)], as indicated by quantum-chemical calculations (Table 13.2). An electron transfer process ( $O_3 + H^\bullet \rightarrow O_3^{\bullet-} + H^+$ ) is less likely.



**Table 13.2** Reactions of reducing free radicals with ozone in aqueous solution. Calculated standard Gibbs free energies ( $\Delta G^0$ , kJ mol $^{-1}$ ) of the overall reaction and of radical–ozone adducts (if formed) and their decay (Naumov & von Sonntag, 2011a)

Reactants	Products	Overall reaction	Adduct formation	Adduct decay
$e_{aq}^-$ , $O_3$	$O_3^{\bullet-}$	( $-374$ ; pH > 11)*		see (Merényi <i>et al.</i> , 2010a)
$\bullet H$ , $O_3$	$\bullet OH$ , $O_2$	$-411$	$-373$	$-38$ [ $-47$ (Naumov & von Sonntag, 2011b)]
$CO_2^{\bullet-}$ , $O_3$	$CO_2$ , $O_3^{\bullet-}$	$-315$	**	
$CO_2^{\bullet-}$ , $O_3$	$CO_3^{\bullet-}$ , $O_2$	$-370$	**	
$O_2^{\bullet-}$ , $O_3$	$O_3^{\bullet-}$ , $O_2$	$-176$	**	

\*Calculated from reported reduction potentials (Wardman, 1989); \*\*an adduct cannot be calculated as a potential minimum on the reaction path.

$HO_3^{\bullet}$  is a strong acid [ $pK_a(HO_3^{\bullet}) = -2$ ], and rapid deprotonation [reaction (3),  $k \approx 10^{12}$  s $^{-1}$ ] and decay into  $\bullet OH + O_2$  [reaction (4)], for which there is also a high driving force (Table 13.2), eventually lead to  $O_2$  and  $\bullet OH$  (see Chapter 10).



Based on the reduction potentials of  $\text{CO}_2^{\bullet-}$  and ozone (see above), there is a considerable driving force for an electron transfer [reaction (5)], but an O-transfer [reaction (6)] is not only energetically (Table 13.2) but also kinetically favoured.



Evidence for this is obtained by the fact that no chain reaction of any importance is observed in the  $\gamma$ -radiolysis of formate solutions in the presence of ozone (Lind *et al.*, 2003).

The reaction of  $\text{O}_2^{\bullet-}$  with ozone is the only one of the reducing radicals that takes place by electron transfer [reaction (7)].



Its conjugate acid, the  $\text{HO}_2^\bullet$  radical, often behaves like a peroxy radical (for ozone reactions with peroxy radicals see below), and as such is not a typical reducing radical. It is, however, in equilibrium with its conjugate base,  $\text{O}_2^{\bullet-}$ , [equilibrium (8);  $\text{p}K_a(\text{HO}_2^\bullet) = 4.8$  (Bielski *et al.*, 1985)], and even in slightly acid solutions the ozone reaction is dominated by  $\text{O}_2^{\bullet-}$ .



### 13.3 OZONE REACTIONS WITH CARBON-CENTERED RADICALS

Oxygen, which is always present when ozone is applied as an oxidant in excess of ozone. Simple carbon-centred radicals react very rapidly with  $\text{O}_2$  ( $k = 2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ) (von Sonntag & Schuchmann, 1997) as does ozone (Sehested *et al.*, 1992). Due to this competition, ozone stands a chance of reacting with this type of radical significantly only as long as it is present at concentrations comparable to that of  $\text{O}_2$ .  $\text{O}_2$  reacts with alkyl radicals by addition, and for simple carbon-centred radicals the ensuing peroxy radicals are stable [cf. reaction (9), for exceptions see below, for their reactions see Chapter 14].



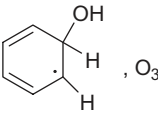
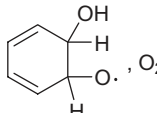
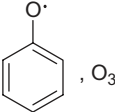
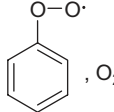
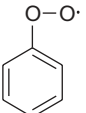
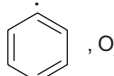
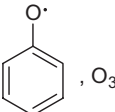
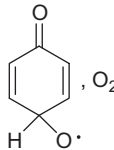
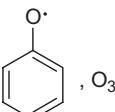
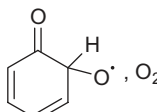
The corresponding reaction with ozone also gives rise to an adduct [cf. reaction (10)], but this adduct is highly unstable (Table 13.3) and releases  $\text{O}_2$ , thereby giving rise to an oxyl radical [cf. reaction (11)].



For larger alkyl radicals, adducts could not be calculated, and the reaction runs through to the oxyl radical (Table 13.3).

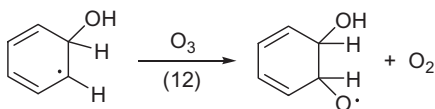
Oxyl radicals are very short-lived undergoing 1,2-H-shift and  $\beta$ -fragmentation reactions (Chapter 14). Thus, their reactions with ozone can be neglected.

**Table 13.3** Reactions of carbon-centred free radicals and phenoxy radicals with ozone in aqueous solution. Compilation of products and calculated standard Gibbs free energies ( $\Delta G^0$ , kJ mol<sup>-1</sup>) of the overall reaction and of radical–ozone adducts (if formed) and their decay (Naumov & von Sonntag, 2011a)

Reactants	Products	Overall reaction	Adduct formation	Adduct decay
$\bullet\text{CH}_3, \text{O}_3$	$\text{CH}_3\text{O}\bullet, \text{O}_2$	-340	-259	-81
$\bullet\text{CH}_2\text{C}(\text{O})\text{O}^-, \text{O}_3$	$\bullet\text{CCH}_2\text{C}(\text{O})\text{O}^-, \text{O}_2$	-344	*	
 , $\text{O}_3$	 , $\text{O}_2$	-259	*	
 , $\text{O}_3$	 , $\text{O}_2$	-85	*	
 , $\text{O}_3$	 , $\text{O}_2$	+61		
 , $\text{O}_3$	 , $\text{O}_2$	-187	*	
 , $\text{O}_3$	 , $\text{O}_2$	-191	*	

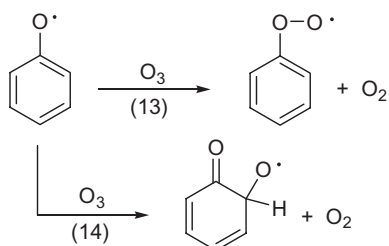
\*An adduct cannot be calculated as a potential minimum on the reaction path.

Hydroxycyclohexadienyl radicals must play an important role, notably in wastewater ozonation, where ozone is converted to a considerable extent into  $\bullet\text{OH}$  (Chapter 3). It reacts predominantly with the aromatic moieties of the organic matter giving rise to hydroxycyclohexadienyl radicals. In contrast to  $\text{O}_2$ , which reacts reversibly with these radicals (Chapter 14), ozone must react irreversibly [reaction (12)] without a detectable adduct as an intermediate (Table 13.3). In this respect, the hydroxycyclohexadienyl radicals differ from simple alkyl radicals, for which an, albeit very labile, adduct has been calculated [cf. reactions (10)/(11) and Table 13.3].



Phenoxy radicals are intermediates in the ozonolysis of phenols (Chapter 7), and phenolic compounds are generated in wastewater (Chapter 3) in the course of ozone treatment. They barely react with  $\text{O}_2$

(see below). Thus their reactions with ozone deserve some consideration. They are commonly written with the free spin at oxygen, but the overwhelming spin density is at carbon at the *ortho* and *para* positions of the benzene ring [(Naumov & von Sonntag, 2011a, SI)]. Recombination of two phenoxyl radicals at oxygen is strongly endergonic and does not take place, but recombination does occur by forming C–O and C–C linkages (Benn *et al.*, 1979; Ye & Schuler, 1989; Jin *et al.*, 1993). Thus, phenoxyl radicals largely behave as carbon-centred radicals. Although ozone addition at oxygen and concomitant O<sub>2</sub> loss is exergonic [reaction (13)], an addition at carbon [reaction (14)] is even more so (Table 13.3).



Since ozone is strongly electrophilic (Chapter 7), an addition at carbon seems to be more likely than an addition at oxygen. Hence reaction (14) may be preferred over reaction (13). O<sub>2</sub> loss from the phenylperoxyl radical is markedly endergonic (Table 13.3), and such peroxyl radicals are indeed well documented (Mertens & von Sonntag, 1994a; Naumov & von Sonntag, 2005). No adducts have been detected as intermediates in the calculations of reactions (13) and (14).

### 13.4 OZONE REACTIONS WITH OXYGEN-CENTERED RADICALS

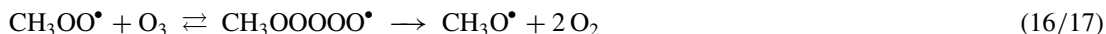
Here, we deal with radicals of strongly varying reactivity towards DOM, the highly reactive  $\bullet\text{OH}$  (for its reactions see Chapter 14), and the practically non-reactive peroxyl and nitroxyl radicals. In their reactivity, alkoxy radicals ( $\text{RO}\bullet$ ) resemble  $\bullet\text{OH}$ . Yet in water, they undergo very rapid unimolecular reactions (Chapter 14) that compete effectively with a reaction with ozone and thus they are not considered here. Calculated standard Gibbs free energies of their ozone reactions are compiled in Table 13.4.

The reaction of  $\bullet\text{OH}$  with ozone has been formulated as an O-transfer [reaction (15)]. This reaction is fast (Table 13.1) and strongly exergonic (Table 13.4). An adduct could not be calculated.

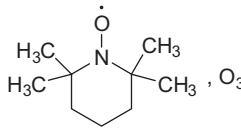
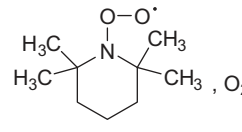
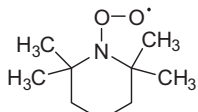
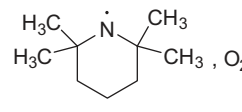
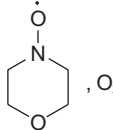
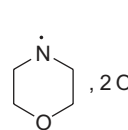


In the absence of  $\bullet\text{OH}$  scavengers, this reaction turns into a chain reaction in which ozone is decomposed into O<sub>2</sub> (Chapter 3).

A number of peroxyl radicals have been generated radiolytically, and their reactions with ozone have been studied (Lind *et al.*, 2003). From an evaluation of the data, rate constants have been calculated and are compiled in Table 13.1. They centre near  $10^4 \text{ M}^{-1} \text{ s}^{-1}$ , except for  $\text{}^-\text{O}_3\text{SOO}\bullet$  which reacts an order of magnitude faster (Table 13.1). For the methylperoxyl radical, a short-lived ozone adduct has been calculated [reaction (16)] that releases O<sub>2</sub> [reaction (17)] (Table 13.4). With other peroxyl radicals, such adducts are only bona fide transition states.

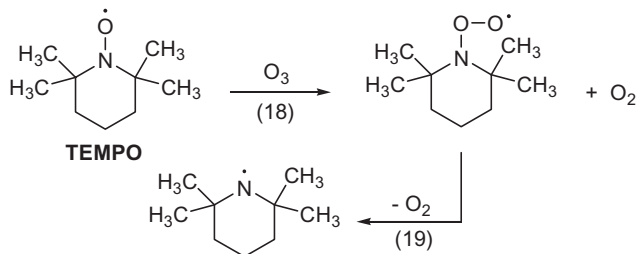


**Table 13.4** Reactions of oxygen-centred free radicals with ozone in aqueous solution. Compilation of products and calculated standard Gibbs free energies ( $\Delta G^0$ , kJ mol<sup>-1</sup>) of the overall reaction and of radical–ozone adducts (if formed) and their decay (Naumov & von Sonntag, 2011a)

Reactants	Products	Overall reaction	Adduct formation	Adduct decay
$\cdot\text{OH}, \text{O}_3$	$\text{HO}_2\cdot, \text{O}_2$	-229	*	
$\text{CH}_3\text{O}\cdot, \text{O}_3$	$\text{CH}_3\text{OO}\cdot, \text{O}_2$	-190	*	
$\text{CH}_3\text{OO}\cdot, \text{O}_3$	$\text{CH}_3\text{O}\cdot, 2 \text{O}_2$	-238	-19	-219
$\text{HOC(O)CH}_2\text{OO}\cdot, \text{O}_3$	$\text{HOC(O)CH}_2\text{O}\cdot, 2 \text{O}_2$	-249	*	
$\text{}^-\text{OC(O)CH}_2\text{OO}\cdot, \text{O}_3$	$\text{}^-\text{OC(O)CH}_2\text{O}\cdot, 2 \text{O}_2$	-272	*	
$\text{}^-\text{OC(O)CHClOO}\cdot, \text{O}_3$	$\text{}^-\text{OC(O)CHClO}\cdot, 2 \text{O}_2$	-362	*	
$\text{CH}_3\text{C(O)CH}_2\text{OO}\cdot, \text{O}_3$	$\text{CH}_3\text{C(O)CH}_2\text{O}\cdot, 2 \text{O}_2$	-255	*	
$\text{HOC(CH}_3)_2\text{CH}_2\text{OO}\cdot, \text{O}_3$	$\text{HOC(CH}_3)_2\text{CH}_2\text{O}\cdot, 2 \text{O}_2$	-398	*	
$\text{}^-\text{O}_3\text{SOO}\cdot, \text{O}_3$	$\text{}^-\text{O}_3\text{SO}\cdot, 2 \text{O}_2$	-253	*	
 TEMPO, O <sub>3</sub>	 O <sub>2</sub>	-46	*	
	 O <sub>2</sub>	-51		
 O <sub>3</sub>	 2 O <sub>2</sub>	-96	*	

\*An adduct cannot be calculated as a potential minimum on the reaction path.

The stable nitroxyl radical TEMPO, often used as ESR standard, reacts rapidly with ozone (Table 13.1). In the first step, one molecule of O<sub>2</sub> is released [reaction (18)] without a detectable adduct as an intermediate. The nitrogen-centred peroxy radical thus formed is unstable and loses O<sub>2</sub> [reaction (19)]. For standard Gibbs free energies see Table 13.4.



The negative standard Gibbs free energy of reaction (19) is in agreement with the general observation, that nitrogen-centred radicals do not react with O<sub>2</sub> (von Sonntag & Schuchmann, 1997). In its reaction

with ozone, the morpholine-derived nitroxyl radical shows the same overall standard Gibbs free energy for the release of two molecules of  $O_2$  (Table 13.4). In contrast to the TEMPO system, an intermediate peroxy radical cannot be calculated here.

### 13.5 OZONE REACTIONS WITH NITROGEN- AND SULFUR-CENTRED RADICALS

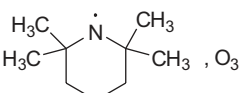
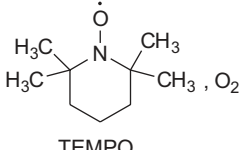
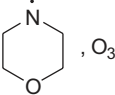
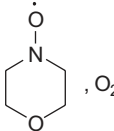
Nitrogen-centred radicals are intermediates in the reaction of ozone with primary and secondary amines, as all amines give rise to  $\bullet OH$  (Chapter 8). The precursor of the latter is  $O_3^{\bullet -}$ , and an amine radical cation must be the corresponding product. Except for tertiary amine radical cations, amine radical cations are in equilibrium with the aminyl radicals [cf. equilibrium (20)].



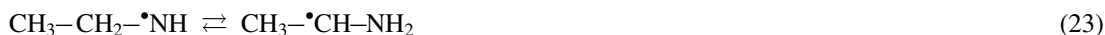
Rate constants for the reaction of aminyl radicals with ozone are as yet not known, but the exergonicity of this reaction is remarkable (cf. Table 13.5), and this reaction (21) may be quite fast.



**Table 13.5** Reactions of nitrogen- and sulfur-centred free radicals with ozone in aqueous solution. Compilation of products and calculated standard Gibbs free energies ( $\Delta G^0$ ,  $\text{kJ mol}^{-1}$ ) of the overall reaction (Naumov & von Sonntag, 2011a)

Reactants	Products	Overall reaction
	 TEMPO	-331
		-320
$CH_3S\bullet, O_3$	$CH_3SO\bullet, O_2$	-356

Considering the fast reactions (18)/(19), reactions (21)/(22) would give rise to an ozone consuming chain reaction without forming products other than  $O_2$ . It has been suggested that such a cycle plays a role in the ozone chemistry of diclofenac to explain the surprisingly low diclofenac consumption (Sein *et al.*, 2008). Further data are required to substantiate this suggestion. In contrast to the  $\bullet OH/HO_2\bullet$  chain reaction, this ozone destroying chain reaction stands a chance of being much shorter and always of importance, as some aminyl radicals can rearrange into the corresponding carbon-centred radicals, for example, reaction (23) ( $\Delta G^0 = -31 \text{ kJ mol}^{-1}$ ).



Such reactions are analogous to the well-documented 1,2-H shift reactions of alkoxy radicals [cf. reaction (24),  $\Delta G^0 = -36 \text{ kJ mol}^{-1}$ ].



The 1,2-H shift reactions of alkoxy radicals are very fast (in the order of  $10^6 \text{ s}^{-1}$ ), and as the driving force for reaction (23) is lower by  $5 \text{ kJ mol}^{-1}$ , its rate may be lower. The rate of reaction (23) will determine whether or not the above chain reaction will become effective.

In the thiol system, in contrast, the equilibrium heteroatom-centred vs. carbon-centred radical lies on the side of the thiyl radical [reaction (25),  $\Delta G^0 = +26 \text{ kJ mol}^{-1}$ ].



Moreover, the reaction of a thiyl radical with  $\text{O}_2$  is also slightly endergonic [reaction (26),  $\Delta G^0 = +15 \text{ kJ mol}^{-1}$ ].



This causes the thiyl radical/ $\text{O}_2$  reaction to become reversible (Zhang *et al.*, 1994; Naumov & von Sonntag, 2005).

Thiols react very rapidly with ozone without giving rise to thiyl radicals (Chapter 9). Therefore, reaction (27) is of little consequence in practice.



Reaction (27) is highly exergonic (Table 13.5) and thus irreversible. This is in contrast to the reaction of thiyl radicals with  $\text{O}_2$  (see above) and, again, is a striking example for how differently ozone and  $\text{O}_2$  may behave in their radical scavenging properties.

### 13.6 OZONE REACTIONS WITH HALOGEN-CENTRED RADICALS

The reactions of ozone with halide ions are discussed in Chapter 11. They do not directly give rise to free radicals. Ozone-induced free-radical formation only sets in when the oxidation proceeds to chlorite and bromite (Chapter 11). Yet,  $\bullet\text{OH}$  radicals, which are abundantly formed in ozone reactions with DOM (Chapter 3), give rise in their reactions with  $\text{Br}^-$  to  $\text{Br}^\bullet$  (Chapter 14), and the  $\bullet\text{OH}$  route in ozone reactions can contribute to bromate formation in drinking water ozonation (Chapter 11). Although the reaction of  $\bullet\text{OH}$  with  $\text{Cl}^-$  to  $\text{Cl}^\bullet$  becomes effective only in acid solution (Chapter 14),  $\text{Cl}^\bullet$  reactions are included here for discussing similarities and differences when compared to  $\text{Br}^\bullet$ . In the presence of halide ions, the halogen atoms are in equilibrium with the corresponding three-electron bonded complexes such as  $\text{Cl}_2^{\bullet-}$  and  $\text{Br}_2^{\bullet-}$  (Chapter 14). Rate constants of halogen-derived radicals are compiled in Table 13.1 and calculated standard Gibbs free energies in Table 13.6.



**Table 13.6** Reactions of halogen-containing free radicals with ozone in aqueous solution. Compilation of products and calculated standard Gibbs free energies ( $\Delta G^0$ , kJ mol<sup>-1</sup>) of the overall reaction and of radical–ozone adducts (if formed) and their decay (Naumov & von Sonntag, 2011a)

Reactants	Products	Overall reaction	Adduct formation	Adduct decay
$\bullet\text{Cl}$ , $\text{O}_3$	$\text{ClO}\bullet$ , $\text{O}_2$	-204	*	
$\text{Cl}_2^{\bullet-}$ , $\text{O}_3$	$\text{ClO}\bullet$ , $\text{O}_2$ , $\text{Cl}^-$	-133	*	
$\text{ClO}\bullet$ , $\text{O}_3$	$\text{OClO}\bullet$ , $\text{O}_2$	-119	*	
$\text{ClO}\bullet$ , $\text{O}_3$	$\text{ClOO}\bullet$ , $\text{O}_2$	-229	+5, see text	
$\text{OClO}\bullet$ , $\text{O}_3$	$\text{ClO}_3\bullet$ , $\text{O}_2$	+9	*	
$\text{OClO}\bullet$ , $\text{O}_3$	$\text{ClO}\bullet$ , 2 $\text{O}_2$	-311	*	
2 $\text{ClO}_3\bullet$	$\text{O}_3\text{Cl}-\text{ClO}_3$	+109		
2 $\text{ClO}_3\bullet$	$\text{ClO}_4^-$ , $\text{ClO}_2^+$	-40	*	
$\text{OClO}\bullet + \text{ClO}_3\bullet$	$\text{O}_3\text{Cl}-\text{ClO}_2$	+93		
$\text{OClO}\bullet + \text{ClO}_3\bullet$	$\text{O}_2\text{Cl}-\text{OClO}_2$	+29		
$\text{OClO}\bullet + \text{ClO}_3\bullet$	$\text{ClO}\bullet + \text{O}_2 + \text{OClO}\bullet$	-222	*	
$\text{Br}\bullet$ , $\text{O}_3$	$\text{BrO}\bullet$ , $\text{O}_2$	-149	*	
$\text{BrO}\bullet$ , $\text{O}_3$	$\text{BrOO}\bullet$ , $\text{O}_2$	-268	*	
$\text{BrOO}\bullet$	$\text{Br}\bullet + \text{O}_2$	-11	*	
$\text{BrO}\bullet$ , $\text{O}_3$	$\text{OBrO}\bullet$ , $\text{O}_2$	-47	*	
2 $\text{OBrO}\bullet$	$\text{OBrOOBrO}$	+11		
2 $\text{OBrO}\bullet$	$\text{O}_2\text{BrOBrO}$	+130		
$\text{OBrOOBrO}$	2 $\bullet\text{Br}$ , 2 $\text{O}_2$	-282		
$\text{OBrO}\bullet$ , $\text{O}_3$	$\text{BrO}\bullet + 2 \text{O}_2$	-380		
$\text{OBrO}\bullet$ , $\text{O}_3$	$\text{O}_2\text{BrO}\bullet$ , $\text{O}_2$	+81	+102	-1
$\text{O}_2\text{BrO}\bullet$ , $\text{O}_3$	$\text{BrO}_4\bullet$ , $\text{O}_2$	+93	+114	-21
$\text{BrO}_3\bullet$	$\text{BrO}\bullet$ , $\text{O}_2$	-506		
$\text{BrO}_4\bullet$	$\text{OBrO}\bullet$ , $\text{O}_2$	-413		

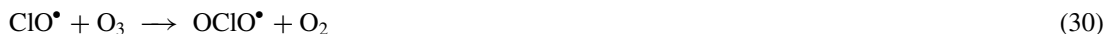
\*An adduct cannot be calculated as a potential minimum on the reaction path.

With ozone,  $\bullet\text{Cl}$  and  $\text{Cl}_2^{\bullet-}$  undergo O-transfer without adducts as potential minima on the reaction paths [reactions (28) and (29)].



A rate constant is only available for  $\text{Cl}_2^{\bullet-}$  (Table 13.1). As expected, the reaction becomes less exergonic, when  $\text{Cl}\bullet$  is complexed to  $\text{Cl}^-$  (Table 13.6). The  $\text{Cl}_2^{\bullet-}$  reaction resembles the reaction of  $\bullet\text{OH}$  with ozone. In the both cases, rate constants are well below the diffusion-controlled limit (Table 13.1) despite the high exergonicity of these reactions. As an explanation, one may tentatively suggest that the pronounced electrophilicity of ozone may play a role in preventing, by electrostatic repulsion, a favourable transition state in reactions of nitrogen-, oxygen- and halogen-centred radicals and thus reducing the rate of reaction (cf. also TEMPO and peroxy radicals, Table 13.1).

For the subsequent oxidation of the  $\text{ClO}^\bullet$  radical by ozone, two exergonic reactions may be written. Reaction (30) gives rise to (stable) chlorine dioxide,  $\text{OClO}^\bullet$ , but a reaction to its isomer, the unstable chlorineperoxy radical,  $\text{ClOO}^\bullet$ , is even more exergonic [reaction (31)/(32), Table 13.6]. Without additional information, a decision as to which of them is kinetically favoured cannot be made.



The  $\text{ClOO}^\bullet$  species has a calculated  $\text{Cl}-\text{OO}^\bullet$  bond length of 2.331 Å and  $\text{ClO}-\text{O}^\bullet$  bond length of 1.888 Å. The latter is practically identical to the  $\text{O}=\text{O}$  bond length, 1.186 Å. This indicates that the  $\text{ClOO}^\bullet$  species detected in these calculations must be a kind of van der Waals complex of  $\text{Cl}^\bullet$  with  $\text{O}_2$ , and the value of  $\Delta G^0 = +5 \text{ kJ mol}^{-1}$  cannot be related to the equilibrium constant of reaction (32). This is in contrast to the only seemingly analogous equilibrium  $\text{HOOO}^\bullet \rightleftharpoons \text{}^\bullet\text{OH} + \text{O}_2$  ( $\Delta G^0 = -47 \text{ kJ mol}^{-1}$ ), where  $\text{HO}-\text{OO}^\bullet$  (1.520 Å) and  $\text{HOO}-\text{O}^\bullet$  (1.243 Å) bond lengths are quite different from those of the final products (Naumov & von Sonntag, 2011b).

In the reaction of chlorine dioxide with ozone, there may be two competing reactions [reactions (33) and (34)].



The observed reaction is only moderately fast (Table 13.6), and this is compatible with reaction (33) being slightly endergonic. Reaction (34) is strongly exergonic (Table 13.6) but complex. Thus, reaction (33) may compete successfully in the case where there is substantial activation energy for reaction (34). Formation of  $^1\text{O}_2$  in uncommonly high yield has been reported for this reaction in  $\text{CCl}_4$  solutions (Chertova *et al.*, 2000).

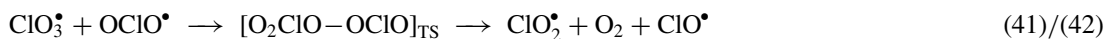
The  $\text{ClO}_3^\bullet$  radical cannot be further oxidised by ozone and has to decay bimolecularly. Among the two potential combination reactions [reaction (35),  $\text{Cl}-\text{Cl}$  2.5 Å] and (36), the high endergonicity of reaction (35) (Table 13.6) prevents this reaction from taking place, and the bimolecular decay of  $\text{ClO}_3^\bullet$  radical must occur via an asymmetrical recombination, reaction (36). Upon trying to calculate the standard Gibbs free energies of this reaction, the program proceeded automatically toward perchlorate ion and  $\text{ClO}_2^+$  [reaction (37), Table 13.6].  $\text{ClO}_2^+$  reacts with water yielding chlorate [reaction (38)].



Perchlorate formation has been intriguing the scientific community for a long time (Rao *et al.*, 2010).  $\text{ClO}_3^\bullet$  has been envisaged as precursor, but details have remained obscure. It is important to note that perchlorate is not an important product in the reaction of  $\text{ClO}^-/\text{ClO}_2^-$  with ozone (Haag & Hoigné, 1983b), and perchlorate formation must be a minor side reaction. This raises the question, whether bimolecular decay of  $\text{ClO}_3^\bullet$  may compete with a termination with  $\text{OClO}^\bullet$  radicals in the case where there is a sufficiently high steady-state concentration of  $\text{OClO}^\bullet$  radicals present in equilibrium (note the relatively slow reaction of  $\text{OClO}^\bullet$  with ozone, Table 13.1). This reaction could eventually give rise to two molecules of chlorate ion in the case where the dimers were sufficiently long-lived to react with water. Yet, reaction (39) is markedly endergonic (Table 13.6) with a long  $\text{Cl}-\text{Cl}$  bond (1.980 Å), and this reaction is most likely reversible. Reaction (40) is less endergonic but also potentially reversible.



Moreover, a highly exergonic termination via the oxygens, proceeding directly, with a peroxidic arrangement only as a likely transition state, to  $\text{OCl}^\bullet$  and  $\text{OCIO}^\bullet$  plus  $\text{O}_2$ , could also take place [reactions (41) and (42)]. To which extent these reactions contribute to chlorate formation has still to be explored.



The reaction of the  $\text{Br}^\bullet$  atom with ozone is strongly exergonic [reaction (43), Table 13.6], and for the ensuing  $\text{BrO}^\bullet$  one can envisage the likewise exergonic reactions (44)–(48).



Preference will be determined by kinetics, that is, whether ozone addition at oxygen or at bromine is preferred.

In the ozonation of  $\text{Br}^-$ -containing waters, there is a second route to  $\text{OBrO}^\bullet$ . There is now strong evidence that the current concept of bromate formation (von Gunten, 2003b) has to be revised. The reaction of bromite with ozone does not give rise to bromate by O-transfer but is an electron transfer reaction that yields  $\text{OBrO}^\bullet$  and  $\text{O}_3^{\bullet -}$  (Chapter 11). Formation and decay of  $\text{OBrO}^\bullet$  has been studied by pulse radiolysis (Buxton & Dainton, 1968) concluding that the bimolecular decay leading to a  $\text{Br}_2\text{O}_4$  intermediate is (i) reversible, (ii) decays by reacting with water and (iii) with  $\text{OH}^-$ . There are two conceivable dimers [reactions (47) and (48)].



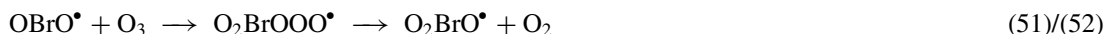
While the symmetrical dimerisation is only mildly endergonic (Table 13.6) and could account for the reported reversibility, the asymmetrical one is strongly endergonic and has to be disregarded.

There is, however, also the possibility that the symmetrical dimer decays according to reaction (49).

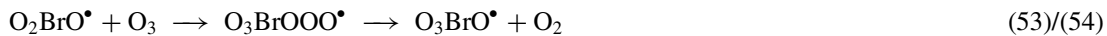


This is the route taken upon prolonged optimisation. Yet in water, where an  $\text{OH}^-$ -induced component of the decay of  $\text{OBrO}^\bullet$  radicals is observed, this reaction seems not to be kinetically favoured despite the high exergonicity (Table 13.6).

The bimolecular decay of  $\text{OBrO}^\bullet$  to  $\text{Br}_2\text{O}_4$  is reversible, but  $\text{Br}_2\text{O}_4$  reacts rapidly with water and  $\text{OH}^-$  and thus sufficiently high  $\text{OBrO}^\bullet$  concentrations should not build up for reactions of  $\text{OBrO}^\bullet$  with ozone to become relevant. Yet in the case where it would, the energetically favoured (Table 13.6) route is reaction (50), while reaction sequence (51)/(52) may not compete (Table 13.6).



Oxidation of  $\text{O}_2\text{BrO}^\bullet$  to  $\text{O}_3\text{BrO}^\bullet$  [reactions (53)/(54)] is endergonic (Table 13.6), and if  $\text{O}_2\text{BrO}^\bullet$  and  $\text{O}_3\text{BrO}^\bullet$  were formed they would undergo the strongly exergonic  $^3\text{O}_2$ -releasing reactions (55) and (56) (Table 13.6).



Thus it seems that  $\text{Br}^\bullet$  is not oxidised by ozone beyond  $\text{OBrO}^\bullet$ .

# Chapter 14

## Reactions of hydroxyl and peroxy radicals

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### 14.1 INTRODUCTORY REMARKS

Hydroxyl radicals are abundant by-products of ozone reactions (cf. Chapters 3, 7, 8, and 11) and are generated in high yields in the reaction of ozone with the DOM of the water matrix of drinking water and wastewater (Chapter 3). They assist in eliminating ozone-refractory micropollutants, as their reactivity is generally high, often close to the diffusion-controlled limit [for a compilation of rate constants see Buxton *et al.* (1988)]. While in pollution abatement, their action is beneficial, they may also contribute to the formation of undesired disinfection by-products such as bromate (Chapters 3, 11 and below). First, the general reactions of  $\bullet\text{OH}$  are discussed [for a more detailed discussion see von Sonntag (2006)]. In technical applications, ozone is always introduced together with a large excess of  $\text{O}_2$ . The radicals that are formed upon  $\bullet\text{OH}$  attack react with ozone (Chapter 13), but many of them also react with  $\text{O}_2$ , thereby forming peroxy radicals. With  $\text{O}_2$  in excess, the formation and reactions of peroxy radicals are of major importance in ozone reactions in aqueous solution. There is a considerable wealth of data on those reactions, and peroxy radical chemistry in aqueous solution is now fairly well understood. Some aspects are discussed below [for more detailed reviews see von Sonntag & Schuchmann (1991, 1997) and von Sonntag (2006)]. At the end of this chapter, the role of  $\bullet\text{OH}$  in disinfection by-product formation and micropollutant abatement is addressed.

### 14.2 HYDROXYL RADICAL REACTIONS

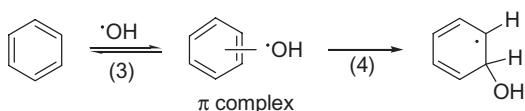
There are three types of reactions, addition reactions, H-abstraction reactions and electron transfer reactions. The most common and fastest reactions are the addition reactions. Many of them are close to diffusion-controlled. When this reaction pathway is not available,  $\bullet\text{OH}$  may also react by H-abstraction. Electron transfer reactions are rare, and the high reduction potential of  $\bullet\text{OH}$  [2.3 V at pH 7 (Wardman, 1989)] is not a measure of its high reactivity. As with many other reactions,  $\bullet\text{OH}$  reactions are often governed by kinetics rather than by thermodynamics (see below), and this has to be recalled when thermodynamic data are used for discussing probabilities of reaction pathways.

#### 14.2.1 Addition reactions

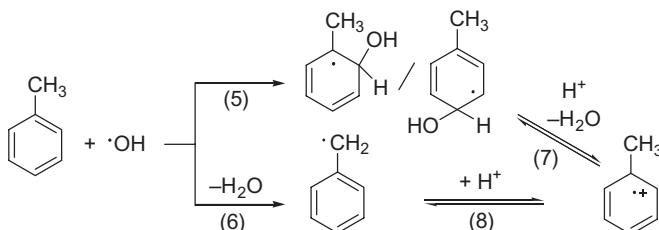
The  $\bullet\text{OH}$  radical adds readily to C–C, C–N and S–O double bonds (with four-valent sulfur) but not to C=O double bonds [e.g. reactions (1) (Söylemez & von Sonntag, 1980) and (2) (Veltwisch *et al.*, 1980)].



Despite this, there is a high regioselectivity in the reaction of the electrophilic (Anbar *et al.*, 1966)  $\bullet\text{OH}$  with C—C double bonds carrying different electron-donating or electron-withdrawing substituents. The first intermediate must be a  $\pi$ -complex as inferred from the kinetics of  $\bullet\text{OH}$  with benzene at very high temperatures (Ashton *et al.*, 1995). The  $\pi$ -complex is in equilibrium with benzene and  $\bullet\text{OH}$  [equilibrium (3)] and subsequently collapses into a  $\sigma$ -complex, the  $\bullet\text{OH}$  adduct proper [reaction (4)]. In the  $\pi$ -complex, the  $\bullet\text{OH}$  radical is guided to its final position, and substituents at the C—C double bond may have a strong directing effect.



The site of addition is dominated by kinetics rather than by thermodynamics, that is, the preferred  $\bullet\text{OH}$  addition may not lead to the thermodynamically favoured radical. A case in point is the  $\bullet\text{OH}$  chemistry of the nucleobases (von Sonntag, 2006; Naumov & von Sonntag, 2008a). Another striking example is the reaction of  $\bullet\text{OH}$  with toluene. Here, formation of a  $\pi$ -complex and subsequent collapse into the  $\sigma$ -complex causes a preferred addition to the ring (92%) [reaction (5)], and only 8% undergo H-abstraction from the methyl group [reaction (6), formation of the thermodynamically favoured benzyl radical] (Christensen *et al.*, 1973).



Upon proton catalysis, the thermodynamic equilibrium can be established by converting the  $\bullet\text{OH}$  adduct into the benzyl radical via a radical cation [reactions (7) and (8)].

Addition reactions also can take place to the lone electron pairs of electron-rich heteroatoms such as in amines, sulfides, disulfides, halide and pseudo-halide ions. Under such conditions, three-electron intermediates are formed [e.g. reactions (9) and (10), for a review see Asmus (1979)].



Experimental evidence for these three-electron-bonded intermediates have been obtained by pulse radiolysis, but in some cases, such as with the amines (Das & von Sonntag, 1986), they are too short-lived for detection and may only be inferred by analogy.

Many oxidation reactions of transition metal ions are in fact also addition reactions [e.g. reaction (11)] (Asmus *et al.*, 1978).



The product to be expected for an electron transfer is often only observed in acid solution such as reactions (12) and (13).



Reactions (10) [ $K_{10} = 1.4 \text{ M}$  (Jayson *et al.*, 1973)] and (12) [ $k_{12} = 5 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$ , cf. (Buxton *et al.*, 2000)] are of importance for  $\text{Cl}^-$ -containing waters, and these data may be used for assessing to what extent  $\bullet\text{OH}$  and  $\text{Cl}^{\bullet}$  play a role at a given pH [note that  $\bullet\text{OH}$  is drawn out of equilibrium (10) by  $\bullet\text{OH}$ -reactive substrates other than  $\text{Cl}^-$  present in such waters, see below; for a discussion of the reactivity of  $\text{Cl}^{\bullet}$  in aqueous solution see (Buxton *et al.*, 1998; Buxton *et al.*, 1999; Buxton *et al.*, 2000)].

Reversibility of  $\bullet\text{OH}$  addition is also observed with other systems such as  $\text{Cu}^{2+}$  in acid solution [equilibrium (14)] (Ulanski & von Sonntag, 2000).



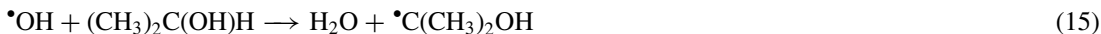
### 14.2.2 H-abstraction reactions

The H-abstraction reactions are typically somewhat slower than addition reactions. Here, the R–H bond dissociation energy (BDE) plays a major role (for a compilation of BDEs see Table 14.1).

**Table 14.1** Compilation of some R–H BDEs (unit:  $\text{kJ mol}^{-1}$ ;  $1 \text{ kcal mol}^{-1} = 4.18 \text{ kJ mol}^{-1}$ )

R–H bond	BDE/ $\text{kJ mol}^{-1}$	Reference
C–H (aromatic)	465	Berkowitz <i>et al.</i> , 1994
C–H (vinylic)	465	Berkowitz <i>et al.</i> , 1994
C–H (primary)	423	Berkowitz <i>et al.</i> , 1994
C–H (primary in MeOH)	402	Berkowitz <i>et al.</i> , 1994
C–H (secondary)	412	Berkowitz <i>et al.</i> , 1994
C–H (secondary in EtOH)	396	Reid <i>et al.</i> , 2003
C–H (tertiary)	403	Berkowitz <i>et al.</i> , 1994
C–H (tertiary in 2-PrOH)	393	Reid <i>et al.</i> , 2003
C–H (allylic)	367	Berkowitz <i>et al.</i> , 1994
C–H (benzylic)	367	Berkowitz <i>et al.</i> , 1994
C–H (pentadienylic)	343	Schöneich <i>et al.</i> , 1990
C–H (in peptides)	330–370	Reid <i>et al.</i> , 2003
O–H (alcoholic)	436	Berkowitz <i>et al.</i> , 1994
O–H (water)	499	Berkowitz <i>et al.</i> , 1994
O–H (phenolic)	360	Parsons, 2000
O–H (hydroperoxidic)	366	Golden <i>et al.</i> , 1990
S–H (thiolic)	366	Armstrong, 1999
S–H (thiophenolic)	330	Armstrong, 1999

With the weak RS—H bond, the rate of reaction is diffusion controlled (in fact, H-abstraction may be preceded by addition to sulfur), but with C—H bonds there is some grading, tertiary > secondary > primary. With 2-propanol, for example, the tertiary hydrogen competes favourably [reaction (15), 86%] over the abstraction of one of the six primary ones [reaction (16), 14%] (Asmus *et al.*, 1973).



An H-abstraction from the OH group [reaction (17)] can usually be neglected (here 3%) due to its high BDE, as a rapid 1,2-H shift converts the oxyl radical into the thermodynamically favoured carbon-centred radical [reaction (18); for competing reactions of the oxyl radical see section on peroxy radicals and (von Sonntag, 2006)].



Addition and H-abstraction reactions may be used for the study of the same intermediate. A case in point is the  $\bullet\text{C}(\text{O})\text{NH}_2$  radical, which is formed from formamide by H-abstraction and from cyanide by addition and subsequent rearrangement of the  $\bullet\text{OH}$  adduct radical (Muñoz *et al.*, 2000). Similarly, there are two ways to generate  $\alpha$ -hydroxyalkyl radicals. One is by H-abstraction [e.g. reaction (15)]. The other is by reacting the corresponding carbonyl compound with the solvated electron and protonation of the thus-formed radical anion. In the absence of  $\text{O}_2$ , carbon-centred radicals decay by dimerisation and disproportionation. The latter occurs typically by H-transfer, but some more complex reactions have also been reported for  $\text{CO}_2^{\bullet-}$  and  $\text{CHO}^{\bullet-}$  (Flyunt *et al.*, 2001b; Wang *et al.*, 1996).

### 14.2.3 Electron transfer reactions

At pH 7, the one-electron reduction potential of the  $\bullet\text{OH}$  radical is 2.3 V (Wardman, 1989). Thus in principle, it could undergo one-electron oxidation reactions quite readily. Yet, this reaction is often kinetically disfavoured, and addition reactions occur instead. A case in point is reaction (11). An interesting example is the reaction of phenol and its halogen-substituted derivatives. The reduction potential of phenol at pH 7 is 0.86 V (Merényi *et al.*, 1988). Yet, phenoxy radicals [deprotonation products of the phenol radical cation,  $\text{p}K_{\text{a}} = -2$  (Dixon & Murphy, 1976)] are formed in very minor primary yield (Mvula *et al.*, 2001). This even holds for a reaction of  $\bullet\text{OH}$  with phenolates. Addition is the dominating reaction, unless the preferred sites of addition (the *ortho* and *para* positions) are blocked by a bulky substituent (Table 14.2) (Fang *et al.*, 2000).

**Table 14.2** Addition vs. electron transfer in the reaction of  $\bullet\text{OH}$  with the anions of halogenated phenols according to Fang *et al.* (2000)

Phenolate	Addition/%	Electron transfer/%
Pentafluorophenolate	73	27
Pentachlorophenolate	47	53
Pentabromophenolate	27	73
2,4,6-Triiodophenolate	3	97



### 14.3 DETERMINATION OF $\bullet\text{OH}$ RATE CONSTANTS

Most of the available  $\bullet\text{OH}$  rate constants [for a compilation see Buxton *et al.* (1988)] were determined by pulse radiolysis. Here, an  $\text{N}_2\text{O}$ -saturated water containing the compound in question at low concentrations is subjected to a short electron pulse of a few nanoseconds to 1  $\mu\text{s}$  duration. Under such conditions, the energy of the electron beam (energy 1–10 MeV) is absorbed by the solvent. This causes ionisations [reaction (19)] and excitations [reaction (20)].



The water radical cation is a very strong acid and rapidly (within pulse duration) deprotonates, giving rise to an  $\bullet\text{OH}$  radical [reaction (21)]. The excited water molecule decomposes into  $\bullet\text{H}$  and  $\bullet\text{OH}$  [reaction (22)]. The electron formed in reaction (19) becomes solvated by water [reaction (23)], and the solvated electron [for rate constants see Buxton *et al.* (1988)] is converted into further  $\bullet\text{OH}$  in the presence of  $\text{N}_2\text{O}$  [reaction (24)].



Of the two radicals,  $\bullet\text{OH}$  (90%) dominates over  $\text{H}\bullet$  (10%). Moreover,  $\bullet\text{OH}$  is considerably more reactive than  $\text{H}\bullet$  [for rate constants see Buxton *et al.* (1988)], and the kinetics of the build-up of transients caused by the reaction of  $\bullet\text{OH}$  with the substrate ( $\text{N}_2\text{O}$  does not react with  $\bullet\text{OH}$ ) can usually be separated from the small contribution of the  $\text{H}\bullet$  atom. The  $\bullet\text{OH}$  radical only absorbs far into the UV, and one has to rely in such measurements on the formation of products (often short-lived transients). In such a case,  $k_{\text{obs}}$  of product build-up is plotted as a function of the substrate concentration. From the slope of this plot, the  $\bullet\text{OH}$  rate constant is calculated ( $k = k_{\text{obs}}/[\text{substrate}]$ ). When the product of  $\bullet\text{OH}$  with the substrate has no marked absorption in the accessible wavelength region, one can measure the  $\bullet\text{OH}$  rate constant by competition with a substrate that gives rise to a strong signal and for which the rate constant is well established.  $[\text{Fe}(\text{CN})_6]^{4-}$  ( $k = 1.05 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$ , product:  $[\text{Fe}(\text{CN})_6]^{3-}$ ) or thymine ( $k = 6.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ , product:  $\bullet\text{OH}$  adduct radicals) may serve this purpose Buxton *et al.* (1988).

In competition kinetics, the product of the competitor (P) at constant competitor (C) concentration and constant  $\bullet\text{OH}$  concentration is measured as a function of varying substrate (S) concentrations. As the  $\bullet\text{OH}$  rate constant of the competitor ( $k_C$ ) is known, that of the substrate ( $k_S$ ) can be determined based on equations (25)–(27).



$$[\text{P}] = [\bullet\text{OH}] \times k_C \times [\text{C}] / (k_C \times [\text{C}] + k_S \times [\text{S}]) \quad (27)$$

At a given  $\bullet\text{OH}$  concentration (kept constant throughout these experiments) and in the absence of the substrate, the product concentration is  $[\text{P}]_0$ . One can then write equation (28).

$$[\text{P}] = [\text{P}]_0 \times k_C \times [\text{C}] / (k_C \times [\text{C}] + k_S \times [\text{S}]) \quad (28)$$

This equation is then transformed into equation (29).

$$[P]_0/[P] = 1 + (k_S \times [S])^{-1} \quad (29)$$

By plotting  $[P]_0/[P] - 1$  vs.  $[S]^{-1}$  one obtains a straight line whose slope is  $1/k_S$ .

An alternative competition kinetics approach is based on the measurement of the decrease in two compounds, a reference compound (R) with a known second order rate constant and a target compound (X) with an unknown second order rate constant [e.g. Huber *et al.* (2003)]. The  $\bullet\text{OH}$  rate constant for the target compound X can be determined by equations (30)–(34)



In an AOP, the time-dependent decrease of R and X can be formulated by equations (32) and (33).

$$\ln \frac{[R]_t}{[R]_0} = k_R \times [\bullet\text{OH}] \times t \quad (32)$$

$$\ln \frac{[X]_t}{[X]_0} = k_X \times [\bullet\text{OH}] \times t \quad (33)$$

Rearranging equations (32) and (33) results in equation (34).

$$\ln \frac{[X]_t}{[X]_0} = \frac{k_X}{k_R} \times \ln \frac{[R]_t}{[R]_0} \quad (34)$$

A plot of the logarithm of the relative decrease of X versus the logarithm of the relative decrease of R results in a straight line with a slope that corresponds to the ratio of  $k_X$  and  $k_R$ . Because  $k_R$  is known,  $k_X$  can be calculated.

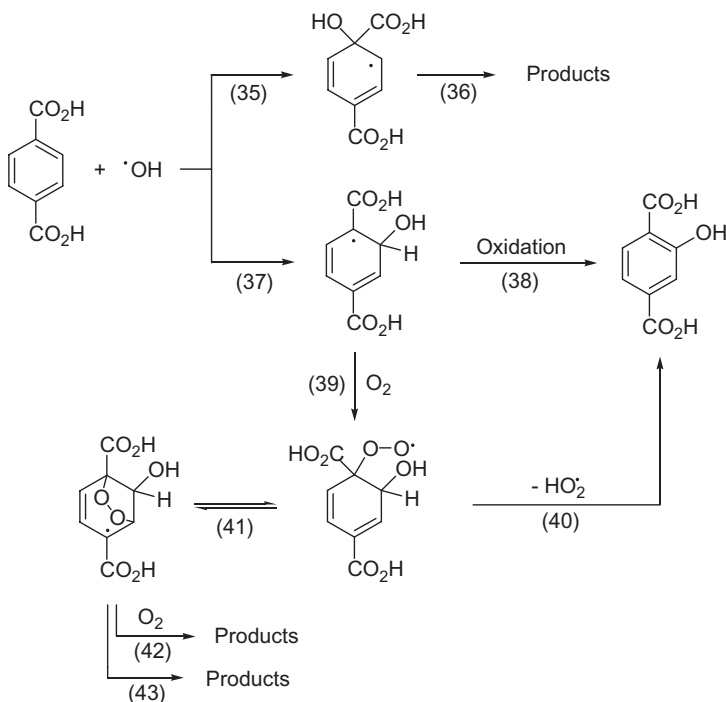
For the determination of an, as yet, unknown  $\bullet\text{OH}$  rate constant by these approaches, any AOP may be used in principle, but certain precautions have to be taken. For example when generating  $\bullet\text{OH}$  by the  $\text{Fe}^{2+}/\text{H}_2\text{O}_2$ ,  $\text{O}_3/\text{H}_2\text{O}_2$  or  $\text{UV}/\text{H}_2\text{O}_2$  processes, one has to take into account that  $\text{H}_2\text{O}_2$  reacts also, albeit slowly, with  $\bullet\text{OH}$  ( $k = 2.7 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ ) and this additional  $\bullet\text{OH}$  scavenging capacity would have to be taken into account when setting up a similar equation system as the one shown above. Obviously, the potential error in the value thus obtained is higher. One also has to ensure that with UV none of the components that we are interested in, S, C, P, R and X are photolysed under such conditions. One also has to ensure that  $\text{H}_2\text{O}_2$  is exposed to a constant photon flux, that is, no UV absorbing compounds build up or that this inner-filter effect is constant for all experiments. With the peroxone process ( $\text{O}_3/\text{H}_2\text{O}_2$ ), there is the additional problem that  $\text{O}_3$  must not react with S, C, P, R or X at an appreciable rate. In the case of ultrasound as AOP, competition kinetics for the determination of  $\bullet\text{OH}$  rate constants fail in the first case, as the accumulation of substrates, here C and S, at the surface of cavitating bubbles strongly depends on their lipophilic/hydrophilic properties (Henglein & Kormann, 1985; Mark *et al.*, 1998; von Sonntag *et al.*, 1999).

## 14.4 DETECTION OF $\bullet\text{OH}$ IN OZONE REACTIONS

In the reaction of ozone with drinking water and wastewater, the DOM present gives rise to the formation of  $\bullet\text{OH}$  radicals (Chapter 3). Their presence has been detected by adding small amounts of *para*-chlorobenzoic acid (pCBA) and following its decay as a function of the  $\bullet\text{OH}$  ( $\text{O}_3$ ) concentration (Elovitz & von Gunten,

1999; Elovitz *et al.*, 2000a). Based on this approach, the  $R_{ct}$  concept has been developed allowing a prediction of micropollutant degradation during ozonation processes (Chapter 3). pCBA reacts rapidly with  $\bullet\text{OH}$  ( $k = 5.0 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ) (Buxton *et al.*, 1988) but very slowly with ozone ( $k = 0.15 \text{ M}^{-1} \text{ s}^{-1}$ ) (Neta *et al.*, 1988). Ozone reacts rapidly with the DOM present in drinking water and in wastewater (for its decay kinetics see Chapter 3), and thus pCBA is protected against destruction by ozone. The DOM also reacts with  $\bullet\text{OH}$  (for rate constants see Chapter 3) in competition with a reaction with pCBA. However, here the competition is not as biased toward a reaction with the DOM due to the much higher rate constant of pCBA for its reaction with  $\bullet\text{OH}$ .

In other AOPs, that is, AOPs such as UV/ $\text{H}_2\text{O}_2$  or the Fenton process, which are not based on a highly reactive agent such as ozone, other  $\bullet\text{OH}$  dosimeters are commonly in use, such as the terephthalic acid (Fang *et al.*, 1996) and the salicylic acid (Ingelmann-Sundberg *et al.*, 1991; Coudray *et al.*, 1995; Bailey *et al.*, 1997) dosimeters. They both have in common that upon  $\bullet\text{OH}$  reaction they form hydroxylated products, 2-hydroxyterephthalate and 2,3-dihydroxybenzoic/2,5-dihydroxybenzoic acids, respectively. 2-Hydroxyterephthalate fluoresces, and thus its yield can be determined without a prior separation by HPLC. The 2,3-dihydroxybenzoic and 2,5-dihydroxybenzoic acids must be separated, and their yields should be practically equal (von Sonntag, 2006). Otherwise, other processes leading to these products are potentially (also) involved. In using these, the fact that the  $\bullet\text{OH}$  radicals do not lead directly to these products, but that  $\bullet\text{OH}$  adducts are formed in the first step and that these have to be further oxidised to the desired products, is often neglected. This additional step allows other reactions to compete. This is shown for the terephthalate dosimeter that has been investigated in some detail [reactions (35)–(43)] (Fang *et al.*, 1996).

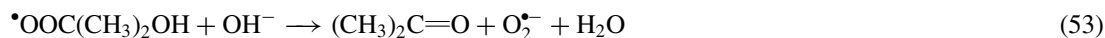
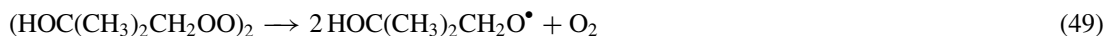
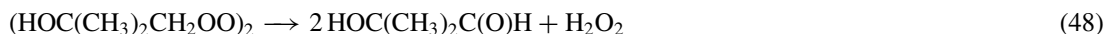
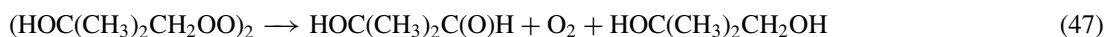
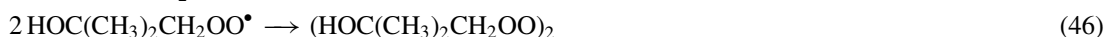


The yield of 2-hydroxyterephthalate is not 100% with respect to  $\bullet\text{OH}$  for several reasons. First, there is a competition between an *ipso* addition and an *ortho* addition [reactions (35) and (37)], and only the latter can

lead to the desired product. Second, the hydroxycyclohexadienyl radical has to be oxidised [reaction (38)].  $\text{Fe}(\text{CN})_6^{3-}$  is often a sufficiently strong oxidant to achieve full oxidation (Buxton *et al.*, 1986), but in the present system a stronger oxidant such as  $\text{IrCl}_6^{2-}$  is required. In its presence, the 2-hydroxyterephthalate yield is 84%. With  $\text{O}_2$  as oxidant, the 2-hydroxyterephthalate yield is much lower (35%), and this is now due to a complex peroxy radical chemistry [cf. reactions (40)–(43)], which has been elucidated with the parent system, benzene (Pan *et al.*, 1993).

## 14.5 DETERMINATION OF $\bullet\text{OH}$ YIELDS IN OZONE REACTIONS

While the above methods can detect  $\bullet\text{OH}$  radicals, the quantification of  $\bullet\text{OH}$  yields is only possible in cases where the  $\bullet\text{OH}$  scavenging rate of the system is known. This is often not the case. A case in point may be an unusual wastewater such as an effluent from an industrial production line. Thus, for an estimation of the  $\bullet\text{OH}$  yield a detection system is required that allows us to overrun the scavenging rate of the system. This can be done with tertiary butanol (tBuOH). This is miscible with water, has a high  $\bullet\text{OH}$  rate constant [ $k = 6 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$  (Buxton *et al.*, 1988)] and barely reacts with ozone [ $k = 1 \times 10^{-3} \text{ M}^{-1} \text{ s}^{-1}$ , Chapter 10]. The major reactions that take place upon  $\bullet\text{OH}$  attack on tBuOH in the presence of  $\text{O}_2$ , which is always in excess over  $\text{O}_3$  in ozonation processes, are depicted by reactions (44)–(54) (Schuchmann & von Sonntag, 1979).



The tBuOH-derived radical formed in reaction (44) reacts with  $\text{O}_2$  giving rise to the corresponding peroxy radical [reaction (45)]. They decay bimolecularly [reaction (46)]. The tetroxide thus formed may decay by various pathways, the Russell-type reaction that gives  $\text{O}_2$ , one molecule of 2-hydroxy-2-methyl-propanal and 2-hydroxy-2-methylpropanol [reaction (47)]. The Bennett-type reaction (48) yields two molecules 2-hydroxy-2-methyl-propanal and  $\text{H}_2\text{O}_2$ . The pathway that has oxyl radicals [reactions (49)–(54)] as intermediates essentially yields acetone and formaldehyde. The 1,2-Hshift reaction (54) seems to be minor compared to the  $\beta$ -fragmentation reaction (50) [for reviews on the chemistry of peroxy radicals in aqueous solution see von Sonntag & Schuchmann (1997) and von Sonntag (2006)]. The aldehydes 2-hydroxy-2-methyl-propanal and formaldehyde are readily quantified by HPLC as their 2,4-dinitrophenylhydrazones, while acetone quantification using this assay is fraught with considerable errors (Flyunt *et al.*, 2003a). Formaldehyde can also be sensitively determined spectrophotometrically using the Hantzsch reaction (Nash, 1953). As a rule of thumb, the  $\bullet\text{OH}$  yield is twice the formaldehyde yield.

There is an additional  $\bullet\text{OH}$  assay in the ozone reaction. Dimethyl sulfoxide (DMSO) reacts only slowly with ozone ( $k = 1.8 \text{ M}^{-1} \text{ s}^{-1}$ , Chapter 9), while its reaction with  $\bullet\text{OH}$  is fast [ $k = 7 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$

(Buxton *et al.*, 1988)]. It gives rise to methanesulfinic acid and a methyl radical in 92% yield [reaction (55), cf. also reaction (2)] (Veltwisch & Asmus, 1982).



The methyl radicals are converted by  $\text{O}_2$  into the corresponding peroxy radicals which partly oxidise methanesulfinic acid to methanesulfonic acid (Flyunt *et al.*, 2001a) in competition with their bimolecular decay (Schuchmann & von Sonntag, 1984a). Thus, another major product is formaldehyde (Yurkova *et al.*, 1999). The sum of methanesulfinic and methanesulfonic acids can be determined by ion chromatography (Yurkova *et al.*, 1999). As some of the methanesulfinic acid is always oxidised to methanesulfonic acid, it does not suffice to determine only the methanesulfinic acid yield by either derivatisation to a coloured compound (Smith *et al.*, 1990; Babbs & Steiner, 1990) or chromatography with electrochemical detection (Jahnke, 1999), as suggested. For the application of the DMSO assay in quantifying  $\bullet\text{OH}$  radical yields in UV/ $\text{H}_2\text{O}_2$  and pulsed electrical discharge systems see Lee *et al.* (2004) and Sahni & Locke (2006). The DMSO assay in ozone reactions has the disadvantage of the much higher ozone rate constant of DMSO and its product methanesulfinic acid (Chapter 9) as compared to tBuOH, but it has the advantage that one does not have to worry about the cross-termination reactions of other radicals with the tBuOH derived peroxy radicals, which may modify the formaldehyde yield. The two assays agree well, as has been shown in the ozonolysis of phenols (Mvula & von Sonntag, 2003).

## 14.6 FORMATION OF PEROXYL RADICALS

Simple carbon-centred radicals react with  $\text{O}_2$  at close to diffusion-controlled rates [reaction (56),  $k = 2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ]. This reaction is practically irreversible.



Bisallylic radicals, such as the  $\bullet\text{OH}$  adducts to aromatic compounds react reversibly with  $\text{O}_2$  (Pan & von Sonntag, 1990; Pan *et al.*, 1993; Fang *et al.*, 1995; Naumov & von Sonntag, 2005). This would give them some advantage to react with ozone in competition (Chapter 13). Nitrogen- and oxygen-centred radicals do not react with  $\text{O}_2$ . This also holds for heteroatom-centred radicals such as the phenoxyl (Jin *et al.*, 1993) and guanyl (von Sonntag, 1994) radicals, although there is considerable free spin also at carbon atoms. To what extent they would react with ozone is as yet not known (for the reactions of radicals with ozone see Chapter 13).

## 14.7 REDOX PROPERTIES OF PEROXYL RADICALS AND REACTION WITH OZONE

Simple alkylperoxy radicals are weak oxidants [reduction potential at pH 7,  $E^7 = 0.77 \text{ V}$ ] (Merényi *et al.*, 1994)]. Electron-withdrawing substituents in the  $\alpha$ -position to the peroxy radical function enhance the reduction potential substantially [ $E^7(\text{Cl}_3\text{COO}\bullet) = 1.6 \text{ V}$ ] and hence the rate of oxidation (e.g. of ascorbate ion). The acetylperoxy radical (Schuchmann & von Sonntag, 1988) is the most strongly oxidising peroxy radical known thus far. In contrast,  $\text{O}_2^{\bullet-}$  is a reducing species [ $E^7 = -0.33 \text{ V}$ ] (Wardman, 1989); the reduction potential relates, by definition, to  $\text{O}_2$ -saturated solutions. For comparison with other values that are based on 1 M, a value of  $-0.18 \text{ V}$  should be taken (Wardman, 1991), see also Chapter 2]. It reacts rapidly with ozone [reaction (57)], and thus its interaction with other peroxy radicals can be neglected under the conditions considered here.



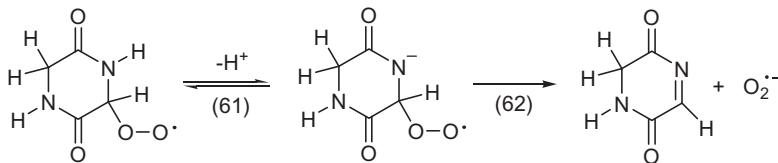
Reaction (57) gives rise to  $\bullet\text{OH} (\text{O}_3^{\bullet-} + \text{H}_2\text{O} \rightarrow \bullet\text{OH} + \text{OH}^-; \text{Chapter 13})$ . Yet, the enhanced  $\bullet\text{OH}$  production also enhances peroxy radical formation. In this context, it may be mentioned that other peroxy radicals also react with ozone, albeit not in a redox reaction. A case in point is the reaction of the tertiary butanol derived peroxy radical (Chapter 13).

## 14.8 UNIMOLECULAR DECAY OF PEROXYL RADICALS

Adequately substituted peroxy radicals may eliminate  $\text{HO}_2^{\bullet}/\text{O}_2^{\bullet-}$ . Typical examples are  $\alpha$ -hydroxyalkylperoxy radicals and their corresponding anions [reactions (58)–(60)].



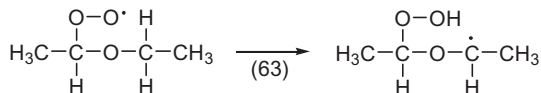
The rate of the  $\text{HO}_2^{\bullet}$  elimination reaction (59) may be slow and varies markedly (many orders of magnitude) with the substituents R (Bothe *et al.*, 1978; von Sonntag & Schuchmann, 1997), but the  $\text{O}_2^{\bullet-}$  elimination reaction (60) is so fast, that this process is typically determined by the rate of the deprotonation reaction (58) ( $k = 2 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$  when  $\text{OH}^-$ -induced, two orders of magnitude slower when phosphate buffer induced) (Bothe *et al.*, 1983). With  $\alpha$ -aminoalkylperoxy radicals the  $\text{O}_2^{\bullet-}$  elimination can already proceed with the help of the lone electron pair, while with  $\alpha$ -amidperoxy radicals, the deprotonated peroxy radical is sufficiently long-lived to establish equilibrium (61) and measure the rate of  $\text{O}_2^{\bullet-}$  elimination (62) by pulse radiolysis (Mieden *et al.*, 1993).



The slow  $\text{HO}_2^{\bullet}$  elimination encountered with many of the peroxy radicals mentioned above implies that at high radical concentrations which one may encounter, for example, with electron beam irradiation, these peroxy radicals may decay by second order kinetics rather than eliminating  $\text{HO}_2^{\bullet}/\text{O}_2^{\bullet-}$ . Thus the product distribution may be both dose rate (here: prevailing ozone concentration) and pH dependent. A case in point is the peroxy radical chemistry of uracil (Schuchmann & von Sonntag, 1983).

When electron-donating substituents are present in the  $\alpha$ -position to the peroxy radical function,  $\text{O}_2^{\bullet-}$  release by an  $\text{S}_{\text{N}}1$  mechanism is also possible, e.g. the rapid release of  $\text{O}_2^{\bullet-}$  from the 1,1-dimethoxyethylperoxy radical (Schuchmann *et al.*, 1990).

The H-abstractive power of peroxy radical is only low, and intramolecular H-abstractions may be of relevance only at long peroxy radical lifetimes. For example, the rate of reaction (63) is only near  $1 \text{ s}^{-1}$  (Schuchmann & von Sonntag, 1982).



In ozone reactions, such slow peroxy reactions are likely to be of minor importance; as long as ozone is still present they may interact with ozone (Chapter 13).

The intermolecular analogue of reaction (63) is the chain autoxidation reaction that can generally be neglected under AOP conditions (low substrate concentrations).

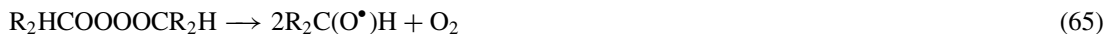
Peroxy radicals may also add intramolecularly to C–C double bonds, when a six-membered transition state sets favourable conditions for this reaction to proceed [reaction (64)] (Porter *et al.*, 1980, 1981).



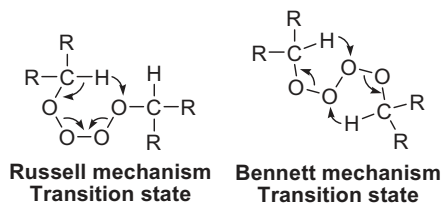
As this reaction is relatively slow, an intermolecular analogue is of no importance for typical AOP applications for the same reason as autoxidations do not take place to any significant extent.

## 14.9 BIMOLECULAR DECAY OF PEROXYL RADICALS

In their bimolecular decay, peroxy radicals first form short-lived tetroxides [cf. reaction (46), well established in organic solvents (Bartlett & Guaraldi, 1967; Adamic *et al.*, 1969; Bennett *et al.*, 1970; Howard & Bennett, 1972; Howard, 1978; Furimsky *et al.*, 1980)], which may either revert to the peroxy radicals or undergo a series of reactions, depending on their structure. Tertiary peroxy radicals, which decay generally more slowly than primary and secondary peroxy radicals, show only one decay route, the formation of oxyl radicals and O<sub>2</sub>. With primary and secondary peroxy radicals, the route to oxyl radicals also plays a role [reaction (65)], but the hydrogens can also take part in the decay of the tetroxides [reaction (66); Russell mechanism (Russell, 1957)] and [reaction (67); Bennett mechanism (Bennett & Summers, 1974; Bothe & Schulte-Frohlinde, 1978)].



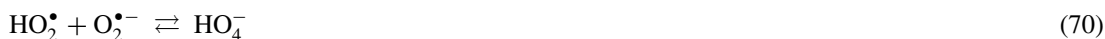
The latter two reactions may be written as concerted reactions with a six-membered transition state (Russell mechanism) and an arrangement consisting of two five-membered rings (Bennett mechanism).



HO<sub>2</sub><sup>•</sup>/O<sub>2</sub><sup>•-</sup> radicals terminate forming H<sub>2</sub>O<sub>2</sub> plus O<sub>2</sub> [reactions (68),  $k = 8.6 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$ , and (69),  $1.02 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$  (Bielski *et al.*, 1985)]. A bimolecular decay of two O<sub>2</sub><sup>•-</sup> radicals does not take place to any significant extent.



Reaction (69) competes with the (reversible) formation of  $\text{HO}_4^-$  [reaction (70)], and this explains why the observed reaction (69) is relatively slow (Merényi *et al.*, 2010b).



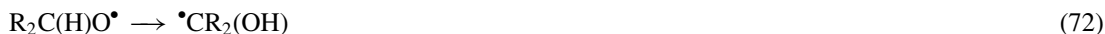
$\text{HO}_2^\bullet/\text{O}_2^{\bullet-}$  also may interact with other peroxy radicals. As yet, there is little information on such reactions. Note that during ozonation,  $\text{O}_2^{\bullet-}$  reacts rapidly with ozone (Chapter 13), and much of the above may not be relevant under such conditions.

## 14.10 REACTIONS OF OXYL RADICALS

The oxyl radicals formed in the bimolecular decay of the peroxy radicals [reaction (65)] and in the reaction of peroxy radicals with ozone (Chapter 13) are highly reactive intermediates. Tertiary oxyl radicals undergo a rapid (in the order of  $10^6 \text{ s}^{-1}$ )  $\beta$ -fragmentation [reaction (71)] (Rüchardt, 1987; Gilbert *et al.*, 1981; Erben-Russ, 1987).



In the primary and secondary oxyl radicals, a 1,2-H shift often competes successfully [reaction (72)]; for mechanistic aspects see Konya *et al.* (2000)].



The driving forces (standard Gibbs free energies) for a number of such reactions are compiled in Table 14.3.

**Table 14.3** Calculated standard Gibbs free energies ( $\Delta G^\circ/\text{kJ mol}^{-1}$ ) for the decay of some oxyl radicals by  $\beta$ -fragmentation and by 1,2-H shift in water (DFT, Jaguar programme, Naumov & von Sonntag, 2011, unpublished)

Reaction	$\Delta G^\circ/\text{kJ mol}^{-1}$
$(\text{CH}_3)_3\text{CO}^\bullet \rightarrow \bullet\text{CH}_3 + (\text{CH}_3)_2\text{C}=\text{O}$	-70 [-57 (gas phase)]
$(\text{tBu, Et, Me})\text{CCO}^\bullet \rightarrow \bullet\text{CH}_3 + (\text{tBu, Et})\text{C}=\text{O}$	-94
$(\text{tBu, Et, Me})\text{CCO}^\bullet \rightarrow \bullet\text{CH}_2\text{CH}_3 + (\text{tBu, Me})\text{C}=\text{O}$	-110
$(\text{tBu, Et, Me})\text{CCO}^\bullet \rightarrow \bullet\text{C}(\text{CH}_3)_3 + (\text{Me, Et})\text{C}=\text{O}$	-154
$\text{CF}_3\text{CF}_2\text{O}^\bullet \rightarrow \bullet\text{CF}_3 + \text{F}_2\text{C}=\text{O}$	-97
$\text{CF}_3\text{CCl}_2\text{O}^\bullet \rightarrow \bullet\text{CF}_3 + \text{Cl}_2\text{C}=\text{O}$	-88
$\text{CCl}_3\text{CCl}_2\text{O}^\bullet \rightarrow \bullet\text{CCl}_3 + \text{Cl}_2\text{C}=\text{O}$	-151
$\text{CCl}_3\text{CCl}_2\text{O}^\bullet \rightarrow \bullet\text{Cl} + \text{CCl}_3\text{C}(\text{O})\text{Cl}$	-86
$^-\text{OC}(\text{O})\text{Cl}_2\text{CO}^\bullet \rightarrow \text{CO}_2^{\bullet-} + \text{Cl}_2\text{C}=\text{O}$	*
$\text{CF}_3\text{CCl}_2\text{O}^\bullet \rightarrow \bullet\text{Cl} + \text{CF}_3\text{C}(\text{O})\text{Cl}$	-71
$\text{CF}_3\text{CF}_2\text{O}^\bullet \rightarrow \bullet\text{F} + \text{CF}_3\text{C}(\text{O})\text{F}$	+55
$\text{CH}_3\text{O}^\bullet \rightarrow \bullet\text{CH}_2\text{OH}$	-35
$\text{CH}_3\text{CH}_2\text{O}^\bullet \rightarrow \bullet\text{CH}(\text{CH}_3)\text{OH}$	-36
$\text{CH}(\text{CH}_3)_2\text{O}^\bullet \rightarrow \bullet\text{C}(\text{CH}_3)_2\text{OH}$	-48

\*This oxyl radical decomposes without barrier upon structure optimisation.



The  $\alpha$ -hydroxyalkyl radicals formed in reaction (72) subsequently give rise to  $\alpha$ -hydroxyalkylperoxy radicals (Berdnikov *et al.*, 1972; Gilbert *et al.*, 1976, 1977; Schuchmann & von Sonntag, 1981), the source of  $\text{HO}_2^*/\text{O}_2^{\bullet-}$  in these systems (see above).

The  $\beta$ -fragmentation of acyloxy radicals is even several orders of magnitude faster than that of tertiary alkoxyl radicals (Hilborn & Pincock, 1991).

## 14.11 INVOLVEMENT OF $\bullet\text{OH}$ RADICALS IN CHLORATE AND BROMATE FORMATION

### 14.11.1 Chlorate formation

Because chloride is oxidised very slowly by ozone (Chapter 11), chlorate is only formed in significant concentrations when ozonation follows a pre-treatment with chlorine or chlorine dioxide (von Gunten, 2003b; Haag & Hoigné, 1983b). The chlorine–ozone reaction system is discussed in detail in Chapter 11; for ozone reactions with halogen-centred radicals see Chapter 13.

Because the reactions in the hypochlorite–ozone system are relatively slow,  $\bullet\text{OH}$  reactions may play an important role under typical treatment conditions with relatively low chlorine concentrations entering an ozonation reactor after pre-chlorination.

The reaction of chloride with  $\bullet\text{OH}$  is given by a pH-dependent equilibrium [reactions (73) and (74);  $k_{73} = 4.3 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Kläning & Wolff, 1985),  $k_{-73} = 6 \times 10^9 \text{ s}^{-1}$  (Kläning & Wolff, 1985),  $k_{74} = 2.1 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$  (Kläning & Wolff, 1985),  $k_{-74} = 2.5 \times 10^5 \text{ s}^{-1}$  (McElroy, 1990)].



Based on this reaction sequence with the two equilibria, the apparent second order rate constant for the reaction of chloride with  $\bullet\text{OH}$  to  $\text{Cl}^\bullet$  can be calculated as a function of pH. The apparent second order rate constant is expressed as in equation (75).

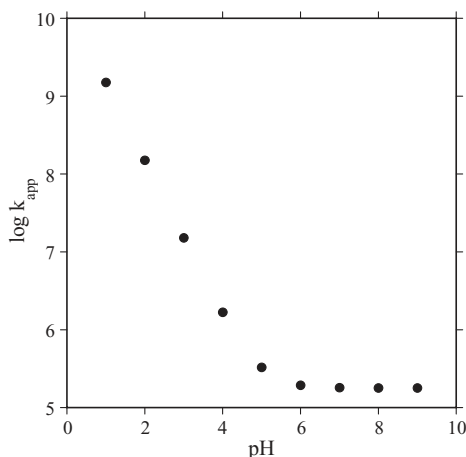
$$k_{app} = \frac{k_{73}}{k_{-73}} (k_{74}[\text{H}^+] + k_{-74}) \quad (75)$$

This is illustrated in Figure 14.1. It is evident that the formation of  $\text{Cl}^\bullet$  is only relevant at  $\text{pH} < 3$ . Therefore, for typical water treatment conditions during ozonation of drinking waters and wastewaters, the formation of chlorinated organic by-products is minimal.

In waters with higher salinity, the  $\text{HOCl}^{\bullet-}$  species may further react with chloride and bromide [reactions (76),  $k = 1.0 \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$  (Grigorev *et al.*, 1987) and (77),  $k = 1.0 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (estimated, (Matthew & Anastasio, 2006)].



The conversion of  $\bullet\text{OH}$  to these more selective radicals ( $\text{Cl}_2^{\bullet-}$  and  $\text{BrCl}^{\bullet-}$ ) may lead to a better abatement of electron-rich micropollutants such as phenols [ $k(\text{Cl}_2^{\bullet-} + \text{phenol}) = 2.5 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$  (Alfassi *et al.*, 1990)] in saline waters (Grebel *et al.*, 2010). For a critical compilation of rate for chlorine and bromine species in saline waters see Grebel *et al.* (2010) and references therein.



**Figure 14.1** pH dependence of the second order rate constant for the reaction  $\text{ClO}_2^- + \bullet\text{OH} \rightarrow \bullet\text{ClO}_2 + \text{OH}^-$ .

In waters containing hypochlorite,  $\bullet\text{OH}$  contributes significantly to its oxidation [reactions (78),  $k = 9 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Buxton & Subhani, 1972) and (79),  $k_{79} < k_{78}$ ].



The reaction product  $\text{ClO}^\bullet$  undergoes a self-reaction with pre-equilibrium ( $\text{Cl}_2\text{O}_2$ ) and a decay to  $\text{OCl}^-$  and  $\text{ClO}_2^-$  [reactions (80),  $2k = 1.5 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$  (Buxton & Subhani, 1972) and (81)].



The overall  $\text{ClO}^\bullet$  self-reaction can be formulated as follows [reaction (82),  $k = 2.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Klänning & Wolff, 1985)].



Chlorite can be further oxidised by  $\bullet\text{OH}$  to chlorine dioxide and finally chlorate which is the end product during ozonation and AOPs of chlorine-containing waters [reactions (83),  $k = 4.2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Klänning *et al.*, 1985) and (84),  $k = 4.0 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Klänning *et al.*, 1985)].



### 14.11.2 Bromate formation

In the following section, the most important bromine reactions occurring in  $\bullet\text{OH}$ -based AOPs at near neutral pH are discussed. For a complete compilation of all reactions occurring in the  $\bullet\text{OH}$ -bromine system see Matthew & Anastasio (2006) and references therein.

The ozone reactions occurring during ozonation of  $\text{Br}^-$ -containing waters are discussed in Chapter 11 and the reactions between ozone and bromine-containing radicals in Chapter 13. The oxidation of  $\text{Br}^-$

by  $\bullet\text{OH}$  to  $\bullet\text{Br}$  proceeds through equilibrium (85) [reactions (85),  $k_{85} = 1.06 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$ ,  $k_{-85} = 3.3 \times 10^7 \text{ s}^{-1}$  (Zehavi & Rabani, 1972)] followed by a decay and reformation of  $\text{BrOH}^{\bullet-}$  [equilibrium (86),  $k_{86} = 4.2 \times 10^6 \text{ s}^{-1}$  (Zehavi & Rabani, 1972),  $k_{-86} = 1.3 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$  (Lind *et al.*, 1991)].



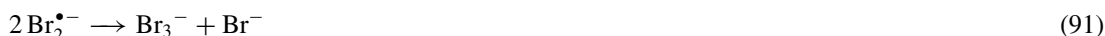
$\text{BrOH}^{\bullet-}$  and  $\text{Br}^\bullet$  react further with  $\text{Br}^-$  [reaction (87),  $k = 1.9 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$  (Zehavi & Rabani, 1972), and equilibrium (88),  $k_{88} \approx 10^{10} \text{ M}^{-1} \text{ s}^{-1}$  (Zehavi & Rabani, 1972),  $k_{-88} = 6.6 \times 10^3 \text{ s}^{-1}$  modelled by (Matthew & Anastasio, 2006)].



In natural waters,  $\text{Br}^\bullet$  can also react with carbonate/bicarbonate [reactions (89),  $k = 2.0 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$ , and (90),  $k = 1.0 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$  (estimated values) (Matthew & Anastasio, 2006)]



The  $\text{Br}_2^{\bullet-}$  species undergoes further reactions, leading to  $\text{Br}_3^-$  and  $\text{HOBr}$ , which are crucial in the context of bromate formation during ozonation (Chapter 11) [reactions (91),  $k = 3.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Ershov *et al.*, 2002), (92),  $k > 1.0 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Wagner & Strehlow, 1987) and (93),  $k = 1.1 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  (Huie *et al.*, 1991)]



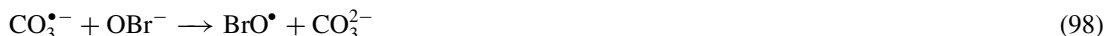
$\text{Br}_3^-$  is in equilibrium with  $\text{Br}_2$  and  $\text{Br}^-$  [equilibrium (94),  $k_{94} = 5.5 \times 10^7 \text{ s}^{-1}$ ,  $k_{-94} = 9.6 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$  (Ershov, 2004)].  $\text{Br}_2$  is in equilibrium with  $\text{HOBr}$  and  $\text{Br}^-$  [equilibrium (95),  $K = 3.5 \times 10^{-9} \text{ M}^2$  (Beckwith *et al.*, 1996)].



As shown in Chapter 11,  $\text{HOBr}$  ( $\text{p}K_a = 8.8$ ) is a crucial intermediate during ozonation of  $\text{Br}^-$ -containing waters, and most mitigation strategies are based on  $\text{HOBr}$  minimisation.  $\text{HOBr}/\text{OBr}^-$  can be further oxidised by  $\bullet\text{OH}$  [reactions (96),  $k = 2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ , and (97),  $k = 4.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Buxton & Dainton, 1968)].



The  $\text{BrO}^\bullet$  species may also be formed by carbonate radicals [reaction (98),  $k = 4.3 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$  (Buxton & Dainton, 1968)].



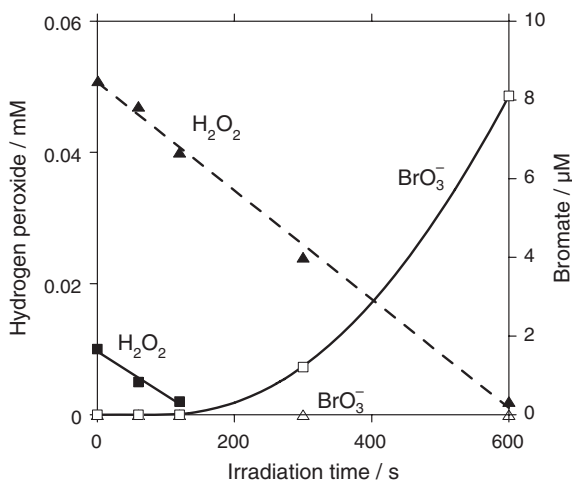
During ozonation, the  $\text{BrO}^\bullet$  species can also be formed from a reaction of  $\text{Br}^\bullet$  with ozone (Chapter 13). It undergoes disproportionation [reaction (99),  $k = 4.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Buxton & Dainton, 1968)].



Subsequently, several oxidation steps lead to bromate which is undesired in drinking waters (Chapter 11) [reaction (100),  $k = 2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ , reaction (101),  $k = 1.1 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$  (Buxton & Dainton, 1968), and reaction (102),  $k = 2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Field *et al.*, 1972)].



Therefore, bromate can be formed by  $\bullet\text{OH}$  radical reactions only. This was demonstrated by  $\gamma$ -radiolysis experiments in which bromate increased as a function of irradiation time in  $\text{N}_2\text{O}$ -saturated solutions (Figure 14.2). Figure 14.2 also shows that bromate is formed only when the  $\text{H}_2\text{O}_2$  concentration decreases to zero. This shows that  $\text{HOBr}$  is an intermediate during the  $\bullet\text{OH}$ -induced bromate formation since this species is reduced by  $\text{H}_2\text{O}_2$  (Chapter 11). Therefore, no bromate is formed in the AOP  $\text{UV}/\text{H}_2\text{O}_2$ , because a  $\text{H}_2\text{O}_2$  is always in excess as long as  $\bullet\text{OH}$  radicals are formed.



**Figure 14.2**  $\gamma$ -Radiolysis of  $\text{Br}^-$  and  $\text{H}_2\text{O}_2$ -containing solutions. The evolution of bromate (open symbols) and  $\text{H}_2\text{O}_2$  (closed symbols) is shown as a function of the irradiation time (dose rate  $0.58 \text{ Gy s}^{-1}$ ) at pH 7.  $[\text{Br}^-]_0 = 50 \mu\text{M}$ ,  $[\text{H}_2\text{O}_2]_0$ : 50  $\mu\text{M}$  (closed triangles), 10  $\mu\text{M}$  (closed squares), 2 mM phosphate,  $\text{N}_2\text{O}$ -saturated solutions. Reprinted with permission from von Gunten & Oliveras (1998). Copyright (1998) American Chemical Society.

From the above reaction sequence, it can be seen that carbonate alkalinity can have a direct influence on bromate formation kinetics and pathways through various reactions with carbonate radicals. Finally, DOM also has an important influence on bromate formation due to its role related to its effect on the ozone chemistry and  $\bullet\text{OH}$  formation during ozonation [Chapter 3, (Pinkernell & von Gunten, 2001)].

## 14.12 DEGRADATION OF OZONE-REFRACTORY MICROPOLLUTANTS BY $\bullet\text{OH}$ /PEROXYL RADICALS

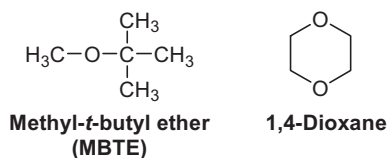
The products of the degradation of ozone-refractory micropollutants have only been studied in detail in some cases. Examples are methyl-*t*-butyl ether (MTBE) and atrazine. For others, only a brief account can be given on likely reactions based on the large body of other studies on  $\bullet\text{OH}$ /peroxy radical reactions in aqueous solution. For the compounds discussed below,  $\bullet\text{OH}$  rate constants are compiled in Table 14.4. For a discussion of the efficiency of the elimination of ozone-refractory micropollutants see also Chapter 3.

**Table 14.4** Compilation of  $\bullet\text{OH}$  rate constants for some selected ozone-refractory micropollutants

Compound	$k/\text{M}^{-1} \text{s}^{-1}$	Reference
Amidotrizoic acid	$9.6 \times 10^8$	Jeong <i>et al.</i> , 2010
	$5.4 \times 10^8$	Real <i>et al.</i> , 2009
Atrazine	$3 \times 10^9$	Acero <i>et al.</i> , 2000
1,4-Dioxane	$2.5 \times 10^9$ – $3.1 \times 10^9$	Buxton <i>et al.</i> , 1988
Geosmin	$7.8 \times 10^9$	Peter & von Gunten, 2007
Ibuprofen	$7.4 \times 10^9$	Huber <i>et al.</i> , 2003
lomeprol	Similar to lopromide	Huber <i>et al.</i> , 2005
lopromide	$3.3 \times 10^9$	Huber <i>et al.</i> , 2003
lopamidol	Similar to lopromide	Huber <i>et al.</i> , 2005
2-Methylisoborneol	$5.1 \times 10^9$	Peter & von Gunten, 2007
Methyl tertiary butyl ether (MTBE)	$1.6 \times 10^9$ – $1.9 \times 10^9$	Cooper <i>et al.</i> , 2009
<i>N</i> -Nitrosodimethylamine (NDMA)	$4.5 \times 10^8$	Lee <i>et al.</i> , 2007
Perfluorooctanoic acid (PFOA)	No significant reaction	Plumlee <i>et al.</i> , 2009
	$\leq 10^5$	Vecitis <i>et al.</i> , 2009
Perfluorooctanesulfonic acid (PFOS)	No significant reaction	Plumlee <i>et al.</i> , 2009
Tetrachloroethene (PER)	$2.3 \times 10^9$	Köster & Asmus, 1971
Trichloroethene (TRI)	$4.0 \times 10^9$	Köster & Asmus, 1971
Tri- <i>n</i> -butyl phosphate (TnBP)	$(2.8 \pm 0.8) \times 10^9$	Pocostales <i>et al.</i> , 2010
	$6.4 \times 10^9$	Watts & Linden, 2009
Tris-2-chloroisopropyl phosphate (TCPP)	$(7 \pm 2) \times 10^8$	Pocostales <i>et al.</i> , 2010
	$1.98 \times 10^8$	Watts & Linden, 2009

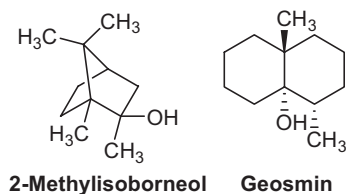
### 14.12.1 Saturated aliphatic compounds

Hydroxyl radicals react with saturated aliphatic compounds by H-abstraction. There is a considerable preference for hydrogens activated by a neighbouring heteroatom [cf. reactions (15) and (16)]. Such a preference also holds for  $\bullet\text{OH}$  attack at methoxy on the gasoline additive MTBE [56% (Acero *et al.*, 2001), 60% (Stefan *et al.*, 2000)]. The rate constant for the reaction of MTBE with  $\bullet\text{OH}$  radicals is given in Table 14.4. Details of the ensuing chemistries have been reviewed in detail (Cooper *et al.*, 2009) and remediation technologies have been discussed (Baus *et al.*, 2005). For a discussion of MTBE removal in multibarrier treatment see Chapter 5.



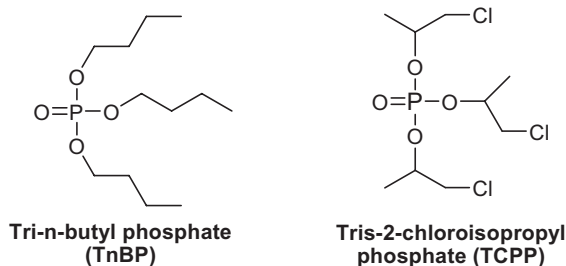
The  $\bullet\text{OH}$ -induced degradation of 1,4-dioxane in the presence of  $\text{O}_2$  has been studied in detail (Stefan & Bolton, 1998) and discussed on the basis of mechanisms shown above. The radicals formed upon  $\bullet\text{OH}$  attack are reducing radicals and, therefore, also react rapidly with oxidants other than  $\text{O}_2$  (Nese *et al.*, 1995).

There are many other ozone-refractory micropollutants, notably the taste and odour compounds 2-methylisoborneol and geosmin (for a compilation of taste and odour compounds see Chapter 5). Their odour threshold is as low as a few ng/L.

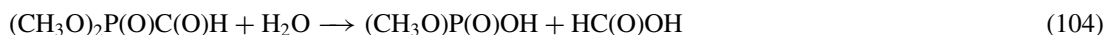
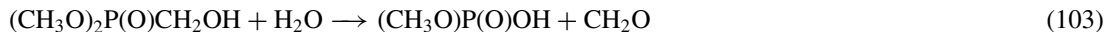


2-Methylisoborneol and geosmin react faster with  $\bullet\text{OH}$  than MTBE (Table 14.4). There are many different hydrogens available for  $\bullet\text{OH}$  attack, and hence there must be a multitude of  $\bullet\text{OH}$ -induced degradation products. They will all be more polar and less volatile than their parents which leads to a loss of their taste and odour properties (Peter & von Gunten, 2007).

There is another important group of ozone-refractory organic micropollutants, namely the organic phosphates. They serve as plasticisers and additives in the clothing industry such as tri-*n*-butyl phosphate (TnBP) or as flame retardants such as tris-2-chloroisopropyl phosphate (TCPP) [for their occurrence in waters of various origin see Andresen & Bester (2006), Andresen *et al.* (2004) and Meyer & Bester (2004); for their degradation in wastewater see Pocostales *et al.* (2010), Chapter 3.

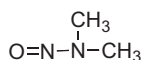


Their  $\bullet\text{OH}$ -induced degradation products have not been determined, but there are detailed studies on trimethyl and triisopropyl phosphates (Schuchmann & von Sonntag, 1984b; Schuchmann *et al.*, 1984, 1995). H-abstraction of the  $\alpha$ -hydrogen and subsequent peroxy radical reactions lead to labile compounds that readily hydrolyse [e.g. reactions (103) and (104)].



The rates of these reactions have been determined by pulse radiolysis.

*N*-Nitrosodimethylamine (NDMA) reacts only slowly with ozone and with  $\bullet\text{OH}$  (Table 14.4). Therefore, the transformation of NDMA in ozone-based AOPs is very slow. One of the main products from NDMA oxidation by  $\bullet\text{OH}$  is methylamine (Lee *et al.*, 2007b).



***N*-Nitrosodimethylamine  
NDMA**

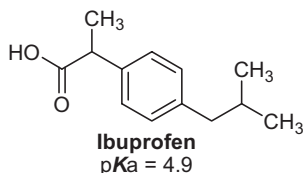
NDMA can be efficiently degraded by direct UV photolysis to mainly dimethylamine, nitrate and nitrite (Stefan & Bolton, 2002). For similar UV fluences, the combination of UV with  $\text{H}_2\text{O}_2$  does not contribute significantly to the degradation rate (Sharpless & Linden, 2003). The dimethylamine formed from NDMA is unproblematic for further NDMA formation in, for example, postchloramination, because the concentration will be very low (NDMA is typically present in the nanograms per litre range) and the NDMA yield from dimethylamine in NDMA formation potential tests with monochloramine is of the order of 3% (Lee *et al.*, 2007a). NDMA can also be partially or fully removed by biological filtration (Schmidt & Brauch, 2008).

### 14.12.2 Aromatic compounds

Abundant aromatic ozone-refractory micropollutants ( $k_{\text{ozone}} < 10 \text{ M}^{-1} \text{ s}^{-1}$ ) are the x-ray contrast media such as amidotrizoic acid, iomeprol, iopamidol and iopromide, the pharmaceutical ibuprofen, the musk fragrance tonalide (AHTN) (Chapter 7) as well as the triazine herbicides such as atrazine (see below).

Second order rate constants for the reaction of x-ray contrast media with  $\bullet\text{OH}$  have been determined, with amidotrizoic acid having the lowest value ( $k = 0.96 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Jeong *et al.*, 2010) and the others having values in a small range between  $2\text{--}3.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  (Huber *et al.*, 2003; Jeong *et al.*, 2010). The x-ray contrast media compounds are characterised by three iodine atoms at the aromatic ring and three further substituents for solubilisation. Iodine is especially bulky and the addition of  $\bullet\text{OH}$  to the aromatic ring will preferentially occur at the  $\alpha$ -positions to the iodines (Fang *et al.*, 2000). Moreover, there will be a considerable contribution of H-abstraction from the side chains. This must lead to a complex peroxy radical chemistry that is difficult to predict.

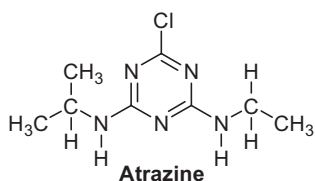
The  $\bullet\text{OH}$ -induced peroxy radical chemistry of ibuprofen is easier to predict.



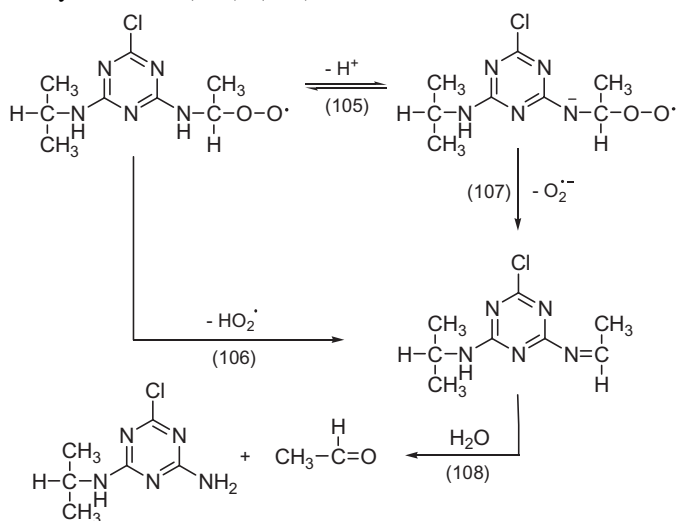
The rate constants for the reaction of ibuprofen with ozone and  $\bullet\text{OH}$  are  $9.6 \text{ M}^{-1} \text{ s}^{-1}$  and  $7.4 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ , respectively (Huber *et al.*, 2003). These values warrant that ibuprofen is mainly degraded by  $\bullet\text{OH}$

during ozonation. This will largely resemble the degradation of its parent benzene, that is, one would expect mainly hydroxylation reactions as depicted above for terephthalate [reactions (35)–(43)]. The resulting phenols will react very rapidly with ozone and thus will be further degraded (Chapter 7).

The  $\bullet\text{OH}$ -induced reactions of atrazine have been studied in quite some detail (Tauber & von Sonntag, 2000; Acero *et al.*, 2000) [for reviews on the degradation of herbicides by ozone and AOPs see (Ikehata & El-Din, 2005a, b)].



The reaction of atrazine with ozone is slow ( $k = 6 \text{ M}^{-1} \text{ s}^{-1}$ ), and it will mainly react with  $\bullet\text{OH}$  during ozonation ( $k = 3 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ) (Acero *et al.*, 2000). The aromatic ring is so electron-deficient, that the reactivity of the triazine ring is low and hence reacts rather slowly with  $\bullet\text{OH}$  (Tauber & von Sonntag, 2000). This allows H-abstraction reactions at the side chains to become of importance (ca. 60% of  $\bullet\text{OH}$  attack) (Tauber & von Sonntag, 2000). The products that are formed upon  $\bullet\text{OH}$  attack at the ring have not yet been elucidated, but the reactions that follow an attack at the side chains are known in quite some detail. The major products are deethyl- and deisopropyl-atrazine (and the corresponding keto compounds, acetaldehyde and acetone) in a 2.6:1 ratio. An example for the reactions that follow an  $\bullet\text{OH}$  attack at the  $\alpha$ -position of the ethyl group and subsequent  $\text{O}_2$  addition is given by reactions (105)–(108).

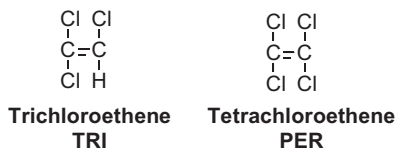


Kinetic data for all the relevant reactions have been determined by pulse radiolysis (Tauber & von Sonntag, 2000) and by competition kinetics in  $\text{O}_3/\text{H}_2\text{O}_2$  systems (Acero *et al.*, 2000). The hydrolysis of the Schiff base is  $\text{OH}^-$ -catalysed and is so slow [ $k(\text{OH}^-) = 5.2 \text{ M}^{-1} \text{ s}^{-1}$ ] that it can be followed conveniently after  $\gamma$ -irradiation. For a study on atrazine degradation using electrolytically generated  $\bullet\text{OH}$  see Balci *et al.* (2009).



### 14.12.3 Chlorinated olefins

Trichloroethene (TRI) and tetrachloroethene (PER) barely react with ozone (Chapter 6), but react readily with  $\bullet\text{OH}$  (Table 14.4).



Attack of  $\bullet\text{OH}$  on the symmetrical molecule PER gives rise to a single radical [reaction (109)].



The observation of trichloroacetic acid TCA (in the presence of  $\text{O}_2$ ) as an important product has led to the suggestion that a rapid rearrangement [ $\text{HOCCl}_2\text{C}(\text{Cl}_2) \rightarrow \text{Cl}_3\text{CC}(\text{OH},\text{H})\bullet$ ] takes place (Glaze, 1986; Mao *et al.*, 1993) in competition with the fast HCl elimination of the geminal chlorohydrin function [reaction (110),  $k > 7 \times 10^5 \text{ s}^{-1}$  (Köster & Asmus, 1971; Mertens & von Sonntag, 1994b)].



A product study in the absence of  $\text{O}_2$  showed that TCA is not a product under such conditions and that the rapid release of HCl must only be due to reaction (110) (Mertens & von Sonntag, 1994b).

In fact, the resulting radicals recombine [reaction (111);  $k = 6.9 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ].

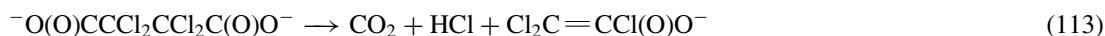


Upon hydrolysis of one of the acyl chloride functions [reaction (112),  $k = 5 \text{ s}^{-1}$ ], an acid is formed that cyclises rapidly upon forming tetrachlorosuccinic anhydride (reaction not shown).



This anhydride hydrolyses more slowly and could no longer be determined by pulse radiolysis with conductometric detection [for a comparison, hydrolysis of succinic anhydride takes place at  $k = 1.8 \times 10^{-3} \text{ s}^{-1}$  (Ebersson, 1964)]. In  $\gamma$ -radiolysis, the  $\text{ClC}(\text{O})\text{Cl}_2\text{C}\bullet$  radicals have a lifetime of 0.1 s, and under such conditions tetrachlorosuccinic anhydride was not detected. From this it follows that either tetrachlorosuccinic anhydride hydrolyses much faster than succinic anhydride or the  $\text{ClC}(\text{O})\text{Cl}_2\text{C}\bullet$  radicals have hydrolysed prior to recombination.

In a much slower reaction tetrachlorosuccinic acid decarboxylates [reaction (113)],  $k = 6.2 \times 10^{-5} \text{ s}^{-1}$  at  $55^\circ\text{C}$ ,  $E_a = 115 \text{ kJ mol}^{-1}$ ].



In the presence of  $\text{O}_2$ , the  $\text{ClC}(\text{O})\text{Cl}_2\text{C}\bullet$  radicals are converted into the corresponding peroxy radicals [reaction (114)].



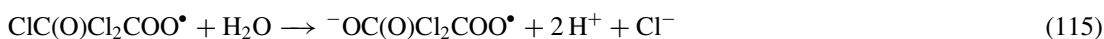
Data from a preliminary  $\gamma$ -radiolytic product study (Mertens, 1994) are given in Table 14.5.

**Table 14.5** Products and their  $G$  values (unit:  $10^{-7}$  mol  $J^{-1}$ ) in the  $\gamma$ -radiolysis of tetrachloroethene (1 mM) in  $N_2O/O_2$ -(4:1)-saturated aqueous solutions. The conversion into mol product per mol  $\bullet OH$  is based on  $G(\bullet OH) = 5.6 \times 10^{-7}$  mol  $J^{-1}$ , the contribution of  $\bullet H$  is neglected

Product	$G$ value/ $10^{-7}$ mol $J^{-1}$	Yield per mol $\bullet OH$
Chloride	33.1	5.9
Carbon dioxide	10.4	1.85
Trichloroacetic acid (TCA)	2.1	0.38
Dichloroacetic acid (DCA)	< 0.1	0.02

From these data, it is seen that a short chain reaction must prevail (the  $Cl^-$  yield is above four times the  $\bullet OH$  yield). Moreover, the formation of TCA shows that chlorine atoms are generated in the course of the reaction.

The acyl-substituted, quasi-primary peroxy radicals may undergo hydrolysis [reaction (115)].



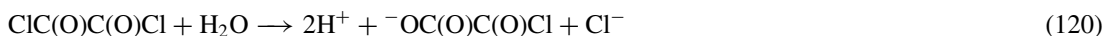
Depending on the rate of  $\bullet OH$  production, bimolecular termination of the peroxy radicals will be by the primary (quasi-primary) peroxy radicals at high initiation rate such as by electron beam irradiation, a mixture of primary (quasi-primary) plus secondary peroxy radicals at moderate  $\bullet OH$  generation rate, and by the secondary peroxy radicals at low  $\bullet OH$  generation rate. This may strongly influence the product distribution. At high initiation rate one may write reaction (116).



The ensuing oxyl radical may undergo two  $\beta$ -elimination reactions [reactions (117) and (118)/(119),  $\Delta G^0(119) = +24$  kJ  $mol^{-1}$  (Naumov & von Sonntag, 2011, unpublished), note that the analogous (reverse) reaction of  $\bullet OH$  with CO is close to diffusion controlled (Buxton *et al.*, 1988)].



One of the products of reaction (117) is oxalyl chloride. It hydrolyses rapidly [ $k > 350$   $s^{-1}$  (Dowideit, 1996; Prager *et al.*, 2001)]. Once the first acyl chloride function has been hydrolysed, the remaining one will decompose into  $CO_2$ , CO plus HCl [reactions (120) and (121)] (Staudinger, 1908).



In most AOP applications, the lifetime of free radicals will be near 100 ms rather than a few ms as in electron beam treatment. This implies that the acyl chloride-derived peroxy radicals stand a good chance

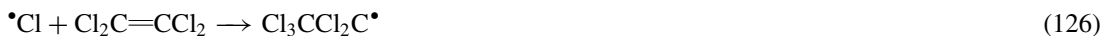
of hydrolysing prior to recombination. As a consequence, one has to take the involvement of the hydrolysed peroxy radicals into account [reactions (122) and (123)].



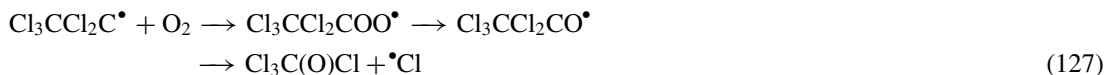
In contrast to reactions (116)–(119), this termination reaction does not liberate  $^\bullet\text{Cl}$  atoms. Similarly, oxyradical formation in the bimolecular decay would give rise to  $\text{CO}_2^{\bullet-}$  [reaction (124), cf. Table 14.3] and subsequently to  $\text{O}_2^{\bullet-}$  [reaction (125),  $k = 2 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ].



Such reactions break the (short)  $^\bullet\text{Cl}$ -promoted chain reaction. The formation of  $^\bullet\text{Cl}$  is responsible for TCA formation. Here,  $^\bullet\text{Cl}$  will have to add to PER [reaction (126)].



Subsequent reactions, abbreviated in reaction (127) give rise to trichloroacetyl chloride which hydrolyses very rapidly [reaction (128),  $k > 350 \text{ s}^{-1}$  (Dowideit, 1996)]



The pentachloroethyl radical is also an intermediate in the photolysis of PER (Mertens & von Sonntag, 1995), as a chlorine atom is released in the photolytic step [reaction (129), for the formation and optical properties of the ensuing vinylperoxy radicals see (Mertens & von Sonntag, 1994a; Naumov & von Sonntag, 2005)].



As the molar absorption coefficient of PER at 254 nm ( $\epsilon = 225 \text{ M}^{-1} \text{ cm}^{-1}$ ) is much higher than that of  $\text{H}_2\text{O}_2$  ( $\epsilon = 20 \text{ M}^{-1} \text{ cm}^{-1}$ ) and the quantum yield is also high [ $\Phi(\text{product forming processes}) = 0.31$ ], PER photolysis (Mertens & von Sonntag, 1995) must always contribute to product formation when  $\text{H}_2\text{O}_2/\text{UV}$  is used as AOP. In the presence of DOM, DOM will act as  $^\bullet\text{Cl}$  scavenger, as will bicarbonate and carbonate. Thus formation of TCA, a highly undesired by-product, may no longer be significant at high concentrations of these scavengers [for model studies see Mertens & von Sonntag (1995)]. It is interesting to note that the ratios of rate constants for  $^\bullet\text{OH}$  and  $^\bullet\text{Cl}$  with carbonate and bicarbonate differ substantially. While for  $^\bullet\text{OH}$  this ratio is 46, it is only 2.3 for  $^\bullet\text{Cl}$  (Mertens, 1994).

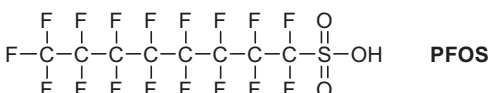
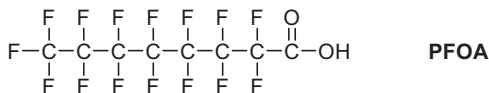
The chemistries of the peroxy radicals derived from TRI will be very similar to those discussed above for PER. In Table 14.6, the products and their yields are compiled [for data on 1,1-dichloroethene, *cis*-1,2-dichloroethene, and dichloromethane see Mertens (1994)].

**Table 14.6** Products and their  $G$  values (unit:  $10^{-7} \text{ mol J}^{-1}$ ) in the  $\gamma$ -radiolysis of trichloroethene (1 mM) in  $\text{N}_2\text{O}/\text{O}_2$ -(4:1)-saturated aqueous solutions. The conversion into mol product per mol  $\bullet\text{OH}$  is based on  $G(\bullet\text{OH}) = 5.6 \times 10^{-7} \text{ mol J}^{-1}$ , the contribution of  $\bullet\text{H}$  is neglected. Source: Mertens (1994)

Product	$G$ value/ $10^{-7} \text{ mol J}^{-1}$	Yield per mol $\bullet\text{OH}$
Chloride	22.6	4.0
Carbon dioxide	8.9	1.6
Formic acid	5.5	1.0
Glyoxylic acid	0.4	0.07
Dichloroacetic acid (DCA)	1.7	0.3
$\text{H}_2\text{O}_2$ (final)	1.6	0.3

#### 14.12.4 Perfluorinated compounds

The environmentally persistent perfluorinated surfactants perfluorooctanoic acid (PFOA) and perfluorooctanesulfonic acid (PFOS) do not react with ozone [for their fate in drinking water treatment see Tagagi *et al.* (2011)].



Even their oxidative degradation by  $\bullet\text{OH}$  is most inefficient (Hori *et al.*, 2004; Schröder & Meesters, 2005), as ET from the anion, the only feasible reaction, is not a favoured  $\bullet\text{OH}$  reaction anyway (see above) and is further hampered by the strong electron-withdrawing effects of fluorine atoms.  $\text{SO}_4^{\bullet-}$  is a better electron acceptor but even with this agent the rate of reaction is low and other reactions compete quite effectively (Hori *et al.*, 2005). The present state of technology in removing these surfactants has recently been reviewed (Vecitis *et al.*, 2009; Lutze *et al.*, 2011b).

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Even though ozone has been applied for a long time for disinfection and oxidation in water treatment, there is lack of critical information related to transformation of organic compounds. This has become more important in recent years, because there is considerable concern about the formation of potentially harmful degradation products as well as oxidation products from the reaction with the matrix components. In recent years, a wealth of information on the products that are formed has accumulated, and substantial progress in understanding mechanistic details of ozone reactions in aqueous solution has been made. Based on the latter, this may allow us to predict the products of as yet not studied systems and assist in evaluating toxic potentials in case certain classes are known to show such effects. Keeping this in mind, *Chemistry of Ozone in Water and Wastewater Treatment: From Basic Principles to Applications* discusses mechanistic details of ozone reactions as much as they are known to date and applies them to the large body of studies on micropollutant degradation (such as pharmaceuticals and endocrine disruptors) that is already available. Extensively quoting the literature and updating the available compilation of ozone rate constants gives the reader a text at hand on which his research can be based. Moreover, those that are responsible for planning or operation of ozonation steps in drinking water and wastewater treatment plants will find salient information in a compact form that otherwise is quite disperse.

A critical compilation of rate constants for the various classes of compounds is given in each chapter, including all the recent publications. This is a very useful source of information for researchers and practitioners who need kinetic information on emerging contaminants. Furthermore, each chapter contains a large selection of examples of reaction mechanisms for the transformation of micropollutants such as pharmaceuticals, pesticides, fuel additives, solvents, taste and odor compounds, cyanotoxins.

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